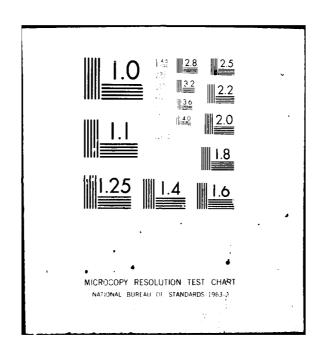
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# HIGH ALTITUDE POLLUTION PROGRAM STRATOSPHERIC MEASUREMENT SYSTEM LABORATORY PERFORMANCE CAPABILITY REPORT CHEMICAL CONVERSION TECHNIQUES

Norman H. Macoy and Richard Weingarten Anthony Pires and Sherman Poultney





February 1980 TECHNICAL REPORT

National Technical Information Service, Springfield, Virginia 22161



Prepared for HIGH ALTITUDE POLLUTION PROGRAM

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# TABLE OF CONTENTS

Section	<u>Title</u>	Page
I	INTRODUCTION	1
II	SUMMARY	5
III	PERFORMANCE TESTING AND EVALUATION	9
	3.1 Nitric Oxide Chemiluminescence Sensor 3.1.1 Theory 3.1.2 Experimental Procedures and Results 3.2 Nitrogen Dioxide Photolytic Conversion 3.2.1 Theory 3.2.2 Stratospheric-Based Instrumentation Modeling 3.2.3 NO <sub>2</sub> Photolytic Converter Design 3.2.4 Experimental Procedures and Results 3.3 Nitrogen Dioxide Catalytic Conversion 3.3.1 Catalytic/Chemical Thermal Converters 3.3.2 Catalytic-Chemical Converters 3.3.3 Catalytic Sorption Converters 3.4 Nitrous Pentoxide (N <sub>2</sub> O <sub>5</sub> ) Generation 3.4.1 Theory 3.4.2 Experimental Procedures 3.5 Nitrous Pentoxide (N <sub>2</sub> O <sub>5</sub> ) Thermal Conversion 3.5.1 Theory 3.5.2 Stratospheric-Based Instrument Modeling 3.5.3 Experimental Procedures and Results 3.6 Nitric Acid (HNO <sub>3</sub> ) Generation 3.6.1 Theory 3.6.2 Experimental Procedures	11 11 15 18 18 20 20 22 24 24 28 30 32 32 33 38 44 49 55 55 60 60 60
	3.7.1 Theory 3.7.2 Stratospheric-Based Instrument Modeling 3.7.3 Experimental Procedures and Results 3.8 Potential Interferents (Specificity) 3.8.1 C10NO <sub>2</sub> Generation and Handling 3.8.2 HO <sub>2</sub> NO <sub>2</sub> Family Compounds 3.9 NO <sub>2</sub> Feasibility	66 66 72 72 82 84
	3.9.1 Stratospheric-Based Instrument Modeling 3.9.2 Heterogenous Sample Changes 3.9.3 NO <sub>z</sub> Baseline Design 3.10 Potential of a New Technique for NO <sub>2</sub> Measurements	87 91 92 95
IV	CONCLUSIONS AND RECOMMENDATIONS	99
	4.1 Conclusions 4.2 Recommendations	99 102
	REFERENCES	104

# TABLE OF CONTENTS (Continued)

<b>Appendices</b>	<u>Title</u>	Page
A	Infrared Absorption Measurements	A-1
В	Computer Simulation of NO $_{\rm Z}$ Thermal Conversion In The Stratosphere	B-1
	LIST OF ILLUSTRATIONS	
Figure	<u>Titl</u> e	Page
3-1	Arrhenius Plot For NO <sub>2</sub> -O <sub>3</sub> Reaction	34
3-2	NO <sub>3</sub> Generation Versus Time (T = 298 K)	35
3–3	Plot of Measured Stoichiometries Versus Initial React- ant Ratio For NO <sub>2</sub> -O <sub>3</sub> Experiments	37
3-4	Simultaneous Rate Constants at T = 500 and 600 K	41
3-5	NO <sub>3</sub> Decay versus Time	42
3-6	Setup for Experiment To Observe Thermal Decomposition of $N_2^{0}$ 5	50
3-7	N <sub>2</sub> O <sub>5</sub> Generation Spectra	51
3-8	Absorption Spectra of $N_2O_5$ and $HNO_3$	54
3-9	Absorbances at Converter Output	56
3-10	HNO3 and N2O5 Absorbance at Converter Output	58
3-11	HNO3 Vapor Pressure Vs Reciprocal Temperature	59
3-12	Response of Perkin-Elmer Model 580 Spectrophotometer vs. Chemiluminescence Monitor	68
3-13	Chemiluminescence Monitor Performance vs. Flow Rate	69
3-14	Vapor Pressure Diagram For ${\tt C10N0}_2$ and ${\tt Suspected}$ Impurities	74
3-15	Thermal Decomposition of ClONO, T ~ 306 K	76
3-16	$NO_2$ and $C10_x NO_x$ Absorption Cross-Sections	78
3-17	Cholorine Nitrate-Nitrogen Dissociation Rates	81
3-18	NO <sub>3</sub> Measurement Bias Error	90
3-19	NO Converter - NO Sensor Sample Flow Layout	94

# LIST OF TABLES

Number	<u>Title</u>	Page
3-1	O <sub>3</sub> k <sub>1</sub> t Term Vs. Altitude For Above Values	14
3-2	Aerochem Research AAS-3S Specifications	15
3-3	Design Comparison of NO Chemiluminescence Sensors	17
3-4	NO <sub>2</sub> Photolytic Cell Design	22
3-5	$^{-1}$ Calculated and Measured NO $_{2}$ Photolytic Converter Efficiencies	23
3-6	Free Energy of Formation $\Delta F'$ (kcal/Oxygen Atom) and Temperature for 98 Percent NO $_2$ Conversion	25
3-7	Ferrous Sulphate Catalytic Converter Test Results	30
3-8	Ferrous Ammonium Sulphate Catalytic Converter Test Results	31
3-9	$\mathrm{N_{2}O_{5}}$ Generation and Stoichiometry Measurements	36
3-10	Predicted Half-Life of N <sub>2</sub> O <sub>5</sub> In A 400 K Thermal Converter	39
3-11	NO <sub>3</sub> Rate Limiting Decay	42
3-12	HAPP Residence Time Study	46
3-13	$NO_{\mathbf{x}}$ Budget	47
3-14	NO <sub>3</sub> Free Radical Photolytic Terms	48
3-15	$\mathrm{NO_2}$ , $\mathrm{N_2O_5}$ and $\mathrm{HNO_3}$ Measured Concentrations vs Thermal Converter Temperature	52
3-16	${ m HNO_3}$ Thermal Converter Performance Characteristics with Cross Calibration High Temperature Catalytic Conversion vs. Chemiluminescence Measurements	70
3-17	ClONO, Thermal Decomposition	77
3-18	CLO NO -NO Photolysis Specificity with Spectral Discrimination	78
3-19	NO, and C10NO, Concentrations	79
3-20	HO NO Reaction Rates	85
3-21	First-Order HO <sub>2</sub> NO <sub>2</sub> Rate Constants and Predicted Thermally Yielded NO <sub>2</sub> as a Function of Sample Residence Time	86
3-22	Net Change of Species (molecules/cm <sup>3</sup> ) vs Temperature for Residence Time of 5 Seconds	89
3-23	High Temperature Reaction Vessel Design Comparison	96
A-1	Infrared Absorption Band Cross Sections For N $_2{}^{\rm O}{}_{\rm 5}$ and HNO $_3$ (cm $^2/{\rm molecule})$	A-4
B-1	Molecular Number Densities used for Sample Modeling Within Instrumentation	B-2

#### SECTION I

## INTRODUCTION

This report documents the laboratory measurements made to resolve specificity questions concerning the Hybrid Chemical Conversion Measurement System and to examine the potential of a conversion technique for total odd nitrogen, as recommended in the High Altitude Pollution Program (HAPP) Stratospheric Measurement System Feasibility Study. That study and these laboratory measurements are part of a large study of the High Altitude Pollution Program Stratospheric Measurement System being done by the Perkin-Elmer Corporation for the Department of Transportation, Federal Aviation Administration under Contract DOT-FA77WA-4080. The goal of this larger study is to define and demonstrate a measurement system consisting of a technique or combination of techniques that can be flown on a series of balloon flights to make prescribed, in situ measurements of the stratosphere in support of the High Altitude Pollution Program. The other components of the total study include the feasibility of the Tunable Diode Laser Spectrometric System for the prescribed measurements, detailed engineering design documentation for the recommended payload, and a summary report. These other components of the study will be reported separately.

The Feasibility Study (Macoy et al., 1978) had concluded that the feasibility of successfully developing and flying a balloon-borne measurement system was high, based on a careful examination of the candidate system from an engineering point of view. The Study recommended that the system, consisting of a hybrid of analytical techniques, should be developed and deployed pending resolution of certain specificity questions. The selection of the Hybrid Chemical Conversion System was based on a comprehensive and critical review of all measurement techniques. This review included molecular chemical conversion, atomic chemical conversion, ion molecular conversion/mass spectroscopy, in situ optical absorption gas chromatography, and resonance fluorescence. Only the Hybrid Chemical Conversion techniques were to be appropriate

for an on-station balloon payload and within current state-of-the-art technology. Even then, certain of these techniques were subject to questions
of conversion specificity. The questions did not invalidate those techniques,
but might place several prescribed species into one class. The resolution
of the specificity questions was therefore necessary and that work is one
of the subjects of this report.

As the Feasibility Study was concluding, it became evident that progress in each of the reviewed techniques was not standing still and certain promising techniques should continue to be investigated in parallel to the resolution of specificity questions. The promising techniques were the Tunable Diode Laser Absorption Spectrometer and the Total-Odd Nitrogen Converter. The latter might turn the very lack of specificity of the conversion techniques into a capability to make the important measurement of total odd-nitrogen in the stratosphere. The study of the potential of this converter is another subject of this report. The Tunable Diode Laser Spectrometer technique gave promise that it might be able to measure all of the prescribed species if the IR signatures of heavier molecules cooperated and the requisite S/N performance could be achieved in the field. The study of the feasibility of a Tunable Diode Laser Spectrometer Measurement System is reported in a separate report (Poultney et al., 1979).

As this report is being written, progress in the reviewed techniques is still being made and the list of prescribed species is being re-examined. The ability to take advantage of advances in measurement capability is one great strength of the hybrid system that is recommended. A new technique can replace or supersede a weaker technique in the hybrid system without making the whole system obsolete. One new technique under development in the community for NO<sub>2</sub> promises to increase the feasibility of the Hybrid Gas Conversion system in that manner. This new technique and its potential impact on the realization of the HAPP Stratospheric Measurement System is also addressed in this report. A second strength of the Hybrid System is the ability to add or delete species (or parameters) without making the whole system obsolete. Instruments are being developed to measure these new species and parameters and could be later included in the Hybrid System. We do not here review any of these new instruments (e.g. a J<sub>NO<sub>2</sub></sub> instrument).

The originally prescribed measurements were NO, NO<sub>2</sub>, N<sub>2</sub>O<sub>5</sub>, HNO<sub>3</sub>, N<sub>2</sub>O and 03 at the same time and place in the stratosphere for the full range of concentrations expected during a diurnal cycle. These trace gases play a key role in the present characteristics of the ozone layer. The prescribed measurements would improve our understanding of how aircraft engine emissions might affect the ozone layer and the stratosphere. The Hybrid Gas Conversion System was selected to make these measurements. As discussed in the Feasibility Study, the hybrid system consists of a UV absorption instrument for  $0_3$ , a gas chromatography instrument for  $N_20$ , and a chemical conversion/chemiluminescent instrument for  $\mathrm{HNO_3}$ ,  $\mathrm{N_2O_5}$ ,  $\mathrm{NO_2}$ , and  $\mathrm{NO}$ . The expected sensitivity for  $0_3$  is 2.7 x  $10^{10}$  and for  $N_2$ 0 is 3.7 x  $10^9$  molecules/cm<sup>3</sup>. The third instrument consisted of a thermal converter for the  ${\rm HNO_3}$  and  ${\rm N_2O_5}$  selective conversions, a photolytic or catalytic converter for the NO, selective conversion, and a chemiluminescent detector for the NO detection. The flow of stratospheric gas through the system would be operated on in appropriate sequences by these converters to measure each species in turn using the sensitivity detector. The expected sensitivity for NO is 1.3 x 10 molecules/cm for a 1-sec integrating time. The expected sensitivity for the remaining species would be comparable. The accuracy for the remaining species, however depends on the specificity of the conversion techniques for each species in the presence of the others and in the presence of other possible nitrogen oxide species in the stratosphere (e.g.  $HO_2NO_2$  and  $CIONO_2$ ).

The Feasibility Study recommended development and deployment of the Hybrid Gas Conversion System and, simultaneously, a laboratory study of the specificity issues. This report documents the laboratory measurements made to resolve specificity and other issues. Particular emphasis was placed on (1) the conversion of NO<sub>2</sub> to NO by both catalytic and photolytic converters, (2) thermal conversion of N<sub>2</sub>O<sub>5</sub> and HNO<sub>3</sub> to NO<sub>2</sub> with and without possible interfering gases, and (3) the feasibility of measuring total odd-nitrogen concentrations using catalytic thermal conversion (in conjunction with the NO and NO<sub>2</sub> measurements). The conversion of NO<sub>2</sub> to NO by catalytic techniques, if reliable, would mean a significant weight reduction in the balloon payload. In brief, the laboratory measurements consisted of breadboarding the various converters, testing

them with known concentrations of species, and generating as necessary those species which are highly reactive. The laboratory measurements were supported by computer modeling of the conversion process and the flow through the instrument. The modeling was then used to extrapolate the performance of the laboratory instrument to its expected performance in the stratosphere. A summary of the results of the laboratory measurements is given in Section II. Section III describes the measurements and their interpretation in detail. Conclusions and recommendations arising from this study are presented in Section IV.

#### SECTION II

## SUMMARY

Extensive laboratory measurements for the detection and measurement of NO, NO $_2$ , N $_2$ O $_5$  and HNO $_3$  have been carried out for various types of chemical conversion instrumentation. Particular emphasis was placed on the conversion of NO $_2$  to NO by both catalytic and photolytic converters, thermal conversion of N $_2$ O $_5$  and HNO $_3$  to NO $_2$  with and without possible interfering gases, and the feasibility of measuring total odd-nitrogen concentrations using catalytic thermal conversion. Computerized chemical kinetics simulations have also been generated to independently support the laboratory measurements and expected performance of instrumentation at stratospheric float altitudes.

For NO measurement, gas phase titration with  $0_3$  is employed followed by the monitoring of the chemiluminescence of an excited state of  $NO_2$  formed during the titration. This method is well understood, and possesses ample sensitivity to meet the HAPP requirement of  $10^8$  molecules/cm $^3$  at stratospheric altitudes.

Analytical methods for the remaining three species employed various techniques for quantitatively converting the molecule directly or indirectly to NO, followed by the chemiluminescent technique cited above.

For NO<sub>2</sub> conversion to NO, four techniques were utilized at a typical laboratory concentration of 1 x 10<sup>14</sup> molecules/cm<sup>3</sup> and less. Three techniques employed some form of catalyst. The remaining technique was the photolytic conversion of NO<sub>2</sub> to NO using radiation the in 300-400 nm spectral region. The reactant, NO<sub>2</sub> was also monitored using a high temperature catalytic converter followed by chemiluminescence. The product, NO was monitored by the chemiluminescence technique. Photolytic converter efficiency has been determined to be as high as 57 percent and is a function of photon flux and sample residence time. Efficiency, therefore, is a design engineering tradeoff problem.

This technique was evaluated because specificity with other possible nitrogen oxide species of the stratosphere is not an issue. Of the catalytic conversion techniques evaluated, only the high temperature (800 K) catalytic conversion was found to be very efficient for NO, but, unfortunately, the technique cannot be used for  $NO_2$  as  $N_2O_5$  and  $HNO_3$  would be simultaneously converted. Chemical-thermal conversion of NO2, an adjunct to thermal-catalytic conversion, although not evaluated in the lab, was reviewed as a technique. Efficiency of conversion for this technique, however, has been found to be low when an oxidant such as ozone is present (Lowenstein, private communication, 1978). Catalytic-chemical conversion of NO2 was evaluated as a technique using both ferrous sulphate, FeSO, and ferrous ammonium sulphate, Fe(NH,)2-(SO4)2. With FeSO4 as a catalyst, not only was the conversion efficiency found to be low but also substantial quantities of NO, were lost, presumably by an adsorption process. This technique is known to be a poor converter of NO, when an oxidant (O3) is present in the sample (Ridley and Schiff, 1978). With  $Fe(NH_{\Delta})_2(SO_{\Delta})_2$  as catalyst, the conversion efficiency was found to be high (greater than 97.5 percent) once procedural problems associated with Viton were eliminated. Catalytic-sorption converters, either platinum or platinum and palladium, on a support column were found to be ineffective for conversion of NO2.

Thermal conversion of  $N_2O_5$  to  $NO_2$  at a typical laboratory concentration of 7 x  $10^{13}$  molecules/cm<sup>3</sup> was found to be straightforward with the decomposition going to completion at a temperature of 475 K. Nitrogen pentoxide which cannot be stored at room temperature for any practical length of time was generated as needed in a kinetic flowing system. Product and reactant species number densities were monitored by IR absorption and, for  $NO_2$  and NO, by catalytic-thermal conversion and chemiluminescence, respectively. The rate limiting reaction rate and stoichiometry were monitored a number of times and found to be in agreement with the other workers in the field.

Viton is a trade name for the copolymer form of vinylindene fluoride and hexafluoropropylene.

Two procedural issues with  $N_2O_5$  observed during the laboratory studies are related to the generation and decomposition of  $N_2O_5$ . First, if moisture is present on the walls of reaction vessels in use during the generation process,  $HNO_3$  is formed and the  $N_2O_5$  yield is less than unity. Although this is a heterogeneous reaction, the homogeneous formation or desorption of  $HNO_3$  was also observed. This  $HNO_3$  formation was employed for simultaneous species testing of thermal converters. Hence the issue was resolved and the artifacts used as an advantage. Second, for most tests carried out, high purity oxygen was employed for generating ozone so as to oxidize  $NO_2$  to  $NO_3$  and thus generate  $N_2O_5$ . For long term stable storage of  $NO_2$ , the diluent gas selected was high purity air. Upon reacting  $NO_2$  and  $O_3$ , the resulting carrier gas was oxygen rich reaching at times 78 percent which is atypical of air. Thus it is conceivable that significant oxidizing reactions were occurring when the experimental objective was to carry out reducing reactions.

Thermal conversion of  ${\rm HNO}_3$  at a typical laboratory concentration of 2  $\times$  10<sup>14</sup> molecules/cm<sup>3</sup> to NO<sub>2</sub> and thermodynamically predicted NO was found to be straightforward with the decomposition going to completion at a temperature as low as 535 K. Product and reactant species number densities were monitored by IR absorption and, for NO, and NO, by catalytic-thermal conversion and chemiluminescence, respectively. The decomposition is not promoted by a catalyst but does require a surface presumably to scavenge the product OH radical. Computer analysis, (Appendix B), does confirm a faster decomposition rate when OH is scavenged from a stream operated at sea level conditions. Computer analysis for stratospheric conditions where there is a preponderance of 0, indicates 0, does not impact conversion, but also that complete conversion requires a temperature of about 800 K. Nitric acid decomposition tests in the presence of nitrogen, separately in the presence of air, and again separately in the presence of oxygen enriched air are presented. Nitric acid decomposition tests in the presence of relatively high levels of 0, have also been carried out.

Potential interferents reviewed analytically or theoretically included chlorine nitrate, ClONO<sub>2</sub>, and permitric acid, HO<sub>2</sub>NO<sub>2</sub>. Both are considered

to be labile with the former undergoing conversion at 350 K and the later at about 300 K. If these species are actually present in the stratosphere at number densities greater than instrumentation detection levels, their presence reduces specificity of a particular thermal conversion.

The lack of specificity of thermal converters can actually be used to advantage for the detection of total odd nitrogen species, NO<sub>z</sub>. Rather than be concerned about the possible presence of such species as C10NO<sub>2</sub> and HO<sub>2</sub>NO<sub>2</sub> or about the partial decomposition of HNO<sub>3</sub> when N<sub>2</sub>O<sub>5</sub> is being totally decomposed, all odd-nitrogen species in the stratosphere would be decomposed to NO using a high-temperature catalytic converter. This possibility was recommended in the Feasibility Study and its feasibility is shown here, based on the above measurements and on analytic modeling. The instrument would consist of two similar channels, an NO channel at 250 K and a total odd-nitrogen channel at 800 K.

One new technique under development for the measurement of NO<sub>2</sub> promises sensitive and specific measurements in a lighter and more compact module. Narrowband UV photolysis of NO<sub>2</sub> leaves NO in an excited state from which its characteristic fluorescence can be measured. Also, the technique could be extended to NO by first converting NO to NO<sub>2</sub> as is done in the chemiluminescent detector. The potential of the technique is critically assessed based on discussions with J. Anderson of Harvard and D. Kley of NOAA.

Finally, the analytic computer models of the conversion techniques developed to model the laboratory measurements have been used to assess the techniques under stratospheric conditions. The modeling results for both laboratory conditions and those for the stratosphere's expected concentrations indicate, with only minor differences, identical conversion trending. This permits valid extrapolation of the laboratory results. Thus, it is concluded that there is no fundamental reason why these techniques would not work at the required sensitivities in the stratosphere. However, sample fidelity and surface reactions which are not amenable to modeling must be given closer attention in laboratory conditions closer to those of the stratosphere.

#### SECTION III

#### PERFORMANCE TESTING AND EVALUATION

This section is devoted to theoretical considerations and laboratory measurements for various analytical methods for the detection of nitric oxide, nitrogen dioxide, nitrous pentoxide and nitric acid. Generation of the latter two gases at quantitative concentrations is also presented. The final three subsections are devoted to considerations of potential interferents, the feasibility of a total odd-nitrogen measurement, and the promise of a new technique for nitrogen dioxide, NO<sub>2</sub>.

Each subsection presents the appropriate theoretical considerations followed by experimental findings.

As many chemical reactions are listed throughout this report, and their reaction rates evaluated, particular conventions and procedures are employed. Often recourse is made to chemical thermodynamic equilibrium constants. In the main, accepted conventions for notation have been used (Hampson and Garvin, 1978). For example, consider the reaction below with the forward reaction rate coefficient  $k_{\rm f}$ ,

$$A + 2B \rightarrow AB_2, \quad k_f,$$

$$\frac{d[A]}{dt} = \frac{1}{2} \frac{d[B]}{dt} = -\frac{d[AB_2]}{dt} = -k_f[A][B]^2,$$

where [A] is the concentration of constituent A and so forth. Similarly, the backward reaction can be expressed with the reverse reaction rate coefficient  $k_r$ ,

$$AB_2 \longrightarrow A + 2B, \quad k_r.$$

$$\frac{d \left[ AB_2 \right]}{dt} = -\frac{d \left[ A \right]}{dt} = -\frac{1}{2} \frac{d \left[ B \right]}{dt} = -k_r \left[ AB_2 \right].$$

At equilibrium, the total time derivatives vanish, leading to the equations

$$k_f [A] [B]^2 = k_r [AB_2];$$

$$K_e = k_f/k_r = \frac{[AB_2]}{[A] [B]^2}, \qquad (3-1)$$

where  $K_e$  is the equilibrium constant for this reaction expressed in units of concentration (usually moles/liter or molecules/cm<sup>3</sup>). Usually, only one reaction rate coefficient is known so that an evaluation of  $K_e$  must be made in order to derive the opposing reaction rate coefficient. The primary source of information with respect to the equilibrium constant is the set of JANAF Thermochemical Tables. These tables list as a function of temperature the thermochemical properties of most of the compounds of interest in this report. These properties are related to the equilibrium constant by the following expression

$$-R \ln K_{p} = \Delta (G_{T}^{\circ} - H_{ref}^{\circ})/T + \Delta (H_{ref}^{\circ}/T)$$
 (3-2)

where K is the equilibrium constant in units of atmospheres (atm).  $\Delta$  represents the sum over the products of the reaction minus the sum over the reactants. The quantity  $(G_T^\circ - H_{ref}^\circ)/T$  is known as the Gibbs-energy function. The subscript, ref, is the reference point temperature (298.15 K for these tables).  $\Delta H_{ref}^\circ$  is the heat of formation of the constituent at the reference temperature. The superscript symbol,  $\circ$ , signifies atmospheric pressure (760 torr).  $K_D^\circ$  can be related to  $K_D^\circ$ .

$$K_p = K_e (RT)^{\Delta n}$$

where  $\Delta n$  is the change in the number of moles of constituents (moles of products minus moles of reactants). Thus,

$$K_e = (RT)^{-\Delta n} \exp \left[ -\frac{1}{R} \Delta \begin{pmatrix} G_T^{\circ} - H_{ref}^{\circ} \\ T \end{pmatrix} \right] \exp \left[ -\frac{1}{RT} \Delta \Delta \begin{pmatrix} H_{ref}^{\circ} \end{pmatrix} \right].$$

Typically, the Gibbs-energy function changes slowly over the temperature range of interest (220 K  $\leq$  T  $\leq$  900 K). The principal temperature dependence is contained in the second exponential factor. For most reactions  $\Delta n = 0$  or  $\pm 1$ , so that the effect of temperature in the leading term in the expression is not pronounced. It proved convenient for computer coding to assume that the leading exponential term was independent of temperature.

As noted, usually only one reaction rate coefficient has been measured. A critical review of such coefficients for reactions among atmospheric constituents has been made by Hampson and Garvin (1978). Their recommended values have been used wherever possible in computer modeling codes. Other sources will be cited as required for any reactions not included in the review. If the opposing reaction rate coefficient has also been measured, then it is incorporated directly. Otherwise, the equilibrium constant is evaluated in the manner described above and the opposing reaction rate coefficient is derived, equation 3-2.

Reactions are numbered sequentially throughout the document. The equilibrium constant is denoted as  $K_{number}$ , -number. Forward reaction rate coefficients are denoted as  $k_{number}$  and reverse reaction rate coefficients as  $k_{number}$ .

In some cases a laboratory or net stoichiometric reaction is presented and followed by a set of redox reactions or mechanism. As none of the authors are kineticists, Glasstone et al. (1941)-type graphical representations of the mechanism, e.g., potential energy, standard-state molal free energy or enthalpy versus reaction coordinate were considered to be qualitative or too symbolic for use in applying reaction rate theory.

#### 3.1 NITRIC OXIDE CHEMILUMINESCENCE SENSOR

# 3.1.1 Theory

As a part of CIAP, stratospheric NO was measured by Ridley et al. (1972) using the chemiluminescent method, specifically the ozone oxidation of NO to an optically excited state of NO<sub>2</sub>. The method is also being used by Dr.

Schmeltekopf's group at NOAA for stratospheric measurements and Dr. Stedman's group at NCAR for tropospheric measurements. The method is based upon the reactions:

$$NO + O_3 \longrightarrow NO_2^* \begin{pmatrix} 2 B_1 \end{pmatrix} + O_2$$
 (1a)

$$\longrightarrow NO_2 \begin{pmatrix} 2A_1 \end{pmatrix} + O_2$$
 (1b)

$$NO_2^*$$
  $\longrightarrow$   $NO_2$  +  $h \vee , \lambda \geq 600 \text{ nm}$  (2)

$$M + NO_2^* \longrightarrow M + NO_2, M = O_2 \text{ or } N_2$$
 (3)

The bimolecular second order rate constants,  $k_{1a}$  and  $k_{1b}$ , are given by Clough and Thrush (1967) as:

$$k_{1a} = 7.6 + 1.5 \times 10^{11} \text{ exp } (-4180 + 300/\text{RT}) \text{ cm}^3 - \text{mole}^{-1} - \text{s}^{-1}$$
  
= 1.26 x 10<sup>-12</sup> exp (-4180/RT) cm<sup>3</sup>-molecule<sup>-1</sup>-s<sup>-1</sup>

and

$$k_{1b} = 4.3 + 1.0 \times 10^{11} \exp (-2330 + 150/RT)$$
  
= 7.13 x 10<sup>-13</sup> exp (-2330/RT)

Since reaction (1a) has a higher activation energy, luminescence is favored if the temperature is as high as practical. At room temperature, 298 K, the rates  $k_{la}$  and  $k_{lb}$  are 1.08 x 10<sup>-15</sup> and 1.39 x 10<sup>-14</sup> cm<sup>3</sup>-molecule <sup>-1</sup>-s<sup>-1</sup>. Therefore, of the NO molecules that react with the  $0_3$ , only  $k_{la}/(k_{la}+k_{lb})$  or 7.2 percent are converted to NO $_2^*$ . These then radiate via reaction (2) or are quenched via reaction (3).

The intensity of the chemiluminescence (CL) emission is given by Clyne et al. (1964) as:

$$I = \frac{\left[I_{o}\right] \text{ NO } \left[O_{3}\right]}{\left[M\right]} \tag{3-3}$$

provided that  $k_3$  [M] >>  $k_2$  with [M] denoting total pressure in molecules/cm<sup>3</sup>. The value of I<sub>o</sub> is given approximately as 12 exp (-4180 ± 300/RT) photons/s

for the spectral region 650 to 875 nm (Fontijn et al., 1970). The broadband output serves to make this a non-specific method for NO, however, experience shows that daytime NO can be reliably measured. Clyne et al. (1964) report a less conservative value of 20.7 for the coefficient. At room temperature, 298 K,  $I_0 = 1.0 \times 10^{-2}$  photon/s and at 316 K, 1.54 x  $10^{-2}$  photon/s. Since  $k_2/k_3 = 2.7 \times 10^{14}$  molecules/cm<sup>3</sup>, the above inequality is valid to pressures as low as 4.5 torr or an altitude of 35 km (Clough and Thrush, 1967).

Achieving linearity with the CL method requires that a negligible net amount of  $0_3$  be consumed by the NO in a flowing system. The combined bimolecular second order reaction rate,  $k_1$ , is given by Johnston and Crosby (1954) as:

$$k_1 = 0.8 \times 10^{12} \exp (-2500/RT) cm^3 - mole^{-1} - s^{-1}$$
  
= 0.13 x 10<sup>-11</sup> exp (-2500/RT) cm<sup>3</sup> - molecule<sup>-1</sup> - s<sup>-1</sup>

The rate constant is related to the concentrations through,

$$-\frac{d \left[0_{3}\right]}{dt} = -\frac{d\left[N_{0}\right]}{dt} = k_{1} \left[N_{0}\right] \left[0_{3}\right]$$
 (3-4)

Assuming that the second reactant gas concentration,  $\begin{bmatrix} 0 \\ 3 \end{bmatrix} >> \begin{bmatrix} NO \end{bmatrix}$ , the integrated second order rate law is:

$$\frac{1}{\begin{bmatrix} 0_3 \end{bmatrix}} \ln \frac{\begin{bmatrix} NO \end{bmatrix}}{\begin{bmatrix} NO \end{bmatrix} - \Delta \begin{bmatrix} NO \end{bmatrix}} = k_1 t = 0.19 \times 10^{-13} t \text{ at } 298 \text{ K}$$

$$\frac{\Delta \begin{bmatrix} NO \end{bmatrix}}{\begin{bmatrix} NO \end{bmatrix}} = 1 - \exp \left( -\begin{bmatrix} 0_3 \end{bmatrix} 0.19 \times 10^{-13} t \right)$$
(3-6)

OI

If the exponent is made large (4 or 5), then the photomultiplier sensitivity (PMT current per unit NO mass flow rate) is proportional to

$$\left(\frac{k_{1a}}{k_{1a} + k_{1b}}\right) \frac{GQ_{NO}}{P}$$

where G denotes a geometric factor. In terms of reactor volume V, temperature T, reactant flow rate  $Q_{NO}$ , and second reactant flow rate  $Q_{03}$ , the quantity  $\begin{bmatrix} 0_3 \end{bmatrix}$  after mixing with the sample stream is for a constant volume sampling pump:

$$\left[o_{3}\right] = \left[o_{3}\right] \frac{Q_{O_{3}}}{Q_{NO} + Q_{O_{3}}} \left(\frac{P}{760}\right) \left(\frac{273}{T}\right)$$
 (3-7)

where  $\begin{bmatrix} 0 \\ 3 \end{bmatrix}$  denotes ozone concentration at the internal generator.

The exponent becomes:

$$\approx 0.19 \times 10^{-13} \left[ o_3^{1} \right] v \left( \frac{Q_{0_3}}{Q_{NO}^{2}} \right) \left( \frac{P}{760} \right)^{2} \left( \frac{273}{298} \right)^{2}$$

Silent discharge  $0_3$  generators can produce as much as 3 percent ozone at a flow rate of 25 scc/s. Using these values and reasonable values for volume and sample flow rate yields:

$$\begin{bmatrix} 0_3^{\prime} \end{bmatrix} = 3\%$$
 so that  $\begin{bmatrix} 0_3^{\prime} \end{bmatrix} = 8.07 \times 10^{17}$  molecules/cm<sup>3</sup>  
 $V = 1.0 \times 10^3$  cm<sup>3</sup>  
 $Q_{0_3} = 25$  scc/s  
 $Q_{NO} = 2.5 \times 10^2$  scc/s

The exponent and relative extent of the reaction taking place within the reactor can be indicated as a function of altitude, as presented below in Table 3-1. Significant departures from a 100 percent extent of reaction can lead to non-linearities and measurement errors.

TABLE 3-1.  $\left\lceil o_3 \right\rceil$   $k_1 t$  TERM VS ALTITUDE FOR ABOVE VALUES

Altitude, H (km)	Pressure (torr)	[0 <sub>3</sub> ] k <sub>1</sub> t	$\Delta [NO] / [NO]$
15	99.0	54.8	1.00
25	21.3	5.9	1.00
35	4.9	86.8	0.934
		4.15	1.00
		0.22	0.98
			0.20

For the parameters selected above, the CL method would be limited to a maximum altitude of about 25 Km. Increased reaction volume, 50 percent, and ozone flow rate, 100 percent, could extend the altitude limit to about 30 Km.

# 3.1.2 Experimental Procedures and Results

An Aerochem AAS-3S chemiluminescence monitor was extensively employed for general purpose and process control mmasurements of NO. By reversing the role of the second reactant gas, in this case  $0_3$ , ozone could also be monitored. The commercial specifications for this instrument are presented below in Table 3-2.

TABLE 3-2. AEROCHEM RESEARCH AAS-3S SPECIFICATIONS

Useful range	0.1 to 10,000 ppb
Scales	Seven full scales 10, 25, 100, 250, 1000, 2500 and 10,,00 ppb
Accuracy	Limited by calibration sample
Linearity	±1% oo full scale
Interferences	NH <sub>3</sub> in NO <sub>x</sub> mode
Time Response	ll sec on all scales
Time to Switch from One Gas to Another	Less than 15 seconds
Zero Drift	±2% in 24 hours
Gas Flow Rates	Sample ≈ 2.1 1(STP)min Air/O <sub>3</sub> ≈ 0.4 1(STP)min <sup>-1</sup>
Normal Temperature Range	15-35°C (59-95°F)
Normal Line Voltage Range	105125 volts
Electronics	Six inch analog meter on front panel with adjustable recorder output of 0 to 1 volt on rear panel.

Calibration of this type of instrument is based upon round-robin intercomparisons of several instruments and several calibration samples. Field collaborative testing of the chemiluminescence procedure is discussed by Paul C. Constant Jr. et al. (1975).

Design details for the Aerochem monitor, as well as those for the original B.A. Ridley et al. (1972) NO sensor, are given in Table 3-3. Although there are significant design differences between the instruments, the basic detection and measurement of NO is the same. The design differences are related primarily to the internal ambient pressures, reaction volumes, and flow rates and secondarily to the mode of operation used for the photomultiplier tube. The PMT is operated in an analog mode for the laboratory unit whereas for the stratospheric unit it is in a photon counting mode.

Two numerical examples are included in the table for each instrument. For the laboratory unit, an NO mixing ratio of 1 ppb(v) is assumed. For equation 3-3, this yields an intensity of 3 x  $10^5 h v/cm^3$ -s. At the anode of the PMT the signal level is given by:

$$S_{a} = IV_{R}eG(Q.E.)$$
 (3-8)

where  $V_R$  denotes reaction volume. For the above example, assuming a 10 percent effective quantum efficiency, there is a 3 x  $10^{-7}$  amp signal level. For the stated anode dark current a noise equivalent detection limit of 7 x  $10^{-3}$  ppb can easily be derived. For the stratospheric unit, an NO mixing ratio of 4 ppb(v) was adopted. For a reaction temperature of 300 K, equation 3-3 yields an intensity of about 1.9 x  $10^4 h v/cm^3$ -s. Since a mixing ratio of 4 ppb yields a signal level of 1.7 x  $10^3$  counts/s, the effective emitting volume-quantum efficiency product of 0.088 cm<sup>3</sup> is obtained. Assuming an effective quantum efficiency of 5 percent, an effective emitting volume of about 1.8 cm<sup>3</sup> is obtained, which is considerably less than the actual reaction volume.

With stratospheric instrumentation, a lowest detection limit of  $5 \times 10^7$  molecules/cm<sup>3</sup> has been verified (B.A. Ridley et al., 1972).

TABLE 3-3. DESIGN COMPARISON OF NO CHEMILUMINESCENCE SENSORS

Developer	Aerochem Research Lab	B.A. Ridley et al., (1972)
Туре	Laboratory Monitor	Stratospheric Research
Operating Pressure	250 torr	33 torr
Sample Flow Rate	35 scc/s	210 scc/s
Reactant Flow Rate	6.7 scc/s	10 scc/s
Reaction Volume, VR	10 cm <sup>3</sup>	400 cm <sup>3</sup>
Reaction Temperature	316 K	≃300 K
Residence Time	0.07 s	1.9 s
Detector	Centronics 4283 RA	EMI 9558 QA <sup>(b)</sup>
Temperature	5°C	-20°C
Gain	6x10 <sup>6</sup>	3x10 <sup>7</sup>
Dark Current	2.0 nA	85 cts/s
Conversion Factor (a)	9.76x10 <sup>-13</sup> cm <sup>3</sup> -cou1	$8.9 \times 10^{-2} \text{cm}^3$
NO Mixing Ratio	l ppb(v)	4 ppb(v) at 33 torr
NO	9.64x10 molecules/cm 3	4.25x10 <sup>9</sup> molecules/cm <sup>3</sup>
03	1.97x10 <sup>16</sup>	4.83x10 <sup>14</sup>
M	7.64x10 <sup>18</sup>	1.06x10 <sup>18</sup>
$I_o[NO][O_3]/[M]$	3.0x10 <sup>5</sup> hv/cm <sup>3</sup> -s	$1.94 \times 10^4 \text{h} \text{ V/cm}^3 \text{-s}$
Signal	3.0x10 <sup>-7</sup> A	1.7x10 <sup>3</sup> cts/s
Responsivity	300 nA/ppb	10 <sup>-1</sup> nA/ppb (360 cts/ppb)
Noise Equivalent Detection Limit	0.007	0.05 ppb
Lowest Detection Limit	0.1 ppb	0.05 ppb
Linearity	0.1-10 <sup>4</sup> ppb (1%)	0.05-34 ppb

<sup>(</sup>a)Conversion factor =  $V_{ReG}(Q.E.)$ .

<sup>(</sup>b) An RCA 31034A photomultiplier was used on the first flight yielding a responsivity of 1855 cts/ppb and a lowest detection limit of 0.02 ppb at an altitude of 22 Km or about 50 torr (Ridley et al., 1974).

#### 3.2 NITROGEN DIOXIDE PHOTOLYTIC CONVERSION

Measurement of stratospheric  $NO_2$  can take place by photolyzing the  $NO_2$  to nitric oxide, followed by gas phase titration with  $O_3$ . This method has been developed and is being used by the NOAA group (MacFarland et al., private communication, 1977). This technique was evaluated because specificity with other possible nitrogen oxide species of the stratosphere is not an issue.

## 3.2.1 Theory

The mechanism for the photolytic conversion of NO<sub>2</sub> to NO and ground state atomic oxygen is at least a four step process; namely:

$$NO_2 + hv \longrightarrow NO + O(^3P) \lambda \ge 300nm$$
 (4)

$$0 + NO_2 + M \longrightarrow NO_3 + M \tag{5}$$

$$0 + NO_2 \longrightarrow NO + O_2$$
 (6)

$$NO + NO_3 \longrightarrow 2NO_2 \tag{7}$$

The above reaction set is a subset of the set employed by Stedman and Niki (1973) to account for the kinetics and mechanism for the photolysis of  $NO_2$  in air. The expanded set includes  $O_3$ ,  $NO_3$  and  $N_2O_5$  reactions. If only reactions 4, 5 and 7 are considered, the net quantum yield is zero. If only reactions 4 and 6 are considered, the net quantum yield is two. The actual yield lies between these values.

For the above set, the rate of change of  $NO_2$  is given by:

$$-\frac{d\left[NO_{2}\right]}{dt} = k_{4}\left[NO_{2}\right] + k_{5}\left[O\right]\left[NO_{2}\right]\left[M\right] + k_{6}\left[O\right]\left[NO_{2}\right] - 2k_{7}\left[NO\right]\left[NO_{3}\right]$$
 (3-9)

Since NO<sub>3</sub> will have a rapidly defined (microseconds) stationary value, i.e.,  $d \left[ NO_3 \right] / dt = 0$ , the equation

$$k_5 \left[ O \right] \left[ NO_2 \right] \left[ M \right] = k_7 \left[ NO_3 \right] \left[ NO \right]$$
 (3-10)

can be used to simplify equation 3-9 to

$$-\frac{d\left[NO_{2}\right]}{dt} = k_{4} \left[NO_{2}\right] - k_{5} \left[0\right] \left[NO_{2}\right] \left[M\right] + k_{6} \left[0\right] \left[NO_{2}\right] \text{ or } (3-11)$$

$$\frac{d\ln\left[NO_{2}\right]}{dt} = \frac{2k_{1}k_{6}}{k_{6} + k_{5} \left[M\right]}$$

Equation 3-11 is often simplified to a first order dissociation. Examining the validity of this statement, one notes that  $k_5 = 1.0 \times 10^{-31} \text{cm}^6$ -molecule<sup>-2</sup> -s<sup>-1</sup> and  $k_6 = 9.2 \times 10^{-12} \text{ cm}^3$ -molecule<sup>-1</sup>-s<sup>-1</sup> (Hampson and Garvin, 1978). At 1 atmosphere M = 2.446 x 10<sup>19</sup> molecules/cm<sup>3</sup>, so that  $k_5 \left[ \text{M} \right] = 2.446 \times 10^{-12} \text{ cm}^3$ -molecule<sup>-1</sup>-s<sup>-1</sup> or about one-fourth that of  $k_6$ . For  $k_4 < 0.75 \ k_6 \left[ 0 \right]$ , the simplification is valid and the integrated form of equation 3-11 becomes:

$$\frac{\left[NO\right]_{t}}{\left[NO_{2}\right]_{0}} = 1-\exp\left(-I \circ t\right) \tag{3-12}$$

$$\Sigma I(\lambda) \sigma (\lambda) d\lambda$$
 (3-13)

where  $I(\lambda)$  corresponds to the photon flux rate and  $\sigma(\lambda)$  the absorption cross-section. This expression assumes a quantum yield of unity for the dissociation, a valid assumption for  $244 \le \lambda \le 398$  nm (Hampson and Garvin, 1973). The cross-section data of Johnston and Graham (1974) and that of NASA Publication 1010 (1977) have been used to obtain a value of  $k_{\Delta}$ .

Since the conversion efficiency is dependent upon k<sub>4</sub> and sample residence time, t, it is important to maximize their product.

When 0<sub>2</sub> is present in the sample stream, the above analysis is inadequate to predict experimental results. Two additional reactions impairing conversion efficiency are:

$$0 + 0_2 + M \longrightarrow 0_3 + M$$
 (8)

$$NO + O_3 \longrightarrow NO_2 + O_2$$
 (1)

when significant amounts of  $0_3$  and NO are formed, reaction (1) inhibits the photolytic dissociation process.

The converter design selected used 1 kw a mercury capillary lamp (Illumination Industries, Inc. type AH6-1BC) in conjunction with Corning 7-54 and Pyrex filters to restrict the photon flux to a spectral region defined by approximately 300-400 nm. The photolytic rate for a unit area of radiation is given by

$$k_4 A = \frac{10^7}{hc}$$
  $\int_{0}^{420} \tau \lambda (P/\Delta \lambda) \sigma \lambda d\lambda cm^2 - s^{-1}$  (3-14)

where

 $\lambda$  denotes wavelength in cm h equals Planck's constant = 6.62 x  $10^{-27} erg\text{-s}$  c equals the velocity of light = 3 x  $10^{10} \text{cm/s}$   $10^7$  denotes conversion factor for joules to ergs  $\tau_{\lambda}$  denotes spectral transmittance of the optical filters  $P/\Delta\lambda$  denotes total radiated watts per 10 nm increments  $\sigma_{\lambda}$  denotes NO<sub>2</sub> absorption cross-section in cm²/molecule, and d denotes variable of integration

With a new lamp operating at 1 kw and with the filters indicated, evaluation of the above expression yields  $k_4A = 74 \text{ cm}^2 - \text{s}^{-1}$  and  $k_4 = 0.26 \text{ s}^{-1}$  for this design. The residence time for this cell is approximately 5 seconds so that the conversion efficiency is predicted to be 73 percent. The actual design and measured results for the photolysis of  $NO_2$  is treated in the next two paragraphs.

## 3.2.2 Stratospheric-Based Instrumentation Modeling

Computer modeling predictions for stratospheric pressure are considered. For the case where P = 19 torr (25km),  $k_5$  [M] is reduced by a factor of 40 and the photolytic conversion efficiency increases from 12.8 percent to 44 percent for  $k_4 = 0.26$  s<sup>-1</sup>. Thus the performance of the photolytic technique improves with reduced pressure.

# 3.2.3 NO, Photolytic Converter Design

Prior to discussing the procedures and results for the NO<sub>2</sub> photolytic converter, the design of the laboratory converter is presented. The design

of the overall converter was based upon the availability of a photochemical lamp, expedience of attaining the proper spectral filtering and material chemistry aspects.

The high pressure mercury arc capillary lamp is of the straight bore type with a rating of 1 kva. The lamp, part number AH6-1BC, was obtained from Illumination Industries, Inc. To dissipate non-radiative heat, a water cooling jacket was provided. The jacket comprises two concentric cylinders made of quartz and Pyrex. The Pyrex was selected to attenuate radiation below about 300 nm. To suppress radiation above about 400 nm, Corning filter glass 7-54 was employed and configured as a hexagonal cylinder circumscribing the outer cooling jacket. The filter glass elements were held in place by teflon disks supported inside a gold-plated aluminum cylinder which served as the photolytic reaction vessel.

Lamp cooling with high pressure Hg lamps is critical and one is constrained to maintaining the temperature over a finite range so that the proper vapor pressure of mercury is attained while simultaneously minimizing stresses in the quartz envelope. Also steam must be prevented from forming on the quartz envelope. To achieve the above requirements the lamp is used in a horizontal position, chilled de-ionized water is flowed through the water jacket assembly at a rate of 1-1.5 gpm, and an inner jacket or "velocity tube" is employed to minimize the water volume near the lamp envelope, thus increasing the flow velocity.

An a-c power supply, employed for driving the lamp, consists of a line voltage variac, 4 kva transformer, current monitor and voltage monitor. The transformer of a soft iron design has built-in leakage inductance. To assist in starting the lamp at a reasonable voltage close to operating voltage, a small amount of argon is contained within the lamp envelope. The voltage waveform is typically a square wave with a slight overshoot on the leading edge.

Design parameters for the photolytic cell are given in Table 3-4.

TABLE 3-4. NO<sub>2</sub> PHOTOLYTIC CELL DESIGN

Parameter	<u>Value</u>
Lamp Luminous Length	2.54 cm
Lamp Bore Diameter	0.2 cm
Quartz Velocity Tube ID, OD	12, 15 mm
Pyrex Tube ID, OD	36, 41 mm
Corning Filter Facet Width	2.2 cm
Sample Cylinder ID	10.3 cm
Effective Radiative Area	280 cm <sup>2</sup>
Radiated Sample Volume	177 cm <sup>3</sup>
Sample Flow Rate	2.1 SLPM
Sample Residence Time	5.05 s
Lamp Current	1.2 amps
Lamp Voltage	435-700 V
Lamp Power	552-840 W
Near UV (320-400 nm) Radiated Power	112.3 w @ 1 kva
365 nm Radiated Spectral Power	3.6 w/nm
Radiated Power/Input Power	0.46
Materials Exposed to NO Sample	Gold, stainless steel 303, Teflon, Corning glass, Pyrex
NO Design Conversion Efficiency @ l kva	73 percent

# 3.2.4 Experimental Procedures and Results

Pre-mixed and calibrated samples of NO<sub>2</sub>/air were obtained from Airco in aluminum Spectra-Seal cylinders. Airco calibrations of 0.6-10 ppm concentrations were verified using the catalytic thermal converter of the Aerochem CL monitor discussed in paragraph 3.1.

Sample pressure was reduced and regulated using Matheson type regulators containing stainless steel diaphragms. Sample flow rate was set by the Aerochem CL monitor pump and internal sonic orifice. All other plumbing was either stainless steel or teflon (PTFE)\*.

<sup>\*</sup>PTFE, polytetrafluorethylene

Relatively new lamps (less than 10 hours of aging) were employed; however no effort was expended in logging the number of on-off cycles which do affect lamp life. In operation the cell was connected in series with the CL monitor. With the Hg lamp in the off state, the CL monitor was set to the NO<sub>X</sub> mode to measure the NO<sub>2</sub> entering the photolytic cell. The lamp was then excited and the CL monitor was placed in the NO mode to measure the amount of NO leaving the photolytic cell. If there was no or negligible NO in the supply gas then the ratio of the two measurements was simply the converter efficiency.

The results of the tests are given in Table 3-5 for various lamp power levels. Assuming a linear relation between input power and radiated power, the various anticipated rates and converter efficiencies are included. The measured efficiencies do not correspond directly to the calculated efficiencies but this is expected, since the rates were derived from brochure data and not measured values. The computer derived efficiencies are in large variance with the measured efficiencies. An attempt to account for this variance is given below.

TABLE 3-5. CALCULATED AND MEASURED NO<sub>2</sub> PHOTOLYTIC CONVERTER EFFICIENCIES

Lamp Voltage (Volts)	Lamp Power (Watts)	k <sub>4</sub> (s <sup>-1</sup> )	First Order Calculated Efficiency (Percent)	Computer Code ∆[NO]/∆[NO <sub>2</sub> ]	Measured Efficiency (Percent)
435	522	0.14	50	0.58	35
525	630	0.17	57	0.64	45
700	840	0.22	67	0.63	57
-	1000	0.26	73	0.62	-

The oxidation of NO<sub>2</sub> by  $0(^3P)$  has a predominating effect for producing the intermediary, NO<sub>3</sub> with  $k_5$  M being 2.36 x  $10^{-12}$  cm<sup>3</sup>/molecule-s. The NO<sub>3</sub> is then available to react with NO<sub>2</sub> forming N<sub>2</sub>O<sub>5</sub>, or with NO forming NO<sub>2</sub>. Formation of NO<sub>2</sub>, reaction (7), proceeds at a rate about an order of magnitude faster than the formation of N<sub>2</sub>O<sub>5</sub>. Thus, as previously mentioned, the quantum

yield is reduced. If the ground state oxygen atom were scavenged by some other means, then the predicted yield would increase.

From this data one notes that efficiency is a design engineering trade relating power with photon flux as well as sample residence time. The residence time is of course related to the selected photolytic cell volume and the flow selected for the high sensitivity NO chemiluminescence monitor.

## 3.3 NITROGEN DIOXIDE CATALYTIC CONVERSION

Results obtained in employing several types of catalytic converters for NO<sub>2</sub> measurements are reported in this section. The types included are (1) catalytic-thermal converters, (2) chemical-thermal converters, (3) catalytic-chemical converters and (4) catalytic-sorption converters.

Significantly different results have been found for type (1) and type (2) converters when O<sub>3</sub> is present. A type (1) converter used in this study employs a noble metal while the type (2) converters investigated by Dr. Max Lowenstein of NASA employed a metal readily oxidizeable. Section 3.3.1.1 attempts to justify the widely disparate results observed with these converters.

# 3.3.1 Catalytic/Chemical Thermal Converters

## 3.3.1.1 Theory

Since much of the data reported upon in subsequent sections is based upon catalytic thermal conversion, a review of thermal converters both catalytic and chemical is warranted.

Table 3-6 lists various metals and carbon which have been used in NO $_{\rm X}$  or NO $_{\rm 2}$  converters. The listing has been arranged in decreasing value of the Gibbs or free energy formation of the oxide of the metal (or carbon). If the free energy value listed is negative, the reaction can occur. The reverse reaction, decomposition, would then have a positive value and would not occur. The last column corresponds to the minimum temperature required to achieve about 98 percent conversion of NO $_{\rm 2}$  for non-oxidized surfaces (L.P. Breitenbach and M. Shelef, 1973).

TABLE 3-6. FREE ENERGY OF FORMATION  $\Delta$  F' (kcal/OXYGEN ATOM) AND TEMPERATURE FOR 98 PERCENT NO, CONVERSION

	1	300 K	400 K	500 K	T(°C)
Unstable Oxide	x <sup>(a)</sup>				600-1000
	Ag			+ 0.06	
	С	-32.8	-35.0	-37.1	400-600
	Ni			-46.1	750 <sup>(b)</sup>
	Fe	-59.2	-57.1	-54.9	725-750 <sup>(c)</sup>
	Мо	-63.6	-61.4	-59.3	525
	W	-63.7	-61.5	-59.3	475
	Mn			-83.1	475
Stable Oxide	v			-89.0	475

- (a) Other noble metals(b) Inconel; 80% Ni, 14% Cr, 6% Fe
- (c) Monel; Stainless steel 304 and 316

As noble metal oxides have positive energies of formation, they are unstable and do not readily form in the presence of oxidants. Generally, they act as catalysts for many oxidizing and reducing reactions. In the case of NO, conversion, their inertness quality must be traded off against minimum conversion temperature.

For the remaining elements, NO, conversion proceeds according to the reactions:

$$NO_2 \longrightarrow NO + 1/2 O_2$$
 (9)

$$M + O_2 \longrightarrow MO_2$$
,  $M = (Mo, W, Mn, V)$  (10)

With increased usage, i.e. surface oxidation, the conversion temperature must be increased to effect the same conversion efficiency.

For the elements with negative free energies of formation, the element acts as an oxygen scavenger. As the free energy of formation becomes more

negative, the conversion temperature can be reduced since the oxidation becomes more preferred. For any given metal, as the temperature is increased, the free energy of oxide formation is shifted toward more positive values, thus reducing its effectiveness for NO<sub>2</sub> reduction. The use of carbon, coke in metallurgical ore reduction, permits lower temperature operation and the conversion proceeds as:

$$NO_2 + C \longrightarrow NO + CO \tag{11}$$

As C is converted to CO or CO<sub>2</sub> in reducing NO<sub>2</sub> or by virtue of the oxygen molecules in an air stream, the surface material, C or M, becomes ineffective.

If a strong oxidant,  $0_3$ ,  $H_2O_2$ ,  $HNO_3$ , or  $HNO_4$ , is present in the sample stream, the surface material, C or M, is rendered ineffective at a faster rate.

From the above discussion, two facts are evident for NO converters. First, thermal converters employing true catalysts, e.g. platinum, stainless steel, and possibly nickel alloys, should be identified as catalytic-thermal converters, whereas the others (eg. Mo) should be identified as chemical-thermal converters. Second, chemical-thermal converters as defined above, can be expected to lose their efficiency if strong oxidants at significant concentration levels are present in the sample. The term "poisoning" is sometimes used to describe this efficiency loss but the definition is loose. Finally, to maintain efficiency, oxidant scavengers or scrubbers are often considered.

In the absence of any catalytic material, thermal conversion of NO $_2$  can also occur (Altshuller, 1957 and Breitenbach, 1973). The reaction, (9), is well understood and has been used to set converter temperatures. For oxygen at 152 torr, the ratio of  $\begin{bmatrix} NO_2 \end{bmatrix}$  to  $\begin{bmatrix} NO \end{bmatrix}$  is given by:

$$\log \left[\frac{NO_2}{NO}\right] = \frac{3002}{T} - 4.2226 \tag{3-15}$$

# 3.3.1.2 Experimental Procedures and Results: Chemical-Thermal Converters

Experimental work by Dr. Max Lowenstein of NASA-ARC (private communication, 1978) has shown that for medium temperature molybdenum-based converter construction, NO<sub>2</sub> conversion may drop to zero if O<sub>3</sub> is present in the sample stream. It is felt that a two-body chemical reaction plus surface chemistry may be occurring.

The following two-body mechanism may also be occurring as an abnormal situation. First,

$$NO_2 + O_3 \rightarrow NO_3 + O_2$$
 (12)

which is very fast, a factor of 50 due to the high temperature, when compared to a 298 K temperature rate. The mechanism continues as follows:

$$NO_2 + NO_3 \rightarrow N_2O_5$$
 (13)

$$NO + NO_3 - 2NO_2$$
 (7)

with a net result of

$$NO + N_2O_5 - 3NO_2$$
 (14)

and also

$$2NO + O_2 - 2NO_2$$
. (15)

This last reaction is of the third order type and extremely slow with a rate constant

$$k_{15} = 3.3 \times 10^{-39} \exp(-1050/RT) \text{ cm}^3 - \text{molecule}^{-2} - \text{s}^{-1}$$
.

#### 3.3.1.3 Experimental Procedures and Results: Catalytic-Thermal Converters

The commercial converter in use at Perkin-Elmer is constructed of incomel, alumina and a 90% Pt-10% Rh wire heating filament. As such, it approximates an catalytic-thermal converter. Conversion efficiency of this unit, without  $0_3$  present, was first determined by the accepted Federal Register (1973) method, which is based upon reaction (15) given above and the fast reaction ( $k_1 = 1.66 \times 10^{-14} \text{ cm}^3/\text{molecule-s}$ );

$$NO + O_3 \rightarrow NO_2 + O_2, \tag{1}$$

both of which produce stoichiometric quantities of NO<sub>2</sub>. For all tests with the converter at its design temperature of 1100°C, conversion was greater than 99.7 percent.

The next set of conversion determinations for the commercial unit were made with about 9 ppm 0<sub>3</sub> present and 9.5 ppm NO<sub>2</sub>. The average conversion efficiency was found to be 97.9 percent or about 1.8 percent less, which is in concurrence with findings at NASA-ARC but not of real significance.

Generation of NO from  $O(^3P)$ , a product of  $O_3$  thermal decomposition, is a possibility if surface recombination of atmoic oxygen does not occur on the platinum surface. A brief series of tests was carried out to assure that the surface recombination mechanism was in fact sufficient to scavenge  $O(^3P)$ . The catalytic thermal converter of the Aerochem CL monitor was used at reduced temperature, approximately 750 K, and a stream of ozonized air was passed over the platinum-rhodium heating filament. The ozone concentration level was typically 2.7 x  $10^{13}$  molecules/cm<sup>3</sup> (1.1 ppm). Measurement of NO<sub>x</sub> downstream from the converter was typically 2.45 x  $10^{10}$  molecules/cm<sup>3</sup> (1.0 ppb) greater than the measured (NO<sub>x</sub>) upstream of the converter. During these tests, the trace contamination NO level of the air source was 1.6 x  $10^{11}$  molecules/cm<sup>3</sup> (6.5 ppb), while the instrument noise level was 2.45 x  $10^9$  molecules/cm<sup>3</sup> (0.1 ppb). Summarizing this test data one may conclude that 99.9 percent of the  $O(^3P)$  atoms recombined, thereby providing effective scavenging.

It is important to note here that (1) catalytic thermal conversion is more effective for reducing  $NO_2$  to NO than thermodynamic conversion and (2) that large relative levels of  $O_3$  do not seriously impact the conversion process.

#### 3.3.2 Catalytic-Chemical Converters

#### 3.3.2.1 Theory

For this type of converter ferrous sulphate and ferrous ammonium sulphate were employed.

Although the gas-solid phase chemistry is not well known for the action of  $NO_2$  and  $FeSO_4$ , the appropriate acidic solution is well known.  $Fe^{++}$  reduces  $HNO_2$  to NO, which in turn combines with  $Fe^{++}$  to form  $Fe(NO)^{++}$ . This ion has a characteristic dark brown color. If  $NO_3$  is present, in the absence of the  $NO_2$ , reduction occurs, forming as before  $Fe(NO)^{++}$ . This latter reaction occurs only when  $H^+$  are prevalent and temperature is relatively higher. These conditions occur at the liquid-liquid boundary layer, and a brown ring forms.

Ferrous ammonium sulphate is the better converter choice since it is known that  $\text{FeSO}_4$  selectively removes oxidants, specifically ozone (Miller et al., 1971). The Ridley-Schiff group also confirmed this fact in early 1978 when employing  $\text{FeSO}_4$   $^{\bullet}$   $^{\circ}$  7H $_2$ O to convert ppb levels of NO $_2$  when ppm levels of O $_3$  were present.

#### 3.3.2.2 Experimental Procedures and Results

Tubular flow converters were constructed with glass, quartz wool packing and stainless steel fittings along with the dehydrated form of the sulphate.

The initial converters were sized to yield a space velocity (flow rate/catalyst volume) of about 93 min<sup>-1</sup> and a superficial linear velocity (flow rate/converter cross-sectional area) of about 2.4 x  $10^3$  cm/min. The final converter used extensively with  $Fe(NH_4)_2(SO_4)_2$  was designed to yield a space velocity of about 17.5 min<sup>-1</sup> and superficial linear velocity of about 5 x  $10^2$  cm/min.

Initial tests (1 through 3) for each catalyst resulted in large percentage losses of the  $NO_2$  as presented in Tables 3-7 and 3-8. Subsequent testing indicated that viton seals were acting as adsorbents. Particular emphasis was placed upon  $Fe(NH_4)_2$  ( $SO_4$ )<sub>2</sub> since  $FeSO_4$  is a selective remover of  $O_3$ . Procedural changes resulted in no detectable  $NO_2$  loss for the subsequent  $Fe(NH_4)_2$  ( $SO_4$ )<sub>2</sub> tests. Conversions were found to be consistently greater than 97.5 percent.

The use of  $Fe(NH_4)_2$  (SO<sub>4</sub>)<sub>2</sub> is a competitive technique to NO<sub>2</sub> 300-400 nm photoylsis, however, careful packaging design of the catalyst bed is required

TABLE 3-7. FERROUS SULPHATE CATALYTIC CONVERTER TEST RESULTS

Test	Species	1	2	3
Pre-converter concentration	NO x	4.2ppm	68ppb	68ррь
	NO <sub>2</sub>	2.4	62	62
	NO	1.8	6	6
Post-converter concentration	NO x	3.6	33.5	30
	NO <sub>2</sub>	0	19.8	17.5
	NO	3.6	13.7	12.5
NO <sub>2</sub> converted	∆ NO	1.8	7.7	6.5
NO <sub>2</sub> unconverted		0.0	19.8	17.5
NO <sub>2</sub> entrapped	∆ NO <sub>x</sub>	0.6	34.5	38.0
NO <sub>2</sub> % conversion		75	12.4	10.5
NO <sub>2</sub> % unconverted		0	31.9	28.2
NO <sub>2</sub> % entrapped		25	55.6	61.3

so as not to reduce sample flow rate significantly nor represent a significant pressure drop.

## 3.3.3 Catalytic Sorption Converters

For this series of tests, Matthey-Bishop catalysts, 1% Pt and 0.4% Pd with 0.1% Pt on support columns, were contained in glass tubing. The combined weight of the pellets was about 5 gms. Nitric oxide was reacted with  $0_3$  to provide NO, NO<sub>2</sub> and a minimal amount of  $0_3$ . The resulting concentrations at the converter input are shown below for two tests using the 1% Pt catalyst.

	Test 1	Test 2
NO	3.15 ppm	5.20 ppm
NO <sub>2</sub>	2.65	2.95
NO <sub>x</sub>	5.8	8.15
03	5.5 ppb	0.5 ppb

FERROUS AMMONIUM SULPHATE CATALYTIC CONVERTER TEST RESULTS TABLE 3-8.

Test (a) Species	-	•	,	•	U	7	_	٥	c
	(ppb)	, dqq)	(qdd)	(bpm)	(mdd)	(mdd)	(mdd)	(mdd)	(mdd)
Pre-converter NO concentration	437	437	443	2.68	07.4	7.20	4.65	2.74	1.55
NO <sub>2</sub>	435	435	429	2.68	7.40	7.20	4.65	2.74	1.55
ON	2	2	14	0.0	0.0	0.0	0.0	0.0	0.0
Post-converter NO <sub>x</sub> concentration	100	80	95	2.68	07.7	7.20	4.65	2.74	1.55
NO <sub>2</sub>	70	30	47	90.0	0.09	0.09	0.015	0.04	0.03
NO.	30	20	87	29.2	4.31	7.11	4.50	2.70	1.52
NO, converted NO	28	48	34	2.62	4.31	7.11	4.50	2.70	1.52
NO, unconverted	20	30	47	90.0	60.0	0.09	0.15	9.0	0.03
NO <sub>2</sub> Entrapped NO <sub>x</sub>	337	357	348	0.0	0.0	0.0	0.0	0.0	0.0
NO, % conversion	6.44	11.0	7.9	97.8	6.76	98.7	8.96	98.5	98.1
NO, Z unconverted	16.1	6.9	10.9	2.2	2.1	1.3	3.2	1.5	1.9
NO2 % entrapped	77.5	82.0	81.1	0.0	0.0	0.0	0.0	0.0	0.0

Tests 1 through 3 employed a converter with a space velocity of about 93 min and a superficial linear velocity of about 2.4 x 10 cm/min. Tests 4 through 9 employed a converter with a space velocity of about 17.5 min and a superficial linear velocity of about 5 x 10 cm/min. Tests 1 through 3 were conducted with viton seals which caused substantial absorption. (a)

The NO, NO<sub>X</sub> concentrations at the output of the converter were found to be equal to each other and equal to 1.42 and 2.80 ppm, respectively. From this data it was concluded that (1) NO<sub>2</sub> either converted, or was adsorbed or both, (2) a portion of the NO was adsorbed, and (3) from this data, it may be concluded that these materials are not considered to be useful. In light of these results, further planned tests were abandoned.

# 3.4 NITROUS PENTOXIDE (N2O5) GENERATION

As nitrous pentoxide  $(N_2O_5)$  is reactive and unstable in the gaseous state, it was generated as needed. For  $N_2O_5$  synthesis, excess  $NO_2$  or excess  $O_3$  and the other reactant were mixed in an elementary type flow system. The reactant product  $NO_3$  and  $NO_2$  combined yielding  $N_2O_5$ . This technique approximates the approach used by others.

Process control and determination of initial concentration levels, i.e., before dynamic dilution, were carried out by IR absorption techniques. Measured concentration levels as opposed to predicted levels were desired because of the reactive nature of the particular species. The levels after dilution were then employed in the overall assessment of an appropriate chemical converter ahead of a chemiluminescent monitor. The specific details of the IR measurements are discussed in Appendix A.

# 3.4.1 Theory

Generation of gas phase  $N_2O_5$  is best carried out by the ozone oxidation of  $NO_2$  as it is reasonably stable in the presence of ozone. The governing reactions are:

$$NO_2 + O_3 \longrightarrow NO_3 + O_2$$
 (rate determining) (12)

$$NO_2 + NO_3 \longrightarrow N_2O_5$$
 and (13)

$$N_2O_5 \longrightarrow NO_2 + NO_3$$
 (-13)

where the equilibrium constant, K = 1.2 x  $10^{-11}$  molecules/cm<sup>3</sup> at a temperature of 300 K. The reaction can be carried out with either  $\begin{bmatrix} NO_2 \end{bmatrix}$  or  $\begin{bmatrix} O_3 \end{bmatrix}$  in excess. Reaction (12) is about 34 kcal/mole exothermic. Measured stoichiometry  $\begin{bmatrix} \Delta NO_2/\Delta O_3 \end{bmatrix}$  values are 1.88 and 1.68 for excess  $O_3$  and  $NO_2$ , respectively (Wu et al., 1973), and 1.89  $\pm 0.08$  (standard deviation) (Graham, 1975).

Various experimental rate constant values for  $k_{12}$  are shown as an Arrhenius plot in Figure 3-1. The Arrhenius parameters for the results of Johnston and Yost (1949) are

$$k_{12} = 9.82 \times 10^{-12} \exp(-7000/RT) \text{ cm}^3 \text{-molecule}^{-1} \text{-s}^{-1}$$

and for the results of Graham (1975) are

$$k_{12} = (1.34 + 0.11) \times 10^{-13} \exp(-4900 \pm 60/RT) \text{ cm}^3 - \text{molecule}^{-1} - \text{s}^{-1}$$

where the uncertainties are standard deviation.

For design purposes an average value of 5.37 + 1.76 x  $10^{-17}$  cm<sup>3</sup>-molecule<sup>-1</sup>-s<sup>-1</sup> (1.32 +0.43 x  $10^{-3}$  ppm<sup>-1</sup>s<sup>-1</sup>) at 298 K and 760 torr was chosen.

The integrated rate equation for the bimolecular reaction is given by:

$$\frac{1}{\left[\frac{NO_2}{NO_2}\right]_o - \left[\frac{O_3}{O_3}\right]_o \left[\frac{\left[NO_2\right]_o - \left[\frac{NO_3}{O_3}\right]}{\left[\frac{NO_2}{O_3}\right]_o - \left[\frac{NO_3}{O_3}\right]}\right)} = k_{12}t \quad (conc)^{-1}$$
 (3-16)

where the subscript denotes original concentration levels. This expression is plotted in Figure 3-2 for  $\left[NO_2\right]_0 = 25$  ppm and  $\left[O_3\right]_0 = 10$  ppm.

# 3.4.2 Experimental Procedures

The attendant measurements required to follow the reaction include: (1) initial concentrations and flow rates, (2) the  $\begin{bmatrix} 0_3 \end{bmatrix}$  as the sample leaves the reaction vessel so that the extent of the reaction (c.f., Figure 3-2) can be determined, and (3) the  $\begin{bmatrix} NO_2 \end{bmatrix}$  as the sample leaves the reaction vessel so that the stoichiometry can be determined. The latter measurement must be made by a technique that does not destroy either  $NO_3$  or  $N_2O_5$  (e.g., IR absorption). The transit time of the sample between the reaction vessel and the appropriate monitor must be known or be small compared to the residence time of the sample in the reaction vessel.

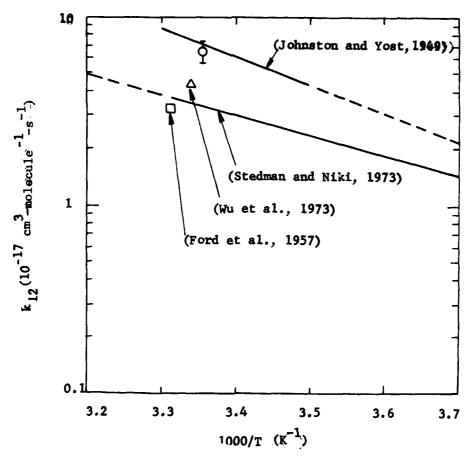


Figure 3-1. Arrhenius Plot For NO<sub>2</sub>-O<sub>3</sub> Reaction

Kinetic runs were carried out initially at 0.25 and 0.50 SLPM with 13.1 ppm NO<sub>2</sub> and 26.0 and 13.0 ppm O<sub>3</sub>, respectively, prior to dilution by the carrier of the other reactant. Subsequent tests were made at a total flow rate of 2.1 SLPM yielding a residence time of about 408 seconds. The reaction vessel volume of 14.3 liters and surface-to-volume ratio of 0.4 cm<sup>-1</sup> consisted of a 1 liter stainless steel sampling cylinder with concentric counter flow tubing, a 7.8 liter stainless steel vessel and a 5.5 liter PTFE-lined vessel with AgCl windows that also served as a 20 meter White cell for IR absorption measurements. Measurements were usually carried out with a pathlength of 15.75 meters. The stainless steel vessels were vacuum baked prior to ozone conditioning of the walls and flow of the reactants. The above conditioning usually lasted for several hours. Flow rates were controlled by Tylan FC-260 flow controllers. These units were modified slightly by substituting

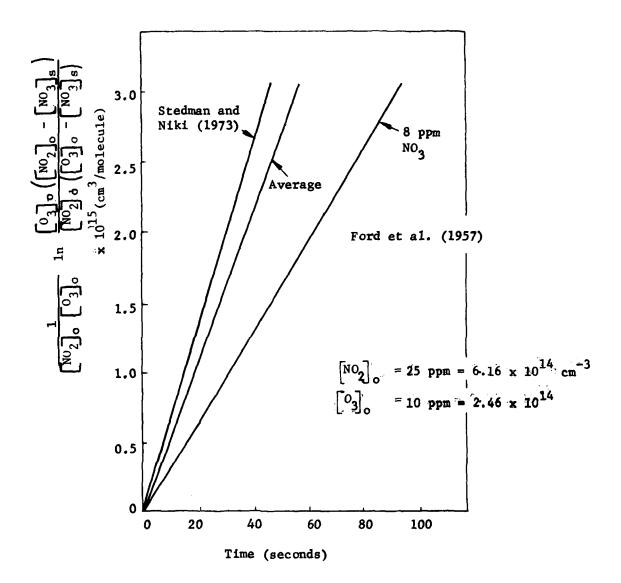


Figure 3-2.  $NO_3$  Generation versus Time (T = 298 K)

PTFE O-rings for Viton O-rings. Steady-state flow conditions were usually reached after about 20 minutes. Infrared transmittances over the 1800-1000 cm<sup>-1</sup> spectral range of the White cell contents were employed to follow the course of the reaction. As the flowing system desiccated itself with use, the relative amount of HNO<sub>3</sub> decreased substantially and improved the N<sub>2</sub>O<sub>5</sub> yield and standard deviation.

The initial quantitative tests are tabulated in Table 3-9. The measured stoichiometry of 1.86  $\pm 0.06$  is in excellent agreement with the work of Wu

TABLE 3-9. N<sub>2</sub>O<sub>5</sub> GENERATION AND STOICHIOMETRY MEASUREMENTS (a)

$(1.44 \pm 0.17) \times 10^{-3}$				1.86±0.06					Mean ± SD
		20	1.96	1.87	0.0	7.39	5.45	9.40	36
		777	1.42	1.76	0.0	5.63	6.30	9.50	ø
1.30, 1.43		54	2.67	1.82	3.94	12.9 <sup>(c)</sup>	2.15	7.10	10
1.60, 1.69		20	2.39	1.90	2.90	12.0	2.40	7.20	6
1.276, 1.323x10 <sup>-3</sup>	0.30	65	2.79	1.93	3.70	12.0	2.15	6.45	<b>&amp;</b>
		41	0.37	٠.	14.2	15.9	0.0	0.0	2 (P)
		23	09.0	1.90	10.0	15.1	0.087	2.66	4
Rate Constant (ppm <sup>-1</sup> -s <sup>1</sup> )	[HNO <sub>3</sub> ]	Yield %	$\begin{bmatrix} N_2 O_5 \end{bmatrix}$	Δ NO <sub>2</sub> /Δ0 <sub>3</sub>	$[NO_2]_{f}$	$[NO_2]_{i}$	[03] f	[0 <sub>3</sub> ] i	Expt.
		CTUTTION	TOCUMENT THE	2.5 The state of t		5.2			

(a) Concentrations in ppm units (= 2.4 x  $10^{13}$  molecules/cm<sup>3</sup>).

For this test 10 ppm NO was also present as an initial reactant and consumed 9.4 ppm  $0_3$  introduced as an initial reactant. This left 0.6 ppm NO by calculation vs a measured quantity of 0.62 ppm NO. The source of 0.37 ppm  $N_2 0_5$  is not clearly understood. **(**P

The average for previous workers is (1.32  $\pm 0.43$ ) x  $10^{-3}$  ppm<sup>-1</sup>s<sup>-1</sup> at T = 298 K. છ

et al. (1973) and Graham (1975) shown in Figure 3-3. For a flow tube reactor operated with homogeneous mixing the rate constant for the reaction can be obtained from the steady-state concentrations of the reactions. For the rate limiting oxidation of  $NO_2$  by  $O_3$  the expression for the rate is given by:

$$k_{11} = \frac{-\frac{Q}{V} \left(-\Delta NO_{2}\right)}{2\left[NO_{2}\right]_{f}\left[O_{3}\right]_{f}} = \frac{-\frac{Q}{V}\left(-\Delta O_{3}\right)}{\left[NO_{2}\right]_{f}\left[O_{3}\right]_{f}}$$
(3-17)

where the factor of 2 denotes the ideal stoichiometry, Q the flow rate, and f the final or steady-state concentration. Where determinant, the two rates are listed in Table 3-9 in the last columns. The value of (1.44  $\pm 0.17$ ) x  $10^{-3} \text{ ppm}^{-1} \text{s}^{-1}$  is in excellent agreement with the work of others. The measured  $N_2O_5$  yield compared to the theoretical yield based upon the stoichiometry and consumption of reactants has improved from about 23 percent to 65 percent.  $N_2O_5$  is easily hydrolyzed by water forming nitric acid as a product. As it is usually a heterogeneous wall reaction, reconciliation of the odd-nitrogen budget is impossible. Circumvention of this problem to date has used in-situ IR absorption.

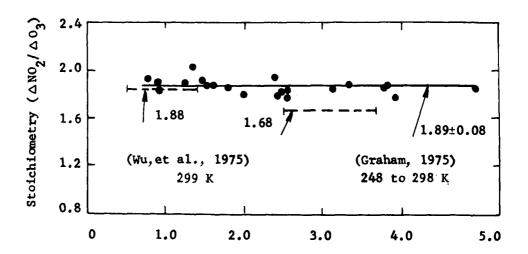


Figure 3-3. Plot of Measured Stoichiometries versus Initial Reactant Ratio For NO<sub>2</sub>-O<sub>3</sub> Experiments

# 3.5 NITROUS PENTOXIDE (N2O5) THERMAL CONVERSION

## 3.5.1 Theory

The thermal conversion of  $N_2O_5$  is a complex reaction with a net stoichiometric reaction:

$$2N_2O_5 \longrightarrow 4NO_2 + O_2$$
 (16)

When NO, NO<sub>2</sub>, and  $O_3$  are present  $N_2O_5$  can either be converted, generated, or serve as a catalyst according to the following net stoichiometric reactions:

$$NO + N_2O_5 \longrightarrow 3NO_2$$
 (14)

$$2NO_2 + O_3 \longrightarrow N_2O_5 + O_2$$
 (17)

$$20_3 + N_2O_5 \longrightarrow 30_2 + N_2O_5$$
 (18)

Reaction 16 will be treated first. The governing mechanistic reactions for reaction 16 are the decomposition and recombination of N205 followed by two simultaneous bimolecular reaction paths, one of which has a fast sequential reaction converting NO, if present. These reactions are (H.S. Johnston, 1951):

$$N_2O_5$$
  $[M]$   $NO_2 + NO_3$  (-13)  
 $NO_2 + NO_3$   $[M]$   $N_2O_5$  (13)

$$NO_2 + NO_3 \stackrel{[M]}{\longrightarrow} N_2O_5$$
 (13)

$$NO_2 + NO_3 \longrightarrow NO + NO_2 + O_2$$
 (19)

$$NO + NO_3 \longrightarrow 2NO_2 \tag{7}$$

$$NO_3 + NO_3 \longrightarrow 2NO_2 + O_2$$
 (20)

Rate limiting is governed by reactions (19) and (20).

The pyrolytic kinetics of these reactions have been studied by Schott and Davidson (1958) for temperatures greater than 450 K with argon as a diluent. The dissociation reaction of N2O5 is unimolecular, close to its secondorder low pressure limit. The differential rate equation is given by:

$$\frac{d \left[N_2O_5\right]}{dt} = k_{-13} \left[M\right] \left[N_2O_5\right] \tag{3-18}$$

with  $k_{-13}$  = 5.0 x  $10^{13}$  exp (-16,500+700/RT)  $(mo1/1)^{-1}-s^{-1}$ . At a pressure of 1 atmosphere and a temperature of 600 K, the concentration of the diluent [M] is 2.01 x  $10^{-2}$  mol/1 and  $k_{-13}$  = 4.85 x  $10^{7}$  (mol/1) $^{-1}-s^{-1}$ . At a reduced temperature of 400 K,  $k_{-13}$  = 4.77 x  $10^{4}$  (mol/1) $^{-1}-s^{-1}$ . Integration of the above expression leads to:

$$\begin{bmatrix} NO_2 \end{bmatrix} = \begin{bmatrix} N_2O_5 \end{bmatrix} \left\{ 1 - \exp \left( -k_{-13} \begin{bmatrix} M \end{bmatrix} \right) t \right\}$$
 (3-19)

or a half-life of

Half-Life = 
$$\frac{\ln 2}{k_{-13} \left[ M \right]}$$
 = 0.70 s for 600 K and (3-20) = 0.48 ms for 400 K

For the conditions of the stratosphere, the half-life is given below in Table 3-10.

TABLE 3-10. PREDICTED HALF-LIFE OF N2O5 IN A 400 K THERMAL CONVERTER

H (km)	P (atm)	[M] (mo171)	1n 2 k-13 [M]
10	0.262	$8.0 \times 10^{-3}$	$1.8 \times 10^{-3}$
15	0.119	3.6	4.0
20	0.054	1.6	9.0
25	0.025	7.6 x 10 <sup>-4</sup>	$1.9 \times 10^{-2}$
30	0.012	3.7	3.9
35	0.0057	1.7	8.5
40	0.0027	$8.2 \times 10^{-5}$	$1.8 \times 10^{-1}$

If the  $0_2$  and  $N_2$  molecules of the stratosphere take on the same role as the argon, then nearly complete conversion of  $N_2 0_5$  will occur if the residence time in the converter is about one second. A constant volume pump with a flow rate of 2.0-2.5 1/s requires a volume of 2.0 to 2.5 liters.

As cleanliness of the cell is a requirement to render heterogeneous wall reactions to negligible level, the converter volume-to-surface (V/S) ratio becomes important. Assuming a 2.5 cm diameter converter, the length required would be about 2 meters to obtain the necessary volume. If, however, the converter is designed to the 35 km specification limit; the residence time is set to four half-lives (94 percent conversion); and the diameter is increased to 5 cm, then the length becomes 35 cm for a 2 liter/s flow rate. The respective V/S ratios for the above converters are 0.61 and 1.23 cm, respectively.

Returning to the simultaneous bimolecular reactions with  $k_7 >> k_{19}$ , the differential rate equation for the intermediary, NO<sub>2</sub> is given by

$$-\frac{d \left[NO_{3}\right]}{dt} = 2k_{19} \left[NO_{2}\right] \left[NO_{3}\right] + 2k_{20} \left[NO_{3}\right]^{2}$$
 (3-21)

For a given reaction chamber, assuming steady-state conditions, a rate relation is written as:

$$R_{NO_3} = {}^{Q}_{V} \left( \left[ NO_3 \right]_i - \left[ NO_3 \right]_s \right)$$
 (3-22)

where  $R_{NO_3}$  is the rate of disappearance of  $NO_3$ , Q is the flow rate, V is the reaction volume, and the subscripts i and s denote initial and steady-state conditions. The ratio Q/V has the units of  $s^{-1}$  and is inversely related to residence time.

Combining the two rate equations and dividing by 2  $\left\lceil NO_2 \right\rceil \left\lceil NO_3 \right\rceil$  yields,

$$k_{19} + k_{20} = \frac{[NO_3]}{[NO_2]} = \frac{1}{t} = \frac{[NO_3]_i - [NO_3]_s}{[NO_2]_i - [NO_3]_s}$$
 (3-23)

where

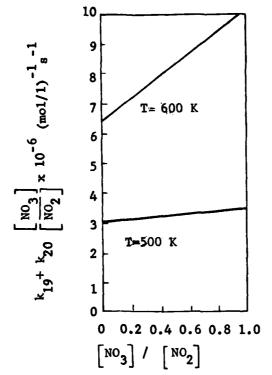
$$\log k_{19} = -(965 \pm 150)/T + 8.41$$
 (3-24)

and

$$\log k_{19} + k_{20} = -(1403 \pm 60)/T + 9.34$$
 (3-25)

- 164.

The left-hand side of the rate equation is shown graphically in Figure 3-4 as a function of  $\left[NO_3\right]/\left[NO_2\right]$  for T = 500 K and 600 K. The intercept at



T	k <sub>19</sub>	k <sub>19</sub> + k <sub>20</sub>
500 600	3.02 x:10 <sup>6</sup> 6.33 x 10 <sup>6</sup>	3.42 x 10 <sup>6</sup> 10.04 x 10 <sup>6</sup>

Figure 3-4. Simultaneous Rate Constants at T = 500 and 600 K a concentration ratio of zero corresponds to  $k_{19}$  and the intercept at unity ratio corresponds to  $k_{19}$ +  $k_{20}$  or the apparent bimolecular rate constant at

the beginning of the reaction. The slope of the function is  $k_{20}$ .

The rate equation can be rearranged to plot the concentration ratio versus time for given temperature and initial concentration conditions. This ratio is shown in Figure 3-5 for initial conditions of 10 ppm and a total pressure of 1 atmosphere.

For conditions more appropriate to the stratosphere, the terms of the rate equation are presented in Table 3-11 for initial conditions of 20 ppb  $N_2O_5$ , an ambient pressure of 0.1 atm and a 400 K thermal converter.

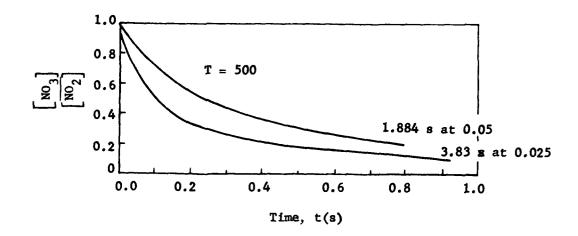


Figure 3-5.  $[NO_3]$  Decay versus Time

TABLE 3-11. NO, RATE LIMITING DECAY

[NO <sub>3</sub> ] (ppb)	[NO <sub>2</sub> ] (ppb)	∆[NO <sub>3</sub> ] (ppb)		t (s)
10.0	10.0	0	1.0	0
9.473	10.526	0.526	0.9	$8.27 \times 10^2$
8.889	1.111	1.111	0.8	1.78 x 10 <sup>3</sup>
8.235	11.765	1.765	0.7	$2.94 \times 10^3$
7.500	12.500	2.500	0.6	$4.38 \times 10^3$
6.667	13.333	3.333	0.5	6.25 x 10 <sup>3</sup>

For Figure 3-5 or Table 3-11 it can be clearly seen that the ratio  $\left[\text{NO}_3\right]/\left[\text{NO}_2\right]$  will be approximately unity for residence times of a few seconds or less and concentrations of a few ppb or less. The thermally converted N<sub>2</sub>O<sub>5</sub> sample must then be analyzed as NO<sub>2</sub> or NO<sub>3</sub>, or a second conversion of either constituent must occur followed by detection of the end products. The stoichiometry of these conversions, however, must be known.

For reaction 16 the growth of NO<sub>2</sub> is given by:

$$\frac{d \left[NO_2\right]}{dt} = k_{-13} \left[N_2O_5\right] - k_{13} \left[NO_2\right] \left[NO_3\right] + 2k_{13} \left[NO\right] \left[NO_3\right]$$
(3-26)

and the growth of the  $NO_3$  radical is

$$\frac{d \left[ NO_{3} \right]}{dt} = k_{-13} \left[ N_{2}O_{5} \right] - \left[ k_{13} + k_{19} \right] \left[ NO_{2} \right] \left[ NO_{3} \right] - k_{13} \left[ NO \right] \left[ NO_{3} \right]$$
 (3-27)

Since NO will generally be present, the net stoichiometric reaction must also be considered:

$$NO + N_2O_5 \longrightarrow 3NO_2$$
 (13)

For this reaction and for lower temperatures, a steady-state approximation for the  $\begin{bmatrix} NO_3 \end{bmatrix}$  intermediary is made, i.e.,  $\frac{d}{dt} = 0$ . With this approximation the growth of  $NO_2$  is given by:

$$\frac{d \left[ NO_{2} \right]}{dt} = k_{-13} \left[ N_{2}O_{5} \right] \frac{k_{19} \left[ NO_{2} \right] + 3k_{7} \left[ NO \right]}{\left[ k_{13} + k_{19} \right] \left[ NO_{2} \right] + k_{7} \left[ NO \right]}$$
(3-28)

with the knowledge that  $k_7 >> k_{19}$  (pg. 38), this expression can be simplified to;

$$\frac{d \left[NO_{2}\right]}{dt} = 3 k_{-13} \left[N_{2}O_{5}\right] \left[\frac{NO}{NO}\right] + k_{13}/k_{7} \left[\frac{NO_{2}}{NO_{2}}\right]$$
(3-29)

Since  $\begin{bmatrix} NO \end{bmatrix} \approx \begin{bmatrix} NO_2 \end{bmatrix}$  in the stratosphere and  $k_{13}$  at 400 K is  $<< k_7, k_7 \begin{bmatrix} NO \end{bmatrix}$  will be much greater than  $k_{13} \begin{bmatrix} NO_2 \end{bmatrix}$ . For these conditions, a first-order rate for reaction 14 will simply be that of the elementary unimolecular rate given for reaction -13.

The third reaction listed in this section is restated;

$$2NO_2 + O_3 \longrightarrow N_2O_5 + O_2$$
 (17)

and has been observed (Section 3.4.1) to be second-order in reactants. The mechanism is simply

$$2NO_2 + O_3 \longrightarrow NO_3 + O_2$$
 (12)

$$NO_2 + NO_3 \longrightarrow N_2O_5 \tag{13}$$

Applying the steady-state assumption for NO3, the loss rate for O3 is simply

$$-\frac{d \left[O_3\right]}{dt} = k_1 \left[NO_2\right] \left[NO_3\right]. \qquad (3-30)$$

The fourth reaction listed in this section is restated:

$$20_3 + N_2O_5 \longrightarrow 30_2 + N_2O_5 \tag{18}$$

This reaction is the well-known  $N_2O_5$  catalytic decomposition of  $O_3$ . The governing mechanistic reactions for reaction (18) are:

$$NO_2 + O_3 \longrightarrow NO_3 + O_2$$
 (12)

$$NO_2 + NO_3 \xrightarrow{(M)} N_2O_5$$
 (13)

$$2NO_3 \longrightarrow 2NO_2 + O_2 \tag{20}$$

$$N_2O_5 \longrightarrow NO_2 + NO_3 \tag{-13}$$

If the pseudo-reference species,  $NO_2$  and  $NO_3$ , are equilibrated with  $N_2O_5$ , they are treated kinetically as though they were intermediaries in a consecutive process. This leads to the following differential rate equation:

$$-\frac{d \left[O_{3}\right]}{dt} 2 \left(\frac{k_{-13}^{2} k_{11}^{2} k_{19}}{4k_{13}}\right)^{1/3} \left[N_{2}O_{5}\right]^{2/3} \left[O_{3}\right]^{2/3}$$
 (3-31)

## 3.5.2 Stratospheric-Based Instrument Modeling

The above reactions plus the ozone oxidation of NO to NO<sub>2</sub> and NO<sub>2</sub> to NO<sub>3</sub> have been modeled using the EPISODE adaptation of the GEARS code (Gear, 1971 and Hindmarsh, 1975). These codes are chemical kinetics programs that solve coupled stiff differential equations. The solutions are obtained by implicit linear multisteps. With the GEAR code, fixed-step formulae are employed with changes in step, when required, by interpolation. In contrast, the EPISODE code is based upon formulae that are of variable step size. This feature

lends stability to the solution. Given the correct set of chemical reactions, the solutions tend to be an exact representation of the products and reactants for homogeneous reactions.

Table 3-12 provides printouts for a 400 K converter with input concentrations set for H = 15 km and H = 25 km. The initial concentrations can be read from the respective first lines at t = 0. Within the first half-second most of the  $N_2O_5$  is converted to  $NO_2$  and  $NO_3$ . Subsequently  $\left[NO_2\right]$  increases to a steady-state level of 9.6 x  $10^9$  molecules/cm<sup>3</sup> and 7.2 x  $10^9$  molecules/cm<sup>3</sup>;  $\left[NO_3\right]$  increases at a slower rate to a steady-state level of 3.5 x  $10^8$  molecules/cm<sup>3</sup> and 1.1 x  $10^9$  molecules/cm<sup>3</sup>; and  $\left[NO\right]$  decays. As an example of the  $\left[NO_x\right]$  budgeting, refer to the case for H = 25 km and t = 5.0 s. These values are given in Table 3-13.

Although the data of Table 3-13 shows acceptable accounting or budgeting of  $\Delta\left[\mathrm{NO}_{\mathbf{X}}\right] = \Delta\left[\mathrm{NO}_{2}\right] + \Delta\left[\mathrm{NO}\right]$  from redox reactions the data does not permit an accurate measurement of  $\left[\mathrm{N}_{2}\mathrm{O}_{5}\right]$ . The principal reason is that some of the unmeasured  $\left[\mathrm{NO}_{3}\right]$  is converted to  $\mathrm{NO}_{2}$  via reaction -13. This in effect alters specificity. If the measurement could be carried out in 2 seconds, the  $\Delta\left[\mathrm{NO}_{3}\right]$  error would be reduced by about 33 percent for the case cited.

From the example cited in Table 3-13, setting aside for the moment the above mentioned problem, a quantitative measure of  $\begin{bmatrix} N_2O_5 \end{bmatrix}$  may be obtained, if the following conditions are met: (1)  $N_2O_5$  is not lost to the instrumentation walls, (2)  $NO_x = NO + NO_2$  was determined accurately, (3) the  $\begin{bmatrix} NO_3 \end{bmatrix}$  from both the ambient stream and as an  $N_2O_5$  decomposition product is quantitatively converted to  $NO_x$  prior to being measured as NO, and (4) the  $NO-NO_2$  instrumentation did not convert any of the ambient  $N_2O_5$  during sample residence. This latter statement is a specificity condition. The third condition is treated next.

Of the intermediary,  $NO_3$  entering an  $NO_2$  photolytic cell, some may be converted according to the spectral energy available as given by Johnston and Graham (1974):

# TABLE 3-12. HAPP RESIDENCE TIME STUDY

T = 400 K

4400	RESIDENCE	TIME	STUDY	H =	16	<b>L</b>
TAPP	MESIDEACE	1145	31001	11 =	73	1.00

TIME (S)	11205	NO2	NO3	NO	U3	02	HN03	но	H2U
0.0	1.0000 07	5.0000 09	2.0000 06	5.0000 09	3.0000 12	8.1000 17	1.3000 09	1.0000 06	6.000D 12
0.50	1.1960 02	5.4120 09	1.3490 07	4.5970 09	3.000D 12	8.1000 17	1.3000 09	8.3900 05	6.000D 12
1.00	1.4180 02	5.7810 09	1.5090 07	4.2260 09	2.9990 12	8.1000 17	1.300D 09	7.046D 05	6.000D 12
1.50	1.6740 62	4.120D 09	1,6820 07	3.886D 09	2.9990 12	B.100D 17	1.1000 09	5.4410 05	6.0000 12
2.00	1.9520 02	6.4310 09	1.8670 07	3.5720 09	2.9990 12	8.1000 17	1.3000 09	5.0330 05	6.000D 12
2.50	2.2530 02	6.7170 09	2.0610 07	3.284D 09	2.9980 12	8.100D 17	1.300D 09	4.286D 05	6.000D 12
3.00	2.5740 02	6.9800 09	2.2660 07	3.0140 09	2.498D 12	8.100D 17	1.3000 09	3.6700 05	6.0000 12
3.50	2.9150 02	7.2210 09	2.4800 07	2.7760 09	2.998D 12	8.1000 17	1.3000 09	3.1630 05	6.0000 12
4.00	3.2750 02	7.4430 09	2.703D 07	2.5520 09	2.9980 12	8.100D 17	1.300D 09	2.7450 05	6.000D 12
4.50	3,6540 02	7.6470 09	2.9350 07	2.346D 09	2.9970 12	8.1000 17	1.3000 09	2.400D 05	6.000D 12
5.00	4.0490 02	7.8340 09	3,1740 07	2.1570 09	2.997D 12	8.100D 17	1.3000 09	2.1150 05	6.000D 12
5.50	4.4600 02	A.005D 09	3.4200 07	1.9820 09	2.9970 12	8.1000 17	1.3000 09	1.8790 05	6.0000 12
6.00	4.8860 02	8.1630 09	3.674D 07	1.8220 09	2.997D 12	8.1000 17	1.300D 09	1.684D 05	6.000D 12
6.50	5.3260 02	8.3070 09	3.9350 07	1.6750 09	2.9970 12	8.1000 17	1.3000 09	1.5220 05	6.000D 12
7.00	5.7800 02	8.4400 09	4.202D 07	1.540D 09	2.9970 12	8.1000 17	1.300D 09	1.387D 05	6.800D 12
7.50	6.2450 02	8.5620 09	4.4750 07	1.415D 09	2.9960 12	8.1000 17	1.3000 09	1.276D 05	6.000D 12
8.00	6.7220 02	8.673D 09	4.754D 07	1.301D 09	2.996D 12	8.100D 17	1.3000 09	1.1830 05	6.000D 12
8.50	7.2090 02	8.7760 09	5.0390 07	1.196D 09	2.996D 12	8.1000 17	1.300D 09	1.1050 05	6.0000 12
9.00	7.7060 02	8.869D 09	5.3290 07	1.0990 09	2.996D 12	8.1000 17	1.300D 09	1.040D 05	6.000D 12
9.50	8.2130 02	8.955D 09	5.624D 07	1.0100 09	2.996D 12	8.100D 17	1.3000 09	9.854D 04	6.000D 12
10.00	8.7280 02	9.034D 09	5.924D 07	9.2860 08	2.9960 12	8.100D 17	1.3000 09	9.396D 04	6.000D 12

#### HAPP RESIDENCE TIME STUDY H = 25 km

TIMF(S)	4205	5014	NO3	NO	U3	02	HN03	но	H2U
0.0	7.0000 08	6.200D 09	2.0000 06	7.000D 08	4.3000 12	1.7000 17	3.000D 09	1.0000 06	6.0000 12
0.50	9.1290 05	6,9820 09	7.0120 08	6.173D 08	4.3000 12	1.7000 17	3.0000 09	8.3840 05	6.0000 12
1.00	9.2520 03	7.0560 09	7.0220 08	5.4380 08	4.300D 12	1.7000 17	3.0000 09	6.5560 05	6.000D 12
1.50	8.1640 03	7.1200 09	7.0270 08	4.7910 08	4.3000 12	1.7000 17	3.0000 09	5.165D 05	6.000D 12
2.00	8.2390 03	7.1760 09	7.037D 08	4.2210 08	4.300D 12	1.7000 17	3.0000 09	4.1060 05	6.0000 12
2.50	8.3120 03	7.2250 09	7.0500 08	3.7190 08	4.300D 12	1.700D 17	3.0000 09	3.3000 05	6.000D 12
3.00	8.3817 03	7.2670 09	7.0570 08	3.2770 08	4.3000 12	1.7000 17	3.000D 09	2.686D 05	6.0000 12
3.50	8.4480 03	7.304D 09	7.087D 08	2.8880 08	4.3000 12	1.700D 17	3.0000 09	2.2190 05	6.000D 12
4.00	8.5130 03	7.3360 09	7.1100 08	2.5450 08	4.3000 12	1.7000 17	3.000D 09	1.8620 05	6.000D 12
4.50	8.5750 03	7.364D 09	7.1350 08	2.243D 08	4.2990 12	1.7000 17	3.000D 09	1.5910 05	6.000D 12
5.00	8.6360 03	7.38AD 09	7.1520 08	1.9770 08	4.2990 12	1.7000 17	3.0000 09	1.384D 05	6.0000 12
5.50	8.6940 03	7.409D 09	7.1900 08	1.7430 08	4.2990 12	1.7000 17	3.0000 09	1.2260 05	6.0000 12
5.00	8.7520 03	7.4260 09	7.2200 08	1.5360 08	4.2990 12	1.7000 17	3.000D 09	1.1060 05	6.000D 12
6.50	8.8080 03	7.4410 09	7.2520 08	1.3540 08	4.2990 12	1.7000 17	3.0000 09	1.0140 05	6.000D 12
7.00	8.8530 03	7.4540 09	7.2840 08	1.1940 08	4.2990 12	1.700D 17	3.000D 09	9.441D 04	6.000D 12
7.50	8.9170 03	7.4650 09	7.3180 08	1.0530 08	4.2990 12	1.700D 17	3.0000 09	8.9050 04	6.000D 12
6.00	8.9710 03	7.474D 09	7.3530 08	9.2900 07	4.2990 12	1.7000 17	3.0000 09	8.496D 04	6.000D 12
8.50	9.0230 03	7.4810 09	7.3890 08	8.1970 07	4.2990 12	1.7000 17	3.000D 09	8.1830 04	6.0000 12
9.00	9.0750 03	7.4870 09	7.4250 08	7.2330 07	4.2990 12	1.700D 17	3.000D 09	7.9440 04	6.000D 12
9.50	9.1260 03	7.4920 09	7.4620 08	6.385D 07	4.2990 12	1.700D 17	3.0000 09	7.7610 04	6.000D 12
10.00	9.1760 03	7.4960 09	7.4990 08	5.6380 07	4.299D 12	1.7000 17	3.0000 09	7.620D 04	6.000D 12

TABLE 3-13. NO<sub>X</sub> BUDGET (for Table 3-12, H = 25 km, T = 400 K, t = 5.0 s)

Species	Decomposition	Species	Combination
ΔN <sub>2</sub> 0 <sub>5</sub>	-7.000 x 10 <sup>8</sup>	∆ no <sub>x</sub>	+ 6.86 x 10 <sup>8</sup>
$_{\Delta}$ no $_{2}$	7.000 x 10 <sup>8</sup>		
△ no <sub>3</sub>	7.142 x 10 <sup>8</sup>		1
$\Delta$ N <sub>2</sub> O <sub>5</sub> - $\Delta$ NO <sub>3</sub>	-0.142 x 10 <sup>8</sup>		
Total ANO X	6.858 x 10 <sup>8</sup>	Total NO <sub>X</sub>	+ 6.86 x 10 <sup>8</sup>

$$NO_3 + hv \longrightarrow NO_2 + O(^3P) \lambda < 578 \text{ nm}$$
 (21)

$$NO_3 + hv \longrightarrow NO + O_2(^1\Sigma) \lambda > 578 \text{ nm}$$
 (22)

There is conjecture, however, that NO +  $0_2(^1\Sigma)$  products also may be formed for wavelengths less than 578 nm.

Photoabsorption cross-sections to  $\lambda \geq 470$  nm and quantum yields in the visible have been determined for reactions 21 and 22 (Graham, 1975). The quantum yields, wavelength averaged cross-sections, and light distributions are given below in Table 3-14. From the fourth column of data it is apparent that the conjecture of the previous paragraph is valid. For a solar spectral distribution and zero zenith angle, Graham's computed rates are  $J_{21} = 0.099 \pm 0.02$  s<sup>-1</sup> and  $J_{22} = 0.040 \pm 0.02$  s<sup>-1</sup>.

The products of reaction 22 will rapidly react as follows:

$$o(^{3}P) + NO_{2} \longrightarrow NO + O_{2}$$
 (6)

where

$$k_6 = 3.5 \times 10^{-12} \text{ cm}^3$$
-molecule<sup>-1</sup>s<sup>-1</sup> (Kaufman, 1961)

Since the NO $_2$  photolytic converter of paragraph 3.2 does not have any substantial flux at  $\lambda > 470$  nm reaction 21 is not anticipated. NO $_3$  absorption cross-sections for  $\lambda < 400$  nm, however, have not been measured.

TABLE 3-14. NO FREE RADICAL PHOTOLYTIC TERMS

			Reaction		
Parameter	$J_{21}$	$J_{21}$	$J_{21}$	J <sub>22</sub>	J <sub>22</sub>
Quantum Yield	0.14	0.23	0,049	0.85	0.63
Avg $\sigma$ NO <sub>3</sub> : $\lambda \le 580$ nm (cm <sup>2</sup> /molec)	1.88x10 <sup>-18</sup>	2.51x10 <sup>-18</sup>		1.88x10-18	2.51x10 <sup>-18</sup>
AVB G NO <sub>3</sub> $\lambda > 580$	2.99	3.11	2.17x10 <sup>-18</sup>	2.99	3.11
Percent light, $\lambda \le 580$ nm	93	37	0	93	37
Percent light, $\lambda > 580$	7	63	100	7	63
Integrated light intensity (10 <sup>16</sup> h v/cm <sup>2</sup> -s)	1.55	1.07	0.33	1,55	1.07

Although an  $N_2O_5$  measurement does not appear feasible due to specificity problems, some of which are deferred to paragraph 3.8, Potential Interferents, the thermal conversion of  $N_2O_5$  was experimentally treated in the lab and is discussed in the next paragraph.

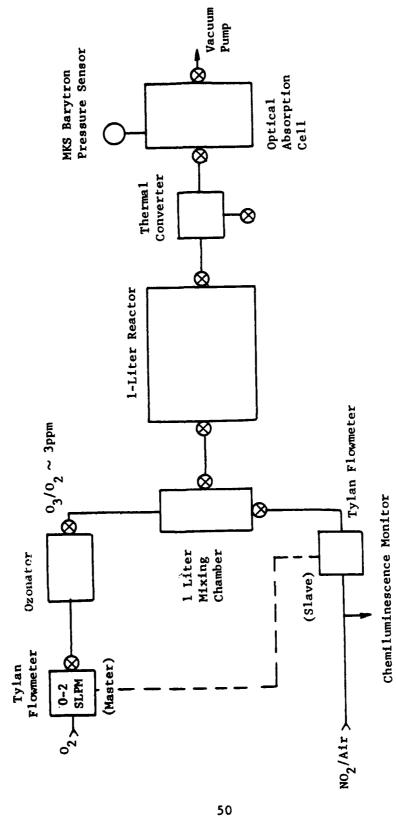
### 3.5.3 Experimental Procedures and Results

The thermal decomposition of nitrous pentoxide was studied using a stain-less steel converter between the  $N_2O_5$  generating apparatus and the long path absorption cell of the Model 580 spectrophotometer. The spectrophotometer enabled observation of the major constitutents involved in the thermal conversion process. A schematic of the apparatus is shown in Figure 3-6.

 $N_2O_5$  was created by the gas phase reaction of  $NO_2$  and  $O_3$  in the presence of excess  $NO_2$  in the same manner as described in paragraph 3.5.1. Several minor changes, however, were made to further reduce water contamination. Two test runs are discussed in detail.

The core of the converter consisted of a 2½-inch diameter x 2-inch long stainless steel block. The gas passed through a ½-inch diameter hole in the center of the block. A sintered stainless disk pressed into the gas channel permitted complete thermalization of the gas. The temperature of the block was monitored using platinum resistance sensors. A cartridge heater inserted into the block was the heat source. The block temperature was not regulated but stayed within ± 1 K during the course of each data run.

For the initial test run, pertinent conversion data of the reactants are presented in Table 3-15. The initial concentrations of  $[NO_2]$  and  $[O_3]$  prior to mixing were 23.5 x  $10^{13}$  and 6.5 x  $10^{13}$  molecules/cm<sup>3</sup>, respectively. The final concentrations of  $[NO_2]$  and  $[O_3]$  were 11.3 x  $10^{13}$  and zero molecules/cm<sup>3</sup>. The ratio  $\Delta [NO_2]/\Delta [O_3]$  is therefore 1.88, as expected. Although the IR scan of Figure 3-7 for T = 23 C shows little evidence of  $H_2O$  being present, the measured yield of  $N_2O_5$  for this test, assuming a stoichiometry of 1.88, is only 43 percent. The remaining 57 percent appears as nitric acid which is evident at 1340 and 1315 cm<sup>-1</sup>. The expected amount of  $HNO_3$  based upon the 57 percent loss of  $N_2O_5$  is 7.44 x  $10^{13}$  molecules/cm<sup>3</sup>. From Table 3-15, it can be seen about 71 percent of the  $HNO_3$  appeared in the gas phase.



Setup for Experiment To Observe Thermal Decomposition of  $\rm N_2 \, 0_5$ Figure 3-6.

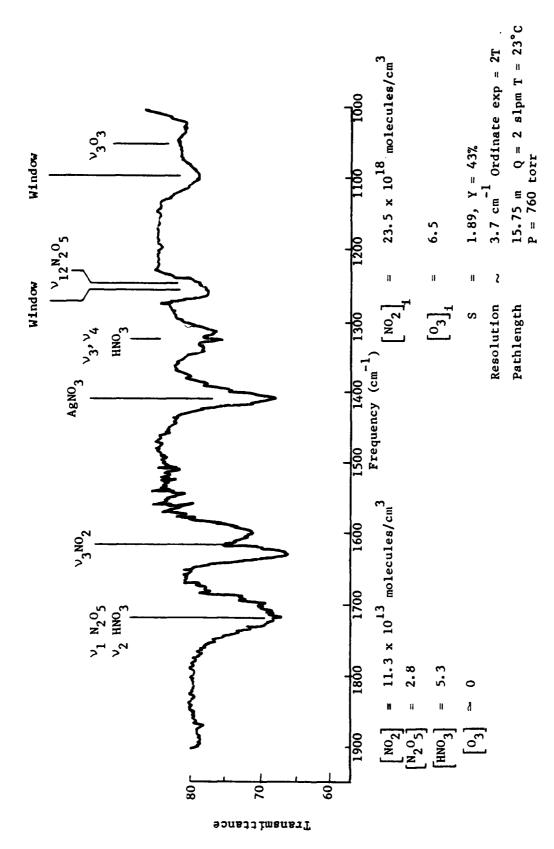


Figure 3-7.  $N_2O_5$  Generation Spectra

TABLE 3-15. NO<sub>2</sub>, N<sub>2</sub>O<sub>5</sub> AND HNO<sub>3</sub> MEASURED CONCENTRATIONS

VS THERMAL CONVERTER TEMPERATURE

Temp. (K)	NO <sub>2</sub>	$N_2O_5$ x $10^{13}$ (molecules/cm <sup>3</sup> )	HNO <sub>3</sub>
298	11.3	2.78	5.32
373	13.1	1.63	7.67
473	18.8	0	5.62
523	17.8		5.96
573	21.7		3.87
623	21.9		1.84
673	25.3		0.71

For the initial testing of the  $N_2O_5$  converter it was decided that a series of thermal tests at differing temperatures should be carried out. From the above table and a sample residence time of about 0.5 second, it can be seen that all of the  $N_2O_5$  accounted for had decomposed at a temperature of 473 K. At this temperature, however, the data indicates that  $\Delta \left[ NO_2 \right]$  is considerably greater than expected from a  $\Delta \left[ N_2O_5 \right]$  of -2.78 x  $10^{13}$  molecules/cm<sup>3</sup>.

In addition, a review of the  $\mathrm{HNO}_3$  concentration versus temperature indicates that possibly  $\mathrm{HNO}_3$  is being desorbed from the converter walls at a temperature of 373 K. As the converter had been used on the two previous days, it is feasible that residual  $\mathrm{HNO}_3$  was present.

Finally, the high temperature  $\mathrm{NO}_2$  and  $\mathrm{HNO}_3$  data are of interest for the conversion of  $\mathrm{HNO}_3$  which is described in detail in paragraph 3.6. At a temperature of 673 K the  $\mathrm{NO}_2$  concentration was determined to be 25.3 x  $\mathrm{10}^{13}$  molecules/cm<sup>3</sup> as compared to the initial concentration of 23.5 x  $\mathrm{10}^{13}$  molecules/cm<sup>3</sup> prior to reaction with  $\mathrm{O}_3$  or about 1.8 x  $\mathrm{10}^{13}$  molecules/cm<sup>3</sup> too high. Undoubtedly this discrepancy contains experimental measurement errors but could also have arisen from the apparent desorbed  $\mathrm{HNO}_3$  which from the first two  $\mathrm{HNO}_3$  entries is seen to be about 2.3 x  $\mathrm{10}^{13}$  molecules/cm<sup>3</sup>. Considering

the 523-673 K temperature range and making the  $\left[\text{NO}_2\right]$  = 1.8 x 10<sup>13</sup> molecules/cm<sup>3</sup> correction, one has a  $\Delta \left[\text{NO}_2\right]$  of 5.7 x 10<sup>13</sup> molecules/cm<sup>3</sup> as compared to a  $\Delta \left[\text{HNO}_3\right]$  of 5.25 x 10<sup>13</sup> molecules/cm<sup>3</sup>. Paragraph 3.6.1, to follow, discusses theoretically a stoichiometry of unity for the decomposition of HNO<sub>3</sub> to NO<sub>2</sub>.

For the second test run emphasis was placed on repeatability and closer monitoring of thermal trends. The concentration of  $NO_2$  prior to dilution was 58 ppm as determined by the chemiluminescence monitor. When diluted with the  $O_3/O_2$  flow, the concentration of  $NO_2$  was 15.7 ppm. The concentration determined by IR absorption was found to be 10 ppm. Ozone was generated by a standard UV lamp ozonator and grade 4.5 oxygen. The spectrum was analyzed using the data of Pitts (1976), c.f. Appendix A. The result was an ozone concentration of 3.3 ppm (NTP) or 3.2 ppm under laboratory conditions of 765 Torr and 26°C. The change in  $NO_2$  concentration following reaction with the ozone was 8.0 ppm with all of the ozone being consumed. The ratio  $\left[NO_2\right]/\left[O_3\right] = 2.5$  for these experiments.

The absorption spectrum of the reacted gases is shown in Figure 3-8. In addition to the NO<sub>2</sub> band at 1620 cm<sup>-1</sup>, bands attributable to HNO<sub>3</sub> and N<sub>2</sub>O<sub>5</sub> are clearly visible. The spectral run of Figure 3-8 extends the spectrum to lower frequencies to present the  $v_{13}$  and  $v_{14}$  bands of N<sub>2</sub>O<sub>5</sub>. Using the absorption crosssections given in Appendix A for HNO<sub>3</sub> at 1315 cm<sup>-1</sup> and 1340 cm<sup>-1</sup>, the concentration of HNO<sub>3</sub> was found to b 3.2 x 10<sup>13</sup> molecules/cm<sup>3</sup> or 1.4 ppm. The maximum amount of N<sub>2</sub>O<sub>5</sub> that could be generated would be equal to the amount of O<sub>3</sub> consumed which was 3.2 ppm. The nitric acid is believed to be formed by heterogeneous wall reactions of N<sub>2</sub>O<sub>5</sub> with adsorbed water. The net reaction is

$$H_2O + N_2O_5 \longrightarrow 2HNO_3$$
 (23)

Thus, 1.4 ppm of HNO<sub>3</sub> represents the reaction of 0.7 ppm of N<sub>2</sub>O<sub>5</sub>. Using the absorption cross sections given in Appendix A for N<sub>2</sub>O<sub>5</sub> at 1246 cm<sup>-1</sup>, the concentration of N<sub>2</sub>O<sub>5</sub> was found to be 4.6 x  $10^{13}$  molecules/cm<sup>3</sup> or 2.0 ppm. This represents a yield of 59 percent with the loss of 0.7 ppm to heterogenously and homogeneously formed HNO<sub>3</sub>. Thus the nominal N<sub>2</sub>O<sub>5</sub> yield is 2.7/3.4 = 0.8 which is quite good.

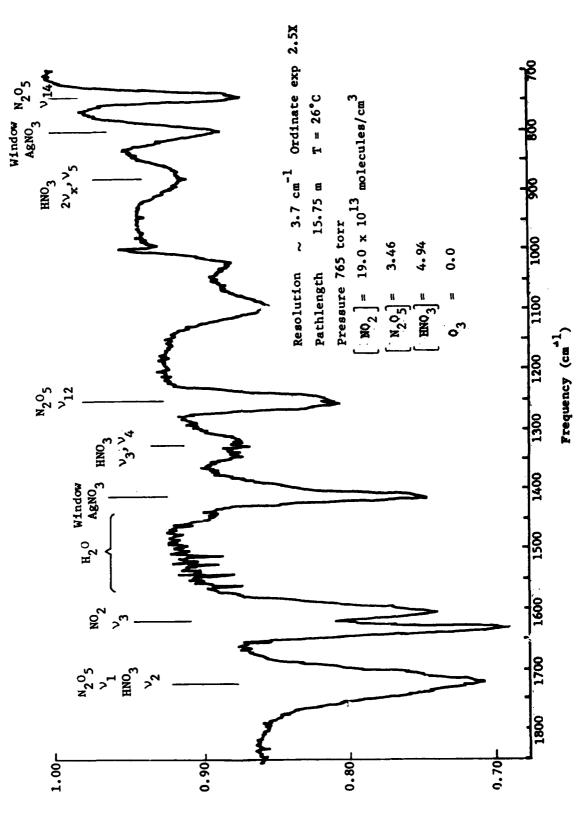


Figure 3-8. Absorption Spectra of  $N_2O_5$  and  $HNO_3$ 

The recorded data consisted of a least three complete spectral scans, similar to Figure 3-8, taken after the block had reached thermal equilibrium. The transmission at various distinct spectral features was recorded and compared to a reference spectrum (pure  $O_2$ ). The absorbance was plotted as a function of temperature for these features of  $N_2O_5$ ,  $HNO_3$ , and  $NO_2$  (Figure 3-9). In addition, the  $N_2O_5$ - $HNO_3$  mixed feature at 1720 cm<sup>-1</sup> was plotted (Figure 3-10). Examining these graphs, it is seen that the amount of  $N_2O_5$  declines steadily with increasing temperatures. The nitric acid concentration peaks near 475 K, while the yield of  $NO_2$  increases steadily to within 1 percent of its unreacted level. The "missing"  $NO_2$  has probably been converted to NO although this was not explicitly checked. The standard deviation of the data was typically 0.1 to 0.3 percent indicating stable conditions during the successive spectral measurements.

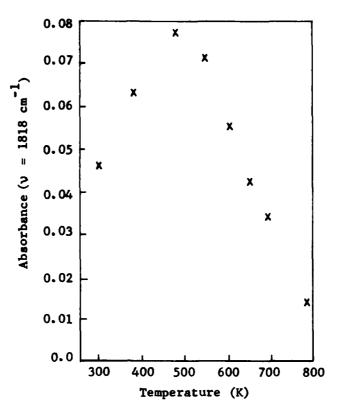
The complicated thermal behavior exhibited in these graphs is related to several factors. Primary among these is the time that the gas spends in the long path absorption cell (~300 sec). This time is long enough to allow some reverse reactions to occur, especially in the oxygen-rich environment of these experiments. Also, the gas temperature in the absorption cell was not well determined. Nevertheless, almost total recovery of the NO<sub>2</sub> has been achieved, thus indicating > 99 percent conversion efficiency.

# 3.6 NITRIC ACID (HNO<sub>3</sub>) GENERATION

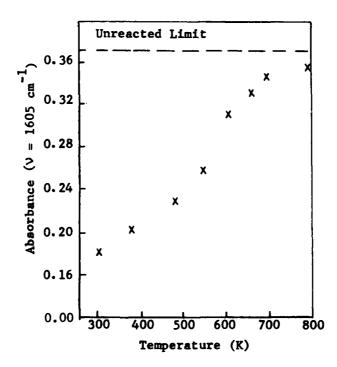
For nitric acid (HNO $_3$ ) synthesis, vapor diffusion of HNO $_3$  from an HNO $_3$ /H $_2$ SO $_4$ /H $_2$ O mixture was employed. This technique approximates the approach used by Stedman (1977).

### 3.6.1 Theory

Generation of  $\mathrm{HNO}_3$  is best carried out by the low pressure distillation of  $\mathrm{HNO}_3/\mathrm{H}_2\mathrm{SO}_4$  (Wilson and Miles, 1940) combined with a diffusion flow technique (Stedman, 1977). A ratio of 100 to 33.3 parts of concentrated 70%  $\mathrm{HNO}_3/\mathrm{30\%}$   $\mathrm{H}_2\mathrm{O}$  and  $\mathrm{H}_2\mathrm{SO}_4$  was used to obtain weight percentages of  $\mathrm{HNO}_3=49$ ,  $\mathrm{H}_2\mathrm{SO}_4=30$ , and  $\mathrm{H}_2\mathrm{O}=21$ . The vapor composition was greater than 98%  $\mathrm{HNO}_3$ . A stream of dry nitrogen or dry air is then blown by the mouth of the flask to create  $\sim 3$  ppm concentrations of  $\mathrm{HNO}_3$  in the flowing gas stream.

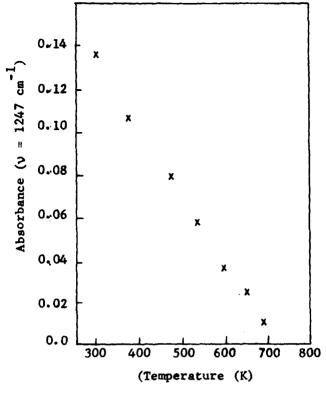


a. HNO<sub>3</sub> Absorbance

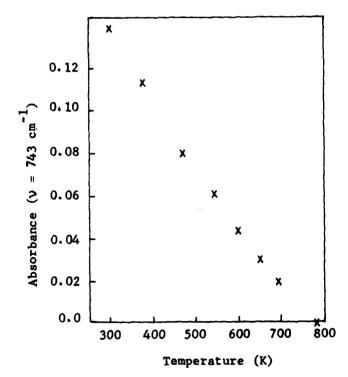


b. NO<sub>2</sub> Absorbance

Figure 3-9. Absorbances at Converter Output (1 of 2)



c. N<sub>2</sub>O<sub>5</sub> Absorbance



d. N<sub>2</sub>O<sub>5</sub> Absorbance

Figure 3-9. Absorbances at Converter Output (2 of 2)

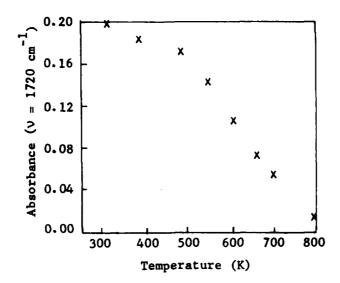


Figure 3-10.  $\mathrm{HNO_3}$  and  $\mathrm{N_2O_5}$  Absorbance at Converter Output

The vapor pressure of the HNO<sub>3</sub> was derived from boiling point data on Gibbs type ternary composition diagrams and plotted versus 1000/T shown in Figure 3-11. For diffusion flow samples of HNO<sub>3</sub>, the solution was held at 35°C yielding a partial pressure of 34 torr. For high spectral resolution measurements at temperatures simulating those of the stratosphere, a differential pumping technique was employed and the Pascal-Saposchnikow data was extrapolated according to the integrated Clausius-Clapeyron expression:

$$\log P = \frac{0.05223A}{T} + B(torr),$$

where A = 45,568 and B = 9.259. This expression permits one to derive from total pressure measurements the saturated partial pressure of  $HNO_3$  as a function of temperature.

Under diffusion flow, the predicted concentration at the upper end of the diffusion tube is given by the expression

$$C = \frac{10^6 \times q_d}{Q} \text{ (ppm)}.$$

where

$$q_d = \frac{DA}{L} \ln \frac{P}{P-P_{HNO_3}}$$

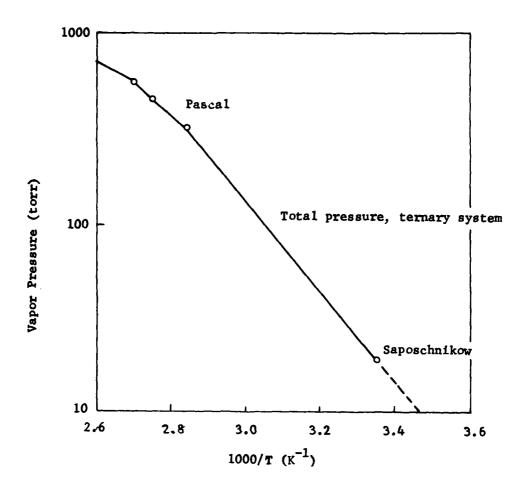


Figure 3-11.  ${\rm HNO}_3$  Vapor Pressure vs Reciprocal Temperature and:

Q = flow rate (ml/s)

 $q_d = diffusion rate (ml/s)$ 

D = diffusion coefficient  $\approx 0.09 \left(\frac{306}{298}\right) \left(\frac{760}{747}\right) \text{ cm}^2/\text{sec}$ 

P = pressure in the diffusion cell

p = partial pressure of the diffusing vapor

A = diffusion tube cross-sectional area (cm<sup>2</sup>)

L = Diffusion tube length (cm)

With 3/16-inch ID tubing, A/L was equal to 0.0124 cm. At a temperature of T =  $35^{\circ}$ C (308 K) and P = 747 torr,  $q_d$  =  $5.6 \times 10^{-5}$  ml/sec. At an initial flow rate of 0.25 SLPM, one has a computed concentration of 13.4 ppm. Maximum flow rate was set to 2.1 SLPM yielding a computed concentration of 1.6 ppm.

#### 3.6.2 Experimental Procedures

Once diffusion was initiated, equilibrium was attained in about 24 hours and remained constant for weeks. Internal pressure disturbances above the solution cause only short-termed fluctuations in concentration.

Materials employed in the diffusion generator included a triple necked pyrex distillation flask fitted with £ 24/40 PTFE stoppers lightly coated with a Hooker Chemical Company fluorolube grease (GR-90), stainless steel fittings and PTFE tubing. Temperature was maintained by an agitated temperature controlled water bath.

# 3.7 NITRIC ACID (HNO3) THERMAL CONVERSION

Thermal conversion of HNO<sub>3</sub> as an analytical method for stratespheric monitoring is, as yet, untried. The method, however, has been laboratory tested by D. H. Stedman (private communication, 1977) for tropospheric monitoring and by the authors as discussed in this section. The converter is constructed of glass and contains glass beads for heat transfer. Temperature is maintained at about 550 K. The kinetics of the various reactions of this section relating to HNO<sub>3</sub> have been carefully reviewed. Decomposition of HNO<sub>3</sub> is often heterogeneous, requiring a surface and its formation rate does not lend itself to description by Arrhenius' equation. The function of the surface appears to be to act as an OH scavenger.

## 3.7.1 Theory

Conversion of HNO<sub>3</sub> has been experimentally treated by Frejacques (1951) and extensively by Johnston et al. (1951, 1953, 1955).

The postulated reaction of Frejacques is the following:

$$2 \text{ HNO}_3 \longrightarrow \text{NO} + \text{NO}_2 + \text{O}_2 + \text{H}_2\text{O}$$
 (24)

with  $N_2O_5$  as an intermediary product. Subsequent measurements by colleagues of Johnston and the authors indicate that the thermal conversion follows the Johnston path. The thermal conversion is a complex reaction with the net stoichiometric reaction:

$$4 \text{ HNO}_3 \longrightarrow 4 \text{NO}_2 + 2 \text{ H}_2 \text{O} + \text{O}_2$$
 (25)

A consecutive side reaction is the thermal conversion of  $NO_2$  to NO which was treated in Section 3.3.1.1. The ensuing analysis does not consider this side reaction.

In the presence of NO, the thermal conversion is also a complex reaction with the net stoichiometric reaction:

$$2HNO_3 + NO \longrightarrow 3NO_2 + H_2O$$
 (26)

This reaction is treated after a discussion of reaction (25).

The governing mechanistic reactions for reaction (25) are the decomposition and recombination of  $HNO_3$  followed by a product-reactant reaction followed by the two  $N_2O_5$  simultaneous bimolecular reaction paths, one of which has a fast-sequential reaction converting NO, if present. These reactions are (H. S. Johnston, 1955):

$$HO + HNO_3 \longrightarrow H_2O + NO_3$$
 (28)

$$NO_2 + NO_3 \xrightarrow{k29} NO + NO_2 + O_2$$
 (19)

$$NO + NO_3 \xrightarrow{k30} 2NO_2 \tag{7}$$

The earlier work of Johnston et al. (1951) indicated that decomposition of  $HNO_3$  was first order for temperatures above 670 K and given approximately as  $k_{25} = 1.34 \times 10^9 \exp{(-32,600/RT)} \text{ s}^{-1}$ . For temperatures below 570 K, the decomposition proceeded initially as a first-order reaction followed by a rate slower than first-order. Appearance of this transition was also a function of the reaction vessel size.

The later work of Johnston et al. (1955) concerning  $\mathrm{HNO}_3$  indicated that for temperatures above 650 K and a 2-liter Vycor bulb, the decomposition of pure  $\mathrm{HNO}_3$  followed reaction (25) with a first-order rate constant proportional to initial concentration. The proportionality is an empirical second-order rate constant given by  $\mathrm{k}_{25} = 9.3 \times 10^{-17} \, \mathrm{exp} \, (-38,300/\mathrm{RT}) \, \mathrm{cm}^3$ -molecule<sup>-1</sup>-s<sup>-1</sup>. Using argon and oxygen as foreign gasses in separate experiments, the first-order rate constant was found to be about 5.38 x  $10^4 \, \mathrm{M}$  + 0.006 s<sup>-1</sup> for  $\mathrm{M} < 2.4 \times 10^{14} \, \mathrm{molecules/cm}^3$ , a temperature of 673 K and initial  $\mathrm{HNO}_3$  concentraction of 1.29 x  $10^{14} \, \mathrm{molecules/cm}^3$ . At temperatures of interest, the second-order rates are

$$k_{25} = 7.3 \times 10^{-35} \text{ cm}^{-3} - \text{molecules}^{-1} - \text{s}^{-1}$$
 (298 K)  
= 5.5 x 10<sup>-22</sup> (550 K)

The primary step in all the reactions of HNO<sub>3</sub> bimolecular decomposition is that of reaction (27), the formation of nitrogen dioxide and the hydroxyl radical. At low total pressures (<5 torr) and, therefore, slower rates, nitric oxide and nitrogen dioxide accelerate and inhibit, respectively, the decomposition.

Atkinson et al. (1976) along with others have studied the formation rate of  $\mathrm{HNO}_3$ , i.e., reaction (-27). The data is summarized in the NASA Reference Publication 1010 (1977). The recommended form for  $\mathrm{k}_{-27}$  is very complex (Hampson and Garvin 1978) but a reasonable approximation can be found in Anderson et al. (1974). The expression they obtain is:

$$k_{-26} = 2.3 \times 10^{-30} \times (295/T)^{2.5} cm^6 - molecule^{-1} - s^{-1}$$
  
 $295 \le T \le 450 K$ 

The forward decomposition reaction rate,  $k_{27}$ , can be derived using the equilibrium constant for the reaction,  $K_{27,-27}$ 

$$K_{27,-27} = (1.3 \times 10^{30}/T \exp \left[-24970/T\right] \text{ molecules-cm}^{-3},$$

where  $K_{27,-27}$  has been evaluated at room temperature using the JANAF tables. The functional form of  $K_{27,-27}$  should not change appreciably with temperature over the range of interest. Thus, the form for the forward reaction can be found

$$k_{27} = K_{27,-27} \times k_{-27} = (3.0/T) (295/T)^{2.5} \exp \left(-24970/T\right) \text{ cm}^3\text{-molecules}^{-1}\text{-s}^{-1}$$
 $k_{27}M = 4.6 \times 10^{-20} \text{ s}^{-1}$  (298 K, 1 atm)
$$= 0.36 \text{ s}^{-1}$$
 (650 K, 1 atm)
and  $k_{-27}M = 6.2 \times 10^{-11} \text{ cm}^3$  -molecule $^{-1}\text{-s}^{-1}$ 
 $-8.6 \times 10^{-12} \text{ cm}^3$  -molecule $^{-1}\text{-s}^{-1}$  (650 K, 1 atm)

Similarly, for reaction (28), the forward rate has been evaluated (Hampson and Garvin, 1978),

$$k_{28} = 8 \times 10^{-14} \text{ cm}^3\text{-molecule}^{-1} \text{ -s}^{-1} (240 \le T \le 406 \text{ K}).$$

The equilibrium constant,  $K_{28,-28}$ , derived from the JANAF tables satisfies the equation

$$K_{28,-28} = 2.6 \exp \left[ 9160/T \right].$$

Thus, the backward reaction rate, k\_28, becomes:

$$k_{-28} = (k_{28}/K_{28}, -28) = 2.4 \times 10^{-14} exp \left| -9160/T \right| cm^3 -molecule^{-1} - s^{-1}$$

$$= 2.6 \times 10^{-41} cm^3 -molecule^{-1} - s^{-1} (298 \text{ K})$$

$$= 1.8 \times 10^{-20} cm^3 -molecule^{-1} - s^{-1} (650 \text{ K})$$

For reaction (25) the growth of NO, is given by:

$$\frac{d(NO_2)}{dt} = k_{25} [HNO_3] - k_{25} [HO] [NO_2] + 2 k_{28} [NO] [NO_3].$$
 (3-32)

Noting that HO,  ${
m NO}_3$  and NO are the temporary or intermediary molecules and employing successive steady-state approximations until a solution is reached, we consider the rate of change of HO with respect to time first. This is given by;

$$\frac{d[HO]}{dt} = k_{27} [HNO_3] - k_{-27} [HO] [NO_2] - k_{28} [HO] [HNO_3]$$
 (3-33)

Accepting the statement that HO will be short-lived at high temperature, the generation and removal rates will be comparable, so that d [HO]/dt will be zero. This is a statement equivalent to the steady-state approximation for kinetic reactions. With this in mind,

$$k_{27} \left[ \text{HNO}_3 \right] = k_{-27} \left[ \text{HO} \right] \left[ \text{NO}_2 \right] + k_{28} \left[ \text{HO} \right] \left[ \text{HNO}_3 \right]$$
 (3-34)

or that

$$\begin{bmatrix} \text{HO} \end{bmatrix} = \frac{k_{27} \left[ \text{HNO}_3 \right]}{k_{-27} \left[ \text{NO}_2 \right] + k_{28} \left[ \text{HNO}_3 \right]}$$
(3-34a)

The rate of change or growth of the radical NO, is given by;

$$\frac{d\left[NO_{3}\right]}{dt} = k_{28} \left[HO\right] \left[HNO_{3}\right] - k_{29} \left[NO_{2}\right] \left[NO_{3}\right] - k_{30} \left[NO\right] \left[NO_{3}\right]$$
 (3-35)

Making the same steady-state approximation for NO3 as with HO, one has;

$$k_{28} \left[ \text{HO} \right] \left[ \text{HNO}_3 \right] = k_{29} \left[ \text{NO}_2 \right] \left[ \text{NO}_3 \right] + k_{30} \left[ \text{NO} \right] \left[ \text{NO}_3 \right]$$
 (3-36)

or that;

$$\begin{bmatrix} NO_3 \end{bmatrix} = \frac{k_{17} \left[ HO \right] \left[ HNO_3 \right]}{k_{29} \left[ NO_2 \right] + k_{30} \left[ NO \right]}$$
(3-36a)

Combining equations (3-36a) and (3-34) one has that;

$$k_{27} [HNO_3] = k_{-27} [HO] [NO_2] + k_{29} [NO_2] [NO_3] = K_{30} [NO] [NO_3] (3-37)$$

when equations (3-37) and (3-32) are combined, one has after factoring;

$$\frac{d[NO_2]}{dt} = NO_3 (k_{29} [NO_2] + 3k_{30} [NO])$$
 (3-38)

From equation (3-36) one has;

$$\begin{bmatrix} NO_3 \end{bmatrix} = \frac{k_{28} \begin{bmatrix} HO \end{bmatrix} \begin{bmatrix} HNO_3 \end{bmatrix}}{k_{29} \begin{bmatrix} NO_2 \end{bmatrix} + k_{30} \begin{bmatrix} NO \end{bmatrix}}$$
(3-39)

or since,

$$[HO] = \frac{k_{28} [HNO_3]}{k_{-27} [NO_2] + k_{28} [HNO_3]}$$
 (3-40)

from equation (3-34),  $NO_3$  can be written as,

$$\begin{bmatrix}
NO_3 \end{bmatrix} = \frac{\frac{k_{28}k_{27} \left[ HNO_3 \right]^2}{k_{-27} \left[ NO_2 \right] + \left[ k_{28} \right] HNO_3}}{k_{102} + k_{28} \left[ NO_1 \right]}$$
(3-41)

The final result desired is obtained by combining equations (3-41) and (3-38) to yield;

$$\frac{d \left[ NO_{2} \right]}{dt} = \frac{k_{28}k_{27} \left[ HNO_{3} \right]^{2}}{k_{-27} \left[ NO_{2} \right] + k_{28} \left[ HNO_{3} \right]} \times \frac{k_{29} \left[ NO_{2} \right] + 3 k_{30} \left[ NO \right]}{k_{29} \left[ NO_{2} \right] + k_{30} \left[ NO \right]}$$
(3-42)

which can be simplified, since  $k_7 >> k_{29}$  (pg 39), to;

$$\frac{d[NO_2]}{dt} = \frac{3k_{28}k_{27} [HNO_3]^2}{k_{-27}[NO_2] + k_{28} [HNO_3]}$$
(3-43)

For reaction (28) the rate of loss for HNO, is given by:

$$-\frac{d[HNO_3]}{dt} = \frac{2k_{27}k_{28}[HNO_3]^2}{k_{-27}[NO_2] + k_{28}[HNO_3]}$$
(3-44)

With NO present, one has the following net stoichiometric reaction:

$$2HNO_3 + NO \longrightarrow 3NO_2 + H_2O$$
 (26)

so that the final concentration of  $NO_2$  is 1.5 times that of the  $HNO_3$ . For low pressure Johnston et al. (1955) has postulated that five steps are required. The governing mechanistic reactions for reaction (26) are the decomposition of  $HNO_3$  followed by a product-reactant reaction followed by a fast

bimolecular reaction converting NO to NO<sub>2</sub> followed by the synthesis of nitrous acid as an intermediary and finally a reaction to consume the nitrous acid.

These reactions are:

$$HNO_3 \qquad [M] \qquad HO + NO_2 \qquad (27)$$

$$HO + HNO_3 \longrightarrow H_2O + NO_3$$
 (28)

$$NO + NO_3 \longrightarrow 2NO_2 \tag{7}$$

$$NO + NO_2 + H_2O \longrightarrow 2HNO_2$$
 (29)

$$HNO_2 + HNO_3 \longrightarrow 2NO_2 + H_2O$$
 (30)

# 3.7.2 Stratospheric-Based Instrument Modeling

The above set of reactions along with the  $N_2O_5$  set of reactions given in paragraph 3.5.1 have been modeled using the EPISODE code to analyze and review concentration-time profiles of the various molecules and radicals. For laboratory conditions the profiles indicate that OH scavenging and elevated temperature promote the decomposition of  $HNO_3$ . For stratospheric conditions the profiles (c.f., Appendix B-2) indicate that only increased temperature promotes the decomposition of  $HNO_3$ , i.e., the intermediary radical, OH does not impede decomposition.

#### 3.7.3 Experimental Procedures and Results

The thermal decomposition of nitric acid was investigated in the laboratory with emphasis placed on a quantitative understanding and investigation of the thermal converter. In addition, ozone was introduced into the HNO3 vapor stream to determine whether it had an effect on the thermal conversion process.

The thermal converter based on a design by Stedman (private communication, 1977), consisted of 40 cm long by 1/2-inch O.D. stainless steel tubing, packed with 1/8-inch diameter Pyrex balls. (The Pyrex balls served to raise the temperature of the gas to that of the tubing.) The tubing was wrapped with electrical heating tape and placed in an insulated cylinder. The temperature of the tubing, which could be raised as high as 500°C, was monitored

by a thermocouple inserted into the gas stream exiting the converter. The temperature could also be monitored by observing the  $\left[\text{NO}_2\right]/\left[\text{NO}\right]$  ratio of the exiting gas stream when  $\text{NO}_2/\text{air}$  was passed through the converter.

The gas leaving the thermal converter was directed into an absorption cell, placed within a Perkin-Elmer Model 580A spectrophotometer. The internal optics of the absorption cell were set to an optical absorption path length of 15.75 m. The infrared absorption properties of HNO3, NO2, and O3 are discussed in Appendix A of this report. By combining the known optical properties of these molecules with the observed IR absorptions, the number density of each specie was determined.

From the absorption cell, the flowing gas was directed to the Aerochem chemiluminescence monitor. The monitor was primarily used to detect NO (whose IR absorption signature is especially weak) and to verify the spectroscopically determined, NO<sub>2</sub> concentrations. A comparison of the analytical methods using the CL monitor as opposed to those of the spectrophotometer was made by using an NO<sub>2</sub>/air span gas diluted by additional nitrogen to maintain a constant flow rate (Figure 3-12). Agreement between the two instruments was quite good. The CL monitor response also was determined as a function of gas flow rate (Figure 3-13). Since the CL monitor has a constant volume bellows pump within it to draw in the gas sample, the pressure in the sample line will vary as the flow rate is externally controlled, but the response remains proportional to the flow rate.

It was shown in paragraph 3.6.1 that the concentration of HNO<sub>3</sub> depended inversely on the gas flow rate. Therefore, to vary the concentration of HNO<sub>3</sub>, the flow rate was varied. However, pressure in the absorption cell was maintained at constant value by adjusting a throttle valve located at the exit port of the cell. CL monitor readings were "normalized" to take into account the varying flow rate.

The results of a set of measurements of the thermal conversion of HNO<sub>3</sub> are given in Table 3-16. The absorption data is based on the average of three or more successive spectra recorded after equilibrium was established. The standard deviation of the data is also shown. The CL monitor response for

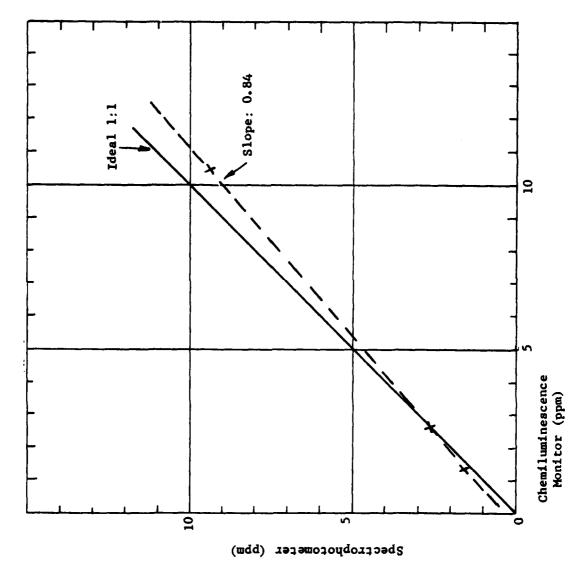


Figure 3-12. Response of Perkin-Elmer Model 580 Spectrophotometer vs. Chemiluminescence Monitor

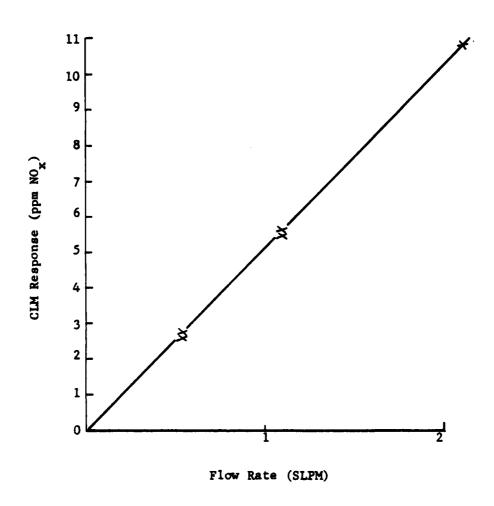


Figure 3-13. Chemiluminescence Monitor Performance vs. Flow Rate

HNO THERMAL CONVERTER<sup>(a)</sup> PERFORMANCE CHARACTERISTICS WITH CROSS CALIBRATION HIGH TEMPERATURE CATALYTIC CONVERSION VS CHEMILUMIN-ESCENCE MEASUREMENTS TABLE 3-16.

Apparatus	Sampling Point	Concentration	Analysis Techniques
Low Temperature Con-	Inlet	$[HNO_3] = 7.2 \pm 0.4 \text{ ppm}$	IR Absorption
Verter, 1 = 333 ± A	Outlet	$[NO_2] = 7.1 \pm 0.4 \text{ ppm}$	IR Absorption
		$\begin{bmatrix} NO_2 \end{bmatrix} = 7.8 \text{ ppm}$	Thermal-CLM
		NO = 0.6 ppm	CIM
		$[NO_2]/[NO] = 14.0^{(b)}$	Ratio
High Temperature	Inlet	$[HNO_3] = 7.2 \pm 0.4 \text{ ppm}$	IR Absorption
catalytic converter and CLM	Outlet Sample	$[NO_2]^n = 7.7$	Thermal-CLM

 $^{(a)}$ Tubular Pyrex Converter with 3 mm Pyrex Spheres

(b) Equivalent to Thermodynamic Conversion Ratio Expected for T = 535 K

the NO  $_{\rm X}$  mode was scaled to compensate for the changing flow rate. The NO and NO  $_{\rm X}$ -NO density data were derived from the NO  $_{\rm X}$  data and from NO concentration data which was also recorded by the monitor.

Comparison of the second and third lines of the table shows that the amount of NO (from the CL monitor) plus NO<sub>2</sub> (from the spectrophotometer) is approximately 7.6 x  $10^{13}$  molecules/cm<sup>3</sup>, which is very good agreement. It is also apparent by comparing lines 3 and 4 that the Aerochem instrument responds accurately to HNO<sub>3</sub> vapor. Comparison of the CL monitor with the Model 580A (Figure 3-12) indicated a 5 to 15 percent disagreement. This uncertainty limits our ability to compare data to an accuracy of no more than 10 percent. Finally, the  $\begin{bmatrix} \text{NO}_2 \end{bmatrix} / \begin{bmatrix} \text{NO} \end{bmatrix}$  ratio indicates a gas temperature in the 520 to 550 K range. The equilibrium constant,  $K_{25,-25}$ , at this temperature indicates that the HNO<sub>3</sub> should be entirely decomposed.

In an earlier experiment, dry nitrogen rather than air was used as the carrier gas for the HNO $_3$  vapor. The products of the decomposition were NO $_2$  and NO, with their ratio being  $\begin{bmatrix} NO_2 \\ NO_2 \end{bmatrix} / \begin{bmatrix} NO \end{bmatrix} = 3.48 \pm 0.91$ ; the HNO $_3$  concentration was 5.68 x 10<sup>13</sup> molecules/cm<sup>3</sup>. The optically detected NO $_2$  density was 4.52 x 10<sup>13</sup>. Taking into account the measured ratio of  $\begin{bmatrix} NO_2 \end{bmatrix}$  to  $\begin{bmatrix} NO \end{bmatrix}$ , the sum of  $\begin{bmatrix} NO \end{bmatrix}$  and  $\begin{bmatrix} NO_2 \end{bmatrix}$  was 5.82 x 10<sup>13</sup> molecules/cm<sup>3</sup> which is, again, very close to the original HNO $_3$  number density. The uncertainty associated with these measurements was on the order of  $\pm$  10 percent. The reason the  $\begin{bmatrix} NO_2 \end{bmatrix}$  to  $\begin{bmatrix} NO \end{bmatrix}$  ratio differed from the data discussed previously is related to the use of nitrogen. The NO $_2$  decomposition reaction to form NO has been discussed (paragraph 3.3.1.1); the equilibrium constant is independent of the carrier gas (air or nitrogen) while the actual ratio of  $\begin{bmatrix} NO_2 \end{bmatrix}$  to  $\begin{bmatrix} NO \end{bmatrix}$  is not. This explains the difference in the ratio for the two cases. For either carrier gas, the thermal decomposition of HNO $_3$  was total to within experimental error. The maximum flow rate used was 2.1 SLPM.

$$\log \frac{\left[\text{NO}_2\right]}{\left[\text{NO}\right]} = \frac{3002}{\text{T}} - 4.223 \tag{3-15}$$

and is applicable at standard pressure and pO2 = 152 torr.

<sup>\*</sup>For determination of the  $\begin{bmatrix} NO_2 \end{bmatrix} / \begin{bmatrix} NO \end{bmatrix}$  ratio, the following expression has been used;

#### 3.8 POTENTIAL INTERFERENTS (Specificity)

Potential interferents that could affect the performance of a hybrid chemical conversion system include members of both the ClO<sub>X</sub>NO<sub>X</sub> family of compounds and the HO<sub>X</sub>NO<sub>X</sub> family of compounds. These potential interferents would effect the performance through either photolytic effects or thermal lability effects. This program has (1) analyzed photolytic effects of the ClO<sub>X</sub>NO<sub>X</sub> compounds, (2) experimentally treated ClONO<sub>2</sub> until accidental loss of all material occurred, and (3) analyzed thermal lability effects of ClONO<sub>2</sub> and HO<sub>2</sub>NO<sub>2</sub>.

# 3.8.1 Clo NO Family Compounds

1

This section treats the potential interference of nitrosyl chloride (C1NO), nitryl chloride, chlorine nitrite (C10NO), and chlorine nitrate (C10NO $_2$ ) with particular emphasis on C10NO $_2$  since it is believed to be the most predominant member of the C10 $_x$ NO $_x$  family with the stratosphere.

## 3.8.1.1 ClONO, Generation and Handling

Chlorine nitrate has been synthesized by three methods. The first method (M. Schmeisser, 1963) is based upon the reaction:

$$C1_2O + N_2O_5 \longrightarrow C10NO_2$$
 (31)

The boiling point of nitrate is about 18 to 22°C and the melting point about -107°C. Decomposition occurs slowly at room temperature, but since C1<sub>2</sub>O is very sensitive to heat, C10NO<sub>2</sub> is commonly stored at -78°C or at 77 K. For research quantities, much of the C10NO<sub>2</sub> used in the United States has been generated and distributed by Dr. Louis C. Glasgow of E.I. DuPont de Nemours and Company. Containerization employs glass ampules or 1 liter stainless steel sampling cylinders.

A second method (Birks et al., 1977) is based upon the reaction:

$$C10 + NO_2 + N_2 \longrightarrow C10NO_2 + N_2$$
 (32)

The initial reactants employed are 0.25 percent  ${\rm Cl}_2$  in He,  ${\rm O}_2$  for the generation of  ${\rm O}_3$  and NO $_2$  in air. Two mixing stations are required; the first

downstream from a microwave cavity, which is used for generating atomic chlorine, and an ozonator. The second is downstream for the ClO and  $NO_2$  sources.

The third method (Schack, 1967) is based upon the reaction:

$$C1F + HNO_3 \longrightarrow C1ONO_2 + HF$$
 (33)

The technique avoids the use of hazardous chlorine oxides since the initial reactants are separately condensed at 77 K into a stainless steel container. Bulb to bulb cryogenic vacuum distillation separates the CloNO<sub>2</sub> com the hydrofluoric acid.

The CloNO<sub>2</sub> used for this program was generated by Dr. Glasgow, on February 3, 1977, using the first method. The batch (about 5 gms material at 77 K) underwent four bulb to bulb distillations before delivery and a fifth distillation to remove further accumulated impurities was carried out at Perkin-Elmer on September 12, 1978. The material was held at 77 K between the last two distillations. Impurities generally include Cl<sub>2</sub>, NO<sub>2</sub>, N<sub>2</sub>O<sub>5</sub>, HNO<sub>3</sub>, and possibly ClO<sub>2</sub>. Absorption spectra in the UV region indicated that the transfered batch contained substantial Cl<sub>2</sub>, but no discernible NO<sub>2</sub>.

The vapor pressure of  $Clono_2$  is given by the expression (Schack, 1967):

$$\log P = \frac{-0.05223 \text{ A}}{T} + B \text{ (torr)}$$

where A = 28,900 and B = 7.9892. This expression versus 1000/T is shown in Figure 3-14 along with similar data from International Critical Tables for the possible impurities  $\text{Cl}_2$ ,  $\text{NO}_2$ ,  $\text{N}_2\text{O}_5$ , and  $\text{HNO}_3$ . For the fifth distillation,  $\text{Cl}_2$  was pumped off at 163 K using a slush of methyl butane (isopentane) and liquid nitrogen. The batch was then elevated in temperature to about 223 K and the  $\text{ClONO}_2$  was allowed to enter an IR absorption cell at a pressure of about 14 torr or condensed in a one-liter stainless steel container.

Materials in contact with the sample included glass, teflon,  $^{\circledR}$ \*, stain-less steel, KBr and halofluorocarbon grease, GR-90.

<sup>\*</sup>PTFE, Polytrifluoromonochloroethylene

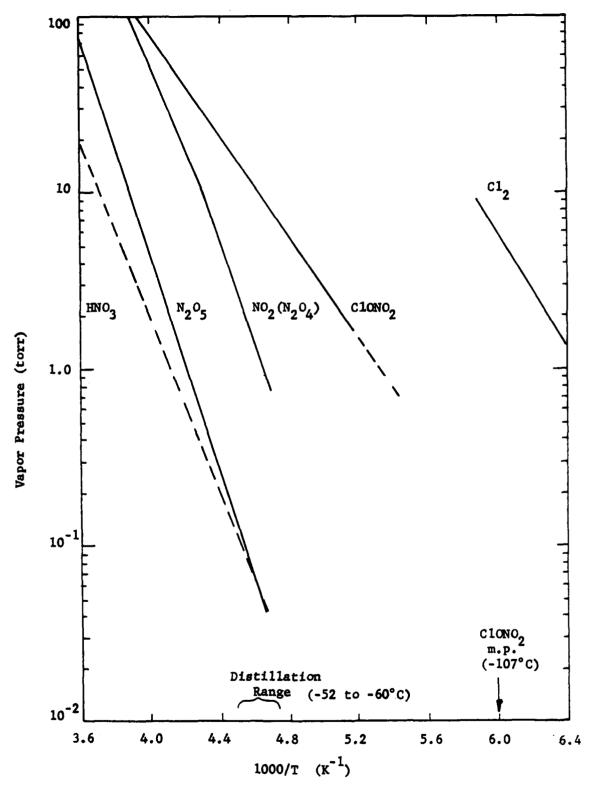


Figure 3-14. Vapor Pressure Diagram For ClONO2 and Suspected Impurities

The Clono<sub>2</sub> absorbance was then measured on a Perkin-Elmer Model 521 spectrometer using a preset resolution of 3 cm<sup>-1</sup> for survey over the region 1800 to 650 cm<sup>-1</sup>. During transfer of the cell to the spectrometer, the sample was held at about 273 K and protected from room lighting by Wratten-type filter material.

Two lengthy survey scans were performed and analyzed as the  ${\rm Clono}_2$  thermally decomposed at a temperature close to 306 K. The decay of  ${\rm Clono}_2$  is shown in Figure 3-15 and a summary of the data is given in Table 3-17. Due to the large absorbance of  ${\rm Clono}_2$ , the initial fill pressure of about 14 torr was reduced to a pressure of about 4.5 torr. The unused portion of  ${\rm Clono}_2$  was diluted with nitrogen and stored at  ${\rm LN}_2$  temperature for later use. Failure of the automatic  ${\rm LN}_2$  transfer system during an unattended period caused the  ${\rm Clono}_2$  to attain room temperature with a subsequent thermal decay.

# 3.8.1.2 $C10_{x}N0_{x}$ Photolytic Interferents

It is possible that, should an NO<sub>2</sub> photolytic converter be used prior to chemiluminescence of NO with O<sub>3</sub>, the ClNO, ClNO<sub>2</sub>, ClONO, and ClONO<sub>2</sub> will be photolyzed to yield a higher reading of NO<sub>2</sub>. This possibility is not considered to be significant as is shown below, where what is believed to be typical concentration levels and a white-light photolytic source appropriately filtered with Corning C.S. 7-54 and 320-nm glass filters are assumed.

Although three members of the  ${\rm C1O}_{_{\rm X}}{\rm NO}_{_{\rm X}}$  family are not considered among the "most important" trace species of the stratosphere and, therefore, have received very little attention, they do have significant near-UV absorption cross-sections as is seen shown in Figure 3-16. The fourth species,  ${\rm C10NO}_2$  is considered to be an important sink as it does not appear to react with  ${\rm O}_3$  and reacts only slowly with  ${\rm O}_3$ .

By employing Corning C.S. 7-54 and 320-nm filters, an  $NO_2$  photolytic technique was developed that rendered  $NO_3$  a negligible interferent. The same analysis was applied to the  $ClO_XNO_X$  family to test the specificity of the technique. The results of the analysis are shown below in Table 3-18 with the appropriate absorption cross-sections taken from Figure 3-16.

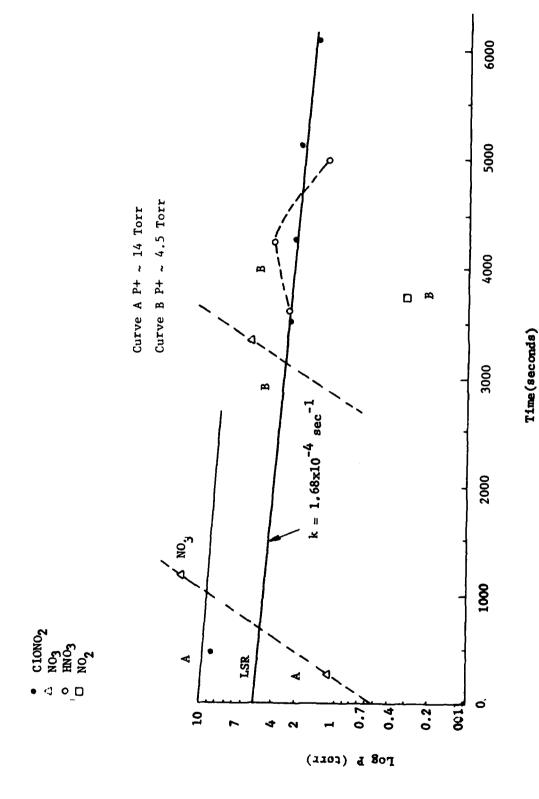
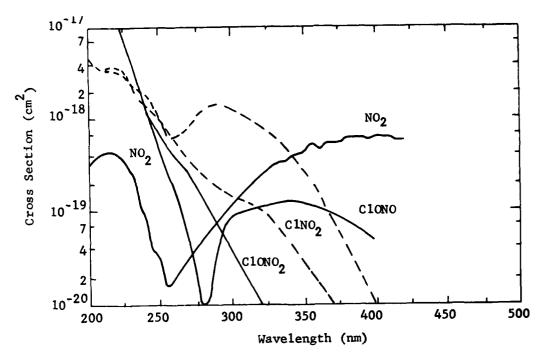


Figure 3-15. Thermal Decomposition of  $\text{CLONO}_2$ , T ~ 306 K

TABLE 3-17. Clono THERMAL DECOMPOSITION

Time (Sec)	Species	Analytical Band (cm )	Number Density (Molec/cm <sup>3</sup> )	Partial Pressure (Torr)	Total Pressure
285	NO 3	1860	0.04x10 <sup>18</sup>	1.13	~14 Torr
480	C10NO <sub>2</sub>	(v <sub>1</sub> )1735	0.27	8.5	
1160	NO <sub>3</sub>	1345	0.48	15	
1250	C10NO <sub>2</sub>	( <sub>v2</sub> )1292	0.34	10.6	
1335	N <sub>2</sub> O <sub>5</sub>	(v <sub>12</sub> )1246	0.0049	0.154	
3330	NO <sub>3</sub>	1860	0.14	4.29	~4.5 Torr
3520	C10NO <sub>2</sub>	(v <sub>1</sub> )1735	0.068	2.14	
3580	HNO <sub>3</sub>	(v <sub>2</sub> )1706	0.071	2.22	
3760	NO <sub>2</sub>	(v <sub>3</sub> )1600	0.0091	0.29	
4280	нио 3	( <sub>4</sub> )1311	0.095	2.98	
4290	C1ONO <sub>2</sub>	1292 (v <sub>2</sub> )(1288)	0.064	2.03	
4970	HNO <sub>3</sub>	890	0.037	1.17	
5140	Clono <sub>2</sub>	( <sub>4</sub> ) 780	0.056	1.77	
6090	Clono <sub>2</sub>	( <sub>v1</sub> )1735	0.044	1.39	



NO Curve Adapted from H.S. Johnston and R. Graham, Can. J. Chem 52, 1415 (1974). Other Curves from NASA Reference Publ. 1010, Chlorofluoromethanes and the Stratosphere, edited by R. Hudson, Aug 1977

Figure 3-16.  $NO_2$  and  $CIO_xNO_x$  Absorption Cross-Sections

TABLE 3-18. C10 NO -NO PHOTOLYSIS SPECIFICITY WITH SPECTRAL DISCRIMINATION

Species	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
Nitrogen dioxide, NO <sub>2</sub>	278	1.00
Nitrosyl chloride, C1NO	74	0.27
Nitryl chloride, ClNO <sub>2</sub>	25.2	0.091
Chlorine nitrite, ClONO	289	1.04
Chlorine nitrate, ClONO 2	2.7	0.01

Almost nothing is known about the stratospheric concentrations or mixing ratios of the  ${\rm ClO}_{\rm X}{\rm NO}_{\rm X}$  species cited above. Modeling efforts to date extend only to  ${\rm ClONO}_2$  (F.M. Luther, 1976; and NAS, 1976), and an upper limit of 2 ppb using the limb sensing techniques has been set (D.G. Murcray et al., 1977).

At stratospheric altitudes chlorine nitrate is produced at night by the combination of the radial ClO with NO $_{\rm 2}$  according to

$$C10 + NO_2 + N_2 \longrightarrow C10NO_2 + N_2$$
 (32)

During periods of high insolution, ClONO, is photolyzed via

$$C10NO_2 + h_V \longrightarrow C10 + NO_2$$
 (34a)

$$\longrightarrow C1 + NO_3 \tag{34b}$$

At high altitude, i.e.  $\rm H>40~km$ , the photolysis takes place over the 200 to 220 nm spectral region, where the absorption cross-section is  $\sim 375~x~10^{-20}~cm^2/molecule$ . At lower altitudes, 20 to 30 km, the diurnal change is much less, with photolysis occurring with radiation greater than 300 nm.

The number density profile of  $NO_2$  and  $Clono_2$  are shown below in Table 3-19. The  $Clono_2$  concentrations are taken from F.M. Luther (1976). As the chlorine nitrate density is well below that of  $NO_2$ , the 0.01 of Table 3-18 is further reduced.  $Clono_2$  photolyization is not considered to be a significant problem.

TABLE 3-19. NO 2 AND C10NO 2 CONCENTRATIONS

H (km)	NO <sub>2</sub> (30 N) (molecules/cm <sup>3</sup> )	C10NO <sub>2</sub> (midnight) (molecules/cm <sup>3</sup> )	C1ONO <sub>2</sub> (noon) (molecules/cm <sup>3</sup> )
20	1.3 x 10 <sup>9</sup>	1.0 x 10 <sup>8</sup>	8.0 x 10 <sup>7</sup>
25	2.2	4.0	3.0 x 10 <sup>8</sup>
30	2.2	1.8	1.0
35	1.4	5.0 x 10 <sup>7</sup>	1.0 x 10 <sup>7</sup>

# 3.8.1.3 ClONO2 Thermal Lability

The thermal lability of ClONO<sub>2</sub> can impact laboratory handling of the material as well as the specificity of a chemical conversion system that relies on thermal converters. A study by Cox et al. (1977), which employed enthalpy data for ClONO<sub>2</sub>, led to a high pressure limiting rate given by 10<sup>14</sup> exp (-12480/T) s<sup>-1</sup> for the decomposition of ClONO<sub>2</sub>. This rate is about 3500 times slower than the data of Knauth cited below. The most recent work concerning ClONO<sub>2</sub> kinetics is that of H.D. Knauth (1978). Thermal decompositions were studied in the presence of NO, ClNO, and N<sub>2</sub> over the temperature range 303 to 363 K at pressures from 3 to 380 torr.

The unimolecular dissociation of ClONO given by:

$$C10NO_2 + (M) \longrightarrow C10 + NO_2 + (M)$$
 (-32)

is followed by the fast reaction:

$$NO + C10 \longrightarrow NO_2 + C1$$
 (35)

and chlorine consuming steps.

For pN<sub>2</sub> less than 220 torr, an empirical first-order linear relationship between  $k_{-32}$  and  $\begin{bmatrix} N_2 \end{bmatrix}$ ,  $k_{-32} = k_{-32a} + k_{-32} \begin{bmatrix} N_2 \end{bmatrix}$ , was determined and suggests that the reaction takes place in the low pressure region or that the departures from the low pressure region are quite small. The rates are given as:

$$k_{-32a} = 2.743 \times 10^6 \text{ exp } (-3350/\text{RT}) \text{ sec}^{-1} \text{ and}$$
  
 $k_{-32}'' = 1.318 \times 10^{-5} \text{ exp } (6030/\text{RT}) \text{ cm}^3 \text{-mole}^{-1} \text{-sec}^{-1}$ 

The Knauth data for T  $\geq$  333 K is shown in Figure 3-17 in log-log form. The data for T  $\leq$  300 K has been extrapolated from the higher temperature data. The solid square points (T = 263 K) correspond to reasonable N<sub>2</sub> diluent storage conditions, but half-life values of only 257 and 82 minutes (at the knee) result. At a temperature of -78°C, the half-line becomes 1.7 x  $10^8$  sec, or  $2 \times 10^3$  days.

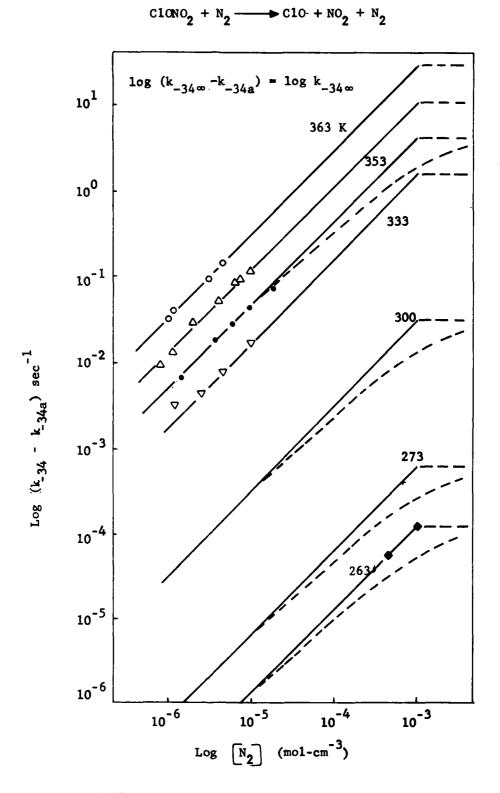


Figure 3-17. Chlorine Nitrate-Nitrogen Dissociation Rates

For the region of the stratosphere of interest  $(N_2) \sim 3 \times 10^{18}$  molecules-cm<sup>-3</sup> and less, so that a 300 K monitoring system with a sample residence time of several seconds would not cause appreciable thermal decay of  $C10NO_2$ . On the other hand, a 400 K converter for  $N_2O_5$  would result in a  $C10NO_2$  half-life of about 0.2 second, causing a lack of specificity for  $N_2O_5$  conversion. Impact on the  $HNO_3$  conversion accuracy due to the relative concentrations would be minimal.

The reaction of NO +  ${\rm ClONO}_2$  leading to an intermediate product but ultimately to ClNO and NO $_2$  or

$$C10NO_2 + 2NO \longrightarrow C1NO + 2NO_2$$
 (36)

was also studied by Knauth. The rate was found to be  $2.09 \times 10^{-12}$  exp (-11,850/RT) cm<sup>3</sup>-molecule<sup>-1</sup>-s<sup>-1</sup> over the 303 to 343 K temperature range. At 300 K, Knauth's value of  $4.8 \times 10^{-21}$  cm<sup>3</sup>-molecule<sup>-1</sup>-s<sup>-1</sup> is in general agreement with that of Rowland et al. (1976). At 800K, the highest anticipated temperature for any of the converters, the rate is still small,  $1.2 \times 10^{-15}$  cm<sup>3</sup>-molecule<sup>-1</sup>-s<sup>-1</sup>, so NO will not be consumed by the ClONO<sub>2</sub>. However, the ClO product from thermal decomposition will consume NO.

# 3.8.2 HO NO Family Compounds

This section treats the potential interference of nitrous acid (HONO) and pernitric acid (HO<sub>2</sub>NO<sub>2</sub>); nitric acid (HONO<sub>2</sub>) having been treated in Section 3.4. Concern with HONO is dismissed by review of pertinent reactions for its generation and high degree of photodissociation during daylight hours. Concern with HO<sub>2</sub>NO<sub>2</sub> is not dismissed.

#### 3.8.2.1 Nitrous Acid (HONO)

Nitrous acid is not expected to be an interferent for reasons cited below. It can be formed by four methods. These reactions are:

$$NO + NO_2 + H_2O \longrightarrow 2HONO$$
 (29)

$$N_2O_3 + H_2O \longrightarrow 2HONO$$
 (36)

$$HO_2 + NO_2 \longrightarrow HONO + O_2$$
 (37a)

$$\longrightarrow HO_2NO_2 \tag{37b}$$

$$N_2O_2 + NO \longrightarrow HONO + HO$$
 (38)

Reaction 31 is favored within power plant stacks and near automobile exhausts. Room temperature kinetic studies have been carried out by Chan et al. (1976). Rate constant estimates that use 0.5 cm<sup>-1</sup> spectroscopy to follow the kinetics are  $k_{31} = 6 \times 10^{-38}$  cm<sup>6</sup>-molecule<sup>-2</sup>-s<sup>-1</sup> and  $k_{20} = 9.4$  $\times$  10<sup>-19</sup> cm<sup>3</sup>-molecule<sup>-1</sup>-s<sup>-1</sup>. Since this is a third-order rate equation, it will not proceed to the right unless the conditions are very favorable. Furthermore, if HONO is formed it will be photolyzed with  $\bar{\textbf{\textit{J}}}$  > 0, since  $\sigma$  > 1 x  $10^{-19}$  cm<sup>2</sup>/molecule for 340  $\leq \lambda \leq$  384 nm (NASA Publ. 1010). Hydridizing nitrogen sesquioxide, reaction 38, has not received much attention. The free radical HO, combination with NO, reaction 39, favors the formation of HO, NO, since  $k_{37a}/k_{37b}$  is about  $10^{-3}$  (Graham et al., 1977). The kinetics of this reaction have also been studied by Simonaitis and Heicklen, (1974).

# 3.8.2.2 Pernitric Acid (HO,NO,)

The formation of HO2NO2 via a two-body or three-body mechanism proceeds well enough that it has been modeled by Jesson et al. (1977) with peak concentrations occurring in the 1- to 3-ppb range. It is therefore considered to be a potential interferent.

The reaction kinetics of  $\mathrm{HO}_2$  and  $\mathrm{NO}_2$  have been studied recently by a number of investigators: Simonaitis and Heicklen (1974, 1976, and 1977), Howard and Evenson (1977), Niki et al. (1977), Jesson et al. (1977), Graham et al. (1977) and Graham et al. (1978). The reactions most often considered are:

$$HO_2 + NO \longrightarrow HO + NO_2$$
 (39a)  
 $\longrightarrow HONO_2$  (39b)  
 $HO_2 + NO_2 \longrightarrow HONO + O_2$  (37a)  
 $\longrightarrow HO_2NO_2$  (37b,-37b)

(37b, -37b)

$$2HO_2 \longrightarrow H_2O_2 + O_2$$
 (40)

$$HO_2NO_2 \longrightarrow HONO + O_2$$
 (41)

Reactions (39a) and (39b) are occasionally written as a three-body reaction. The rate constants are given in Table 3-20 in the usual Arrhenius' form. The disparity in term values for  $k_{-37}$  will be shown below to have little significance for temperatures greater than 298 K.

As the thermal conversion technique is being considered for  $N_2O_5$  and  $HNO_3$  species, the above cited first-order rates for reaction (-39b) have been developed for laboratory ambient temperature, 400 K and 550 K. These rates, half-lives, and  $NO_2$  concentrations are presented in Table 3-21 for resident times of 1, 2, and 5 seconds. For temperatures above 298 K, conversion is complete in less than a second and yields  $NO_2$ . This conversion reduces the specificity of  $N_2O_5$  and  $HNO_3$  measurements. For an  $NO_2$  measurement at an instrument temperature of 298 K, lack of specificity is also present, but to a lesser degree. Straightforward solution to this problem, if the published rates have been correctly extrapolated, is not apparent at this time.

Finally, since the thermal decomposition of  $HO_2NO_2$  changes from first order to second order with reduced pressure,  $k_{-37b}$  should be investigated at stratospheric temperatures and pressures 760 >> p > 7 torr.

# 3.9 NO FEASIBILITY\*

For a selective hybrid chemical conversion (SMS), thermal partitioning of thermally labile molecules, N<sub>2</sub>O<sub>5</sub> and HNO<sub>3</sub>, has led to ambiguous results and therefore such a system is not recommended. The method is also particularly susceptible to interfering species as mentioned in Paragraph 3.8. A non-selective or total odd nitrogen SMS, however, is feasible and described below.

NO is defined to be the sum of NO, NO<sub>2</sub>, N<sub>2</sub>O<sub>5</sub>, HNO<sub>3</sub>, ClONO<sub>2</sub>, and HO<sub>2</sub>NO<sub>2</sub>. Adsorbed NO<sub>2</sub> on particulate matter is not specifically treated in the text. Three modes of sampling are believed to be possible. First by using a fluoropore-type filter only, a gas phase sample will be accepted. Second, by employing no filter, both gas phase and adsorbed NO<sub>2</sub> will be accepted. A third conceivable mode would be a time shared combination of the first two modes.

TABLE 3-20. HO NO REACTION RATES

) Reference	Simonaitis and Heicklen (1977)	Howard and Evenson (1977)	Simonaitis and Heicklen (1976)	Howard and Evenson (1977)	Simonaitis and Heicklen (1977)	Simonaitis and Heicklen (1977)	Howard and Evenson (1977)	Simonaitis and Heicklen (1977)	Graham et al, (1978)	Graham et al, (1978)	Simonaitis and Heicklen (1977)	Simonaitis and Heicklen (1977)
Rate (295-300 K) (cm <sup>3</sup> -molecule <sup>-1</sup> - $^{-1}$ )	1.14x10 <sup>-12</sup>	8.03x10 <sup>-12</sup>	2.0210-15	4.5x10 <sup>-30</sup>	1.63x10 <sup>-13</sup>	4.2x10 <sup>-13</sup>	$1.97 \times 10^{-31} \text{cm}^6$	5.16x10 <sup>-2</sup> s <sup>-1</sup>	9.04x10 <sup>-2</sup> s-1	1.30x10 <sup>-20</sup>	3.3x10 <sup>-12</sup>	5.4x10 <sup>-3</sup> g <sup>-1</sup>
Rate $(cm^3$ -molecule $^{-1}$ -s $^{-1}$ )	1.2x10 <sup>-11</sup> exp [-(1400+500)/RT]	3.0x10 <sup>-11</sup> exp (-775/RT)			1.7x10 <sup>-12</sup> exp (-1400/RT)	Temperature Independent		6x10 <sup>17</sup> exp (-26000/RT) s <sup>-1</sup>	1.4x10 <sup>14</sup> exp (-20700/RT) s <sup>-1</sup>	5.2x10 <sup>-6</sup> exp (-19,900/RT)	Temperature Independent	1x10 <sup>8</sup> exp (-14000/RT) s <sup>-1</sup>
Reaction	(418)		(414)		(398)	(39b)	_	(-39b)			(42)	(43)

Table 3-21. First-order  ${\rm HO_2\,NO_2}$  rate constants and predicted thermally yielded NO\_2 as a function of sample residence time (a)

	NO <sub>2</sub> (a)	(qdd)	1	0.18	0.13	0.72	2	2	- 2	2	2	2	
Decay	t R	(s)	,	-	2	יע	ı	2	<u>۱</u>	1	2	2	
Graham et al., Rate	-39b	(8)	1.84x10 <sup>6</sup>	7.66			1.03x10 <sup>-3</sup>			8.45x10 <sup>-7</sup>			
S	<sup>k</sup> -39b	(s <sup>-1</sup> )	3.76×10 <sup>-7</sup>	9.04×10 <sup>-2</sup>			6.75x10 <sup>2</sup>			8.20x10 <sup>5</sup>			
	NO <sub>2</sub> (a)	(qdd)		0.10	0.20	0.45	2	2	2	2	2	2	
and Heicklen Rate	t <sub>R</sub>	(s)	,	7	2	5	-	2	2	1	2	5	
Simonaitis and Decay Rate	-39b	(s)	7.8x10 <sup>7</sup>	13.43			1.8x10 <sup>-4</sup>			2.5x10 <sup>-8</sup>			
8.1	<sup>k</sup> -39b	(s-1)	8.86×109	5.16x10 <sup>-2</sup>			$3.80 \times 10^3$			2.79x10 <sup>7</sup>			(6)
		т (X	220	298			400			550			

The proposed  $\mathrm{NO}_2$  instrumentation includes a NO chemiluminescence monitor in series with a high temperature catalytic converter ( $\mathrm{NO}_2$  channel) along with a second NO chemiluminescence monitor operated in parallel. This instrumentation would permit NO,  $\mathrm{NO}_2$ , and  $\mathrm{NO}_2$ -NO measurements. To maintain equivalent flow parameters, e.g. identical residence times, the NO channel would be made equivalent to the  $\mathrm{NO}_2$  channel except that a uniform low temperature would be employed. Experimental data for an  $\mathrm{NO}_2$  type channel was presented in paragraphs 3.3.1 and 3.5.2. To better understand the sample reaction kinetics, stratospheric simulations of the sample passing through the instrumentation have been modeled and analyzed by the GEARS/EPISODE code. An understanding of these analyses is required to determine the feasibility of an  $\mathrm{NO}_2$  or total odd-nitrogen monitor.

Finally, as part of the overall feasibility of NO type of instrumentation, wall effects and the propagation of very low levels of certain species are considered by drawing upon vacuum technology in an attempt to develop a physical description of sorption processes. Simulations are treated first, while a baseline design for the sample handling is treated last.

## 3.9.1 Stratospheric-Based Instrument Modeling

The instrument will naturally induce changes in the incoming ambient air sample. These changes must be minimized if an accurate determination of the unperturbed atmosphere is to be made. These internal changes depend in part on temperature, pressure, specie concentrations, reaction rates and sample flow rate. The calculations have been carried out assuming inviscid flow of a perfect gas at low Reynolds number for several pressures. The instrumentation has been assumed to be athermalized to pre-selected model values and heterogenous reactions have been assumed to be negligible.

The EPISODE code was employed to analyze NO $_2$ , N $_2$ O $_5$ , HNO $_3$ , C ONO $_2$ , and HO $_2$ NO $_2$  conversions. Criteria for reaction selection was based upon known mechanisms, a reasonable knowledge of the rates, the magnitude of the rate and the reactant number density. Appropriate O $_3$  reactions were included since  $\left\lceil \text{O}_3 \right\rceil \sim 10^{12}$  molecules/cm $^3$ .

The reaction set for  $N_2O_5$  thermal decomposition was listed at the beginning of Paragraph 3.5.1 with the exception of the ozone oxidation of NO to  $NO_2$ .

The reaction set for  ${\rm HNO}_3$  thermal decomposition consists of the Johnston mechanisms listed in Paragraph 3.7.1 for reactions (25) and (26), i.e.,  ${\rm HNO}_3$  in the presence of NO, and the ozone oxidations of NO and NO<sub>2</sub> to NO<sub>2</sub> and NO<sub>3</sub>.

Both reaction sets, 16 reactions in total, have been combined and computer printouts of concentration versus time for a 25 km altitude situation are provided in Appendix B. Instrumentation temperatures of 250, 300, 400, 550, 600, 700, and 800 K have been selected. The first two values correspond to instrumentation temperatures where no active thermal heating would be occurring. The last temperature value corresponds to an upper limit value for the conversion of HNO<sub>3</sub> and nearly complete conversion of NO<sub>2</sub>.

A portion of the profile data of Appendix B has been selected and the gradient of appropriate species is presented in Table 3-22 for an assumed residence time of 5 seconds and initial concentrations representative of 25 km. These initial concentrations are; NO = 7.0 x  $10^8$ , NO<sub>2</sub> = 6.2 x  $10^9$ , N<sub>2</sub>O<sub>5</sub> = 7.0 x  $10^8$ , HNO<sub>3</sub> = 3.0 x  $10^9$ , O<sub>3</sub> = 4.3 x  $10^{12}$  and H<sub>2</sub>O = 6.0 x  $10^{12}$  molecules/cm<sup>3</sup>. At reduced temperatures, e.g., 250 and 300 K, where one is interested in an [NO] determination, NO is oxidized by O<sub>3</sub> forming NO<sub>2</sub>. The loss or measurement bias can be determined with a knowledge of the ambient  $\begin{bmatrix} O_3 \end{bmatrix}$ , the measurement of [NO], instrumentation temperature and sample flow rate. At the intermediate temperatures tabulated, where conversion of HNO<sub>3</sub> is only partial, the gradient ratio given in the last column shows significant departure from unity. At the higher temperatures tabulated, the ratio converges to unity. The small departure from unity is attributable to a small increase in the [NO<sub>3</sub>] and represents a measurement bias error since NO<sub>3</sub> is not measured.

TABLE 3-22. NET CHANGE OF SPECIES (molecules/cm<sup>3</sup>) VS TEMPERATURE FOR RESIDENCE TIME OF 5 SECONDS

T(K)	Δ NO	△ NO <sub>2</sub>	∆ 2N <sub>2</sub> O <sub>5</sub> +HNO <sub>3</sub>	- Δ NO <sub>2</sub> +2N <sub>2</sub> O <sub>5</sub> +HNO <sub>3</sub> /Δ NO
250	-0.090 x 10 <sup>9</sup>	+0.090 x 10 <sup>9</sup>	-0.0	1.000
300	-0.212	+0.219	$-0.023 \times 10^9$	0.924
400	-0.502	0.119	-1.400	2.551
550	+0.538	+0.042	-1.400	2.524
600	+3.115	-2.487	-1.403	1.249
700	+7.110	-5.554	-1.947	1.054
800	10.18	-6.058	-4.400	1.027

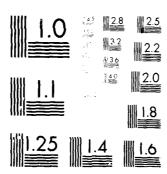
From the data tabulated in this table and various instrumentation parameters cited above, it may concluded that  $\begin{bmatrix} NO \end{bmatrix}$  can certainly be determined and that the summation term  $\begin{bmatrix} NO_2 + 2N_2O_5 + HNO_3 \end{bmatrix}$  can be determined at 800 K by differencing the two  $\begin{bmatrix} NO \end{bmatrix}$  measurements after correction for the NO oxidized during instrument transit time. For short duration flights, the use of dry ice is practical for further reducing the oxidation.

A design analysis or tradeoff study employing the EPISODE code to determine altitude, temperature, and residence time effects was conducted to verify the engineering feasibility of a high temperature  $NO_z$  converter. Figure 3-18 presents the parametric results of this analysis where the gradient ratio defined in Table 3-22 is plotted against altitude for temperatures of 800 and 900 K and residence times of 1.0, 2.5, and 5.0 seconds.

The sigmoidal shapes of the parameter curves of Figure 3-18 is an artifact of the representative species concentration profiles of the stratosphere selected for the calculation. No analysis was carried out for grossly perturbed profiles.

To minimize the  ${
m NO}_3$  measurement bias error, the  ${
m NO}_z$  high temperature converter should be operated at as high a temperature as practical and retain

PERKIN-ELMER CORP NORWALK CONN ELECTRO-OPTICAL DIV F/G 13/2 HIGH ALTITUDE POLLUTION PROBRAM STRATOSPHERIC MEASUREMENT SYSTEM-ETC(U) FEB 80 N H MACOY, R WEINGARTEN, A PIRES DOT-FA77WA-4080 PZ-14262 FAA/EE-80-11 NL AD-A085 198 UNCLASSIFIED 20r3 A0 408519#



MICROCOPY RESOLUTION TEST CHART NATIONAL BUREAU OF STANDARDS 1963-2

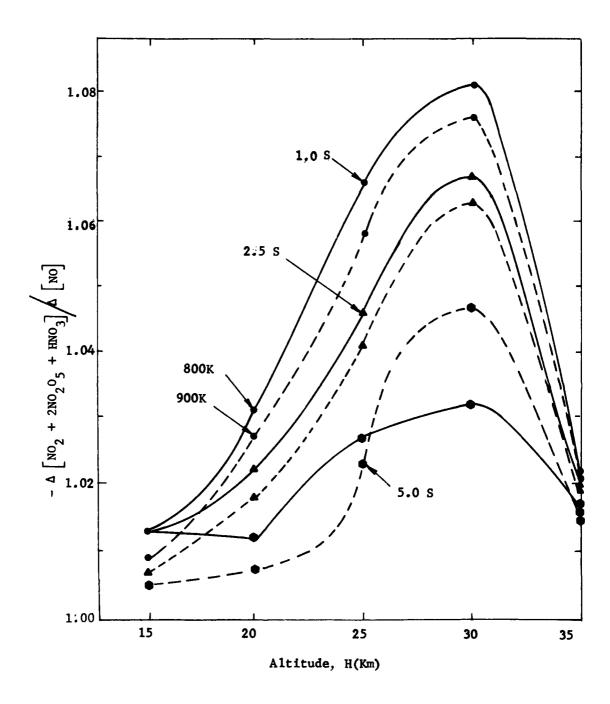


Figure 3-18.  $NO_3$  Measurement Bias Error

the sample for as long as practical. Based upon a temperature of 800 K and a residence time of 5 seconds, Figure 3-18 suggests that the measurement uncertainty will be less than 4 or 5 percent.

The thermally labile species,  $\text{ClONO}_2$  and  $\text{HO}_2\text{NO}_2$ , were then considered and their decomposition reactions added to the EPISODE code file. The reactions and rates are listed below for reference. The dimensional units are  $\text{cm}^3$ -molecule $^{-1}$ -s $^{-1}$ .

$$c_{10NO_{2}} + M \longrightarrow c_{10} + NO_{2} + M$$

$$k_{-32} = k_{-34a} + 1.32 \times 10^{-5} \exp(-11,980/T) \left[N_{2}\right]$$

$$k_{-32a} = 2.74 \times 10^{6} \exp(-3350/T)$$

$$HO_{2}NO_{2} + M \longrightarrow HO_{2} + NO_{2} + M$$

$$k_{-37b} = 6 \times 10^{17} \exp(-2600/RT)$$

$$(-37b)$$

Computer printouts for the expanded set are included in Appendix B for temperatures of 250, 300, 700 and 800 K.

#### 3.9.2 Heterogenous Sample Changes

Internal sample changes will also result if adsorption-desorption phenomena are occurring. Molecular adsorption takes place until a condition of equilibrium with desorption is realized. The following treatment, based on both kinetic theory and activation energy, is adopted from the work of Santeler et al. (1966). For the major species of the stratosphere, H<sub>2</sub>O will be of most concern. For water with a molecular weight of 18, the surface concentration (ideal monolayer) S<sub>m</sub> is, from kinetic theory,

$$S_{m}(300 \text{ K}, 18) = 3.7 \times 10^{-5} \text{torr-liter/cm}^{2} = 1.2 \times 10^{13} \text{molecules/cm}^{2}$$
  
 $S_{m}(800 \text{ K}, 18) = 6.0 \times 10^{-5} \text{torr-liter/cm}^{2} = 2.0 \times 10^{13} \text{molecules/cm}^{2}$ 

for temperatures of 300 and 800 K, respectively. At a pressure of 0.1 atm, the time needed to form a monolayer is about 33 nS.

Applying the activation energy concept for residence time gives

$$t_r = t_o \exp(\Delta E/RT)$$

where  $t_0$  = the vibrational period of the lattice,  $10^{-13}$ s at 300 K

E = characteristic energy, 24,000 cal/gm-mole

R = gas constant, 1.986 cal/deg-mole

T = temperature, 300 or 800 K

Therefore,  $t_r = 3 \times 10^4$  and 3.6 x  $10^{-7}$  seconds for the low and high temperatures. Thus one can expect that the room temperature NO instrumentation ahead of the gas phase titration region will scavenge  $N_2O_5$  and possibly  $HNO_3$  from the sample stream. Conversely, the 800 K  $NO_z$  instrumentation ahead of the gas phase titration region will not scavenge either  $N_2O_5$  or  $HNO_3$  from the sample stream. A recommended preflight task, however, is a thermal vacuum cycling of the high temperature converter.

Finally, it is recommended that all materials exposed to the sample during handling be restricted to glass; quartz; corrosion resistant steels, such as hastelloy, monel, inconel, nickel, gold, or Durimet 20<sup>TM</sup>; or the austenitic steels, such as stainless steel 316 (Grade CF8M) for general use or stainless steel 347 (Grade CF8C) should welding be required; and finally polytetrafluorethylene (PTFE). Glasses and metals should be scrupulously cleaned in benzol and distilled acetone while the polymer materials should be used in the asprocessed condition. The use of polymer materials is a controversial subject. In studying part per trillion levels of NO, NOAA scientists have found that, at that level, NO may or may not interact with PTFE, depending upon the ambient humidity (MacFarland, private communication, 1979). Reactivity is reduced to acceptable levels when humidity is low.

# 3.9.3 NO Baseline Design

This section considers the sample handling design for an  $NO_z$  converter and NO monitor. A discussion of payload consumables, signal processing, and many other engineering details are therefore missing.

The basic design includes three reaction volumes, sample ingress and egress ports, and reaction volume interconnections. The three reactions volumes are defined to be: (1) the high temperature NO<sub>2</sub> converter, (2) an instrument zeroing or background volume where O<sub>3</sub> is injected periodically to consume ambient NO, so as to establish a zero level signal, and (3) a chemiluminescence volume where gas phase titration of O<sub>3</sub> and NO occur. From the data of Figure 3-18, a baseline flow rate of 1 SLPS is selected. This rate would be derived from a servo controlled motor operating a high efficiency-zero-head lobe pump such as employed by NOAA (Drummond, private communication, 1979). This method of sample transport has two immediate advantages: (1) the flow rate is independent of ambient pressure and (2) once the pump and motor are characterized, an on-board flow meter is not required.

A general description follows. Upon sample entry to the instrumentation, the sample is exposed to a high temperature catalytic furnace or reaction vessel where  $\mathrm{NO}_{\mathrm{Z}}$  is converted to NO. For monitoring of only NO, the sample passes through a similar and parallel vessel whose temperature is maintained below 300 K. Each channel contains a pre-reaction vessel where  $\mathrm{O}_{3}$  may be periodically injected to generate a zero-reference level. Provision for injecting known levels of NO and NO<sub>2</sub> are also included for calibration purposes.

The design layout for the NO $_{\rm Z}$  converter/NO monitor is shown in Figure 3-19. The NO monitor reaction vessel design closely approximates the design used by NOAA for tropospheric sensing of NO. The design has been altered for stratospheric sensing.

The NO<sub>Z</sub> moderate temperature reaction vessel is spherically shaped to maximize the volume to surface ratio. The volume, 4070 cm<sup>3</sup>, was selected to provide a residence time of about 5 seconds, actually 4 seconds at a flow rate of 1 SLPS. A platinum-rhodium heating filament on an alumina support and sample ingress-egress deflection baffles of stainless steel material will be located within the sphere. The platinum filament serves two functions. First, as catalyst, it promotes the conversion of NO<sub>2</sub> to NO as discussed in paragraph 3.3.1. Secondly, it tends to scavenge atomic oxygen by surface

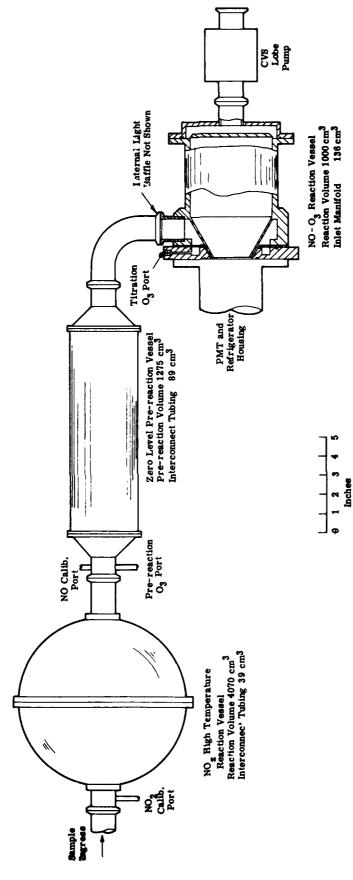


Figure 3-19. No Converter - NO Sensor Flow Layout

recombination produced by the thermal decomposition of 03. To minimize conductive heat losses, the sample ingress and egress flanges and tubing would be constructed of gold plated, thin walled, commercially pure titanium since titanium has a low heat conductivity.

The design details for the high temperature  $NO_2$  catalytic converter used in the laboratory as well as the moderate temperature  $NO_2$  catalytic converter are given in Table 3-23.

The function of the zero level pre-reaction vessel permits chemilumine-scence to occur before the sample reaches the photomultiplier tube, thereby allowing the PMT counter to accumulate a base level dark count. This count is then used as the zero reference level. The ozone is injected 1500 cm $^3$  ahead of the titration ozone manifold. At a sample flow rate of 0.25 SLPS, the residence time is 6 seconds. Using expressions 3-6 and 3-7, and the  $0_3$  parameters of paragraph 3.1.1, yields

$$\frac{\Delta[NO]}{[NO]} = 1 - \exp(-4.9) = 0.983$$

at an altitude of 25 km so that all but 0.7 percent of the NO is consumed ahead of the  $NO-O_3$  reaction vessel. At reduced altitudes the reaction is more complete.

The NO-O<sub>3</sub> reaction vessel contains an ozone inlet manifold and a sample inlet manifold. Mixing is initiated concentrically about the axis of the vessel near the PMT end of the vessel. At the opposite end of the vessel, a gold coated mirror is placed in conjunction with the gold plated cylindrical vessel to form a photon integrating cavity. A sample pumping port and lobe motor pump are located behind the mirror. For a sample residence time of 4 seconds, the data of Table 3-1 predicts total conversion to NO<sub>2</sub> of which about 7.2 percent is converted to the optically active state <sup>2</sup>B<sub>1</sub>.

### 3.10 POTENTIAL OF A NEW TECHNIQUE FOR NO, MEASUREMENTS

J.G. Anderson of Harvard University (private communication, 1979) is making laboratory measurements on a new technique for the measurement of NO<sub>2</sub>.

TABLE 3-23. HIGH TEMPERATURE REACTION VESSEL DESIGN COMPARISON

Parameter	Aerochem NO <sub>2</sub> Converter	Perkin-Elmer Converter	Relative Factor
Flow Rate	0.035 SLPS	1.0 SLPS	28.6
Temperature	~ 1373 K	~ 800-900 К	-
Ambient pressure	1000 mb	6 to 120 mb	-
Filament material	Pt 10% Rh	Pt 10% Rh	-
Filament casing	McDanel Refractory 99% alumina	Omega Engineering 99% alumina	-
Bonding material	Aremco Ultrabond 552	Sodium Silicate cement or Ultra- bond 552	-
Filament size	Avg No.30 (0.010")	Avg No. 24 (0.020")	_
Filament length	120 inches	600 inches	5.0
Contiguous sample volume	1.14 cm <sup>3</sup>	26 cm <sup>3</sup>	22.7
Contiguous sample residence time	33 mS	26 mS	0.8
Contiguous filament surface area	27.9 cm <sup>2</sup>	235 cm <sup>2</sup>	8.4
Heat equivalent power	14 watts	11 watts @ 50 mb	-

This new technique is very similar to the technique recently used for water vapor measurements in the stratosphere (Kley and Stone, 1978) and was suggested in the same report. The technique consists of the photodissociation of NO<sub>2</sub> using Lyman alpha (1216 A) light and the detection of the characteristic gamma-band fluorescence of the excited NO produced.

$$NO_2 + h v (1216 A) = NO(A^2 \Sigma^+) + 0$$
 (3-45)

$$NO(A^2 \Sigma^+) = NO + hv (1900 A)$$
 (3-46)

The detected signal in cts/sec-molecule/cc is proportional to the fluorecence intensity multiplied by optical efficiencies and by geometrical factors.

The fluorescence intensity can be expressed by

$$I = \frac{\left[NO_{2}\right] \cdot J \cdot \emptyset \cdot A}{A + \text{air } K_{q}^{\text{air}}}$$
 (3-47)

The photodissociation process is described by  $\emptyset$ , the quantum yield, and by J, the photodissociation coefficient. This coefficient is related to the light source photon flux  $\psi$  and the absorption cross section,  $\sigma_{\lambda}$ ,

$$J = \psi_{\lambda} \sigma_{\lambda} \tag{3-48}$$

The fluorescence process is described by A, the transition probability per second, and  $k_q^{\ air}$ , the quenching rate coefficient for air.

reliminary results of Anderson indicate that the sensitivity of the technique is  $5 \times 10^{-8}$  cts/sec-molecule/cc or about  $10^8$  molecules/cc of NO<sub>2</sub> at a S/N of 1. His results indicate a quantum yield smaller than 1% for all gamma-bands. This photoyield is smaller than that of  $\rm H_2O$  for  $\rm OH(A^2 \ \Sigma^+)$  and smaller than anticipated (Kley and Stone, 1978). Anderson is considering means to improve the sensitivity, and Kley (private communication, 1979) will also make laboratory measurements. These means are, to select a better photolyzation wavelength where either the cross section or quantum yield is larger or to utilize a more intense source according to 3-47 and 3-48. The present sensitivity is adequate to meet the HAPP requirements.

Several specificity issues remain to be studied, but are not expected to affect the  $\mathrm{NO}_2$  measurements. The photolyzing radiation will act on all stratospheric species and could produce interfering fluorescence or secondary fluorescence. The low quantum yields mean that secondary fluorescence (i.e.,  $\mathrm{NO}_2$  fluorescence from an  $\mathrm{NO}_2$  product of another dissociation) will be very

small. One does not expect interfering fluorescence from other product species. On the contrary, these product species may themselves be measured at the same time using other spectral channels. Complete identifications of their parents may, however, require use of several excitation wavelengths (Kley and Stone, 1978). Finally, the need to view as much fluorescence from excited NO as possible could cause acceptance of scattered sunlight.

The demonstration of this dissociation/fluorescence technique for  $NO_2$  would also lead to a more specific technique for NO. One would convert the NO to  $NO_2$  using titration with  $O_3$  as is done in the chemiluminescence technique for NO. Its drawback is that  $NO_2$  concentrations are usually larger than NO and so one would lack sensitivity for NO concentrations much lower than  $NO_2$  concentrations (e.g., during sunrise, sunset, and night).

The new technique for NO<sub>2</sub> promises both sensitive and specific measurements of NO<sub>2</sub> in a lighter and more compact module than the broadband dissociation module. If all these potentials are demonstrated, the dissociation/fluorescence technique should replace the broadband technique in the Hybrid Gas Conversion System. Flight demonstration may be carried out in 1979 by Anderson in his configuration of a fast-flow, parachute drop payload. This configuration is not essential to the technique, which is also applicable to the slow-flow sampling envisioned for the HAPP Stratospheric Measurement System. Slow-flow sampling and calibration techniques have been demonstrated for NO in the stratosphere (B.A. Ridley, et al., 1972).

### SECTION IV

## CONCLUSIONS AND RECOMMENDATIONS

This section is devoted to conclusions drawn from the experimental work as well as the analytical work undertaken during this program. A summary of this work is given in Section II.

Recommendations are also presented in the context that only hybrid chemical conversion techniques were reported upon. The validity of the hybrid technique for carrying out the scientific and engineering objectives of the HAPP Stratospheric Measurement System is paramount. The merits of only this system are considered in developing a recommended position. Where appropriate, further areas of investigation, again only for this type of system, are recommended.

### 4.1 CONCLUSIONS

Conclusions for the laboratory findings associated with molecular chemical conversion techniques are arranged in the same order as the evaluation of the technique appeared in Section III.

Measurement of stratospheric NO is basically carried out by gas phase titration with  $0_3$  immediately followed by the sensing of the chemiluminescence of the product molecule,  $NO_2^*$ . With laboratory instrumentation used in this study, a sensitivity of  $1.6 \times 10^{10}$  molecules/cm<sup>3</sup> could be routinely measured. With stratospheric instrumentation, a lowest detection limit of  $5 \times 10^7$  molecules/cm<sup>3</sup> has been verified (B.A. Ridley, et al., 1972).

Conversion of  $NO_2$  to NO and  $O(^3P)$  by the photolytic process is complex and may result in substantial changes of the relative concentrations of other species in the sample stream. These changes in turn can bias the readings. In addition, dissipated heat from the photolytic lamp could assist in the

premature thermal decomposition of  $N_2O_5$ , and certainly  $Clono_2$  and  $HO_2NO_2$ , the latter two species being particularly labile and believed to be present in the stratosphere. Further, as shown in the Feasibility Study Report, this method requires substantial amounts of electrical power derived from light weight primary cells or heavier secondary cells. Reduction of the premature decomposition of  $N_2O_5$ ,  $Clono_2$  and  $HO_2NO_2$  to negligible levels would require that the photolytic cell be packed in dry ice. A lowest detection limit of about 1 x  $10^8$  molecules/cm<sup>3</sup> is achievable but depends upon engineering trades relating electrical power and radiated flux.

Concerning the measurement of N<sub>2</sub>O<sub>5</sub> the conclusions may be grouped into categories of (1) generation and handling of  $N_2^{0}$  in known quantities and (2) conversion of N<sub>2</sub>O<sub>5</sub> into product molecules which can be quantitatively measured. Firstly, ppm quantities of N205 can be easily generated, the process followed by IR absorption techniques followed in turn by stoichiometric and rate limiting evaluations. Handling of  $N_2O_5$  is more difficult because water tends to combine, thus forming HNO3. This artifact of the generation and handling of  $N_2O_5$  can be routinely evaluated by monitoring the IR signature of  ${\rm HNO}_{\rm q}$ . Secondly, thermal conversion of  ${\rm N}_{\rm 2}{\rm O}_{\rm 5}$  is complete at temperatures in the 450-473 K range. Obtaining a measurable decomposition product quantitatively, however, is not straightforward. For example, computer analysis shows that at an altitude of 15 km, the net change of NO, exceeds the net change of  $N_2O_5$ ; while at a altitude of 25 km, the net change of  $NO_3$  is less than the net change of N205. Computer analysis and laboratory tests at higher temperatures, up to and including 800 K, indicate that the thermal conversion process becomes substantially more quantitative. At this point on the temperature scale, however, specificity to HNO, is lost, leading to the concept of NO, instrumentation.

Thermal conversion of HNO<sub>3</sub> is a non-catalytic process, but one that requires a surface. Surface materials employed during this program included Pyrex and stainless steel. Temperature ranges employed were 520-550 K for Pyrex and up to 673 K for stainless steel. Thermal decomposition of HNO<sub>3</sub> was found to be complete at the lower temperature range with the principal

product being NO $_2$ . A quantitative portion of the NO $_2$  is thermally converted to NO. Stoichiometry of the conversion to NO $_2$  prior to allowance for NO $_2$  thermal decomposition was found to be unity within experimental error. In summary, the conversion of HNO $_3$  to NO $_2$  and NO was found to be straightforward for concentrations as high as 1.7 x 10 $^{14}$  molecules/cm $^3$ .

Interferents impacting the specificity of thermal conversion instrumentation include  $\text{ClONO}_2$  and  $\text{HO}_2\text{NO}_2$  to the extent that they are present in the stratosphere. Conversion of  $\text{HO}_2\text{NO}_2$  will be present for temperatures  $\geq 300$  K. Conversion of  $\text{ClONO}_2$  will be present for temperatures  $\geq 350$  K.

Conversion of total odd-nitrogen, to measurable NO, without regard to specificity, can be carried out using the high temperature catalytic thermal technique. The stoichiometry of the various molecules,  $\mathrm{HNO_3}$ ,  $\mathrm{N_2O_5}$ ,  $\mathrm{C10NO_2}$ ,  $\mathrm{HO_2NO_2}$  and  $\mathrm{NO_2}$  is well understood. Passage of the sample through a converter operated at 500-800 K would decompose the heavier molecules, including  $\mathrm{NO_2}$ , at stratospheric pressures. The resulting product, NO, would then be measured by the GPT-chemiluminescence method. Measurement of only NO would be carried out in an identical, parallel path but without thermal conversion.

The narrow-band photolysis/fluorescence technique for NO<sub>2</sub> is being investigated by J. Anderson in the laboratory. His best result thus far indicates a sensitivity of about 10<sup>8</sup> molecules/cc, which meets the HAPP NO<sub>2</sub> specification. Specificity is not expected to be a problem. Conversion of NO to NO<sub>2</sub> by titration with ozone may allow the same technique to measure NO to the same precision. Anderson tentatively plans a demonstration flight during 1979 in his unique parachute package. The same technique is applicable to the slow-flow sampling envisioned for the HAPP Stratospheric Measurement System. In both cases, on-board calibration is advisable.

The GEARS/EPISODE computer code was found to be a valuable analytic modeling tool for developing laboratory apparatus as well as for developing design and performance parameters for instrumentation intended for stratospheric conditions. The modeling results for both laboratory conditions and those

for expected concentrations of the stratosphere indicate, with only minor differences, identical conversion trending. This permits valid extrapolation of the laboratory results. The code provides a rigorous analysis that will also benefit pre-launch and in-flight calibration tasks.

Sample fidelity, transport, radical chemistry and surface reactions which are not amenable to modeling must be given particular attention in the instrumentation design, use and interpretation of data.

#### 4.2 RECOMMENDATIONS

From the results of the Feasibility Study and the results of the laboratory performance studies reported here, Perkin-Elmer recommends the development of a flight prototype of the Hybrid Gas Conversion Measurement System. It is recommended that the flight prototype consist of a number of instrumentation modules that can be improved, changed, or added to achieve the scientific objectives of the High Altitude Pollution Program. Candidate modules are the total odd-nitrogen (including NO) module, the NO<sub>2</sub>/NO module, the O<sub>3</sub> module, and the N<sub>2</sub>O module. Measurements with these modules would meet all requirements on the Stratospheric Measurement System except the partitioning of the heavier odd-nitrogen species. Each of these modules is considered to be feasible from an engineering point of view. It may be possible to add a partitioning module at a later time, depending on the technology of stratospheric measurements. In no case, however, would a module be flown before testing in the laboratory under stratospheric conditions.

Perkin-Elmer recommends that the development of a flight prototype of the Total Odd-Nitrogen Instrumentation Module be initiated. Functional design would be based upon chemiluminescence detection for NO and high-temperature catalytic conversion for the HNO<sub>3</sub>, N<sub>2</sub>O<sub>5</sub>, NO<sub>2</sub>, and other odd-nitrogen species. As documented in this report, the measurement technique is demonstrated under laboratory conditions, no new technology is being advanced, and none of the module components are state-of-the-art. This development should be carried out jointly by the system contractor and a stratospheric chemistry laboratory group.

Perkin-Elmer further recommends that the development of a flight prototype  $\mathrm{NO}_2/\mathrm{NO}$  Instrumentation Module be initiated. This module is essential for obtaining the important measurements of  $\mathrm{NO}_2$ . Functional design would be based upon chemiluminescence detection of NO and the narrowband photolysis fluorescence technique for  $\mathrm{NO}_2$  if that technique is demonstrated in the stratosphere as expected. In this case, a balloon version of the latter technique would have to be developed. If the narrow-band photolysis techniques does not work as expected, the broad-band photolysis technique should be further optimized for  $\mathrm{NO}_2$  detection as indicated in this report.

Perkin-Elmer also recommends that two other Instrument Modules be considered as part of the flight prototype at this time. These modules are the flyable gas chromatograph for  $N_2O$  and the UV photometer for  $O_3$ . Both modules are in states of advanced development and testing. The flyable gas chromatograph is being developed by Valco Instruments and Baseline Instruments and is being tested by NOAA in Boulder. The flyable UV photometer is made by DASIBI Environmental Corporation and has been tested by NASA Johnson Space Center.

Perkin-Elmer finally recommends that provision be included in a flight prototype for one or two other instrumentation modules. The volume set aside could be utilized for batteries, permitting longer flights until additional candidate modules are developed.

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#### APPENDIX A

### INFRARED ABSORPTION MEASUREMENTS

## A.1 N2O5 AND HNO3 CONCENTRATION DETERMINATION

Prior to evaluating a particular analytical method for a species, as well as following the course of a reaction, IR band spectra were recorded to obtain the quantitative concentration of the species.

The analytical method (Lambert-Beer's Law) was employed using band model absorption cross sections. The method utilized either a Perkin-Elmer Model 521 or Model 580 spectrophotometer equipped with an ambient temperature Foxboro/Wilks 20-meter cell lined with PTFE. Because of the corrosive nature of HNO<sub>3</sub>, the KBr windows usually used were replaced with AgCl windows. In all cases, the sample and diluent carrier were allowed to flow freely through the cell. Measurements were carried out at ambient pressure, 747-755 torr and temperature, 296-298 K.

The number density, N, or partial pressure p of the species was calculated on the basis of the Lambert-Beer Law:

$$N = \frac{\ln\left(\frac{I_o}{\sigma I}\right)}{\sigma L} \quad \text{(molecules/cm}^3) \text{ and}$$

$$p = \frac{RT \ln\left(\frac{I_o}{I}\right)}{N_{Av}L} \quad \text{(torr)}$$

where:  $\ln \left(\frac{I_o}{I}\right)$  corresponds to the base e absorbance

 $\sigma$  = effective cross section in cm<sup>2</sup>/molecule

L = pathlength in cm

R = gas constant = 62366 torr-cm<sup>3</sup>/mole-K

T = temperature of the sample during measurement

 $N_{AV} = Avogardro's number = 6.023 \times 10^{23} molecules/mole$ 

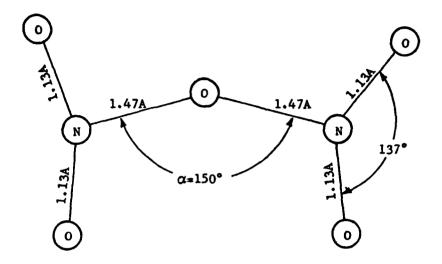
 $N_2O_5$  and  $HNO_3$  have similar molecular structures, as shown in Figure A-1 (Hisatune et al., 1962 and McGraw et al., 1965). Therefore, low resolution spectra may occur at the same frequencies. The  $v_1$  asymmetric N-O stretch,  $A_1$  symmetry, and  $v_{11}$  asymmetric N-O stretch,  $B_2$  symmetry, modes of  $N_2O_5$  are shown schematically. These modes are observed at a frequency of about 1728 cm<sup>-1</sup>. The  $v_2$  asymmetric N-O stretch mode (R-branch) of  $HNO_3$  is observed at about 1720 cm<sup>-1</sup>.

If both species are present, then the  $\nu_2$  band for  $\mathrm{HNO_3}$  cannot be used for quantitative measurements without other spectral information. In cases where two materials are present in a sample mixture, each absorbing at the same frequency or frequencies, the mixture can be analyzed for the concentration of each component by determining the absorbance for the mixture at two or more frequencies.

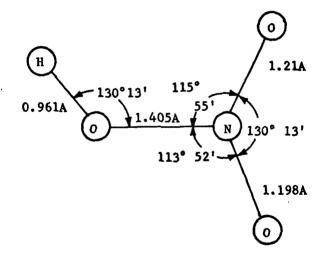
$$A_{e,v} = \sigma_{A,v} N_A L + \sigma_{B,v} N_B L$$

where  $A_{e,v}$  denotes absorbance to the base e at frequency v and the subscripts A,B denote  $N_2O_5$  and  $HNO_3$ . The cross section,  $\sigma$ , as obtained from the data of Nightingale et al., (1954); Goldman et al., (1971); Goldman et al., (1975); and Graham (1975) are tabulated in Table A-1.

With the synthesis and handling of  $N_2O_5$  the possibility exists for heterogeneous wall reactions if adsorbed water is present. The product of the reaction is  $\text{HNO}_3$  since  $\text{H}_2\text{O}_5$  is the anhydride of  $\text{HNO}_3$ .



0<sub>2</sub>N-0-NO<sub>2</sub>



H-0-NO2

Figure A-1. Molecular Structures for Nitrous Pentoxide and Nitric Acid

TABLE A-1. INFRARED ABSORPTION BAND CROSS SECTIONS FOR N<sub>2</sub>O<sub>5</sub> AND HNO<sub>3</sub> (cm<sup>2</sup>/molecule)

	Frequency (cm <sup>-1</sup> )					
	<u>1728</u> <u>1340</u> <u>1315</u> <u>1246</u>					
$A = N_2O_5$	2.4 x 10 <sup>-18</sup>	$0.15 \times 10^{18}$	0.02 x 10 <sup>18</sup>	1.75 x 10 <sup>-18</sup>		
B = HNO <sub>3</sub>	0.82	0.76	0.98	0.00		

From the general expression for absorbance and the data of Table A-1, one may derive the working expressions for number densities as:

$$N_{A} = \frac{A_{1728} - \frac{1.08A_{1340}}{2.28 \times 10^{-18}L} = \frac{\frac{1.19A_{1728} - A_{1315}}{2.85 \times 10^{-18}L} = \frac{\frac{A_{1246}}{1.75 \times 10^{-18}L}$$

$$N_{B} = \frac{A_{1728} - \frac{1.37A_{1246}}{0.82 \times 10^{-18}L} = \frac{\frac{A_{1340} - 0.086A_{1246}}{0.76 \times 10^{-18}L} = \frac{\frac{A_{1315} - 0.011A_{1246}}{0.98 \times 10^{-18}L}$$

## A.2 BAND MODEL CROSS SECTIONS

For reference purposes the band model cross sections for the various gases considered during the program are listed. This data was utilized when low resolution IR spectroscopy was employed as a laboratory analytical method for monitoring reactions and concentrations. The spectral resolution of the instrument is also provided. In all cases the data presented corresponds to room temperature data. Where possible, the most accepted data is employed. A summary chart of the medium strength and stronger bands is presented in Figure A-2.

## A.2.1 Nitric Oxide

The data presented for the  $v_1$  band was taken from laboratory measurements utilizing a Perkin-Elmer model 580 spectrometer set at resolutions of 2.8 and 1.0 cm<sup>-1</sup>. The 1.0 cm<sup>-1</sup> data corresponds to the envelope of the resolved lines of the P and R branches. The NO gas at 6 torr was pressure broadened by  $N_2$  with a total pressure of 760 torr. A path length of 8.25 meters was employed.

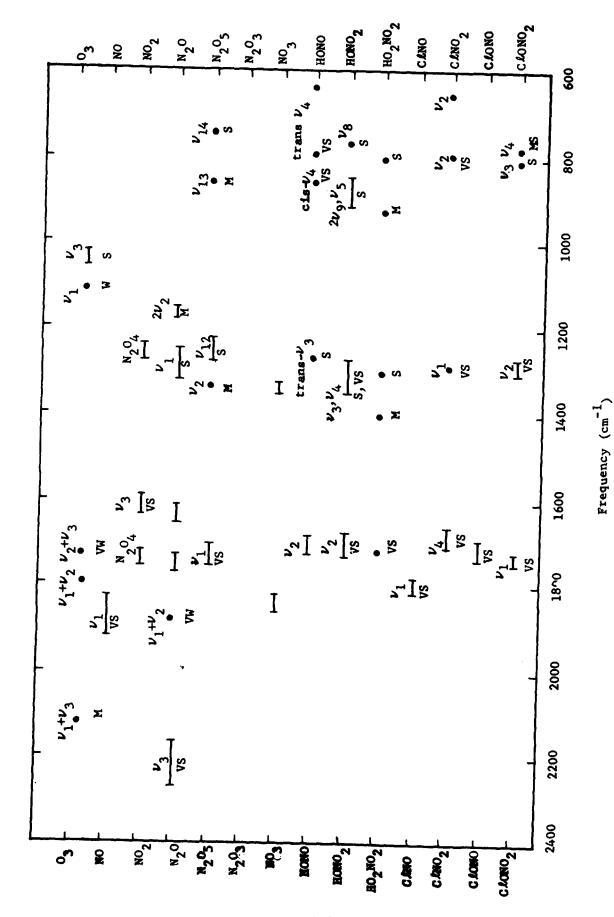


Figure A-2. Summary Chart of Medium Strength and Stronger Bands

y (cm <sup>-1</sup> )	$\sigma(\text{cm}^2/\text{molecule})$ $\Delta v = 2.8 \text{ cm}$	ν (cm <sup>-1</sup> )	$\sigma \left( \frac{\text{cm}^2/\text{molecule}}{\Delta v = 1.0 \text{ cm}} \right)$
1950	$1.30 \times 10^{-21}$	1950	$0.44 \times 10^{-21}$
1945	2.22	1945	0.94
1940	3.23	1940	1.55
1935	4.24	1935	2.23
1930	5.41	1930	3.06
1925	6.78	1930	4.17
1920	7.49	1920	4.91
1915	8.03	1915	6.17
1910	8.17	1910	6.95
1905	8.32	1905	7.29
1900	7.63	1900	7.13
1895	7.46	1895	6.28
1890	6.58	1890	5.25
1885	4.21	1885	3.81
1880	1.99	1880	0.04
1876(Q)	7.53	1876(Q)	10.18
1870	3.81	1870	0.49
1865	7.04	1865	5.44
1860	8.68	1860	6.61
1855	6.47	1855	6.72
1850	7.55	1850	6.01
1845	10.3	1845	6.01
1840	7.07	1840	4.49
1835	6.83	1835	4.04
1830	6.41	1830	3.97
1825	6.02	1825	4.22
1820	4.46	1820	2.60
1815	3.48	1815	2.12
1810	2.51	1810	1.60
1805	2.51	1805	1.96
1800	2.27	1800	1.44

## A.2.2 Nitrogen Dioxide

The data presented for the  $\nu_3$  band was taken from Goldman et al., (1975), and corresponds to a resolution of about 10 cm<sup>-1</sup>.

ν (cm <sup>-1</sup> )	$S^{\circ}/d (cm^{-1}-atm^{-1})$	$\sigma(\text{cm}^2/\text{molecule})$
1650	3.0	$0.128 \times 10^{-18}$
1645	7.7	0.330
1640	18.0	0.768
1635	25.0	1.066
1630	31.5	1.343
1625	27.0	1.151
1620	17.5	0.746
1615	15.4	0.659
1610	19.0	0.811
1605	23.0	0.981
1600	25.0	1.066
1595	23.0	0.984
1590	18.0	0.768
1585	12.3	0.533
1580	8.7	0.373
1575	5.7	0.245
1570	3.5	0.149

## A.2.3 Nitrogen Trioxide Radical

Nitrogen Trioxide is a free radical intermediate in the  $N_2O_5-O_3$  system and was also observed in room temperature decomposition of  $\text{ClONO}_2$ . The data presented for the 1360 cm<sup>-1</sup> band was extracted from Cramarossa and Johnston (1965), and corresponds to a resolution of about 3 cm<sup>-1</sup>.

$v (cm^{-1})$	σ (cm <sup>2</sup> /molecule)	
1410	$0.029 \times 10^{-18}$	
1400	0.038	
1390	0.054	

v (cm <sup>-1</sup> )	$\sigma$ (cm <sup>2</sup> /molecule)
1380	0.072
1370	0.098
1360	0.150
1350	0.088
1340	0.060
1330	0.040
1320	0.022
1310	0.016

## A.2.4 Nitrous Pentoxide

The data presented for the  $v_1$  band was extracted from Nightingale et al., (1954) and the  $v_2$  cross-section data given below. The data presented for the  $v_2$  and  $v_{12}$  bands was extracted from Graham (1975) and corresponds to a resolution of 5.10 cm<sup>-1</sup>.

$v (cm^{-1})$	σ (cm <sup>2</sup> /molecule)	ν (cm <sup>-1</sup> ) σ	(cm <sup>2</sup> /molecule)	$v (cm^{-1}) \sigma$	(cm <sup>2</sup> /molecule)
1780	$0.338 \times 10^{-18}$	1370	$0.065 \times 10^{-18}$	1260	$0.50 \times 10^{-18}$
1770	0.595	1365	0.080	1255	1.30
1760	0.910	1360	0.097	1250	1.52
1750	1.295	1355	0.113	1245	1.73
1740	1.824	1350	0.127	1240	1.58
1730	2.380	1345	0.142	1235	1.01
1720	2.169	1340	0.149	1230	0.24
1710	1.546	1335	0.135		
1700	1.082	1330	0.111		
1690	0.732	1325	0.089	1252	1.55
1680	0.393	1320	0.068	1246	1.75

## A.2.6 Chlorine Nitrate

The data presented for the  $\nu_1$  and  $\nu_2$  bands was taken from Graham et al., (1977), and corresponds to a resolution of about 0.0625 cm<sup>-1</sup>. The cross-section values are independent of resolution and pressure.

$v (cm^{-1})$	σ (cm <sup>2</sup> /molecule)	$v (cm^{-1})$	σ (cm <sup>2</sup> /molecule)
1760	$0.186 \times 10^{-18}$	1310	$0.186 \times 10^{-18}$
1755	0.335	1305	0.595
1750	0.744	1300	1.116
1745	1.339	1295	0.476
1740	0.893	1290	0.707
1735	1.041	1285	0.986
1730	1.320	1280	0.558
1725	1.004	1275	0.186
1720	0.707	1270	0.074
1715	0.446		
1710	0.242		
1731(P)	1.361	1286(P)	1.004
1738(Q)	1.153	1292(Q)	1.897
1744(R)	1.413	1300(R)	1.116

## A.2.7 Ozone

The data presented for the  $\nu_3$  band was extracted from Pitts et al., (1976) and corresponds to a resolution of about 1.3 cm $^{-1}$ .

ν (cm <sup>-1</sup> )	$\sigma (cm^2/molecule)$	
1065	$0.0614 \times 10^{-18}$	
1060	0.1235	
1055	0.1717	

A.2.5 Nitric Acid

The data presented for the  $\nu_2$  and  $\nu_3$  bands was taken from Goldman et al., (1971), and corresponds to a resolution of  $\sim 0.5~{\rm cm}^{-1}$ .

v (cm <sup>-1</sup> )	S°/d (cm <sup>-1</sup> -atm <sup>-1</sup> )	σ (cm <sup>2</sup> /molecule)
1735	9.420	$0.4017 \times 10^{-18}$
1730	17.68	0.7539
1725	24.79	1.057
1720	25.84	1.102
1715	26.99	1.151
1710	21.09	0.899
1705	23.22	0.990
1700	23.58	1.005
1695	23.31	0.994
1690	19.83	0.845
1685	14.12	0.602
1680	8.803	0.375
1350	8.716	0.3717
1345	14.87	0.6340
1340	17.87	0.7620
1335	16.42	0.7001
1330	16.82	0.7172
1325	21.32	0.9091
1320	21.68	0.9244
1315	23.09	0.9845
1310	21.51	0.9172
1305	18.00	0.7675
1300	13.74	0.5859
1395	10.51	0.4481
1290	8.759	0.3735

ν (cm <sup>-1</sup> )	σ (cm <sup>2</sup> /molecule)
1050	0.1376
1045	0.0530
1040	0.0793
1035	0.1200
1030	0.1306
1025	0.1323
1020	0.1253
1015	0.0956
1010	0.0819
1005	0.0716
1000	0.0530

### APPENDIX B

# COMPUTER SIMULATION OF NO THERMAL CONVERSION IN THE STRATOSPHERE

The computer code was developed to evaluate the performance of ideal thermal converters operating on stratospheric gas samples. The intent was to follow the temporal evolution of the sample to determine the decomposition paths and the significance of the final product abundances. The model included most of the major odd-nitrogen compounds and other important stratospheric constituents. The constituent set was extended until it included chlorine nitrate and chlorine oxide. At that point, the set was fixed because further expansion would have involved the entire family of chlorine compounds and their associated reactions. Such an expansion would have been beyond the scope of this study. Table B-1 contains a list of the molecules considered and the abundances used as the initial conditions for the computer code. In all, nineteen constituents were used together with forty reactions among them. Reactions with unknown products were ignored. Also, an NO<sub>2</sub> photolysis reaction was included but not used for this computation.

The evolution of the abundances was determined using the EPISODE version of the GEARS code. EPISODE is a computer algorithm for the solution of ordinary differential equations. Reaction rates were taken from the literature (principally the review by Hampson and Garvin, 1978). When both forward and backward rates were known, they were used directly. Otherwise, the equilibrium constant was evaluated and used to determine the "missing" rate (cf; Section 3.1).

The output format begins with a listing of the reactions and their evaluated rates at the initial conditions of temperature and pressure. The third body or "M" dependence is included in the reaction rates both as a computational convenience and as an aid to highlighting the significant rates. The temporal evolution of each constituent then follows.

TABLE B-1. MOLECULAR NUMBER DENSITIES USED FOR SAMPLE MODELING WITHIN INSTRUMENTATION

251 2.6(2.0) 40	6.0 x 10 <sup>11</sup> 7.0 x 10 <sup>8</sup> 7.0 x 10 <sup>8</sup> 3.5 x 10 <sup>6</sup> 1.0 x 10 <sup>6</sup> 1.0 x 10 <sup>7</sup> 4.0 x 10 <sup>7</sup> 6.0 x 10 <sup>5</sup>	
237 6(4.6) 35	1.3 x 10 <sup>12</sup> 5.5 x 10 <sup>8</sup> 2.2 x 10 <sup>9</sup> 5.5 x 10 <sup>7</sup> 4.9 x 10 <sup>7</sup> 4.0 x 10 <sup>7</sup> 1.7 x 10 <sup>7</sup> 2.0 x 10 <sup>6</sup> 5.0 x 10 <sup>6</sup> 5.3 x 10 <sup>11</sup> 1.0 x 10 <sup>6</sup>	5.0 x 10 <sup>7</sup>
227 12(9.1) 30	2.5 × 10 <sup>12</sup> 4.5 × 10 <sup>8</sup> 4.2 × 10 <sup>8</sup> 4.0 × 10 <sup>8</sup> 2.0 × 10 <sup>8</sup> 1.5 × 10 <sup>9</sup> 2.5 × 10 <sup>7</sup> 3.0 × 10 <sup>6</sup> 3.0 × 10 <sup>6</sup> 1.2 × 10 <sup>12</sup> 1.2 × 10 <sup>12</sup> 1.0 × 10 <sup>6</sup>	4.5 x 10 <sup>7</sup>
222 25(19) 25	4.2 x 10 <sup>12</sup> 7.0 x 10 <sup>8</sup> 6.5 x 10 <sup>9</sup> 7.0 x 10 <sup>8</sup> 2.0 x 10 <sup>9</sup> 4.0 x 10 <sup>8</sup> 3.5 x 10 <sup>9</sup> 2.3 x 10 <sup>7</sup> 1.7 x 10 <sup>17</sup> 1.5 x 10 <sup>6</sup> 1.0	5.7 x 10 <sup>7</sup>
217 55(42) 20	4.5 x 10 <sup>12</sup> 1.5 x 10 <sup>9</sup> 8.0 x 10 <sup>9</sup> 4.0 x 10 <sup>9</sup> 4.0 x 10 <sup>9</sup> 1.0 x 10 <sup>9</sup> 2.0 x 10 <sup>7</sup> 5.0 x 10 <sup>7</sup> 5.0 x 10 <sup>7</sup> 1.0 x 10 <sup>6</sup>	3.5 x 10 <sup>7</sup>
217 120 mb(91) 15	2.5 x 10 <sup>12</sup> 5.0 x 10 <sup>9</sup> 4.5 x 10 <sup>9</sup> 1.0 x 10 <sup>7</sup> 1.5 x 10 <sup>9</sup> 5.0 x 10 <sup>7</sup> 2.0 x 10 <sup>6</sup> 2.0 x 10 <sup>6</sup> 2.0 x 10 <sup>6</sup> 7.3 x 10 <sup>12</sup> 1.0 x 10 <sup>6</sup> 8.5 x 10 <sup>8</sup> 8.5 x 10 <sup>8</sup> 8.5 x 10 <sup>8</sup> 8.5 x 10 <sup>8</sup> 8.5 x 10 <sup>6</sup> 1.0 x 10 <sup>6</sup> 8.5 x 10 <sup>6</sup> 8.5 x 10 <sup>6</sup> 8.5 x 10 <sup>6</sup>	$2.0 \times 10^7 (est)$
T(K) Pmb(Torr) H(km)		
MOLECULE	03 NO NO <sub>2</sub> NO <sub>2</sub> HNO <sub>3</sub> C10NO <sub>2</sub> HO <sub>2</sub> NO <sub>3</sub> O <sub>2</sub> HO HO H <sub>2</sub> O <sub>3</sub> H <sub>2</sub> H <sub>2</sub> H <sub>2</sub> H <sub>2</sub> H <sub>2</sub> H <sub>3</sub> H <sub>4</sub> H <sub>2</sub> H <sub>4</sub> H <sub>2</sub> H <sub>4</sub> H <sub>4</sub>	

T=250 K, H=15 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> N02 +N03 + M	1.940-05	6.070-13
5	2*N03 >>> 2*N02 + 02	4.710-17	7.469-62
3	SO + 00 + 20M - < E0M + 20M	4.210-15	1.190-34
4	NO3 + NO >>> 2*NO2	1.900-11	3.290-32
5	NO + 03 >>> NO2 + 02	6.360-15	1.080-56
6	NO2 + 03 >>> NO3 + O2	6.650-18	8.330-39
7	HN03 + M >>> H0 + N02 + M	2.58D-27	1.180-11
A	HN03 + H0 >>> H20 + N03	8.000-14	2.800-29
9	M + SO << M + O + O	1.290-14	3.310-56
10	0 + 02 + M >>> 03 + M	2.770-15	7.76D-12
11	0 + 03 >>> 2*02	1.920-15	0.0
js	0 + NO + M >>> NO2 + M	5.440-13	4.030-47
13	0 + NO2 >>> NO + O2	5.120-12	6.270-53
14	0 + N02 + M >>> N03 + M	3.390-13	2.720-23
15	HO + HO >>> H2O + O	1.090-12	9.77D-27
16	05 + 5400 >>> 5405	2.750-38	3.880-35
17	NO2 + H-NU >>> NO + 0	0.0	0.0
18	0 + H0 >>> H + O2	4.200-11	7.730-25
19	0 + H05 >>> H0 + 05	1.080-11	5.45D-6n
20	02 + H + M >>> H02 + M	1.340-13	1.710-30
<b>2</b> 1	03 + H >>> HO + 02	1.270-11	0.0
55	03 + HO >>> HO2 + O2	2.750-14	1.040-48
<b>2</b> 3	03 + HO2 >>> HO + 2*02	4.450-16	2.41D-6R
24	H + H0 + M >>> H20 + M	2.720-12	0.0
25	H + H05 >>> 54H0	9.400-12	1.620-46
26	H + H05 >>> H5 + 05	1.040-11	2.550-61
27	H + H20 >>> H2 + H0	2.340-28	1.140-15
28	H + H202 >>> H2 + H02	8.360-15	5.620-29
29	H + H505 >>> H0 + H50	1.090-14	1.350-75

30	S#H0 + M >>> H202 + M	1.550-12	4.170-31
31	HO + HOS >>> HSO + OS	1.120-11	3.890-74
32	5+H05 >>> H505 + 05	2.300-12	8.580-49
33	HO2 + H20 >>> H202 + H0	1.020-39	5.490-13
34	NQ + H + M >>> HNO + M	8.450-14	1.320-32
35	NO + HO >>> NO2 + H	3.05n=3d	3.010-11
36	NO + HO + M >>> HNO2 + M	1.110-11	4.210-28
37	NO + HO2 >>> NO2 + HO	1.650-13	7.470-21
38	H + H + M >>> H2 + M	3.390-15	0.0
39	HN04 + M >>> H02 + N02 + M	3.640-05	6.730-13
40	CLN03 + M >>> CL0 + N02 + M	1.570-06	6.110-13

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•	74.20-0	-01110		0 0750	0 0000				00000
. «	7320-0	-0925.		9 0	5000		4780 0		0450 0
•	.7230-0	-3590-	0 0000	6540 0	5000 0	0 0000	4840	0 0000	0 0940
~	.7140-0	-1980-	0 0000	6540 0	.5000 0	0 0000	490	0 0000	.0480
•	.7050-0	-0630-	0 0000	250 0	.5000 0	0 0000	0 0965	0 0000	0 0650
9	0-0169.	-893D-	0000	0 0559	2000	0 00	.501	0 0000	0 0050
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•	.6530-0	-0876	0000	28	.5000	•	.5360 0	0 0000	.0590

T=300 K, H=15 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> N02 +N03 + M	1.570-02	2.850-13
5	20 + 20Nos - 02	2.410-16	1.750-54
3	NO2 + NO3 >>> NO2 + NO + O2	8.210-15	4.920-35
4	NO3 + NO >>> 2*NO2	1.900-11	6.980-29
5	NO + 03 >>> NO2 + 02	1.670-14	2.850-49
6	NO2 + 03 >>> NO3 + 02	3.410-17	2.00D-34
7	HN03 + M >>> HO + NO2 + M	1.920-20	6.24D-12
9	HN03 + H0 >>> H20 + N03	8.00D-14	1.250-26
9	0 + 0 + M >>> 02 + M	5.910-15	1.26D-56
10	0 + 02 + M >>> 03 + M	1.640-15	1.320-08
11	0 + 03 >>> 2*02	8.900-15	0.0
12	0 + N0 + M >>> N02 + M	3.070-13	1.200-37
13	0 + NO2 >>> NO + O2	6.250-12	3,730-46
14	0 + N02 + M >>> N03 + M	2.830-13	2.260-23
15	HO + HO >>> H2O + O	1.570-12	4.630-24
16	02 + 2+N0 >>> 2*N02	1.930-38	2.260-31
17	NO2 + H-NU >>> NO + 0	0.0	0.0
18	0 + H0 >>> H + O2	4.200-11	2.160-22
19	0 + H05 >>> H0 + 05	1.510-11	8.510-52
20	02 + H + M >>> H02 + M	7.980-14	6.510-24
21	03 + H >>> H0 + 02	1.790-11	1.620-69
22	03 + HO >>> HOZ + OZ	5.350-14	8.980-43
23	03 + H02 >>> H0 + 2402	1.040-15	1.530-63
24	H + HO + M >>> H2O + M	1.410-12	1.14D-74
25	H + HOS >>> Z#HO	1.770-11	1.140-40
26	H + H02 >>> H2 + 02	1.310-11	6.80D-53
27	H + H20 >>> H2 + H0	2.1AD-25	6.41D-15
28	H + H202 >>> H2 + H02	2.130-14	2.960-26
29	H + H202 >>> H0 + H20	2.760-14	2.950-65

30	2*H0 + M >>> H202 + M	7.100-13	5.180-24
31	HO + HO2 >>> H2O + OZ	1.570-11	1.980-63
32	24H05 >>> H2US + 05	3.210-12	1.980-42
33	HOS + HSO >>> HSOS + HO	6.110-35	8.570-17
34	NO + H + M >>> HNO + M	5.770-14	1.480-25
35	NO + HO >>> NO2 + H	7.190-34	4.920-11
36	NO + HO + M >>> HNO2 + M	4.420-12	2.480-21
37	NO + HO2 >>> NO2 + HO	3.660-13	3.740-19
38	H + H + M >>> H2 + M	2.930-15	2.43D-6A
39	HN04 + M >>> H02 + N02 + M	2.520-02	3.020-13
40	CLN03 + M >>> CLO + NO2 + M	2.280-03	3.07D-13

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DENCE TIME	20N	5000 0	552D 0	.603D 0	.6540 0	.7040 0	.7540 0	0 (1408	0 0206	.9510 0	0 0666.	.0470	.0940	0 0141.	0 0962	.2800 0	.3260 0	.3710 0	.416D 0	0.0508	5490	.5930 0	•636D 0	6790 0	7640	.8060 0	.8470 0	0 0688	0 0056	.0110	.0510 0	0 0060.	1690 0	.2080 0	0. 09%2*	6.2840 09	3600 0	3970	.4340 0	.4710 0	5080 0	0 0445	0000
HAPP RESI	N205	0 0000	0 0696	.9370 0	0 0906.	.8750 0	.844D 0	0 0418.	0 0557	.7220	.692n o	.6620 0	.632n 0	.6020 0	0.0543.	.5130 0	.484D 0	•4550 0	• 476D 0	3680	3390 0	.3110 0	.282D 0	.254D 0	0 0522.	1690 0	.1420 0	1140 0	0.0860	.0310 0	.0040	0 0776	9230 0	.8960	.8700 0	6.8431) 06	7400 0	7640 0	.7380 0	.7120 0	0 0989	6610 0	0.000
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T=700 K, H=15 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + M	2.31D 06	2.370-14
S	2*N03 >>> 2*N02 + 02	2.570-14	7.440-49
3	NOS + NOS >>> NOS + NO + OS	5.510-14	3.970-36
4	NO3 + NO >>> 2*NO2	1.900-11	2.230-19
5	NO + 03 >>> NO2 + 02	2.650-13	4.540-ZR
6	NOS + 03 >>> NO3 + 02	3.620-15	6.560-22
7	HN03 + M >>> H0 + N02 + M	1.92D-01	3.210-13
В	HN03 + H0 >>> H20 + N03	8.000-14	4.740-19
9	0 + 0 + M >>> 02 + M	4.56D-16.	1.430-19
10	0 + 02 + M >>> 03 + M	2.66D-16	1.610 01
11	0 + 03 >>> 2*02	7-110-13	8.630-43
15	0 + NO + M >>> NO2 + M	4.330-14	1.030-10
13	0 + NOS >>> NO + OS	1.110-11	8.500-27
14	0 + NO2 + M >>> NO3 + M	1.210-13	9.700-24
15	HO + HO >>> H2O + O	4.530-12	2.040-16
16	02 + 2*N0 >>> 2*N02	7.040-39	9.370-21
17	NO2 + H-NU >>> NO + 0	0.0	0.0
18	0 + H0 >>> H + 02	4.200-11	2.110-15
19	0 + H02 >>> H0 + 02	3.910-11	2.190-29
20	02 + H + M >>> H02 + M	1.320-14	2.960-05
21	03 + H >>> H0 + 02	4.780-11	5.620-37
55	03 + H0 >>> H02 + 02	3.590-13	8.310-26
23	03 + H02 >>> H0 + 2+02	1-180-14	1.120-49
24	H + H0 + M >>> H20 + M	6.58D-14	1.610-26
25	'H + H02 >>> 2#H0	1.080-10	5.870-24
26	H + H02 >>> H2 + 02	2.550-11	8.030-29
27	H + HSO >>> HS + HO	6.56D-17	8.900-13
28	H + H505 >>> H5 + H05	3.060-13	1.770-18
29	H + H202 >>> H0 + H20	3.98D-13	1.020-35

30	2+H0 + H >>> H202 + H	5.480-14	5.020-04
31	HO + HO2 >>> H2O + O2	4.06D-11	7.730-33
32	S+H05 >>> H505 + 05	P+32D-12	3.020-24
<b>33</b> <	HO2 + H20 >>> H202 + H0	2.720-21	3.070-12
34	NO + H + M >>> HNO + M	1-40D-14	1.050-05
35	NO + HO >>> NO2 + H	2.230-21	2.020-10
36	NO + HO + M >>> HNO2 + M	2.28D-13	2.840-02
37	NO + HOZ >>> NOZ + HO	3.600-12	2.68D-14
38	H + H + M >>> H2 + M	1.210-15	1.010-24
39	HN04 + M >>> H02 + N02 + M	2.49D 06	2.330-14
40	CLN03 + M >>> CLO + NO2 + M	1.80D 06	1.140-14

	HAPP RESID	SIDENCE TIME	STUDY							
TIME (S)	N205	40N	NO3	0N		63	<b>~</b> 0	~	9	2021
0.0	.0000	.5000 0	2.000n 0	5.00	0	.5000 1	.2000 1	.5000 0	0 00000	.3000
~	.246P-0	.185n o	4.2140 0	Ġ	C	.2260 1	.2000 1	0 0444.	.0120 0	.3000
*	.9720-0	.350D 0	6.6480 0	7.26	c	.1280 1	.2000 1	.3890 0	.1400 0	.300D 1
Ö	.388n-0	. A53D 0	8.558D 0	7.79	0	.0350	.2000 1	.3370 0	2020 0	.300D 1
8	0-0569*	.552D 0	1.0120 0	8.12	0	.9570 1	.2000 1	2870 0	•254D 0	3000
•	9510-0	.369D 0	1.1440 0	8° 34	0	. 8810 1	. 2005.	0 0623	3020 0	3000
Ň	-0212°	0 0952.	0 0852.1	200	- 0	1 0018	1 0002	0 0261	0 0000	1 0005
•	0-0564. 6-0564	0 0/91.	1.3590 0	0 0 0 0	> 0	1 0547	70007	1050	0 0000	ממטני
9.1	4.9070-03	3.1220.09	1.5290	8 8.7290	6	1.6260 12	8-2000 17	1.0630 09	1.4580 09	7.3000 12
9	1180-0	1080	1.6020 0	8.77	0	5720 1	2000	023D 0	0 U684°	3000
?	.318n-0	1030 0	1.6680 0	8.81	0	220 1	.2000 1	8490 0	5170 0	8
*	.5050-0	.101D 0	1.7270 0	8.8	C	.4740 1	.200D 1	.480D 0	.5430 0	93
•	<b>.6800-0</b>	.103D 0	1.7810 0	8.87	0	4590 1	.200D 1	1250 0	2660 0	٠ و
₩.	.8420-0	•107D 0	1.8290 0	8.89	0	3870 1	. 2000	.7840 0	5870 0	9
•	.9920-0	1130 0	1.8730 0	8.91	0	.3470 J	2000	4550 0	•6050 0	9
٠,	.130D-0	1190 0	1.9120	E 0.0	0	1 0605	1 0002	0 0661.	0 0229	֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֡֓֓֓֡֓֓֓֓֓֡֓֓֡֓֡
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8	.8560-0	1750 0	2.1010 0	•	0	.0650	.2000	00200	6950 0	5
•	9070-0	.1820 0	2.1120 0	9.08	0	.0410 1	.2000 1	.7820 0	6980 0	.30
Š	.950n-o	.1880 0	2.1210 0	9.10	0	.017D 1	.2000 1	.5670 0	7000 0	.30
•	.986n-0	.194D 0	2.1280 0	9.11	0	.9460 1	.2000 1	3600 0	7020 0	39
•	·0150-0	.201D 0	2.133n 0	9.12	0	. 7290 1	.2000 1	.1610 0	.7020 0	9
æ	.0380-0	.2060 0	2.136D 0	9.13	C	. 5220	2000 1	0 0026	7010 0	90
•	0560-0	.2120 0	2.1370 0	9.15	0	3220 1	2000	7860 0	. 700D 0	96.
٠,	0-0/90	.218D 0	2.1370 0	9.16	0 (	1300	2000	0 0809	0 0869.	פרי
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9	7.0650-03	2380 0	2-1230 0	02.0		4300	1 0002	9640	6850 0	1 0000
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*	.0390-0	.2480 0	2.1090 0	9.22	C	1170 1	.2000 1	.6770	.6750 0	.3000
٥	.0200-0	.2520 0	2.1000 0	9.23	C	.9680 1	.2000	.541D 0	0 0699	.300D 1
6	.998n-0	.2570 0	2.0910 0	9.54	0	8240 1	.2000 1	.4110 0	.6630 0	3000
0	9730-0	.261D 0	2.0810 0	9.25	C	6850 1	2000 1	.286D 0	570 0	3000
٩	9450-0	.2650 0	2.070D 0	9.56	0	5510 1	2000	1650 0	6510 0	3000
•	9140-0	.2690 0	2.058n 0	9.26	0	421D 1	2000	0 0690	0 0449	3000
ġ.	8810-0	2720 0	2.0460 0	9.27	0	2950 1	2000	9370 0	637D 0	1 0000
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					•			0.010	2000	

T= 800 K, H=15 km

R-NUH	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + M	1.270 07	1.780-14
2	2*N03 >>> 2*N02 + 02	3.9AD-14	5.950~48
3	NO2 + NO3 >>> NO2 + NO + O2	6.59D-14	3.130-36
4	NO3 + NO >>> 2*NO2	1.900-11	1.740-18
5	NO + 03 >>> NO2 + 02	3.430-13	4.42D-26
6	NO2 + 03 >>> NO3 + 02	5.610-15	9.780-21
7	M + SON + OH	9.110 00	2.010-13
8	HN03 + H0 >>> H20 + N03	8.00D-14	2.430-18
9	0 + 0 + M >>> 02 + M	3.400-16	4.320-15
10	0 + 02 + M >>> 03 + M	2.130-16	1.08D 02
11	0 + 03 >>> 2*02	1.070-12	6.110-39
12	0 + NO + M >>> NO2 + M	3.410-14	3.250-0A
13	0 + NO2 >>> NO + O2	1.170-11	5.550-25
14	0 + NO2 + M >>> NO3 + M	1.060-13	8.480-24
15	HO + HO >>> H2O + O	5.000-12	1.06D-15
16	05 + 5+N0 >>> 5+N05	6.400-39	8.780-20
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	0 + H0 >>> H + O2	4.200-11	9.550-15
19	0 + HO2 >>> HO + O2	4.280-11	3.430-24
20	02 + H + M >>> H02 + M	1.060-14	1.580-03
21	03 + H >>> H0 + 02	5.250-11	6.310-34
<b>22</b>	03 + H0 >>> H02 + 02-	4.30D-13	3.240-24
23	03 + H02 >>> H0 + 2*02	1.480-14	2.350-4A
24	H + HO + M >>> H2O + M	4.130-14	4.090-22
25	H + HOS >>> S+HO	1.280-10	2.160-22
26	H + H02 >>> H2 + 02	2.710-11	1.450-26
27	H + H2O >>> H2 + HO	4.09D-16	1.410-12
28	H + H202 >>> H2 + H02	3.930-13	9.470-18
29	H + H205 >>> H0 + H20	5.110-13	6.020-33

30	2+H0 + M >>> H202 + M	4.08D-14	3.370-02
31	HO + HO2 >>> H2O + O2	4.44D-11	5.700-30
32	2*H02 >>> H202 + 02	9.100-12	1.530-22
33	HOS + HSO >>> HSOS + HO	5.190-20	3.460-12
34	NO + H + M >>> HNO + M	1.160-14	6.88D-04
35	NO + HO >>> NO2 + H	3.300-20	2.300-10
36	NO + HO + M >>> HNO2 + M	1.64D-13	1.560.00
37	NO + HO2 >>> NO2 + HO	4.46D-12	7.660-14
38	H + H + M >>> H2 + M	1.060-15	1.120-20
39	HN04 + M >>> H02 + N02 + M	1.330 07	1.750-14
40	CLN03 + M >>> CLO + NO2 + M	1.160 07	6.670-15

8 1.2280 10 4.4650 11 8.2000 17 1.18 8 1.2280 10 4.0460 11 8.2000 17 1.20 8 1.2270 10 3.6890 11 8.2000 17 1.22 7 1.2260 10 3.3820 11 8.2000 17 1.23	08 1.0270 08 1.2280 10 4.4650 11 8.2000 17 1 1 08 1.0190 08 1.2280 10 4.0460 11 8.2000 17 1 1 08 1.0190 08 1.2270 10 3.6890 11 8.2000 17 1 1 08 9.9530 07 1.2260 10 3.1850 11 8.2000 17 1 08 9.8040 07 1.2260 10 3.1160 11 8.2000 17 1 08 9.4640 07 1.2250 10 2.4980 11 8.2000 17 1 08 9.2830 07 1.2240 10 2.4980 11 8.2000 17 1 08 9.0930 07 1.2240 10 2.3360 11 8.2000 17 1 1
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	08 8.8990 07 1.2240 108 8.3020 07 1.2230 108 8.3020 07 1.2230 108 7.9020 07 1.2220 108 7.7040 07 1.2220 108 7.5090 07 1.2220 108 6.3250 07 1.2220 108 6.3250 07 1.2210 108 6.3250 07 1.2210 108 6.3250 07 1.2200 108 6.3200 07 1.2200 108 6.3250 07 1.2200 108 6.3250 07 1.2200 108 6.3250 07 1.2200 108 6.3250 07 1.2200 108 6.3250 07 1.2200 108 6.3250 109 109 109 109 109 109 109 109 109 10
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*	2	=	.225	90	_	.6250 0	8.4800 0	1.0000 0	5.2780 06	.1460-0	.672D-0
۰,	.22	:	.157	90	2830 0	.1150 0	8.5440 0	1.0000 0	.8270 0	.9520-0	.9040-0
₽,	4.	1	• 164	90	4280 0	.461D 0	8.6480 0	1.0000 0	.5150 0	0-0990	.7140-0
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*	6	=	.872	90	.3850 0	9770	1.0030 0	1.0000	.8340 0	-0669.	.8450-0
·°.	7.		.543	90	.4610 0	.926n o	1.0200	1.0000	.8930 0	·679D-0	.8710-0
₽,	• 66	Ξ	.249	90	.5300 0	.867D 0	1.036D 0	1.0000	.902D 0	.6560-0	.8970-0
٠.	.55	11	•984	90	.5910 0	.8030 0	1.0500 0	1.0000	.8700 0	.6270-0	.9220-0
~	4	=	747	90	49.	.7360 0	1.0640 0	1.0000	.805D	.5920-0	9460
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•		2 6	427	9	0450	0.001	1.1450 0	9.9950	5870	1900-0	1300-0
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1 4	֓֞֜֜֜֜֜֜֜֜֝֓֜֓֓֓֓֜֜֜֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓֓	2 0	100	9	9810	00200	1.1540 0	0 0E66*6	2860	1000-0	164D-0
	76	-	184	90	0 0966	9440	1.1580 0	0.9920	1390	0-0990-0	1810-0
. 6		0	117	90	0 0000	6880	1.1510 0	9,9910 0	0966	0130-0	
•	. 15	0.0	.054	90	0230 0	.834D 0	1.1640 0	0 0066.6	.8560	.971D-0	.212D-0
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4	.61	10	434	92	0450 0	.730D 0	1.1680 0	9.9880 0	.5870	.8890-0	.2430-0
۰	.37	10	.941	92	.054n 0	.6810 0	1.1690 0	9.9870 0	.458D	.850 <b>n-</b> 0	.2570-0
æ	₹.	10	• 485	05	.0620 0	.6340 0	1.1700 0	9.9860	3330	.8120-0	.2710
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9	58		552	S	0 0601	2700 0	1.1620 0	9,9750 0	3740	5080-0	3850-0
	4		.321	0.5	1120 0	.2360 0	1.1590 0	9.9740 0	.2830	4790-0	39
0	.32		.103	92	.114n o	.2030 0	1.1570 0	9.9730 0	1960	.4500-0	.408D-0
۶.	•20		.898	92	.1170 0	.170D 0	1.1540 0	9.9710 0	.1110 0	.4220-0	-4190-
*	8		9	S	= =	1390 0	1.1520 0	0 0026.6	0 0620	3940-0	-430D-
٠,	.97		523	S.	1200 0	1080 0	1.1490 0	0 0696.6	0 0056	3670-0	-0144
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•			9	v	.1230 0	0200	1.1420 0	0 0996.6	. 1980	3160-0	•

T= 250 K, H= 20 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> N02 +N03 + M	8.900-06	2.780-13
2	200 + 20N9\$	4.710-17	7.460-62
3	SO + 00 + SON << 50N + 80N	4.210-15	1.190-34
•	NO3 + NO >>> 2*NO2	1.900-11	3.290-32
5	NO + 03 >>> NO2 + 02	6.360-15	1.080-56
6	NO2 + 03 >>> NO3 + O2	6,650-18	8.330-39
7	HN03 + M >>> H0 + N02 + M	1.180-27	5.410-12
A	HN03 + H0 >>> H20 + N03	8.00D-14	2.800-29
9	0 + 0 + M >>> 02 + M	5.920-15	6.950-57
10	0 + 02 + M >>> 03 + M	1.270-15	3.550-12
11	0 + 03 >>> 2*02	1.920-15	0.0
12	0 + N0 + M >>> N02 + M	2.490-13	1.850-47
13	0 + NOS >>> NO + OS	5.120-12	6.270-53
14	0 + NO2 + M >>> NO3 + M	1.560-13	1.240-23
15	HO + HO >>> H2O + O	1.090-12	9.770-27
16	05 + 5*40 >>> 5*405	2.750-38	3.880-35
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	0 + H0 >>> H + O2	4.200-11	7.730-25
19	0 + H02 >>> H0 + 02	1.080-11	5.450-60
50	02 + H + M >>> H02 + M	6.130-14	7.850-31
21	03 + H >>> H0 + 02	1.270-11	0.0
SS	03 + H0 >>> H02 + 02	2.750-14	1.040-48
53	03 + H02 >>> H0 + 2*02	4.450-16	2.410-68
24	H + H0 + M >>> H20 + M	1.250-12	0.0
25	H + H02 >>> 2*H0	9.400-12	1.620-46
26	H + H02 >>> H2 + 02	1.040-11	2.550-61
27	H + H20 >>> H2 + H0	2.340-28	1.140-15
28	H + H202 >>> H2 + H02	8.360-15	5.620-29
29	H + H202 >>> H0 + H20	1.090-14	1.350-75

30	2+H0 + M >>> H202 + M	7.110-13	1.910-31
31	HO + HO2 >>> H2O + O2	1.120-11	3.890-74
35	2+H02 >>> H202 + 02	2.300-12	8.580-49
33	HO2 + H20 >>> H202 + H0	1.020-39	5.490-13
34	NO + H + M >>> HNO + M	3.870-14	6.060-33
35	NO + HO >>> NO2 + H	3.05D-3H	3.010-11
36	NO + HO + M >>> HNO2 + M	5.090-12	1.930-28
37	NO + HO2 >>> NO2 + HO	1.650-13	7.470-21
38	H + H + M >>> H2 + M	1.560-15	0.0
39	HN04 + M >>> H02 + N02 + M	2.060-05	3.790-13
40	CLN03 + M >>> CLO + NO2 + M	7.180-07	3.180-13

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000	8.0830	9.4700	4170 0	000	.8000 1	0 000	.850N 0	.800D 1
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000	8.1380 0	1.2490 0	3610 0	000	8000	0 0000	.7230 0	. 800D
9	8.1460 0	1.2910 0	0	000	.8000	0 0000.	.5840 0	8000
9	8.153D 0	1.3340 0	0	000	.8000	00000	.449D 0	. 800D
000	8.1610 0	1.3769 0	3380 0	000	.800D 1	0 0000	3190 0	. 8000
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000	8.270D 0	1.9920 0	2270 0	2000 1	.8000 1	0000.	.828D 0	.800D 1
000	8.277D 0	2.032D 0	2200 0	00	.8000 1	0 0000.	.7540 0	.800D 1
000	8.2840 0	2.0720 0	140 0	.5000 1	.8000 1	0000.	ຣຸ	.800D
000	8.2910 0	2.112n 0	2070 0	1 000	. 6000	0 0000.	.6130 O	8000
000	8.2980 0	2.1520 0	2000 0	5000 1	.8000 1	0000.	460 0	.8000
000	A.305D 0	2.1910 0	930 0	5000 1	.8000 1	000	001	.800D 1
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000	8.3180 0	2.2700 0	190 0	000	. 8000	000	580 0	.8000
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000	8.331D 0	2,3490 0	1660 0	000	.8000	0 000	0 074	1 0000
000	8.3380 0	2,3	0 06	500D 1	.9000	4.000D 09	1890 0	. 0008
000	8.3450 0	2.4270 0	1530 0	5000	. 8000 1	0 0000	1370 0	. 8000
000	8.3510 0	2.46	0	000	.8000	4.000D 09	0 860 0	. 0008
000	8.3580 0	2.5050 0	1390 0	5000	1 000	0 0000	0370 0	1 0008
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80	.5041)-0	-433D-	0 6000	7	0 00	0 0000	90	0000	0 0100
٥.	4950-0	.3260-	0 0	1080 0	5 5				
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, 4	4450-0	6690-	0 0000	1180	3000 0	0 0000	150 9	0 0000°	0020 O
9	0-0044	-0785	0 0000	0611.	1.3000 09	0 0000	010	0 0000	0020
æ	4350-0	-0605	0 0000	120D	3000	0 0000	0170	0 0000	00200
ಿ	.430n-0	•4330 <del>-</del>	0 00	•	3000 0	0 0000	0180 0	0 0000	96
'n	.4250-0	•360D-	0000	1230	3000	000	0 0670		
•	.4210-0	-2882-	0 0	1240	3000 0	0000			
٠.	.4170-0	-2210-	0 0000	0521	3000	0000	0 0000		
8	4130-0	.1550-	9	1260	3000		1.0220 00	60 0000	1,000,000
0	0-0604	-0260	0	0921	3000		1000		0400
٥	.4050-0	-0300-	0 0000	0/21	0000	0 0000	1400		
4.	•402D-0	-9710-	0000	1280	1.3000 09	1.0000 06	1 0260 06	\$0 0000°*	
•	3990-0	-0140-	0 0000	0.621.	3000		0000		
€,	.396D-0	-8580-	0 0000	0 1300	3000				1.0040 08
•	3930-0	-0408-		0 0161.	2000		0.00		1.0050 08
٠,	0-0066	-0567•	1.0000 000	1 13161	_	9 0			00200
•	0-0000	10401		0 0561			0000	0 0000	0 0500
٠°	0-058t •	-0000		0561	60 000E-1	1,0000 05	0300	0 0000	0 0500
•	0-0106	5640	; c	: -	3000	0 0000	0310	0 0000	0 0500
•	3790-0	5210-	0 0000	1350	3000 0	0000	0310	0 0000	0 0900
	3770-0	0624	0 0000	1350 0	3000	0 0000	0350	0	ö
۰.	3750-0	-4390-	0 0000	.1360	0	0		0	0
æ	.373n-0	-400h-	0 6000	7	3000 0	0	0330	0 0000	0 0900
•	.3719-0	•362D-	0.0	1370	3000 0	0 000	0340 0	0 0000	0 0000
5	.370n-0	.3260-	0	1370	3000 0	0000	1.0340 06	\$0 (1000° \$	1 0000 00
4.	.3680-0	-2910-	1.0000 06	1360	3000		26.0		2 6
o a	0-01105.	2240		: -	1.3000 09	000	0360	0 0000	0 0200
•	3640-0	1920-	0 0000	1390	3000	0 0000	370 0	0000	0 0700
• ^	3630-0	1620-	0 0000	1400	3000	0 0000	0370 0	0 0000	0 0700
. *	3620-0	1320-	0 0000	.1400 0	0	0 0000	0380	0 00	80
્	.3600-0	-1040-	0000	.1400 0	300D	0 0000	138D	0 0000	8
₩,	.3590-0	-0760-	٥	.141n n	3000	000	390 0	0 0000	0 0800
•	.3580-0	-0500-	0.0	1410 0	3000 0	0000	0 360	0000	0 0 0 0 0
~	.3570-0	-024D-	6	1420 0	3000 0	0	000	60 G000 • •	
•	.3560-0	-0666	6	<b>.</b>	3000		<b>&gt;</b> <		
•	.356D-0	-9720-	0 0000	0 02*1.	0000				) c
÷.	.3550-0	-9520-	1.0000 06	*!	2000	1.0000	200		9
•	.3540-0	-0626•	1.0000 06	0000	1.3000	•	0 0340		

T=300 K, H= 20 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + M	7.20D-03	1.310-13
5	20 + 2004 >>>	2.410-16	1.750-58
3	NO2 + NO3 >>> NO2 + NO + O2	8.210-15	4.920-35
4	SON-S - NO ->> SON-S	1.900-11	6.980-29
5	NO + 03 >>> NOZ + 0Z	1.670-14	2.850-49
6	NO2 + 03 >>> NO3 + 02	3.41D-17	2.000-34
7	HN03 + M >>> H0 + N02 + M	8.820-21	2.860-12
A	HN03 + H0 >>> H20 + N03	8.00D-14	1.250-26
9	0 + 0 + M >>> 02 + M	2.710-15	2.650-57
10	0 + 02 + M >>> 03 + M	7.520-10	6.040-09
11	0 + 03 >>> 2*02	8.900-15	0.0
12	0 + N0 + M >>> N02 + M	1.410-13	5.520-38
13	0 + NOS >>> NO + OS	6.250-12	3.73D-46
14	0 + NO2 + M >>> NO3 + M	1.300-13	1.040-23
15	HO + HO >>> H2O + O	1.570-12	4.630-24
16	SON+2 - CON+2 + SO	1.930-38	2.260-31
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	0 + H0 >>> H + 05	4.200-11	2.160-22
19	0 + HO2 >>> HO + O2	1.510-11	8.510-52
20	02 + H + M >>> H02 + M	3.66D-14	2.980-24
21	03 + H >>> H0 + 02	1.790-11	1.620-69
55	03 • H0 >>> H02 • 02	5.350-14	8.980-43
23	03 + HOZ >>> HO + 2+02	1.040-15	1.530-63
24	H + H0 + M >>> H20 + M	6.470-13	5,240-75
25	·H + H02 >>> 2+H0	1.770-11	1.140-40
26	H + H02 >>> H2 + 02	1.310-11	6.800-53
27	H + H20 >>> H2 + H0	2.180-25	6.410-15
28	H + H202 >>> H2 + H02	2.130-14	2.960-26
29	H + H202 >>> H0 + H20	2.760-14	2.950-65

30	24H0 + W >>> H505 + W	3.250-13	2.370-24
31	HO + HOZ >>> H2O + OZ	1.570-11	1.980-63
35	5+H05 >>> H505 + 05	3.210-12	1.980-42
33	HO2 + H20 >>> H202 + H0	6.110-35	8.570-13
34	NO + H + M >>> HNO + M	2.640-14	6.770-26
35	NO + HO >>> NO2 + H	7.190-34	4.920-11
36	NO + HO + M >>> HNO2 + M	5.050-15	1.140-21
37	NO + HOZ >>> NOZ + HO	3.660-13	3.740-19
38	H + H + M >>> H2 + M	1.300-15	1.120-68
39	HNC4 + M >>> HO2 + NO2 + M	1.400-02	1.680-13
40	CLN03 + M >>> CLO + NO2 + M	1.050-03	1.570-13

1,000   0.0   1,000   0.0   1,500   0.0	13   15   15   15   15   15   15   15	HAPP RES N205	SIDENCE TIME	1001S	C	č	ò	E ONH	Ç	H20
1,000   0.5   2,1240   0.6   1,4540   0.5   2,5400   1.5   3,6400   1.5   4,640   0.5   1,440   0.	1940   1941		0000	5.00	5000 0	. 000c.	3000	0000	0 00	8000
1910 09 2.9360 06 1.4560 09 4.5000 12 3.6000 11 4.0000 09 9.6660 05 3.81 11.91 09 5.9360 06 1.44120 09 4.5000 12 3.6000 11 4.0000 09 9.6660 05 3.81 11.91 09 6.5590 06 11.3100 09 4.5000 12 3.6000 11 4.0000 09 1.0540 05 3.81 12.20 09 6.1260 06 11.3100 09 4.5000 12 3.6000 11 4.0000 09 1.0540 05 3.81 12.20 09 6.1260 06 11.3100 09 4.5000 12 3.6000 11 4.0000 09 1.0540 05 3.81 12.20 09 6.1260 06 11.3100 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 6.1260 06 11.3100 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 6.1260 06 11.3100 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 06 11.20 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 06 11.20 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 06 1.20 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.20 07 1.1250 09 4.5000 12 3.6000 11 4.0000 09 1.0540 06 3.81 12.20 09 1.2	1,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0,0		.0340 0	9 1.316n 0	4780 0	.5000	8000	0 00000	.8030 0	.8000
1.134	1.01		.068D 0	9 2,1280 0	4560 0	.5000 1	.8000	0 0000	.6750 0	.800D 1
1,550 10 5,1250 10 1,1391 10 5,200 11 2,300 11 4,000 10 1,131 10 10 2,300 11 4,000 11 4,000 10 1,131 10 10 3,300 11 4,000 11 4,000 11 4,000 10 1,131 10 10 3,300 11 4,000 11 4,000 11 4,000 10 1,131 10 10 3,300 11 4,000 11 4,000 11 4,000 10 1,131 10 10 3,300 11 4,000 11 4,000 11 4,000 10 1,131 10 10 3,300 11 4,000 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 4,500 11 4,000 11 4,000 10 1,131 10 10 4,500 11 4,000 11 4,000 10 4,500 11 4,000 11 4,000 10 4,500 11 4,000 11 4,000 10 4,500 11 4,000 10 4,00	1,240   0.5   0.		1010 0	9 2.9360 0	4340 0	.5000 1	. 8000	0 0000	.6660 0	8000
1,1945    1,19	1340 09 6.1350 06 1.1350 09 4.5000 12 3.4000 17 4.0000 09 1.0236 06 3.4000 19.2240 09 6.2150 09 6.1250 09 4.5000 12 3.4000 17 4.0000 09 1.1370 06 3.4000 17 4.0000 09 1.1370 09 3.4000 17		1560 0	9 4.539D 0	3910 0	20005	8000	0000	975D 0	8000
7.5300 09 6.1266 06 1.13100 09 4.5000 12 3.6000 17 4.0000 09 1.1177 06 3.8   7.5930 19 7.6990 06 1.13100 09 4.5000 12 3.6000 17 4.0000 09 1.13170 06 3.8   7.5930 19 7.6990 06 1.13100 09 4.5000 12 3.6000 17 4.0000 09 1.1310 06 3.8   7.5930 19 7.6990 06 1.2510 09 4.5000 12 3.6000 17 4.0000 09 1.1310 06 3.8   7.5930 19 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.1310 06 3.8   7.5930 19 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.1510 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.1510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 1.6550 06 3.8   7.5930 10 1.2510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 2.0910 06 3.8   7.5930 10 1.2510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 2.0910 06 3.8   7.5930 10 1.2510 07 1.1510 09 4.5000 12 3.6000 17 4.0000 09 2.0910 06 3.8   7.5930 10 1.2510 07 1.0500 09 4.5000 12 3.6000 17 4.0000 09 2.0910 06 3.8   7.5930 10 1.2510 07 1.0500 09 4.5000 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 1.0500 09 4.5000 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 1.0500 09 4.5000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8   7.5930 10 1.2510 07 9.5200 08 4.4990 12 3.6000 17 4.0000 09 3.5510 06 3.8	7.5370 09 6.91550 06 1.3307 09 4.5000 12 3.6000 17 4.0000 09 1.1077 06 3.8000 13.500 09 5.9150 06 1.3307 09 4.5000 12 3.6000 17 4.0000 09 1.1777 06 3.8000 13.500 09 5.9150 06 1.3307 09 4.5000 12 3.6000 17 4.0000 09 1.1377 06 3.8000 13.500 09 6.9150 06 1.3307 09 4.5000 12 3.6000 17 4.0000 09 1.3307 06 3.8000 13.500 09 9.2597 09 1.0307 07 1.2520 09 4.5000 12 3.4000 17 4.0000 09 1.3400 09 1.3400 09 1.3507		.1980	9 5,3350	3700 0	1 000c.	.800N 1	0 0000.	.028D 0	.8000
	7.570 09 7.5970 06 1.3100 09 4.5000 12 3.4000 17 4.0000 09 1.2340 06 3.8000 1.3570 09 9.2591 06 1.2340 09		.2300 0	9 6.1260	3500 0	.5000 1	8000	0 0000	0	.8000
1840 0	135.0 9 9.559) 05 1.250 09 4.5000 12 3.4000 17 4.0000 09 1.2340 06 3.8000 1.2470 09 1.2570 09 4.5000 12 3.4000 17 4.0000 09 1.5270 09 3.8000 1.2470 09 1.5270 09 4.5000 12 3.4000 17 4.0000 09 1.5270 09 3.8000 1.2470 09 1.5270 09 4.5000 12 3.4000 17 4.0000 09 1.5270 09 3.8000 1.2470 09 1.5270 09 4.5000 12 3.4000 17 4.0000 09 1.5270 09 3.8000 1.2470 09 1.5270 09 4.5000 12 3.4000 17 4.0000 09 1.5270 09 3.8000 1.2570 09 1.5270 09 4.5000 12 3.4000 17 4.0000 09 1.5270 09 3.8000 1.2570 09 1.2370 07 1.1270 09 4.5000 12 3.4000 17 4.0000 09 1.5570 06 3.8000 1.2570 09 1.2370 07 1.1270 09 4.5000 12 3.4000 17 4.0000 09 1.5570 09 3.8000 1.2570 09 1.5270 09 4.5000 12 3.4000 17 4.0000 09 2.2090 09 3.8000 1.2570 09 1.2470 09 4.5000 12 3.4000 17 4.0000 09 2.2090 09 3.8000 1.2570 09 1.2470 09 4.5000 12 3.4000 17 4.0000 09 2.2090 09 3.8000 1.2570 09 1.2470 09 4.5000 12 3.4000 17 4.0000 09 2.2090 09 2.2090 09 3.8000 1.2570 09 1.2470 09 4.5000 12 3.4000 17 4.0000 09 2.2090 0		0 0202.	(1016)	3300 0	1 0000	7 0000	0 0000	9 0	1 0000
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.184D 09 3.297D 07 7.827D 08 4.499D 12 3.800D 17 4.001D 09 5.513D 06 3.802D 09 3.3297D 07 7.709D 08 4.499D 12 3.800D 17 4.001D 09 5.667D 06 3.802D 09 3.441D 07 7.709D 08 4.499D 12 3.800D 17 4.001D 09 5.821D 06 3.802D 09 3.541D 07 7.478D 08 4.499D 12 3.800D 17 4.001D 09 5.976D 06 3.802D 09 3.584D 07 7.365D 08 4.499D 12 3.800D 17 4.001D 09 6.13DD 06 3.802D 09 3.655D 07 7.254D 08 4.499D 12 3.800D 17 4.001D 09 6.284D 06 3.802D 09 3.726D 07 7.254D 08 4.499D 12 3.800D 17 4.001D 09 6.284D 06 3.802D 09 3.726D 07 7.144D 08 4.499D 12 3.800D 17 4.001D 09 6.43BD 06 3.802D 09 3.726D 09 6.43BD 06 3.802D	.184D 09 3.297D 07 7.827D 08 4.499D 12 3.800D 17 4.001D 09 5.513D 06 3.800D 1 3.205D 09 3.369D 07 7.709D 08 4.499D 12 3.800D 17 4.001D 09 5.67D 06 3.800D 1 3.227D 09 3.441D 07 7.478D 08 4.499D 12 3.800D 17 4.001D 09 5.821D 06 3.800D 1 3.249D 09 3.586D 07 7.345D 08 4.499D 12 3.800D 17 4.001D 09 6.130D 06 3.800D 1 3.291D 09 3.555D 07 7.254D 08 4.499D 12 3.800D 17 4.001D 09 6.284D 06 3.800D 1 3.20 09 3.726D 07 7.144D 08 4.499D 12 3.800D 17 4.001D 09 6.438D 06 3.800D 1 3.333D 09 3.797D 07 7.036D 08 4.499D 12 3.800D 17 4.001D 09 6.591D 06 3.800D 1 3.800D 1 3.797D 07 7.036D 08 4.499D 12 3.800D 17 4.001D 09 6.591D 06 3.800D 1 3.800D		,161D n	3.2260	.9470 0	4990 1	.8000 17	4.0010 0	.3590 0	.8000 1
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.227D 09 3.441D 07 7.593D 08 4.499D 12 3.800D 17 4.001D 09 5.821D 06 3.8 .249D 09 3.512D 07 7.478D 08 4.499D 12 3.800D 17 4.001D 09 5.976D 06 3.8 .270D 09 3.584D 07 7.365D 08 4.499D 12 3.800D 17 4.001D 09 6.130D 06 3.8 .291D 09 3.555D 07 7.254D 08 4.499D 12 3.800D 17 4.001D 09 6.284D 06 3.8 .312D 09 3.726D 07 7.144D 08 4.499D 12 3.800D 17 4.001D 09 6.438D 06 3.8	.2270 09 3.4410 07 7.5930 08 4.4990 12 3.8000 17 4.0010 09 5.8210 06 3.8000 1 1.2490 09 3.5120 07 7.4780 08 4.4990 12 3.8000 17 4.0010 09 5.9760 06 3.8000 1 1.2700 09 3.5840 07 7.3650 08 4.4990 12 3.8000 17 4.0010 09 6.1300 06 3.8000 1 1.2910 09 3.6550 07 7.2540 08 4.4990 12 3.8000 17 4.0010 09 6.2840 06 3.8000 1 1.3120 09 3.7260 07 7.1440 08 4.4990 12 3.8000 17 4.0010 09 6.4380 06 3.8000 1 1.3330 09 3.7970 07 7.0360 08 4.4990 12 3.8000 17 4.0010 09 6.5910 06 3.8000 1		.2060 0	3,3690	.7090 0	4990 1	.8000 1	.0010 0	.667n 0	.8000 1
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.3120 UY 3.(20) U/ (.144) UB 4.499 IZ 3.8000 I/ 4.0010 UY 6.4380 UB 3.8	.3120 07 3.720 07 7.1360 08 4.4990 12 3.8000 17 4.0010 09 6.5910 06 3. <b>8000 1</b>		0 0162	3,6550	6240	7 0669	. 0008	0 0100	2840 0	. 8000
	.3330 09 3.7970 07 7.0360 08 4.4990 12 3.8000 17 4.0010 09 6.5910 06 3.8000 1		.3120 0	3.7200	0 0441	1 0669	1 0008	0 0100	0 0854.	1 0000

TIME (S)	c		1	ì	н02	4702	0114	HN02	40NH	CLN03
•	.0000		0 0000.	0 00	.0000	1.300D 09	0 00	0	.0000 o	_
~	.5040		-0462.	0 0000	.2200 0	3000 0	0 0000	0 0100	0 4686	0666
•	.5040	ء و	7.1980-07	00	4.3360 07	300D 0	1.0000 06	1.0010 06	3.9780 09	9.9980 07
٥	0000		0-0161.		0 (1044)	3000				0000
9	2000		0-0224		0 (1456.	- c		0 000	9440 0	0 0766
~	.5040		0-0679°	0 0000	.7540 0	300D 0	0 0000	0030 0	.9330 0	.9930
*	.5041		.9460-0	0 0000	470 0	300D	0	0 0400	.9220	9920 0
٠.	.5049		.304D-0	0000	0 0860	300	0 0000	0.050	.9110	0 0066.
•	.5040		.730D-0	0 000	2020 0	0 000	0 000	0 0500	.9010 0	890 0
•	.5040		-0602	0 0000	3100 0	3000	0 (1000	0 090¢	.890n 0	988
~	.504n		.7420-0	0000	4170 0	3000 0	0 0000	0000	.8790 0	.9870 0
•	5047		0330-0	0 0000	5240 0	3000 0	0 (1000	0 40 0	.868D 0	9860 0
৽৽	.5040		-0880-	0000	1.6310 08	3000	0	00800	.8570	9.9850 07
٥	0000		0-(ISO1.	1.0000 00	0 00 00				0 0360	0 0000
٠,	5050		3100-0		0.0840	0 0000			8250	9810 0
•	5050		3880-	0 000	.0530		0 0000	0110	.8140 0	0 0086
့စ	.5050		471D-0	000	0 0721.	3000 0	0 0000	120 0	.8040 0	.9790
۰,	.505p		.5560-0	0 0000	.2610 0	3000	0 0000	0130 0	.7930 0	.9780 0
0	.5060	0	.6440-0	0 0000	.3640 0	3000 0	0 000	0 0410	.7830 0	.9770
ş	.506ŋ	01	.1350-0	0 0000	.4680 0	3000 0	0 0000	0150 0	.7720 0	.9750 0
*	.5060	0	.828D-0	1.0000 06	.570D 0	0 00	0 000	160 0	.7620 0	6
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æ, '	.5070	- C	0-0120	0 000	.7740 0	3000	8	80 0	0 0192	-972
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~	5080		-0222.	0000	0 (19/6.	3010	0000	0 0120	0 2027	0076
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é e	0800.	<u>.</u>	0-000-		2740 0	3010 0	0000	0 530	0 (1669*	0 0896
9 0		3 6	0-0000		3760	2 6	3 6	0 0400	4700	0 0196
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	5110	. E	.860D-0	0 0000	.5730 0	3010 0	00000	0 0620	0 0659	9630 0
۰	5110	50	.9700-0	0 0000	.670D 0	0 01	0 0000	0 300 0	6480 0	9620 0
	.5120	=	.0810-0	0000	.768D 0	0	0 0000	0350 0	.6380 0	.9610 0
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N.	5130	٦ و	.3060-0	0 0000	0 0196	3010	0	0320	.6180 0	290 0
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*	5180	70	0-0686°	0 0000	532D 0	3020	0 0000	0 440	.5590	.9520 0
•	.5190	10	.1040-0	0 000	.6250 0	3020 0	0 0000	0 0940	.5490	.9510 0
8	.5200	5	.2190-0	000	.7180 0	3020 0	0 0000	0480 0	.5390 0	0 0056
0	.521n	01	3340-0	0000	.8110 0	3020 0	0 0000	200 0	.5290 0	0 0646
ď	5210	<b>~</b>	0-0644	8	.9030	3030 0	0000		.5200 0	0 0846
0.40	5220	5	-5640-	0000		3030	0 0000	50.	2100	0440
٠	5230	<b>7</b>	0-06/9		0 0000.	0 050	0000	.0550	.5000 o	0000
Ď.	5250	57	0-046/	<b>&gt;</b> C	5.2670 08	7	0000	0570		
	(10)(	7	-0004	3		2020	<b>3</b>	0660•	0 019**	•

T=700 K, H= 20 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + M	1.060 06	1.090-14
5	2*NO3 >>> 2*NO2 + O2	2.570-14	7.440-49
3	NOS + NO3 >>> NOS + NO + OS	5.510-14	3.970-36
•	NO3 + NO >>> 2*NO2	1.90D-11	2.230-19
5	NO + 03 >>> NO2 + 02	2.650-13	4.540-29
6	NO2 + 03 >>> NO3 + 02	3.62D-15	6.56D-22
7	M + SON + OH	8.810-02	1.470-13
8	HN03 + H0 >>> H20 + N03	8.000-14	4.740-19
•	0 + 0 + M >>> 02 + M	2.090-16	3.010-20
10	0 + 02 + M >>> 03 + M	1.220-16	7.38D 00
11	0 + 03 >>> 2*02	7-110-13	8.630-43
15	0 + NO + M >>> NO2 + M	1.980-14	4.70D-11
13	0 + NO2 >>> NO + O2	1-110-11	8.500-27
14	0 + NO2 + M >>> NO3 + M	5.560-14	4.44D-24
15	HO + HO >>> H2O + O	4.530-12	2.040-16
16	05 + 5400 >>> 5405	7.040-39	9.370-21
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	0 + HO >>> H + O2	4.200-11	2.110-15
19	0 + H02 >>> H0 + U2	3.910-11	2.190-28
20	02 + H + M >>> H02 + M	6.050-15	1.360-05
21	03 + H >>> H0 + 02	4.78D-11	5.620-37
55	03 + HO >>> HO2 + O2	3.590-13	A.310-26
23	03 + HO2 >>> HO + 2*02	1.180-14	1.120-49
24	H + HO + M >>> H2O + M	3.060-14	7.360-27
25	.H + H0S >>> 5+H0	1.080-10	5.870-24
26	H + H02 >>> H2 + 02	2.550-11	A.03D-29
27	H + H20 >>> H2 + H0	6.560-17	8.900-13
28	H + H505 >>> H5 + H05	3.060-13	1.770-18
29	H + H202 >>> H0 + H20	3.98D-13	1.020-35

30	2*H0 + M >>> H202 + M	2.510-14	2.300-04.
31	HO + HO2 >>> H2O + U2	4.060-11	7.730-33
35	2*H02 >>> H202 + 02	A+320-12	3.020-24
33	HOS + HSO >>> HSOS + HO	2.720-21	3.07D-12
34	NO + H + M >>> HNO + M	6.400-15	4.830-06
35	NO + HO >>> NOZ + H	2.230-21	2.020-10
36	NO + HO + M >>> HNO2 + M	1.050-13	1.300-02
37	NO + HOZ >>> NOZ + HO	3.600-12	2.680-14
38	H + H + M >>> H2 + M	5.560-16	4.650-25
39	HN04 + M >>> HOZ + NOZ + M	1.310 06	1.230-14
40	CLN03 + M >>> CLO + NO2 + M	8.25D 05	5.490-15

	HAPP RESI	RESIDENCE TIME	STUDY						
TIME (S)	N205	20N	NO3	01	60	20	HNO3	9	H20
•	.0000 0	0 0000	0 0000.	.5000 0	.500	. 800D 1	0000	0 0000	8000
	.277D-0	.842D 0	.574D 0	.1700 0	.4220 1	8000	.9300	3030 0	8000
*	.3440-0	.7990 0	200	.1270 1	.0120 1	.8000	.8620 0	3720 0	8000
ď	820-0	.2690 0	.6390 0	1870 1	. 6880 1	8000	.7940 0	4260 0	1 0008
œ	9410-0	1190 0	.5660 0	. 2100 1	4250 1	. 8000 I	.7280 0	4710 0	1 0008
٠,	.5560-0	0 01.10	0 06/4.	1 0000	1 0 7 6 7	1 0000	0 0000	0 0/00	
Ÿ	0-0125°	0 0170	3760	1 (1422	1 0 0 4 0		5360 0	4 7000	
	570-0		4.170.08	1.2410 10	2 6	8000	0 0 0 2 4 9	5760 0	8000
	7860-0	0 0,00	0620	2470 1	.6160	8000	4140 0	5900 0	8000
	.608n-0	1180 0	9540 0	2530 1	120 1	. HOOD 1	3540 0	. 599n o	.8000
?	4310-0	1330 0	. R460 0	580 1	.421D 1	.8000 1	.2950 0	.6050 0	1 0008
*	.251D-0	.148D 0	.738n o	2630 1	.340D 1	.8000	.238D 0	.608D 0	8000 1
9	0-0690-	.1620 0	.631D 0	ر و	.266D 1	.8000	1810 0	0 0609	. 0008.
€,	.886n-0	1770 0	.5250	.2740 1	9:	. 8000	0 0921	.607D 0	20008
9 (	0-(120/	0 4161	0 617		1 0767	1 0000			
•		0 ()()2.	2170	1 0000	1 0360	4008	0 6550	5010	8000
,	1530-0	0 0252	1180 0	2930 1	9080	8000	9130 0	5820 0	. 0008
9	9710-0	2450 0	0220	_	.4870 1	.8000 1	.8620 0	.5730 0	1 0008
•	7920-0	.258n 0	.927D 0	3030 1	.0980 1	.8000	.9120 0	5620 0	.800D 1
2	.6150-0	.270D 0	.835D 0	3070 1	.738D 1	.800D 1	.7630 0	.551D 0	.8000
*	400-0	.282D 0	.7450 0	.3120 1	.4040 1	. 8000 I	.1150 0	• 5390 o	1 0008
•	.2670-0	.294D 0	.6580 0	.3160 1	1 0260	. 8000 Y	.6680 0	.5260 0	. 0008.
	-0770-0 0-0760-	3060	.5730	.3200 1	1 0108.	1 0009	0 0129.	0 021c.	7 0008*
91	0-0066.	.3170 0	0 0165	.3240 1	1 0625.	8000	0.0575.	0 0864.	7 0008
•	0-0/9/•	3280 0	0 0014.	י מכמני	1 00/20	1 0000	0 0000	0 0000	7 0000
• •	0-0000.	3380 0	0.3530 0	1 0225	1 0000	7 0000	0 0004.	0 0404.	7 0000
	0-0502	0 0056	<b>&gt;</b> c		5970		0 0004	0 000	8000
•	1450-0	3690 0	1130 0	3440 1	3960 1	8000	3580 0	4230 0	8000
~	0-0866.	.3780 0	.0450	.3480 1	.2070 1	.800D 1	.317D 0	4080 0	.8010 1
•	.8550-0	.3880 0	.9780 0	.3520 1	.027D 1	. 8000	.2770 O	3920 0	. 8010
9	.7150-0	.3970 0	0 0416.	.3550 1	.856D 1	8000	.2370 0	3760 0	. 0108.
φ.	-2625	0 0904	.852D 0	.3590 1	46950 1	1 0008	0 0861.	3600 0	6010
7.30	0-0/44	0 0414.	1 7340 08	1.3630 10	7 010	3.6000 17	<b>9 C</b>	3280	
	1930-	4210	: 5	3690	2550	2000	0850 0	3120	8010
. •	.071D-0	4390 0	.6240 0	3730 1	1220 1	. HOOO 1	0 0650	2960	8010
	.9530-0	.4470 0	C	.3760 1	1 0566	.800D 1	0130 0	.2800 O	.8010 1
•	.839D-0	.454D 0	0	3790 1	~	.8000	0 0826	.2640 0	.8010 1
?	.7260-0	4620 0	730 0	.3820 1	.7580 1	8000 1	9430 0	2480 0	. 90108
*	.618D-0	0 0694	4260 0	3850 1	.6460 1	1 0006	0 0016	2320 0	1 0108
•	•5130-0	0 0924	3810 0	3880 1	.5400 1	8000	8760 0	2160 0	8010
8	•4110-0	482D 0	3370 0	3910 1	.4370 1	1 0008	8440 0	2000	1 0108
•	-313D-0	0 0664	0 0000	3940	1 0655	1 0008	0 0119	0 0591	1 0108
Ÿ	0-0/17:	0 0000	2150	2004	<b>-</b>		2000	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	4 0100
•	0-05210	5080	6	1 0204	1 0490	4000	: =	1380	
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TIMETO	c		1		î		C 0 H		7074	CZ	CONH CONH		40NH	CL NO3
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~	.2230	11	5.	0	1300	و	8	60	0 07	000	1.2	0	630-0	.3450-0
٠.	.6210	11	.41	0		90	1.9090	60	1.3110 09	0000	-	90 O	.993h-0	.511D-0
۰,	1390	11	6.	0	4040		•	60	5D 0	0100	2,3	0	.1570-0	.0360-0
Φ,	.7450	11	2.	0	1.5360 0		.00		320D	-	5.94	0	0	901
٩.	.4175	_	.12	C	٠.		• 03		35	0100	3.57	0	.9530-0	864D-0
ď	1400	7.	9	0	• 77	<u>.</u>	0.0		3300	010	4.21	0	.9950-0	.8590-0 6756
•	.902n	_	. 7	0	.87		.085		335N 0	0100	4.85	90 09	0-0050.	0-0508.
٠,	0269		÷;	C	.97		102	6.0	3400 0	010	5.508	0	990	0-05/90
8	.5180		9	0	0		۲ <u>۱۱</u> ۰	2 (	3450 0	0100	0		0-0500	00000
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Ÿ	0417		9 6	0	•	0 4	134	2 0	3610		- a		2830-0	07.60
•	200	٠.		> 0	0356.		125	. 0	0 0100		ď		7150-0	0400
9 4	6 6	1.		9 9	2.4810 0	990	2.134D	60	1.3720 09	1.0020 06	0	90	3420	·
9	7870	: [	6	0	.5500		131	60	3770	0020	~	0 07	.3640-0	9996
~	.7030	11	8	0	.6150		.127	60	3830 0	.0020	-	70 d	.3830-0	.979
•	.6250	1	.61	0	0229	ç	.12	60	8	00	-	D 07	.3980-0	66.
9	.5550	11	.35	90	•73			60	30 0	020	-	0 07	.410D-0	8
æ	.4890	11	=	90	• 19		.106	60	0 086	•0030	<u>.</u>	0 07	.419D-0	5
ç	062**	_	8	90	. 844		60.	60	4030 0	0 0500	<b>–</b>	20.0	•425D-0	.0260
Š	.3730	11	.69	90	.894D	9	•	60	4080 0	.0030	-	0 0	.4290-0	.03
•	.3210	=	4	90	245	•	•	60	30	0030 0	<u></u>	0 0	.430D-0	0480
ŝ	.272h	11	5	90	٠.		9	60	4180 0	0030	<b>~</b>	06 04 06	.4290-0	0230
₩.	.227D	1	. 12	0	.0310	9	•	0.0	230 0	30 0			4260-0	90
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٠,	1450		8	0	1120	۰ و	٠,		330 0	0 유	1.7440		•416D-0	0880
•	•107D		99	0	٦,	•	•		370 0	0030	æ, '		-408D-0	0860
٠,	•072D	~ :	55	0	.1850	۰ م	00		4420	0030	.87	c 1	• 399n-0	3:
8	0390	·		c '	0022	۰ م	1.9900		4460 0	0030	986.	0	-389D-0	7
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	.739D	01	7.5	0	3960	•	1.9070	60	471D 0	00400	2,3090		3050-0	19
~	.510n	10	•66	0	4	9	1.8930	60	47	0 0700	್		Ó	1740-0
*	.291D	10	57	0	.4457	9	819	60	190 0	1.0040 06	.430	0	Ó	.18
÷.	.0820	20	64.	0	4690	9	865	60	42D 0	040	490	$\overline{}$	.2530-0	. 18
Φ,	.8830	10	Ŧ.	0	4910	ş	85	60	860 0	040	.549	_	Ö	÷.
e	.693D		÷.	0	.5120	9	93	60	489D 0	40 0	.608	_	.215n-0	2020
٧.	.5110		2	Ō	.5320	•	O.	60	930 0	0040	ŝ.		o	2090
*	•3360		2	Õ	•5520	9	810 10	60	0 (1967	0 0700	~ '		0	2150-0
9	1690	10	۳.	Ċ	•5710	9	6		0 000	0 0400	2,7820		0	-2222
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Ÿ	0907			0		• •	ردر <del>ر</del>	) (	5090	900	•		0-0460	å.
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9	2000		9 6	> 0	0460	D 4	<b>u</b> -	9 0	0010		• -			26.0
10.00	6.1670 1	20	1.7500	ŏ	940	•	- 1	200	9 0		22	000		2.2610-03
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T= 800 K, H=20 km

R-NUM	REACTION	FORWARD RATE	RACKWARD RATE
1	N205 + M >>> N02 +N03 + M	5.840 06	8.150-15
2	SO + SON#S <<< £00#\$	3.990-14	5.950-48
3	NOS + NO3 >>> NOS + NO + OS	6.590-14	3.130-36
4	SON*S << 0N + EON	1.900-11	1.740-18
5	NO + 03 >>> NO2 + 02	3.430-13	4.420-25
6	NOS + 03 >>> NO3 + 02	5.610-15	9.780-21
7	M • SON • OH <<< M • EONH	4.18D 00	9.230-14
8	HN03 + H0 >>> H20 + N03	8.00D-14	2.430-18
9	0 + 0 + M >>> 0	1.560-16	9.070-16
10	0 + 02 + M >>> 03 + M	9.750-17	4.97D 01
11	0 + 03 >>> 2*02	1.070-12	6.110-39
12	0 + N0 + M >>> N02 + M	1.560-14	1.49D-0A
13	0 + NOS >>> NO + OS	1.170-11	5.550-25
14	0 + NO2 + M >>> NO3 + M	4.86D-14	3.890-24
15	HO + HO >>> H2O + O	5.000-12	1.060-15
16	02 + 2*N0 >>> 2*N02	6.40D-39	8.780-21
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	S0 + H >>> H + 0	4.200-11	9.550-15
19	0 + H05 >>> H0 + 05	4.280-11	3.430-26
20	02 + H + M >>> H02 + M	4.840-15	7.220-04
21	03 + H >>> H0 + 02	5.250-11	6.310-34
SS	03 + H0 >>> H02 + 02	4.300-13	3.240-24
53	03 + HO2 >>> HO + 2+02	1.48D-14	2.35D-48
24	H + HO + M >>> H2O + M	1.890-14	1.870-22
25	.H + HOS >>= S#HO	1.240-10	5.160-55
26	H + H05 >>> H5 + 05	2.710-11	1.450-26
27	H + H20 >>> H2 + H0	4.090-16	1.410-12
28	H + H505 >>> H5 + H05	3.930-13	9.470-18
29	H + H505 >>> H0 + H50	5.110-13	6.020-33

30	2+H0 + M >>> H202 + M	1.870-14	1.540-02
31	HO + HOZ >>> H2O + OZ	4-44D-11	5.700-30
35	2+H05 >>> H505 + 05	9.100-12	1.530-22
33	HOZ + HZO >>> HZOZ + HO	5.190-20	3.46D-12
34	NO + H + M >>> HNO + M	5.300-15	3.150-04
35	NO + HO >>> NOZ + H	3.300-20	2.300-10
36	NO + HO + M >>> HNO2 + M	7.510-14	7.160-01
37	NO + HOZ >>> NOS + HO	4.460-12	7.66D-14
38	H + H + M >>> H2 + M	4.860-16	5.130-21
39	HN04 + M >>> H02 + N02 + M	6.970 06	9.130-15
40	CLN03 + M >>> CLO + NO2 + M	5.340 06	3.20D-15

	HAPP RESI	RESIDENCE TIME S	STUDY						
TIME (S)	N205	V07	EON	00	03	20	HN03	9	ĩ
•	4.0000 08	0 0000	.0000	0 000	.500D 1	.800D 1	0 0000	0 0000	. 8000
~	0-0694.	620 0	.5210	.5350 1	.2870 1	.8000 1	.735D 0	.9220 0	. 1990 1
*	66.	.5620 0	.3640	.6550 1	.5390 1	.8000	.5280 0	.0480	. 7980 1
٠,	.3619-0	830 0	.1620	080	.4970 1	.8000	.2660 0	170 1	. 7970
€.	·0300-0	.332D O	.947D	.7320 1	.1240 1	. 800h	4170 0	.0730	1 0767.
0	.6550-0	.0950	. 7320	7450 1	.141D 1	. 0008.	0 0561	1 0860.	1 0/6/6
Š	.455P-0	0 0266.	.5220	.7510 1	1 (1007)	. 0008.	0 09/9.	10401	1 0/6/-
٠,	-3030-	9670 0	.3210	7550 1	1 0460	1 0008	1320 0	1 0960	1 0/6/0
٠	0-08/1.	0 (1554.	0621	1 (1)	1 0100		2040	1 0490	70707
Ď.	0-0740	0 0520	(1047	7600 1	1 0012		0620	1 0540	7970
? ^	9	1320 0		7610 1	455D 1	8000	2690	1.0220 10	970
*	-1677.	1880 0	.4550	620 1	.2390 1	.8000 1	0 Q0%6°	.9830 0	1970 1
9	.691n-0	.243D 0	.310D	7630 1	.0540 1	.8000 1	.9210	.7430 0	1970 1
₽.	.6070-0	.2950 0	.1730	7640 1	.8930 1	. 800D	4700 0	5040 0	. 7980 1
0	•525n-	.3450 0	.0440	7650 1	.7530 1	8000	2650 0	2700 0	1 0867
Š	0-0244	3920 0	.9220	7650 1	.630D 1	. 0008	1660 0	0410	1 0962
•	3720-0	0 0/5%	.8080	1 (1997	ו מזכי	1 0000	0 0020	0 0000	7080
٥	•		0001		1 020		0.0450	2050	7980
	1660-0	0.0555.	5040	7680 1	2590 1	8000	0330	1960	1980
2	1040-0	0 0065	4140	7680 1	1880 1	.800h	0140	0 0400	. 1990 1
4	0-0440-	6230 0	.330D	7690 1	1 1240 1	.8000	.9620 0	.820D 0	. 1990 1
•	.877n-0	0 0759	.2510	7700 1	0650 1	.800D 1	.7870 0	.6440	1 0661.
₽,	.3399-0	.683D 0	.1770	00	.0120	.8000 1	.6170 0	.475D 0	. 1990 1
0	.8290-0	.7110 0	.1070	00	. 430D 1	.800D 1	.4510	3120 0	1 0662
?	.3450-0	.7370 0	0450	- -	1790 1	. 8000	2900	1570 0	1 0667
•	.8860-0	.761D 0	. A020	7710 1	. 7630 1	. 8000	1330	.0080	1 0667.
٠,	.452n-0	.7850 0	.2250	7720 1	.3780 1	1 0009	0086	0650	1 0667
Ď.	0-0190	0 0/08	0280	1 022	1 0120	1 0006	1250	0 0207.	7 0667
٥,	0-1260	0 0070	4050	ו מפגנ	7 0 0 0		5480	0 0174	
•	0-0866	8680 0	24.70	38	1 0160	8000	4130	3500 0	8000
. •	.611n-n	.8870 0	.8250	7730 1	8210 1	.800D 1	.2810	.2330 0	.8000
80	.3020-0	0 0506.	.4300	7730 1	.5680 1	.8000 1	.1540	.1210 0	.8000 1
0	0100-0	.9220 o	.0580	7740 ]	•330D 1	8000	0310	0 0410	.800D 1
~	.7350-0	9390 0	.7105	7740 1	10701.	. 8000	9120	0 0016.	8000
• •	0-00/4	5.9550 08	3820	- - -	2 6	1 0008	7.6850 04	200	1 0008
8	0010-0	9860 0	.7860	7740 1	.5110 1	8000	5770	.6220 0	.8000
•	.783n-0	0 0000	.5150	7740 1	.3340 1	.8000	4720	.5330 0	.8000 1
~	.5790-0	.0150	.2410	.7750 1	.1660 1	.9000	.371D	.4460 0	.8000 1
*	.3860-0	.029n 0	.0220	7750 1	.007D 1	.8000 1	.2730	.3630 0	.800D 1
9	-0402	0420 0	0767.	.7750 1	8560 1	8000	1770	.2830 0	.800D 1
æ .	0335-0	.0560 0	.5870	. 7750	1 120 1	8000	0820	2050 0	1 0109
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Ÿ	0-0021	0 0290	66030	2 6	1 0044	7 0000	0014	0 0800	7 0108
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	916016		7100	7750	2000		4440	A540 6	
10.00	2,1970-05	6.1330 08	2.5650 07	1.7750 10	3.9820 10	3.8000 17	6.5900 04	4.7900 09	3.8010 12
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HF (S)	c		I		Ţ		40S		H202	ON H		HNOZ	40NH	CLNO3
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Ñ.	.7340		=:	20	7390	9 ;	2310 0	<b>э</b> с	1.2980 09	001	ς,	1.7770 06	.5290-	0160-
•	0787		, a	) (	0 00	و د	ט טצלע.	<b>&gt;</b> 0	30000	<b>~</b> •	0 4	2050	5230-0	6840-0
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	. H920		. 8	0.7	7.1050	9	.6070		324D 0	_		.752D	4050-0	.1270-0
N	.9030		8	0.7	1590	90	.6240 0	•	1.3340 09	0700		.0280	.3680-0	043
•	.1390		.31	07	.0610		ŝ	•	0	0		1620	3410-0	0230
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8	.5360		.84	20			.0870 0	0	930 0	0110		1.6170 07	1390-	2890
0	3490		.6	20	2860	6	0 0900		3970 0	9110		6330	٠	3290
٠,	.1840		5.	70	3090	<b>~</b> ~		. 0	1.4000 09	0 0210.1	0 4	1.6430 07	Z-0600-0	4.4040-05
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•	.6860		• 06	07	3750	20	.6370	•	0 09	0120	9	6180	1.9170-03	0
Š	.5920		.77	90	860		.5710	<u>o</u>	90	0130	£	6030	881	528
*	.5060		6.	90	970	<b>~</b> 10	.508D 0		4060 0	0130	ς,	5850	845	4.5540-05
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~	.230n		75	90	4270	0.7	.28	0	4020 0	0130		4970	712	40
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.69	.123n		2,5	90	370	<b>~</b> [	1810 0	σ (	1.3990 09	1.0130 0	œ v	4480	97	4.6860-05
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R-NUM	REACTION	FORWARD RATE	BACKWARD . RATE
1	N205 + M >>> NO2 +NU3 + M	4.050-05	1.270-13
2	20 + 50/45 <<< 5.00	4.710-17	7.460-62
3	SU + UN + SON << EON + 20N	4.210-15	1.190-34
4	NO3 + NO >>> 2*NO2	1.900-11	3.290-32
5	NO + 03 >>> NO2 + 02	6.360-15	1.080-56
6	NO2 + 03 >>> NO3 + 02	6.65!)=1n	8.330-39
7	HN03 + M >>> H0 + N02 + M	5.360-28	2.460-12
А	HN03 + H0 >>> H20 + N03	R • 000-14	2.800-29
9	0 + 0 + M >>> 02 + M	2.690-15	1.440-57
10	0 + 02 + M >>> 03 + M	5.760-16	1.620-12
11	0 + 03 >>> 2*02	1.920-15	0.0
12	0 + N0 + M >>> N02 + M	1.130-13	8.390-48
13	0 + NO2 >>> NO + O2	5.120-12	6,270-53
14	0 + N02 + 4 >>> N03 + M	7.070-14	5.66D-24
15	HO + HO >>> H2O + O	1.090-12	9.770-27
16	05 • SeNO >>> SeNOS	2.750-38	3.880-35
17	NO2 + H-NU >>> 110 + 0	0.0	0.0
18	0 + HO >>> H + US	4.200-11	7.730-25
19	0 + H02 >>> H0 + 02	1.080-11	5.450-60
Su	02 + H + M >>> H02 + M	2.780-14	3.570-31
21	03 + H >>> H0 + 02	1.270-11	0.0
22	03 + H0 >>> H02 + 02	2.750-14	1.040-48
23	03 + HO2 >>> HO + 2*02	4.450-16	2.410-64
24	H + H0 + M >>> H2O + M	5.670-13	0.0
25	H + H02 >>> 2#H0	9.40D-12	1.620-46
26	H + HUS >>> HS + 0S	1.040-11	2.550-61
27	H + H20 >>> H2 + H0	2.340-24	1-140-15
28	H + H202 >>> H2 + H02	8.360-15	5.620-29
29	н + н202 >>> но + н20	1.090-14	1.350-75

30	2*H0 + M >>> H2U2 + M	3.230-13	8.680-32
31	HO + HO2 >>> H20 + U2	1-120-11	3.890-74
32	2*H02 >>> H202 + 92	2+300-12	A.580-49
33	HOS + HSO >>> HSOS + HO	1+020-39	5.490-13
34	NO + H + M >>> HNO + M	1.760-14	2.750-33
35	NO + HO >>> NO2 + H	3.050+34	3.010-11
36	NO + HO + M >>> HNO? + M	2.310-12	H.77D-29
37	NO + HOZ >>> NOZ + HO	1-650-13	7.470-21
38	H + H + M >>> H2 + M	7.070-16	0.0
39	MN04 + M >>> H02 + N02 + M	1.090-05	2.020-13
40	CLN03 + M >>> CLO + NO2 + M	3.260-07	1.590-13

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3.00	A.3347-02	7.4950-07	1.0000 06	2.4	400D 0	0000	910	0	00500
3.20	A.283:3-02	2.646n-07	1.0000 06	2.4	MOOD 0	0000	0640	0	4.002D 08
3.40	8.2350-02	2.59AD-07	1.0000 06	2.4	1.400D 09	0000	.0680	0	00200
3.50	8.1980-02	2.5520-07	1.0000 06	7.5	1.8000 09	0		0	0
3.80	8.1440-02	2.5070-07	1.0000 06	2.4	0		.0740	500D 0	4.0020 08
	8.1020-02	2.4630-07	=	2.4	0	1.0000 04	.0770	0	0
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0	7.9165-02	2.2610-07	<b>C</b>	2.4460	<b>-</b>	9	0160.	5000 0	õ
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5.80	7.79411-02	2.117n-07	= (	2.4510	000	000	010	500n o	00
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7.40	7.6050-02	1.8730-07	1.0000 06	2.4	9 U009	0 0000	1200	.5000 0	0400
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T=300 K, H= 25 km

R-NUM	REACTION	FORWARD HATE	BACKWARD RATE
1	N205 + M >>> NO7 +NO3 + M	3.279-03	5.940-14
2	SO + SON#S <<< FON#S	2.419-10	1.750-54
3	NOS + NO3 >>> NOS + NO + OS	H-210-15	4.9211-35
4	NO3 + NO >>> 2*NO2	1.900-11	6.980-29
5	NO + 03 >>> NO2 + 02	1.670-14	2.850-49
6	NO2 + 03 >>> NO3 + 02	3.410-1/	2.000-34
7	HN03 + M >>> HO + NO2 + M	4.010-21	1.300-12
я	HN03 + H0 >>> H20 + N03	N+00D-14	1.250-26
9	0 + 0 + M >>> 02 + M	1.230-15	5.480-58
10	0 + 02 + M >>> 03 + M	3.420-16	2.740-09
11	0 + 03 >>> 2*02	8.900-15	0.0
12	0 + N0 + M >>> N02 + M	6.400-14	2.510-38
13	0 + NOS >>> NO + OS	6.250-12	3.730-46
14	0 + NO2 + M >>> NO3 + M	5.490-14	4.710-24
15	0 + 05H >>> OH	1.570-12	4.630-24
16	05 + 5440 >>> 54405	1.930-34	2.260-31
17	NO2 + H-NU >>> NO + 0	0.0	0.0
18	S0 + H0 >>> H + US	4.200-11	2.160-22
19	0 + HOS >>> HO + OS	1.510-11	8.510-52
20	02 + H + M >>> H02 + M	1.660-14	1.360-24
21	03 + H >>> H0 + 02	1.790-11	1.620-69
22	03 + HO >>> HOZ + OZ	5.350-14	8.980-43
23	03 + HO2 >>> HO + 2*02	1.040-15	1.530-63
24	H + HO + M >>> HZO + M	2.940-13	2.380-75
25	H + H02 >>> 2*H0	1.770-11	1.140-40
26	H + HUS >>> HS + US	1.310-11	6.800-53
27	H + H20 >>> H2 + H0	2-18D-25	6.410-15
28	H + H202 >>> H2 + H02	2.130-14	2.460-24
29	H + H202 >>> H0 + H20	2.760-14	2.950-65

30	24H0 + M >>> H202 + M	1.441)-13	1.080-24
31	HO + HOZ >>> H20 + OZ	1.579-11	1.980-63
32	24H02 >>> H2O2 + O2	4.210-12	1.940-42
33	HOS + HSO >>> HSOS + HO	6-110-35	8.570-13
34	NO + H + M >>> HNO + 1	1.200-14	3.040-25
35	NO + HO >>> NOS + H	7.190-34	4.92D-11
36	NO + HO + M >>> HNO2 + M	9.200-13	5.170-22
37	NO + HO2 >>> NO2 + HO	3.660-13	3.740-19
38	H + H + M >>> H2 + M	5.890-16	5.070-69
39	HN04 + M >>> H02 + N02 + 4	7.360-03	8.820-14
40	CLN03 + M >>> CLO + NO2 + M	4.760-04	7.770-14

HAPP RESIDENCE TIME STIBY

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T= 700 K, H= 25 km, 19 torr

R-NUM	REACTION	FORWARD HATE	BACKWAPD RATE
1	N205 + M >>> N02 +N03 + M	4.800 05	4.940-15
2	24NO3 >>> 241102 + 02	2.570-14	7.446-49
3	NO2 + NO3 >>> NO2 + NO + 02	5.510-14	3.970-36
4	NO3 + NO >>> 2*NO2	1.900-11	2.230-10
5	NO + 03 >>> NO2 + 02	2.650-13	4.540-24
6	NO2 + 03 >>> NO3 + 02	3.620-15	6.560-22
7	HN03 + M >>> H0 + N02 + M	4.010-02	6.700-14
A	HN03 + H0 >>> H20 + N03	H_00n-14	4.740-19
9	0 + 0 + M >>> 02 + M	9.500-17	6.210-21
10	0 + 02 + M >>> 03 + M	5.550-17	3.360 00
11	2045 <<< 50 + 0	7-110-13	8.630-43
12	0 + NO + M >>> NO? + "	4.010-15	2.140-11
13	0 + 002 >>> 00 + 02	1.110-11	8.500-27
14	0 + NO2 + M >>> NO3 + M	2.530-14	2.020-24
15	HO + HO >>> H2O + O	4.530-12	2.040-15
16	SON+S - SON+S + SO	7.040-39	9.370-21
17	NO2 + H-NI1 >>> NO + 0	0.0	0.0
14	So + H >>> H + 0	4.200-11	2-110-15
19	0 + 405 >>> 40 + 05	3.910-11	2.190-28
20	02 + H + M >>> H02 + "	2.750-15	6.180-06
21	03 + H >>> H0 + 02	4.78()-11	5.620-37
55	03 + HO >>> HO2 + O2	3.590-13	8.310-26
23	03 + HO2 >>> HO + 2*02	1.180-14	1.120-49
24	H + HO + M >>> H20 + 4	1.390-14	3.350-27
25	H + H05 >>> 2*H0	1.080-10	5.870-24
26	H + H05 >>> H5 + U5	2.550-11	8.030-20
27	H + H20 >>> H2 + H0	6.560-17	8.900-13
29	H + HSUS >>> HS + HUS	3.06N-13	1.770-19
29	H + H202 >>> H0 + H20	3.980-13	1.020-35

30	74H0 + M >>> H2G2 + M	1+140-14	1.040-04
31	HO + HOS >>> HSO + OS	4.050-11	7.730-33
32	54H05 >>> 4505 + 05	H+320-12	3.020-24
33	H02 + H20 >>> H202 + H0	15-057.5	3.070-12
34	NO + H + M >>> HNO + 15	2.910-15	2.200-06
<b>3</b> 5	NO + HO >>> HOP + H	2.230-21	2.020-10
36	NO + HO + M >>> HNO2 + M	4.760-14	5.930-03
37	NO + HOS >>> NOS + HO	3.600-12	2.680-14
38	H + H + M >>> H2 + 4	2.530-16	2.110-25
39	HN04 + M >>> HO2 + NO2 + M	5.57D 05	6.14D-15
40	CLN03 + M >>> CLO + NO2 + M	3.750 05	2.590-15

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T=800 K, H= 25 km

R-NUM	REACTION	FORWARD RATE	RACKWARD RATE
1	N205 + M >>> N02 +N03 + M	2.650 0o	3.700-15
5	S0 + 50M#S E0M#S	3.9417-14	5.950-48
3	NO + NO3 >>> NO + NO + CO	6.590-14	3.130-36
4	NO3 + NO >>> 2*1'02	1.900-11	1.740-14
5	NO + 03 >>> NO2 + 02	3.439-13	4.420-26
6	NOS + 03 >>> NO3 + 05	5.610-15	9.780-21
7	HN03 + M >>> H0 + NU2 + M	1.900 00	4.200-14
А	HN03 + H0 >>> H20 + N03	~.00D-14	2.43D-1A
٥	0 + 0 + M >>> 02 + M	7.080-17	1.870-16
10	0 + 02 + M >>> 03 + M	4.430-11	2.260 01
11	0 + 03 >>> 2*02	1.070-12	6.110-39
12	0 + NO + M >>> NO2 + 4	7.110-15	6.780-09
13	0 + NO2 >>> NO + O2	1.170-11	5.550-25
14	0 + NO2 + M >>> NO3 + M	2.210-14	1.770-24
15	HO + HO >>> H2O + O	5.000-12	1.060-15
16	02 + 2400 >>> 2402	6.400-39	8.780-20
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	0 + H0 >>> H + U2	4.200-11	9,550-15
19	0 + HOS >>> HO + OS	4.240-11	3,430-26
50	02 + H + M >>> HOP + 4	2.200-15	3.240-04
21	03 + H >>> H0 + 02	5.250-11	6.31D-34
55	03 + H0 >>> H02 + 02	4.300-13	3.24D-24
23	03 + HO2 >>> HO + 2402	1.489-14	2.350-40
24	H + H0 + M >>> H20 + 1	H•610=15	8.520-23
25	H + HUS >>> 5#HU	1.280-10	2.160-22
26	H + H02 >>> H2 + D2	2.710-11	1.450-26
27	H + H20 >>> H2 + H0	4.090-10	1.410-12
28	H + H202 >>> H2 + 402	3.430-13	9.470-18
29	H + H202 >>> H0 + H20	5.110-13	6.020-33

31	20H0 + M >>> H202 + H	H.500-15	7.010-03
31	HO + HOS >>> HSO + OS	4.441)-11	5.700-31
32	S#H05 >>> H202 + US	9.100-12	1.530-22
33	HO2 + H20 >>> H202 + H0	5.190-20	3,460-12
34	NO + H + M >>> HNO + 4	2.410-15	1.430-04
35	NO + HO >>> 1102 + H	3.300-20	2.300-10
36	NO + HO + M >>> HNO2 + A	3.421)-14	3.250-01
37	NO + HOS >>> NOS + HO	4.460-12	7.660-14
3A	H + H + M >>> H2 + M	2.210-15	2.330-21
39	HN04 + M >>> HO2 + NO2 + M	3.480 06	4.550-15
40	CLN03 + M >>> CL0 + N02 + M	2.430 06	1.500-15

	HADP UFSTOENCE	1111	STUDY						
LIME (C)	412115	<b>20</b> N	£00.	6.0	* ?	2	E () PM	우	
0.0	7.0000 08	4. COOD 64	2.000n us	FO 000007	_	~	C		-
۲.	950,	Ĭ.	0 1780.	1,2130 10	1. 1780 11	_	. 3680 0	.7710	1 0668
٠.	.1531,-0	.2751	_	1.755	-	-	3600 0	.384D	_
٤.	0-0600	OF 72.	-	=	4.4400 11	~	.4030 0	.5520	.8980 1
α.	8480-0	.169n		- =	٠٠,	-	. 3800 0	3910	980 1
°	13811-0	=	(15)	1. 1400 10	4. 1441) 11	1 (10)	960 0	.9870	70 1
٠,	0-0124.	.0750.	(:0 <b>+</b> 5.	1. 3530 10	11 (1941)	1000	500 0	.400D	2
۹.	.51An-0	9 (1440.				1 0007	0 0704.	6740	0268
9	0-(1/24.	0 (15 20.	0644.	<u>.</u> G		<b>-</b>	0 0255	CE SE	1 0768
æ	34917-0	0 0010	€ 20 ×	_	` '	7 0007	.5630 0	.4330	07.69
9	0-UZZZ	.00¢n	C245.	<b>~</b> .	7.0700 11	1 000/	0064.	9620	1 0/68
•	.2130-0	.00400	. 33.33 . 33.33	-	11 ((45)	٠,	0 (35) 0	(15.45.	2 :
٠,	1540-0	0 0 0 0	. 14.)		1. 659.1	1 000/	05 u I	0694	1 0768.
٠,	1000-0	0170	0906	٠.	1.0414.1	1 0007	0 (10***	37.5	7 0/68
٠,	.050.	.02M) 0	50%		-	7 0007	. 366D 0	:	07.69
c.	0-0800	0040	2025	~	1.3980 11	7000 1	.7620	0209	8970
٠,	.5410-0	0 6530	3420	450	1.3070 11	1 6007	0049	. 4 7.8D	1 0768.
•	.1530-0	0670		_	1 027	1 0007	0/8	0.34 (0)	1 0369.
e.	.7430-0	0 0040.	0100	-	1540 1	1 0007	1940	2110	8970
۰	.3507-0	0 08.60	٠,	1 600	1 CRRO.	1 0007	0415	01/0	7 0969
•	9730-0	1050	GII)	1 010	1 (6)	1 0007	06.00	0064	1 0868.
٧.	.6100-0		2.7720 118		. (500)	1 (100/	3100	0887	-
•	.2509-0	1300	6410	030	.2560 1	7000	310	•	1 0868.
•	0-6426.	~		050	. 3040 1	7000	6400	.506D	→ .
æ,	-0109	1520	.1970	1.4060 10	<b>-</b>	7000	081	.3680	1 0868.
9	-0162.	1510 0	0.450	970	1 0500	1 0007	0.16	6310	1 0969
ν.	0-0866	0071	0976	1.4080 10	1 0159.	1 0007	9.0	٠	1 0968
• •	0-0101		000	<b>-</b>	<b>-</b>	1 0007	0001.	0996	7 0000
۰	0-026 6.	מילטן. מימנסי	9	4 100 1	1 (810.	(100)	0 0000	0758	1 0060
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ָּי ר		- '	1000001	1 0017	2007	2007	0 00 36	(1400)	7 0000
` •	0-01/10				1 (1000)	7000 17	0 0200	7 3530 09	1 0000
9	4.22A0-05		; ;			1.7000 17	430D 0	2390	• •
Œ	0-CH10.	0 UHIC.	こまるへ	4140 1	.5710 1	7000	1510 0	1290	1 0668
	.8180-0	.2210	7 410	4150 1	1 0675.	7000 1	₹.	.0210	1 0668*
٠,	J-U829.	٠,		_	- O.	-	06H1.	.9160	.8990 1
٠.	4460-0	.2270	í Buði.	160 1	.0870.	000	.5680 0	.8150	1 0668.
ŝ.	0-LEZZ.	0 UUE2.	. 141.	160 1	1 (176%	7000	.5690 0	.7169	1 0668.
₩,	0-0801	.232n 0	0 0116	170 1	. 7140 1	10007	• 4880 0	0619	1 0668
9	0-4156	. 734n n	4591		1 00/4.	7000	.4180 0	.5250	1 0668
ď.	. ROZO-0	.2340 0	9740	1 4U 1	.433D 1	7000	3560 0	4340	1 0668.
4	-6660-F	.237F	•5140 0	- CR.	10.05	000	3000	.3460 0	1 0668
ô,	.525n-0	0 0662	0 (18/0.	1 061	1 790 1	10007	2480 0	•259D 0	066
æ,	.397n-n	0 0052	66410 0	1 061	1 0190	70007	. 2005 .	1750 0	1 0668
ç	0-(19/2	0 (1142)	0 (2) V	1 002	- CA44.	1 (100)	0.0961.	0 0560	1 0668.
Ņ.	.160n-0	2450	9 (3005)	1.4200 10	.4420 ]	7000	0 0011	140 0	1 0006
•	0-050	* i	3473	- G02	•	1 0007	0.0690.0	9 360	1 0006
٩	9460-0	2430	, 2130.0	1 6124	. 142)	1 0007	0220	9610 0	1 0006
08.7	0-0148.	(1447)	70 (1468)	1 (1124	•	0007		9;	1 0000
•	0-(15-67-	C \$ \$ \$ .	•	1.4210 10	1 0644.	1 000	Ť.	0917.	7 0006.

CLNU3	.4530-05	.4460-05	J	.1450-05	3	æ 1	20-0267	•	67 A D	•	9	7160-05	.7460-05	٦.	.8170-05	8550-05	.8940-05	. 9310-05 0485-05	0030-05	.0360-05	•	90-0960-	7	1480-05	1710-05	1920-05	2280-05	-2440-0	-2580-05	.271D-05	6.2830-05	3020-05	.3110-05	•	.3240-05	.330	•	33.40-05	•	3490-05	3510-05	6.3540-05	.3550-05	٣.	
404 5000 09	4	4.3H()-04	4	4	401)-04	540-04 5	24.1640=04 74.10±04 6	7730-04	2720-04	74.30-04	n er	7250-04	6990-04	6690-04 5	ın	98D-04	5570-04	C +0-UFIC**	180-04	3680-04	_	2620-04	_		•	6.042D-04 6	3.9310-04	.8760-04	3.8210-04 6	<u>.</u> .	3.7140-04 6	•	570-04	.507D-04	•457D-04	9 +0-0604	3610-04	.3150-04 3400-04	2240-04	1810-04	1380-04	<b>*0-0960</b>	0550-04	.0150-04	
4402 •0000 05	05	• 1860 96	90	46AD 06	• 0H0I) 06	. 706D 0	> <	4.940I) US	0.50	0000	7-1030 06	5600 0	0	.3670 0	.720n	0380 0		90 0585.6	0200		10	07	0	0680 07		1.0820 07	1.0890 07	10 0160	200	1.0900 07	0840 07	20	10 0610	0750 07	0690	0630 07	10 0150	0500 07	70 0450	0.0360 0.0280 0.0280	70 0020	0120	10 0400	9520 06	
					<del>-</del>	0040	20 clock c		1110		3 8	0140	0150	0115		3	0170	0110	1.0180 06	0180	0180	0100	190	0610	0190	0200	1.0200 06	0500	0500		1.0210 06		0510	0210	0510	0210	0570	1 0220 06	0220		0220	0550	0 520	1.0220 06	
1.4000 09				1.7710 09	Ξ,	<b>G</b> (	1. (46) 04					0164	0689	6410			6580	90 (1050°)		528D	620D					1.5840 09		5430		5490	1.350 09	5290	5230			5030		1.4910 09	47AD	4720	4660 0	4600 0		1.4480 09	
2,3000 07	4.554P 09		1.3720 09	1.1250 09		2	70 07 97 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1					3			1.7250 09			1.64/0 09								1.4130 09		3440 0	1.3220 09	1.3000 09	20 0357°I		2200 0	020	Ç (	1560 0	1 1330 60		0 000	0	0 7070	0	0410 0	1.0270 09	
90 0000 °1	1.7340 06	3.1150 06	こできる。	.714:1	8.4.140 05	<u>.</u>	- -		1,427710 07	100 0000		: 0	(1631)	1650 0	.23811	.3041)	_	0.14.	•	•	5870	2.6200 07	=		7020	2.7240 07	040		c		70 0564.0	091	0 U9		730 o	2.8800 07		0 (1000	0 (1)	0806	2,9130 07	9160	9200	2.9220 07	
. 0000	0.775.	• 4.3 30	.3740	935P	0.560	A430				1 2 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0.00	00.00	` ^	0587·	.831n	• 74	.7130 0	-2340		0500	.7250 0	.428n	.156n n	0606.	6790	3.4690 07	0.0960	.9310	.7780	6360	1.	2670	1600 0	.0600	.967n 0	29900	79%0 0	0 0077	5810	5170 0	4560 0	1.3990 07	3450 0	2950 0	
• 0000	.315n 1	.8410 1	.5150	.2Ann 1	.1030 1	. 6540 ]	ניילללי	וייייים.	1 (10114.		2700	8780 1	5270 1	.2170 1	.9420 ]	.6960 ]	.476n l	1 0112	1 0460	784.	.6470 1	.5220 1	.406n 1	.299n 1	.2001) 1	2.1087 11	1 05.40	.849n 1	.799n l	.7340 1	6150	5600	.5090 1	.4610 1	.415n l	.3710 1	.3300 1	1 (1167.	1 081C	1850 1	1530	1220	.0930 1	.0650 1	
TIME (<)	÷	⁴.	ç	α.	ç	٠.	•	۰	٠	٦,	۹۰		, <b>s</b>	ć.	٥.	•	9	9	•	*	٠,	8	ç	2	*	•	• •	2	•	ø,	E c	^	4	•	æ	ç	Ņ.	•	•	•	•	•	•	•	

T=250 K, H=30 km

9-10JH	REACTION	FORWARD RATE	BACKWARD RATE
1	N295 + 4 >>> NO2 +NO3 + M	1.940-06	6.060-14
2	20 + SONPS - CE	4.710-17	7.460-62
3	NO2 + NO3 >>> NO2 + NO + OS	4.210-15	1.190-34
4	NO3 + NO >>> 2+NO2	1.900-11	3.290-32
5	HO + Q3 >>> NOZ + Q2	6.360-15	1.080-56
•	NO2 + 03 >>> NO3 + 02	6-650-18	8.330-39
7	M + SON + DH M + EDMH	2.570-28	1.180-12
8	HN03 + H0 >>> H20 + N03	8-900-14	2.800-29
9	M + SO << M + D + O	1.290-15	3.300-5A
10	0 + 02 + M >>> 03 + M	2.760-16	7+740-17
11	0 + 03 >>> 2*02	1.920-15	0.0
12	0 + NO + M >>> NO2 + M	5.430-14	4.020-48
13	0 + NOS >>> NO + OS	5.120-12	6.270-53
14	0 + NO2 + M >>> NO3 + M	3.390-14	2.710-24
15	HO + HO >>> H2O + O	1-090-12	9.770-27
16	SON+2 * CON+2 + 20	2.750-38	3.880-35
17	NO2 + H-NU >>> NO + 0	0.0	0.0
10	0 + H0 >>> H + O2	4.200-11	7.730-25
19	0 + H05 >>> H0 + O2	1.080-11	5.450-60
20	05 + H + M >>> H05 + W	1.330-14	1.710-31
21	03 + H >>> H0 + 02	1.270-11	0.0
22	03 + HQ >>> HO2 + O2	2.750-14	1.040-48
23	03 + HOS >>> HO + 2*05	4.450-16	2.410-68
24	H + HO + M >>> H2O + M	2.710-13	0.0
25	H + HO2 >>> Z*HO	9.400-12	1.620-46
26	H + HOS >>> HZ + Q2	1.040-11	2.550-61
27	H + H2O >>> H2 + H0	2.340-28	1.140-15
29	H + H202 >>> H2 + H02	4.360-15	5.620-29
29	H + H202 >>> H0 + H20	1.090-14	1.350-75
30	SeH0 + M >>> H505 + M	1.550-13	4.160-32
31	HO + HOZ >>> H2O + OZ	1.120-11	3.890-74
32	5eH05 >>> H505 + 05	2.300-12	8.580-49
33	MOS + M20 >>> M205 + H0	1.020-39	5.490-13
34	NO + H + M >>> HNO + M	8.430-15	1.320-33
34	NO + HO >>> NO2 + H	3.05D-3H	3.010-11
36	M + SONH << M + DH + DN	1.110-12	4.20D-29
37	NO + HO2 >>> NO2 + HO	1.650-13	7.470-21
34	H + H + M >>> H2 + M	3.390-16	0.0
39	HN04 + M >>> H02 + N02 + M	5.800-06	1.070-13
40	CFM03 + M >>> CF0 + MOS + M	1.560-07	6.150-14

FIME (S)	K205		N02		N03	97	!			20			91	H20
•	4.0000	E (	4.2000		3.0000 06	\$	.5000 08			0008.	<u>•</u>	80 Q0QQ ·	3.0000 06	21 0002.1
02.0		E (	0102.4		3.0090 06	•	4 4 4 5 D B			(1004.)	<u>.</u>	* 0000 08	2,9910 06	21 0002-1
			0000		3,010,00	•		2.5000		0000	٠.		90 0716.2	1.2000 12
	0000		2060			•		-	. ~	8000	2	BO 000014	2.8770 06	1.2000 12
1.00	0000	e e	2010	66		•	RO 0624		_	9000	<u>.</u>	4.0000 08	2,8400 06	1.2000 12
1.20	4.000	K 0	4.7040		_	•			-	. 8000	9	4.000D 08	2,8040 06	1.2000 12
1.00	4.0040	9	4.2100		3.0620 06	;	.4010 08	_		0000	9	ō	2,7680 06	1.2000 12
1.50	4.0000	<b>E</b>	4.2110	_	3.0710 06	•	.3870 08		- 1	0000	9	4.0000 08	2,7330 06	1.2000 12
e	.0000.	z (	4.6130	7 6	3.0400 B		. 37.30 BR			0000	٠.	5 6	3 4450 04	31 0002-1
00.7		E 4	0.01		3.0890 00	• •	3450 08	2.5000			0 4	90 0000	90 0169.5	1.2000 12
2 2	0000		4.2175		0701					9000		Ö	2.5980 06	1.2000 12
2.40	4.0000	80	4.2190		_	•			_	0008	*	4.0000 08	2.5650 06	1.200D 12
2.90	4.0000	80	4.2190		_	•	-	_		0008	£	4.0000 08	2,5330 06	1.2000 12
3.00	4.0000	60	4.2210	_		•	-	2.5000	•	0008	9	4.0000 BB	2.5020 06	1.2000 12
3.20	4.0000	90	4.2220		3,1420 06	•		2.5000	د د	9000	9	4.0000 08	2.4710 06	1.2000 12
3.40	4.0000	60	4.2240			•	_	2.5000	۰. د به	8000	9	4.0000 08	2.4400 06	1.2000 12
3.60	*.000°	6	4.2250		3.1600 06	•		2.5000	 	9000	9	ō	-	1.2000 12
3.50	4.0000	<b>6</b>	4.2260		3.1690 06	•	•2350 08 5155 08	2.5000	·,	0008	•	õ	2.380D 06	21 00021
00.	0000	60	0422.4	_		•		0005-2	٠,	2008	<u>.</u>	5		21 0002*1
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	.0000	60	7300	0		•	1950 08	2.5000	·,	0006	•	õ	2.2940 06	21 00021
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\$ .00	4.999	. e	4.2410	_	2681)	•		2.5000 1	7	0000	9	4.0010 08		1,2000 12
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6.60	4.0000	£	4.2440	_	2950	•	-		~	0008	9	õ	0000	1.2000 12
5.00	4.3000	£ 1	4.7460	60	3.3040 06	•	.0370 08	-	~	0008	9	ō	1.9850 06	1.2000 12
7.00	4.0000	E (	4.24.70		3135	•	_		_ '	9000	9	ō	1.9610 06	1.2000 12
1.50	0000	F 6	- V - H	•	3.3220 06	•	00110 08	0005.2		0000	٠.	# 0100 0H	90 0964.1	1.6000 12
			152.4		100	ה	3. 9860 BB	•		2000	<u>.</u>	4.0100.4	1.8940 06	1.2000 12
7.80	4.9000	5	4.2520		3507	, (1)	_		. ~	0000	و د	4.0010 08	1.9720 06	1.2000 12
9.00	4.000	Ē	4.2530		3,3590 06	9.0	_	-		8000	9	4.0010 08	1.8500 06	1,2000 12
02.8	4.0000	69	4.2550		3,3687 06	ŕ	_			8000	9	4.001D 08	1.8290 06	1.2000 12
9.40	4.0000	60	4.2560	ċ	3,3770 06	~	_	2000	۲.	8000	9	4.001D 08	1.6080 06	1.2000 12
8.50	4.0000	60	4.2570	0	346.)		3,9230 08	2000	~	000R	•	4.0010 08	1.7870 06	1.2000 12
9.80	4.0000	80	4.2540		3950		_		, ·	8000	9	4.0010 08	1.7670 06	1.2000 12
00.0	4.0000	9 9	4.2600		000	m (	80 0868		- 1	.8000	9	4.0010 08	1.7470 06	1.2000 12
9.20	4.0000	8 6	4.2610	60	3.4130 06		-	2000		6000	٠ و	4.0010 08	1.7270 06	27 0002.1
	4.0000	9 6	0202.		3.466.00	יי יי	90 067			0000		90 0100**	1.7080 00	21 0407 1
	0000-	8 8	06020	2 9	3.4410	7 .	3.0010 08	0000		00001		80 0100-	1.0550 00	21 2402:1
		5 6	0446	5 6	3 45 00 00	2 0	200	2 6000			2 2	0700*	10,00	
		Š	1000	2	20 0000	•	200					00 01000	AA 070001	11 000701

	1	<b>H</b>	70 <del>1</del>	4202	ONI	HNOZ	40NH	CLN03
-	•0000	1.0000 06	2.5000 07	1.2000 09	1.0000 04	8.0000 05	1.5000 09	2.000D 06
-	.60-0-03	-		1. 2000 no	1.0000 06	6.0030 05	1.5000 09	2.0000 08
~	50-6244	_		1.2000 09		6.0060 05	_	2.0000 OR
	00-00-0					6.00000	- '	0000000
2	3.1210-05	1.0000) 06	2.6160 07	1.2000 09	1,0000	20 0510.A	1.5000 000	2,0000 68
9	1.0340-06		2.4170 07		1.0000 06	8.0170 05	_	2.0000 08
2.0	9970-06	_	2.6200 07	1.2000 09	3.0000 06	8.0200 05	1.5000 09	2.000D 08
٠.	.9580-06	_	2,6230 07	1.2000 09	1.0000 06	8.0230 05	1,5000 09	2.000D 08
	90-0616	- '	2.6260 07	1.2000 09	1.0000 06	6.0250.0	1 5000 09	80 0000
0 0	00-0164	1.0000	2.6320.07	1.2000 09	90 0000	20 0000	1.5000	2,000.5
	90-0406	-	2.6350 07	1.2000 09	1.0000 06	8.0330 05	• •	2,0000 08
~	.7710-06	1.0000 06	2.6370 07	1.2000 09	1.0000 04	8,0350 05	1.5000 09	2.0000 OR
~	.735D- 06	1.0000 06	2.6400 07	1.2000 09	1.0000 06	8,0380 05	1.5000 09	2.000D 08
~	.7010-06	1.0007 06	2.6430 07	1.2000 09	1.0000 06	8.0400 05	1.5000 09	2.0000 08
2.	.6670-06	_	2.6460 07	1.200D 09	1.0000 06	8.0430 05	1.5000 09	2.0000 08
~	.6330-06	1.0000 06	2.6480 07	1.2000 09	90 0000	8.0450 05	1.5000 09	2.001D 08
~ .	•600n-06	•	2.6510 07	1.2000 09	90 0000 1	8.0470 05	1.5000 09	20010 08
2 .	-57 CD-00	1.0000 00	2 4540 01	1.2000 000	90 0000	0.0500	40 000c*	20000
	50-0505.	1.000	2.6580 07	50 G002-1	3.0000.0	A.0340 AS	1.5000 09	2.0010 08
	4720-06	1.0000 06	2.5510 07	1.2000 09	1.0000 06	8,0560 05	1.5000 09	2.0010 08
~	.441n-06	_	2,6630 07	1.2000 09	1.0000 06	8.0560 05	1.500D 09	2.0010 08
2.	.4110-06	1.0000 06	2.6660 07	1.2000 09	1.0000 06	8.0600 05	1.5000 09	2.0010 06
~	3910-96	_	2.6680 07	1.2000 09	1,0000 06	8,0620 05	1.5000 09	2.0010 08
~	3520-06	1.0000 06	2,6700 07	1.2000 09	3,0000 06	8,0640 05	1.5000 09	2.0010 08
	.3630-05		10 (12) 0.2	40 000C	2000	2000000	1.5000 000	0100.0
	00-0292	1.0000	2.6770 07	1.2000 09	1.0000	8.0700 05	1.5000 09	2-0010 06
~	-2390-06	1.0000 05	2.6790 07	1.2000 09	1.0000 06	8.0720 05	1.5000 09	2.0010 08
2.	.2120-06	1.0000 06	2.6810 07	1.2000 09	1.0000 06	8.074D 05	1.5000 09	2.0010 08
?	.1950-06	_	2,5830 07	1.2000 09	1.0000 06	8.0760 05	1.5000 09	2.0010 08
N, C	1345-06	1.0000 06	2.6850 07	1.2000 09	1.0000 06	8.07.80 05	1.5000 09	2.0010 68
: <	1080-06	1.0000 06	2.6890 07	1,2000 09	1.0000 06	8.0810 05	1.5000 09	2.0010 08
N	.0830-06	1.0000 06	2.6910 07	1.2000 09	1.0000 06	8.0830 05	1.5000 09	2.0010 0A
2	90-0650.	~	2.6930 07	1.2000 09	1.0000 06	8.0850 05	_	2.001D 08
Ň	.0340-06	_	2.6950 07	1.2000 09	1.0000 06	8,0860 05	1.5000 09	2.0010 08
~	.010n-05	_	2.6960 07	1.2000 09	1.0000 06	8.0880 05	1.5000 09	2.0010 08
_	.9870-06	_	2.6980 07	1.2000 09	_	8.0900 05	1.5000 09	2.0010 08
-	.9649-06	_	2,700D 07	0	1.0000 06	8.0910 05	1.5000 09	2.0010 08
=	94-10-06	_	2.7020 07	1.2000 09	1.0000 06	8.0930 05	1.5000 09	2.0010 06
-	90-0616	_	2.7030 07	1.2000 09	Ō	8.0940 05	1.5000 09	2.0010 08
-	.894n-06	•	2. 7050 07	1.2000 09	ŏ	8.0960 05	1.5000 09	2.0010 08
	00-05/90	00001	20,070,07	1.2000 09	1.0000 05	8.0970 05	1.5000 09	2 0010 08
-	8220-06	40000	2,7100 07	1,2000 00	1.0000 000	8.0000	20000000	
: -	-6110-06	1.0000 06	2,7120 07	3.2000 09	2000.	8.1020 05	1.5000 09	2.0010 00
-	.7910-06	1.0000 06	2.7130 07	1.200D 09	1.0000 06	8,1030 05	1.5000 09	2.0020
-	.7710-06	1.0000 06	2.7150 07	1.2000 09	1.0000 06	8.1050 05	1.5000 09	2.6020 00

T=300 K, H=30 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + M	1.570-03	2.840-14
5	2*N03 >>> 2*N02 + 02	2.410-16	1.750-58
3	NOS + NO3 >>> NOS + NO + QS	A.210-15	4.920-34
•	SON+5 >>> SON+5	1.900-11	6.980-29
4	NO + 03 >>> NO2 + 02	1.670-14	2.850-49
6	NOS + 03 >>> NO3 + 05	3.410-17	2.000-34
7	HN03 + M >>> HO + NO2 + M	1-920-21	6.220-13
A	HN03 + H0 >>> H20 + N03	8.000-14	1.250-26
9	0 + 0 + H >>> 02 + H	5.900-16	1.260-5a
10	M • 60 * M + 50 • 0	1.640-16	1.310-09
11	0 + 03 >>> 2+02	8.900-15	0.0
12	N + SON << M + ON + O	3.060-14	1.200-38
13	0 + NOS >>> NO + OS	6.250-12	3.730-46
14	M + EON << M + SON + 0	2.820-14	2.260-24
15	HO + HO >>> H2O + O	1.570-12	4.63D-24
16	05 + SeNO >>> S#M05	1.930-38	2.260-31
17	NOS + H-NU >>> NO + 0	0.0	0.0
19	0 + 40 >>> H + 05	4.200-11	2.160-22
19	U + HUS >>> HO + OS	1.510-11	8.510-52
20	02 + H + M >>> 405 + M	7.960-15	6.500-25
<b>S</b> 1	03 + H >>> HO + 05	1.790-11	1.620-69
55	03 + HO >>> HOS + 05	5.350-14	8.980-43
23	03 + HOS >>> HO + S+OS	1.04D-15	1.530-63
24	H + HU + M >>> HSO + M	1.410-13	1.140-75
25	M + HO2 >>> 2*HO	1.770-11	1.140-40
26	H + HO2 >>> HZ + OZ	1.310-11	6.800-53
27	H + H2O >>> H2 + H0	2.180-25	6.410-15
28	H + H202 >>> H2 + H02	2.130-14	2.960-26
29	H + H202 >>> HQ + H20	2.760-14	2.950-65
30	2+M0 + M >>> H202 + M	7.080-14	5.17D-25
31	HO + HO2 >>> H20 + OZ	1.570-11	1.980-63
32	24H05 >>> H505 + 05	3.210-12	1.980-42
33	HOS + HSO >>> HSOS + HO	6.110-35	8.570-17
34	NO + H + M >>> HNO + M	5.750-15	1.470-26
35	NO + NO >>> NO + H	7.190-34	4.920-11
36	NO + HO + M >>> MNO2 + M	4.410-13	2.470-22
37	NO + HOZ >>> NOZ + HO	3.660-13	3.740-19
3A	H + H + M >>> H7 + M	2.820-16	2.430-69
39	HN04 + M >>> H02 + N02 + H	3.85D-03	4.650-14
40	CFN03 + M >>> CF0 + NOS + M	2.2AD-04	3,940-14

HAPP RESIDENCE TIME STUDY

1146 (4)	1205		40v		N03		92		03		95		HVO3	9		02H	
0.0	4.0000	8	-	60	3.0000		4.5000	80	2.5000 1	~	7.8000	9	4.0000 08	3.0000	٥ ل	1.2000	2
0.70	3.944D	4	4.2050 4	6	3.1920	90	4.46.30	æ	2.500D 1	^	7.4000	÷	4.0000 0A	5.0000	\$0 C	1.7000	~
0.40	3.9970	99	_	3.	3.3830		4.4550	40	1 000ו>	~	7.8000	ž	4.000U 0H	2.4320	90 0	1.2000	~
0.60	3,9950	80	_	60	3,5741		4.3860	08	2.5000 1	Ņ	7.8000	:	_	2.8680	90 0	1.2000	75
0.40	3,9950	8		60	3,7650		4.3520	80	2.5000 1	٠,	7.8000	<u>.</u>	4.0000 08	2.8050	900	1.2000	2 :
1.00	3.9940	80		o .	3.9569		4.3160	E (	2.5000	~	7.800D	9	_	2.147	900	1.2000	2 :
1.20	3.9920	£ 6	0622.4	2 0	4.1460		00H2.	5 6	2.5000	ų,	7.800n	9 ;		2.6400	900	0002-1	2:
	11000	E 4		• 0	5270	9 4	0405		00000	ųο	7.0000	91	0000	2 5820	9 6	1000	2 -
	0860		-	. 0	4.7170		1730	æ	0004.5	۰, ۸	7.8000	9	40000	2.531		0002-1	2 2
2.00	3.9870	. 6	_	. 6	4.9060		4.1380	9	2.5000	٠,	7.800D	9	4.000D 08	2.483	90	1.2000	2
2.20	3,9460	6	_	6	5.1950	9	4.1040	99	2.5000 1	٠.	7.800D	16	4.0000 08	2.4360	90 0	1.2000	2
2.40	3.9850	60	4.2540	6(	5,2450	90	4.070n	99	2.5000 1	~	7.8000	16	4.0000 08	2.3910	0 و د	1.2000	- 15
2.60	3.9840	5	4.2520	60	5.4740		4.0369	60	2.5000	Ŋ	7.8000	16	_	2.3480	90 0	1.2000	12
2.80	3,982n (	60	4.267D	•	5,6630		4.002D	90	2.5000 1	۰,	7.8000	<u>ب</u>	4.0000 08	2.3070	90 0	1.2000	2
3.00	3,9910	60	4.2710	5	5.4520	9 ;	3,9690	£ .	2.5000	N, I	7.8000	9:	4.0000 08	2.2680	900	1.2000	2:
3.20	3.9400	9 6	09/2.4	2 0	00000	9 6	3.4350	9 5	0000	ų r	7.5000	9 :	90 0000	2.630	9 6	0000	2.5
2000	0.70	E 6	0002.	2 9	0 . 6 6 7 1		3.9030	D 0	0005.5	ų (	4.6000	9	90 0000	0.61.7	9 6	00000	2:
0.00	3.47.50	0 0	10000		41.4	9 4	00.00 E	C 0	0000	م ب	0000	9 1	4 0000	2.127		1000	2 .
	10750		0400		6.7930	9	3.8060	8	2000	٠,	7.8000	<u> </u>	4.0000	2.0450	9	1.2000	: _
- 20	3.9740	<b>E</b>	4.2980	6	6.9800		3.7740	90	2.5000	. ~	7.8000	9	4.0000 08	2.0650	90	1.2000	15
4.40	3,9737	60	4.3030	6	7.1580		3.7420	98	2.500D	~	7.8000	9	4.0000 08	2.0370	90 0	1.2000	2
4.60	3.9710	80	4.3070	6	7.1550	90	3.7110	80	2.5000 1	~	7.8000	9[	4.0000 08	2.0100	90 0	1.2000	21
4.80	3.970h (	80	4.3110	6	7.5430	9	3.6800	90	2.5000 1	~	7,8000	92	4.0000 08	1,9840	90 0	1.2000	21
2.00	3.959n t	Œ C	4.3150	6	7.7300		3.6490	98	2.5000 1	~	7.8000	9	4.0000 08	1.9590	90 0	1.2000	2
5.29	3,9680 (	60	4.320D (	٠	7.9170		3.6190	90	2.5000 1	۸.	7.8000	÷.	4.0000 08	1.9360	90	1.2000	2 :
5.40	3.9450 (	6	4.3240	œ .	8,1030	90	3.5890	90	2.5000 1	~	7.8000	<b>9</b>	4.0000 08	1.9140	90 0	1.2000	2
5.60	3.9450	<b>8</b> 0 !	4.3240	<u>.</u>	8.790n	90	3.5590	60	2.5000 1	٠,	7.8000	9[	4.0000 08	1.8940	90 0	1.2000	2
5.80	3.9540	E (	4.33An	6	8.4770	-	3.5290	6	2.5000	~	7.9000	9	* 0000 OB	1.874	900	1.2000	2:
00.9	3.9530	E 6	4.337D	<u>.</u>	8.6630	-	1.4990	80	2.5000	~ (	7.8000	9:	4.0000 08	1.8560	8	1.2000	2:
9.0	0146	r ø		2 9	0.00	9	3.4.6	9 0	0005.2	v	7.8000	9 :	90 0000	1.6380	9 6	3.2000	2 ^
	1.9590	, e	3490	. 6	9.2220	9	3.4.5	0 E	2.5000	۰ ۸	7.8000	2 4	4-0000 08	1.807		1.2000	. ~
6.80	3.9530	80	4,3530 (	•	9.4080	9	3,3840	90	2.5000 1	. ~	7.8000	9	4.000D 08	1.7920	90	1.200D	2
7.00	3.9560	90	4.3570	6	9.5930	90	3,3550	96	2.5000 1	~	7.8000	91	4.0000 08	1.7790	90 0	1.2000	- 12
7.20	3.955n (	£ 0	4.3619 (	•	9.1790	90	3,3270	C	2.5000 1	~	7.800D	16	_	1.7670	90 0	1.2000	12
7.40	3.9540	9	4.3650	6	9.9650	9	3.3000	õ	2.5000 1	~	7.8000	16	4.0000 08	1.7560	90 0	1.2000	2
7.60	3.9430	8	4.3690	6	1.0150	20	3.2720	0	2.5000 1	~ .	7.8000	٤.	4.0000 08	1.7450	90	1.2000	2 :
1.50	1150	9 0	(15.15.4)	2.5	(1961)	2	000000	0	0005-2	<b>.</b>	00087	<u>.</u>	BO 0000**	1.1350	90	0007-1	7:
9.00	3.9500	E 9	0116	2 9	1,020	20	3.6170	9 0	2.5000	<b>.</b> .	7.8000	<u> </u>	90 0000	1.7270	9 6	1.2000	2:
9.50	0.000	9 6	0166.	2 9	61/0-1	2 6	3.1910	9 6	2.5000	<b>.</b> .	00000	9 ;	80 0000.		9 2	1000	2 :
	0.00000 E	D 9	0400	2 9		5 6	3.1040	0	1 0004.5	٠,	00000	9 :	90 0000 **	2017		0002-1	<u> </u>
	3 9450	. a	1000	. 0	1000		2011	D 0	2 6000	۰,	1000	9 1		7000			2 ^
	2.0440		13660		1 1 5 5 5	2	0.0850 E	9	2.5000		2000	9 4	0000	2004		1.2000	. ^
02.6	3.9430	E C	4.4000	. 0	1.1630	6	3.0540	80	2.5000	٠ م	7.8000	9	4.0010 08	1.6910	9	1.2000	2
9.40	3,9420	80	4.4030	6	1.1820	20	3.0340	80	2.5000	. ~	7.8000	16	4.001D 08	1.6870	90	1.2000	2
9.60	3.9400	8	4.4070	<u>\$</u>	1.2000	6	3.0080	90	2,5000 1	~	7.8000	16	4.0010 08	1.6850	90	1.2000	2
4.89	3.9390	80	4.4110	6	1.2180	07	2.9830	80	2.5000	~	7.8000	91	4.001D 08	1.6920	90 0	1.2000	12
••••	3.9380 (	80	4.4150	6	1.2370	0.7	2.9580	90	2.5000 1	~	7.800D	16	4.0010 08	1.6810	900	1.2000	2

0.6 2,7160 07 1,2000 09 1,0000 06 8,000 09 1,4990 09 1, 4990 09 1,		1	CH.	H02	,	H202	ONH		I		•	40NH		CLNO3	:
10000   05   2.0450   07   1.2000   08   1.0000   08   1.0000   08   1.0000   09   1	1.000.	90 0	1.0000 06	2.500	200	1.4000	60.	90 00	o o			0000	•	20000	
1,0000   06   2,0810   07   1,0000   06   8,0001   05   1,4970   09   1,0000   06   8,0000   05   1,4970   09   1,0000   06   8,0000   05   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09   1,0000   06   1,4970   09	1.19 5	1-03	1.0000		16	1.2000 0	00.1	90 (10	Ė	0020		11167	60	2.0000	. E
1,0000	1.5430	*0-		~	0 07	1.2000 0	00.1 6	90 00	8	0030 0	5.1	0269	60	2.000D	90
1,000, 06 3,446	7.890F	50-0	_		0 07	1.200D 0	00.1 6	90 00	æ (			0564		2.0000	60
1,0000	5.957				20	1.2000	00.1	9	ė			0664	2 6	20000	9 6
1,0000 06 3,5660 07 1,2000 09 1,0000 06 8,0100 05 1,4901 09 1,0001 10 00 1,4660 07 1,2000 09 1,0000 06 8,0110 05 1,4901 09 1,0000 10 0 3,4901 07 1,2000 09 1,0000 06 8,0110 05 1,480 09 1,480 09 1,0000 06 8,0110 05 1,480 09 1,480 09 1,0000 06 8,0110 05 1,480 09 1,480	6.812	9-02	_		7 u 0	1.2000 0	9 1.00	90 00	•	0080 0	5	0261	60	0666.1	90
1,0000	6.674	20-0	_	(m) r	7000	1.2000 0	00.	90 00	œ ·	0 0600		0164	60	0666	80 6
1,000, 06   3,926, 07   1,200   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   8,0110   05   1,485   09   1,000   06   4,437   07   1,200   09   1,000   06   8,0110   05   1,475   09   1,000   06   4,437   07   1,200   09   1,000   06   8,0110   05   1,475   09   1,475   09   1,000   06   8,0110   05   1,475   09   1,000   06   8,0110   05   1,475   09   1,475	414	0.00		• •	5 6	2000		200	•	2010		700	<b>.</b> 0	0000	9 6
1.0000	795	50-0	_		, c	1.2000 0	00.1	900	6	0110		6870	60	0666	8
1,0000 06	6.179	50-0	_	-	0 07	1.2000 0	9 1.00	90 00	60	0120 0	2	4850	60	0666.1	80
1,0000 06	5.067	9-02	_	*	n 07	1.2000 0	9 1.00	90 00		0130 0	5	4850	60	0666*1	90
1,0000 05	5.961	50-6	_	•	200	1.2000 0	00.1	90 00	ė	0140		4840	60	0666.1	8
1,0000   06	4.459	50-0		•	0 04	1.2000 0	00.1	8	•	0 250		0830	6	0666*1	8 6
1,0000   06	707.0	2 d	-	• •	56	1 20.00		900	ė a	960			<b>.</b>	0000	9 6
1,0000 06	5.57.8	2010	_			1.2000 0	00-1	00 00	é	0170		4790	60	0666	9
1,0000 06	5.493	50-0	_	•	20 0	1.2000 0	00.1	90 00		0 0010	2	4780	60	06661	8
1,0000 06	5.411	n-05	_	•	0 07	1.2000 0	9 1.00	90 00		0180 0	2	4770	60	0866.1	80
1,000	5,334	9-05	_	-	£ 0.0	1.2000 0	9 1.00	90 00	•	0190 0	5	4760	60	1.9980	8
1,0000 05	5.26	50-0	•	-	0 0.	1.2000 0	00.1	90 00	6	0 0026		0524	60	1.9980	9
1,000	5.190	50-0	-	v.	~ ;	1.2000 0	00.1	90 00	<b>.</b>	0 0120		0.0	50	0966	8 9
5 1.0000 06 5.8010 07 1.2000 09 1.0000 06 8.0220 05 1.4090 09 1.0000 06 8.0220 05 1.4090 09 1.0000 06 8.0220 05 1.4090 09 1.0000 06 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.4020 09 1.4000 00 8.0220 05 1.4090 09 1.4000 00 8.0220 05 1.40	2010	20-07		~ 4	2 6	1.2000		900	• a	0170		02/	2 0	1966	8 8
5 1,0000 06 5,4010 07 1,2000 09 1,0000 06 8,0230 05 1,4690 09 1,0000 06 6,0310 05 5,4610 09 1,0000 06 8,0240 05 1,4680 09 1,0000 06 8,0240 05 1,4680 09 1,0000 06 8,0240 05 1,4680 09 1,0000 06 6,3460 07 1,2000 09 1,0000 06 8,0250 05 1,4640 09 1,0000 06 8,0250 05 1,4640 09 1,0000 06 8,0250 05 1,4640 09 1,0000 06 8,0250 05 1,4640 09 1,0000 06 8,0250 05 1,4640 09 1,0000 06 8,0250 05 1,4640 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,4620 09 1,0000 06 8,0250 05 1,4620 09 1,46	2000	50-0				1.2000 0	6	90 00	ė	9220 0		202	. 0	0866	8
1,0000   06   5,9160   07   1,2000   09   1,0000   06   8,0220   05   1,4680   09   1,0000   06   6,0220   05   1,4680   09   1,0000   06   6,0220   05   1,4680   09   1,0000   06   6,2760   07   1,2000   09   1,0000   06   8,0250   05   1,4650   09   1,0000   06   6,2760   07   1,2000   09   1,0000   06   8,0250   05   1,4650   09   1,0000   06   8,0270   05   1,4650   09   1,0000   06   8,0270   05   1,4650   09   1,0000   06   8,0270   05   1,4650   09   1,0000   06   8,0270   05   1,4650   09   1,0000   06   8,0270   05   1,4650   09   1,0000   06   8,0270   05   1,4650   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4500   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,0000   06   8,0270   05   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09   1,4400   09	E 40 . 4	0-05	_	S)	20 0	1.2000 0	0 1.00	90 00	•	0230 0	2	0699	60	1.9980	90
1,0000 06 6,0310 07   1,2000 09   1,0000 06 8,0240 05   1,4650 09   1,0000 06 6,1460 07   1,2000 09   1,0000 04 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0250 05   1,4650 09   1,0000 06 8,0220 05   1,4650 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4550 09   1,0000 06 8,0220 05   1,4450 09   1,0000 06 8,0230 05   1,4450 09   1,00	4.889	9-05	_	Š	0 01	1.2000 0	9 1.00	90 00	6	0540 0	5 1.1	089	60	1.9980	80
1,000	4.834	50-0		•	200	0 0002.	00.1	90 00	e c	0540	5	0.04	60	08667	9
1,000   06   6,374   07   1,200   09   1,000   06   8,025   05   1,463   09   1,000   06   6,489   07   1,200   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,462   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,450   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   07   1,200   09   1,000   06   8,025   07   1,200   09   1,000   06   8,025   05   1,440   09   1,000   06   8,025   02   1,440   09   1,000   06   8,025   02   1,440   09   1,000   06   8,025   02   1,440   09   1,000   06   8,025   02   1,440   09   1,000   06   8,025   02   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,440   09   1,4			_	0 4	200	1.2000		90 00	e a	0 0520		000	5 0	0956	6 6
1,000 06 6,4890 07 1,2000 09 1,000 06 8,0250 05 1,4620 09 1,000 06 8,0250 05 1,4620 09 1,000 06 8,0250 05 1,4610 09 1,000 06 8,0250 05 1,4610 09 1,000 06 8,0250 05 1,4610 09 1,000 06 8,0250 05 1,4610 09 1,000 06 8,0250 05 1,4500 09 1,000 06 8,0250 05 1,4500 09 1,000 06 8,0250 05 1,4500 09 1,000 06 8,0250 05 1,4500 09 1,000 06 8,0250 05 1,4500 09 1,000 06 8,0250 05 1,4500 09 1,000 06 8,020 05 1,4500 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,450 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,000 06 8,020 05 1,440 09 1,440 09 1,000 06 8,020 05 1,440 09 1	4.704	90	_	. •	0	1.2000	00-1	9	e e	0250		10.00		0800	8
1,000,0   06 6,7160   07   1,200,0   09   1,000,0   06   0,0270   05   1,4610   09   1,000,0   06   0,0270   05   1,4610   09   1,000,0   06   0,0290   05   1,4590   09   1,000,0   06   0,0290   05   1,4490   09   1,000,0   06   0,0290   05   1,4490   09   1,000,0   06   0,0290   05   1,4490   09   1,000,0   06   0,0290   05   1,4490   09   1,000,0   06   0,0290   05   1,4490   09   1,000,0   06   0,0290   05   1,4490   09   1,000,0   06   0,0290   09   1,000,0   06   0,0290   09   1,000,0   06   0,0290   09   1,4490   09   1,000,0   06   0,0290   09   1,4490   09   1,4490   09   1,000,0   06   0,0290   09   1,4490   09   1,000,0   06   0,0290   09   1,4490	4.664	50~0	_	٠	10 07	1.2000 0	9 1.00	00 00		0 2920	-	4620	60	0266.1	6
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1,0000   05   0,000   07   1,2000   09   1,0000   06   0,0280   05   1,4590   09   1,0000   06   0,0280   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1,0000   06   0,0290   05   1,4590   09   1	. 59	50-03	_	•		1.2000 0	00.	90 00	æ .	0290	2	009	60	0.66.1	8
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5 1.0000 06 7.7290 07 1.2000 09 1.0000 04 8.0120 05 1.4500 09 1 5 1.0000 06 7.8410 07 1.2000 09 1.0000 06 8.0130 05 1.4460 09 1 5 1.0000 06 8.0630 07 1.2000 09 1.0000 06 8.0130 05 1.4460 09 1 5 1.0000 06 8.1550 07 1.2000 09 1.0000 06 8.0130 05 1.4460 09 1 5 1.0000 06 8.2550 07 1.2000 09 1.0000 06 8.0130 05 1.4450 09 1 5 1.0000 06 8.3960 07 1.2000 09 1.0000 06 8.01350 05 1.4450 09 1	4.402	90-0	-	_	0 07	1.2000 0	9 1.00	00 00	ě	0320 0	2	4510	6	1.9970	80
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5 1,0000 06 8,2850 07 1,2000 09 1,0000 06 8,0000 05 1,4450 09 1 5 1,0000 06 8,3960 07 1,2000 09 1,0000 06 8,0000 05 1,4440 09 1 5 1,0000 06 8,3960 07 1,2000 09 1,0000 05 8,0090 05 1,4430 09 1		0-02		6 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2 6	1.2000	00.	90 00	•	0 0150	-	000	2 6		: :
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	4.33	20-05			_	1.2000 0	00.7	00 06		0350		90		9	3

T=700 K, H=30 km

R-NU	REACTION	FORWARD HATE	BACKWAHU RATE
1	N205 + M >>> NO2 +NO3 + M	2.300 05	2.360-15
2	\$*H03 >>> Z*H02 + 02	2.570-14	7.440-49
3	SO + 00 + 50M <<< 50M + 20M	5.510-14	3.970-34
•	NO3 + NO >>> 2*NO?	1.900-11	2.230-19
5	NO + 03 >>> NO2 + 02	2.650-13	4.540-28
4	NO2 + 03 >>> NO3 + 02	3.620-15	6.560-22
7	HN03 + M >>> HO + NO2 + M	1.920-02	3.210-14
•	HN03 + H0 >>> H20 + N03	8.000-14	4.74D-19
9	0 + 0 + M >>> 02 + M	4.550-17	1.420-21
10	0 + 02 + M >>> 03 + M	11-088.5	1.610 00
11	0 + 03 >>> 2+02	7.110-13	8.63D-43
12	0 + NO + M >>> NO2 + M	4.320-15	1.020-11
13	0 + NOS >>> NO + OS	1.110-11	8.500-27
14	0 + NO2 + M >>> NO3 + M	1.210-14	9.680-25
15	HO + HO >>> H2O + O	4.530-12	2.040-16
16	05 + 5+00 >>> 5+005	7.04D-39	9.370-21
17	0 + 0A <<< UN-H + 50A	0.0	0.0
14	0 + H0 >>> H + 02	4.200-11	2.110-15
19	0 + H05 >>> H0 + O2	3.910-11	2.190-28
20	02 + H + M >>> H02 + M	1.320-15	2.960-06
51	03 + H >>> H0 + 02	4.780-11	5.620-37
55	03 + HO >>> HO2 + D2	3.590-13	8.310-26
53	S0#S + 0H << S0H + E0	1.180-14	1.120-49
24	H + H0 + M >>> H20 + M	6.670-15	1.600-27
25	H + H05 >>> 5+H0	1.080-10	5.870-24
24	H + HUS >>> HS + OS	2.550-11	8.030-20
27	H + HSO >>> HS + HO	6.560-17	8.900-13
20	H + HSOS >>> HS + HOS	3.060-13	1.770-18
29	H + H202 >>> H0 + H20	3.980-13	1.020+13
30	54H0 + M >>> H2O2 + M	5.470-15	5.000-05
31	HO + HOS >>> H20 + O2	4.060-11	7.730-33
32	20 + 202H <<< \$0H9\$	H+320-12	3.020-24
33	HOS + HSO >>> HSOS + HO	2.720-21	3.070-12
34	NO + H + M >>> HNO + 4	1.390-15	1.050-06
35	H + SOM << OH + ON	2.230-21	2.020-10
36	NO + HO + M >>> HNO2 + M	41-08S.S	2.840-03
37	0H + SON <- < SOH + ON	3.600-12	2.680-14
34	M + SH <<< M + H + H	1.210-16	1.010-25
39	HN04 + M >>> H02 + N02 + M	3.350 05	3.130-19
40	CLN03 + M >>> CLO + NO2 + M	1.800 05	1.270-15

	HAPP RESI	HAPP RESIDENCE TIME STUDY	STUDY						
TIME (S)	4205	NO.	₩03	Õ	60	20	HWO3	9	H20
•	4.000n 04	4.20AD 09	_	4.500n 0B	2.5000 12	-	4.0000 08	3.0000 06	1.2000 12
0.20	1.4407-07	3.469n n9	-		_	_	3.9450 08		1.2000 12
0.0	5.0770-03	1.2040 09			-	_	3.9700 08	1.1290 09	1.2000 12
6.69	2.1210-03	5.1210 08			1.1620 12	_	3.9540 08		1.2000 12
0.00	1.3250-03		_		<b>-</b>	_	3,9390 08		21 0002-1
1.00	1.0740-03	_		\$0 U\$05°9	H-5030 11	7.8000 14	3.4240 08	1.22.10 09	700071
	9.7150-04			0 6 6 6	11 0694.7	7 9000 14	_		1 2000 12
•	40-00/1-6	20 0424.2	3.5750		4.3420 11	7.8000 14	3.8790 08	_	1.2000 12
	#0-0115-0			780	5.4460	-	_		1.2000 12
2.00	8-3370-04		_	0686	5-4240 11	_	3.8490 08	_	1.2000 12
2.20	A.1467-04		_		5.0580 11	~	3.8340 08	-	1.2000 12
2.40	7.9700-04	2.3790 nB	3.2590 08		4.7380 11	7.9000 16	3.820D 08	_	1.2000 12
2.60	7.8030-04		_		4.4550 11	-	3.8050 08	1.3960 09	1.2000 12
2.80	7.6430-04			6.6230 09	4.2030 11	-	3.7900 08	1.4080 09	21 0002 1
9.00	#0-0164*1	B0 04044	3,0,501) 08		3.77.70	7 9000 10	3.7410 08		21 0002 1
	7.1850-04				3.5480 11	7.8000	3.7470 08	_	1.2000 12
3.50	7.0380-04		_	5540	3.4200 11	-	3,7320 08		1.2000 12
3.80	6.8930-04				3.2660 11	-	3,7180 08	_	1.2000 12
• 00	6.7510-04		_		3.1240 11	-	3,7040 08	1.4550 09	1.2000 12
4.20	6.5109-04	2.4590 08	_	•	2.9940 11	7.800D 16		1.4590 09	1.2000 12
C	4.4720-04		_		2.4740 11	-	3.6750 08	_	1.2000 12
4.60	6.3350-04		_		2.7620 11	٠.		1.4660 09	1.2000 12
C :	40-L-202-4		80 0624.2		11 0950.2	٠.	-	60 0900	71 0007-1
2.00	6.0700-04			6.7030 09	2.5610 11			-	21 0002-1
D	3.440-1-04	80 Gunc.5		060	11 01/4.2	-	3.6190 08	60 01.4.1	21 0002-1
0 4 4	5.5160-04		20 0000 0	6, 120 09	2-3650 11	7 9000 7	3,5000	1.4.10 09	1.2000
	5.55.7.0	_		_	2.2320 11	7.8000 16	•	_	1.2000 12
9.00	5.44911-04		_		2.1420 11	-	_	_	1.2000 12
6.20	5.3210-04	360	-	7390	2.0960 11	7.8000 14	_	_	1.2000 12
6.40	5.2037-04	5420	_		2.0330 11	7.8000 16	_	_	1.2000 12
9.60	5.0470-04		_		1.04740	-	_	-	1.2000 12
6.80	4.9745-04	2.5550 08	1.4940 08	6,7560 09	1.9180 11	~ -		1.4640 09	1.2000 12
00.7	4.7527-04		80 CCOH-1	6, 1670	11 0500.1	7.4000 16	3.4900 08	1.4600 09	21 0002.1
7	40-0549-4		_		1.7660 11	-		•	1.2000 12
7.60	4.5390-04		_		1.7200 11	7.800D 16	_		1.2000 12
7.80	4.435n-04	0	_		1.6760 11	7.8000 16	_	0	1.2000 12
9.00	4.334P-04	5870	_		1.6350 11		_	0	1.2000 12
9.20	4.2340-04		_		1.5950 11	_	_	_	1.2000 12
64.6	4.1360-04		_		1.5570 11	<u>.</u>	_		1.2000 12
C (	40-U140.4		_	6.801D 09	11.5200 11	٠.	_	0	1.2000 12
0 0	3.94.01.04	2 6000 08	1.4280 08	4 4000 00	11.05451	7.8000 16	3,3700 08	1.4330 09	21 0000
	3.7650=04	2.6130 08	_	300	1.4200 11	• ~			1.2001 12
6	3.6760-04		1.3670 08		1.3890 11	• -	3,3380 08	•	1.2000 12
9.60	3.5900-04		_	6,8230 09	1.3590 11	7.8000 16			1.2000 12
9.80	3.5050-04		1.3000 08		1.3300 11	7.800D 14	3,3120 08	1.4110 09	1.2000 12
.0.0	3.4220-04	2.6270 08	1.2670 08	6.8320 09	1.3030 11	_	3.2990 08	1.4070 09	1.2000 12

1100	5	1		Ŷ		204		7071	ONH		#ONH	*07	CCWOS
	1.5000 06	1.0000	90	1.0000	90	2.5000	-	1.2000 09	1.0000	90		1.5000 09	2.0000 88
	4.8270 11	G. 40. A	2	1.0800	ź	4.3640 0	•	1.2010 09	1.0000	90		1.4150-02	6.0110-93
-	2.283.1	8.8470	~	1000	į	3.8840 0	Ŧ	1.2010 03	1.0000	š		4,3730-03	2.0470-03
9.40	6.5000 11	9.7570	20	1.4340	9	4.0800	ŗ	1.2000 09	1.0000	90		1.9530-03	8.8/40-04
0.0	5.2520 11	9.9240	20	1.658n	9	4.2830	60	1.1990 09	1.0000	90	8.9210 05	1.3090-03	5.6670-04
1.00	5.4517 11	9.7290	20	1.4860	90	4.473D 0	Œ	1.1990 09	1.0010	90		1,1350-03	4.7020-04
1.20	5.4220 11	9.3900	0.7	-	90	4.6460 0	9	1.1980 09	1.0010	90	9.6350 05	1.0910-03	4.3530-04
1.40	5.0150 11	8.974D	07	-	ş	4.8010	•	1.14HD 09	1.0010	90	1.0010 06	1.0690-03	**-0102·*
1.60	4.6450 11	9.5590	0.7	_	9	_	Œ.	1.1970 09	1.0010	90	1.0390 06	1.1040-03	*0-0F*I*
1.80	4.3160 11	9.1550	07	_	90	_	60	1.1960 09	1.0010	9	1.0780 06	1.1240-03	0-0411.
2.00	4.0250 11	7.7739	0.7	_	ş.	_	er e	1.1960 09	1.0010	9	1.1170 06	1-1470-03	*0-0011.*
2.20	3.757 11	7.4150	<u>-</u>	-	9	_	<b>.</b>	1.1950 09	1.0020	9	1.1570 06	50-00/101	*0-0511.*
2.40	3,5390 11	7.0810	<b>~</b>		2	5.3590	9	1.1950 09	1.0020	90	1.1980 06	1.1920-03	*0-0571**
2.50	3,3339 11	6.1700	20		9 :	5.4360	<b>9</b> 9	1.1940 09	1.0020	9	1.2390 06	10-0617-1	*0=0ef**
2.90	3.1500 11	6.4910	20	3.7980	2	5.506n C	r e	1.1940 09	1.0020	ŝ	90 0182*1	1 2510-03	0-01010
0 · 0	2.9840 11	6.2110		3.9860	2 :	0000.0	0 9	11930 09	1.0020	9 6	1.3630 00	260000	40-00-0
62°E	2.8350 11	5.9590	2	1000	9 4	0220.5	<b>0</b> q	1.1930 09	1.0020	0 4	1.4090 00	1.2840-03	4.1480±04
0 F .	2.5980 11	5.7230		0.3350	2 2	01/00	9	1 1920 09	1.0020	9 6	1.4500 06	- 2000	40-041-04
200	2.5/40 13	3.5060		1044	9	0000	•	101010	0000		20040	1.3120-03	4.2300-04
2 4	2 3550 11	0.000		4. H. S.	2 2	5.7850	2 05	1.1900 00	1.0030	4	1.5370 06	1.3250-03	4.2460-04
9 6	2 2540 11	4 9150		4.9670	2	5. A. b.D		1.1900 09	1.0030	9	1.5800 06	1.3360-03	4.2610-04
	7. [497 1]	7410	. ~	5.1130	9 9	5-4340	. ≪	1.1840 09	1.0030	90	1.6240 06	1.3470-03	4.2760-04
•	2.0860 11	4.5770	20	5.2550	9	5.4600	9	1.1890 09	1.0030	90	1.6680 06	1.3560-03	4.2910-04
4.80	2.0090 11	4.4220	20	5.3920	ě	5.8780	9	1.188D 09	1.0030	90	1.7110 06	1.3650-03	4.3050-04
5.00	1.9170 11	4.2750	10	5.5250	90	5.8930	•	1.1880 09	1.0030	9	1.7550 06	1.3730-03	4.3190-04
5.20	1.4690 11	4.1360	10	5.6530	9	5.9050	œ	1.1870 09	1.0030	90	1.7990 06	1.3800-03	4.3330-04
5.40	1.4050 11	OF 00.4	07	5.1780	9	5.9150	9	1.1870 09	1.0030	2	1.8430 06	1.3870-03	4.3460-04
5.64	1.7460 11	3.8770	20	5.8990	و	5.9220	•	1.1860 09	1.0030	90	1.8870 06	1.3920-03	40-0656.4
5.80	1.6910 11	3.7570	2	0910.9	9	5.928D (	<u> </u>	1.1860 09	1.0030	9 0	1.9310 06	1.3980-03	*0-01/E**
6.00	1.6380 11	3.6430	<u>-</u>	6.1290	9	5.9310	<b>e</b>	1.1850 09	1.0030	9	1.9750 06	1.4040-03	40-0000 · 4
6.20	1.5487 11	3.5340	2	6.2390	2	5.9320	20 9	1.1850 09	06 00 -1	s s	20120 00	50-000-1	40-0404
0.40	1.5410 11	3.4300	>:	0.1460	9 4	5.9310	<b>2</b> 9	1.1840 09	0400	s s	2 1070 06	50-001-1	10-02-14-4
		3.3310	. h		9 4	5. 926n	. 4	90 0581.1			2.1510 06	1.4150-03	4.4270-04
	11.6514.1	3.1450	. ~		9	5.9200	9	1.1830 09	1.0040	90	_	1.4170-03	4.4370-04
7.20	1.3770 11	3.0580	20	6.7410	9	5.9140	<u> </u>	1.1A20 09	1.0040	ç	2.2390 06	1.4190-03	4.4470-04
7.40	1,3410 11	2.9740	10	6.8330	2	_	8	1.1820 09	1.0040	90	2.2820 06	1.4200-03	4.4570-04
7.50	1.3060 11	7.89.0	10	6.9220	9	-	90	_	1.0040	90	2,3260 06	1.4210-03	4.4660-04
7.80	1.2730 11	2.8170	0	7.0090	9	5.8890	9	1.1810 09	1.0040	90	2.3700 06	1.4210-03	4.4750-04
00.0	1.2420 11	2.7440	10	7.1930	9	5.8780	æ	1.1800 09	1.0040	90	2.4130 06	1.4210-03	4.4830-04
8.20	1.2120 11	2.6730	07	7.1740	90	5.8670	<b>6</b>	1.1900 09	1.0040	9	2.4560 06	1.4210-03	*0-016+*
A.4.	1.1430 11	2.6040	70	7.2530	9	_	9	1.1790 09	1.0040	9	2.5000 06	1.4210-03	*0-066**
8.50	1.1560 11	2.5390	0.7	7.3300	9	_	9 9	1.1790 09	1.0040	9	2.5430 06	1.4200-03	40-010-0
	1.1290 11	2.4760	21	7.4050	2 :	5.8280	<b>2</b> 9	1.1780 09	1.0040	\$	2.5860 06	E0-0614-1	*D=0*1C**
00.0	1.104011	0514.5	5	1000	2 :	5.6130	9 1	10.0971.1	300	9 3	2002000	20-0014-1	40.02.00
9.20	11.0900	2.3560	> 6	7.5490	8 6	7980	2 5	1.1770 09	0.00	9 4	2,115,00	10-0014-1	
	1.050.1	2.2450	- 6	7.6840	) <b>(</b>	7670	2 2	1.1770 69		) 2 2	2.7570 06	1.4130-03	4-9-10-04
	וב (הנטין נו הנוסין	2.1930	; <b>~</b>	7.7500	9 6	3,7500	3 5	1.1760 00	0400	2	2.7990 06	1.4100-03	40-07-3
:	9.9180 10	2.1420	6	7.6130	9	5.7330	. e	1.1760 09	040	3	2.8420 06	1.4660-03	1-058.1

T=800 K, H=30 km

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
ı	M + EON+ SON <<< M + 2054	1.270 06	1.770-15
5	\$*NO3 >>> Z*NO2 + O2	3.980-14	5.95D-4A
3	NO2 + NO3 >>> NO2 + NO + O2	6.590-14	3.130-34
4	HO3 + NO >>> 2*1102	1.900-11	1.74D-18
5	SO + SON << E0 + ON	3.430-13	4.420-26
•	NO2 + D3 >>> ND3 + D2	5.610-15	9.780-21
7	M + SON + OH - CC M + EONH	9.090-01	2.010-14
5	HN03 + H0 >>> H20 + N03	9.000-14	2.430-18
9	0 + 0 + M >>> 0 + M	3.390-17	4.300-17
10	0 + 02 + M >>> 03 + M	2.120-17	1.080 01
11	0 + 03 >>> 2+02	1.070-12	6.110-39
15	0 + NO + M >>> NO2 + M	3,400-15	3.250-09
13	0 + NOS >>> NO + OS	1.170-11	5.550-25
14	M + EON << M + SON + D	1.060-14	8.470-25
15	HO + HO >>> H2O + O	5.000-12	1.060-15
16	05 + S+NO >>> S+NOS	6.400-39	8.780-20
17	NO2 + H+NIJ >>> NO + 0	0.0	0.0
18	0 + HO >>> H + OZ	4.200-11	9.550-15
19	0 + HOS >>> HO + OS	4.280-11	3.430-24
20	02 + H + M >>> H02 + M	1.050-15	1.570-04
<b>21</b>	03 + H >>> H0 + 02	5.250-11	6.310-34
55	03 + H0 >>> H02 + 02	4.300-13	3.24D-24
23	03 + H02 >>> H0 + 2*02	1.480-14	2.350-4A
24	H + H0 + M >>> H20 + M	4.120-15	4.080-23
25	H + HOS >>> S+HO	1.280-10	5.160-55
56	H + HO2 >>> HZ + O2	2.710-11	1.450-26
27	H + H20 >>> H2 + H0	4.09D-16	1.410-12
ZA	H + H202 >>> H2 + H0\$	3.930-13	9.470-18
29	H + H505 >>> H0 + H50	5.110-13	6.020-33
30	24HU + W >>> HSUS + W	4.070-15	3.360-07
31	HO + HOS >>> HSO + OS	4.440-11	5.700-30
35	\$*HOS >>> H203 + 05	9.100-12	1.530-22
33	HO2 + H20 >>> H202 + H0	5.190-20	3.460-12
34	NO + H + M >>> HNO + 4	1.150-15	6.860-85
35	NO + HO >>> NO2 + H	3.30D-20	2.300-10
34	NO + HO + H ->> HNO2 + M	1.640-14	1.560-01
37	NO + HOS >>> NOS + HO	4.46D-12	7.66D-14
34	H + H + M >>> H5 + M	1.060-16	1.120-21
39	HM + SON + SOH <<< M + 40MH	1.760 06	2.310-15
40	CFM03 + H >>> CF0 + H05 + H	1.160 06	7.360-16

1000	3000	ç	500	914	7 (3	60	, C227	ş	
	4.0000	4.2000 09	3.0000 06	4.5000 08	2. Sagn 12	7.8000 14	4.0000 BR	3.0000 06	1.2000 12
0.50	2.54411-04	4.4840 08	** 0/10 08	6.3640 09	3.4750 11	7.4000 16	3.3351 08	1.8750 09	1.2000 12
0.40	3.3167-05	5.9740 07	3.974n nB	6.818n 09	2.1030 11	7.800n 14	2.7A10 08	2.6270 09	1.1990 12
0.50	2.4330-05	4.85RD 07	3.473D DH	6. AASD 00	2.0460 11	7.4000 14	2.31MD 0A	3.124P 09	1.1490 12
0.90	50-0625-2	4.7990 07	3.7741) OR	6.9340 09	1.4960 11	-	1.9330 08	3.9530 09	21 0661-1
00.	5.4530-05	4.7790 07	3.6760 08	6.9760 09	1.7690 11	-	1.6110 08	4.5170 09	21 0861.1
1.29	2,3420-05	4.7640 07	3.5810 08	7.0130 09	1.0550.1	7 9000 16	1.3430 08	5.0610 09	21 0961 1
	2.249:1-05	4.7430 07	3.3950 06	-	1.4610 11	-	9.3370 07	5.8670 09	1.1980 12
1.80	2,1870-05	4.7380 07	3,3060 08	7.0970 09	1. 3770 11	_	7.7840 07	6.216D 09	1.1970 12
2.00	2.1290-05	4.7370 07	3.2180 08	7.1180 09	1. 3010 11	7.8000 16	6.4890 07	6.5260 09	1.1970 12
2.20	2.0730-05	4.7400 07	3.1330 08	7.1370 n9	1.2320 11	7.8000 16	5.4100 07	6.1960 09	1.1970 12
5.40	2.0210-05	4.7460 07	3.0490 08	7.1550 09	1.1680 11	7.8000 16	4.5100 07	7.0310 09	1.1970 12
2.50	1.9710-05	4.7550 07	2.9680 08	7.1700 09	1.100	7.8000 16	3.7600 07	7.2340 09	1.1970 12
2.89	1.4230-05	4.7670 07	2.488D 08	7.1840 09	1.0560.1	7.8000 16	3.1350 07	7.4080 09	21 02011
00.0	1.8770-05	4.7820 07	2,8110 08	7.1970 09	1.0000.1	7.8000 14	2.6140 07	7.5550 09	1.1970 12
200	1.6330-05	0 0667.4	2 4420 08	4 2100 00	01 0000.6	7. 4000	1 20 07	7,7430,00	1 1970 12
	1 7500-05	0 0010.4 4 0 00 00 0	2 5900 04	7 2240 00	A. 7840 10	7.8000 14	1.5150 07	7.8660 09	21 020
	7100.0	70 0040	2.5200 08	7.2340 00	8.4160 10	7.8000 16	1.2630 07	7.9330 09	1.1970 12
00.4	1.6720-05	4.8830.07	2.4520 0B	7.2470 09	8.0720 10	7.8000 16	1.0530 07	7.9850 09	1.1970 12
4.20	1.6350-05	4.907n 07	2,3850 08	7.2550 09	7.7510 10	7.8000 16	8.7800 06	8.0220 09	1.1970 12
64.4	1.5980-05	4.9320 07	2,3210 08		7.4510 10	7.8000 16	7.3210 06	8.0480 09	1.1970 12
4.50	1.5430-05	4.9570 01	2.2580 08	7.2490 09	1.1590 10	7.8000 16	6,1050 06	8.0620 09	1.1970 12
4.80	1.5280-05	4.9830 07	2,1960 08	7.2760 09	6.9050 10	7.8000 16	5.0910 06	8.0670 09	1.1970 12
5.00	1.4940-05	5.0040 07	_	7.2830 09	6.6560 10	7.8000 16	4.2450 06	8.0630 09	1.1970 12
5.20	1.4510-05	5.0330 07	2.0780 NB	7.2890 09	6.4220 10	7.8000 16	3.5410 06	8.052D 09	1.1970 12
5.40	1.4247-05	5.0590 07	2.022n u8	7.2950 09	6.2010 10	7.8000 14	5.9530 06	8.0330 09	1.1970 12
5.50	1.1960-05	5.083h 07	_	7,3000 09	5.9920 10	7.8000 14	2.4640 06	8.0090 09	1.1970 12
5.30	1.3540-05	5.10AD 07	1.013n n.H	7.3060 09	5.7950 10	7.8000 16	2.0540 06	7.990D 09	1.1970 12
0.00	1.3330-05	5.1320 07	1.8510 08	_	2.5090 10	7.8000 16	1.7150 06	7.9460 09	1,1970 12
02.0	1.3030-05	5.1560 07	1.9100 08	7,3160 09	5.4320 10	7.8000 16	1.4310 06	7.908D 09	21 0/61-1
	1.2739-05	5-1780 07	1.7600 08	_	5.2550 10	7.4000 16	1.1950 06	7.8660 09	21 0/611
6.0	1.243-05	2.2010 07 2. dr.cc	1.120 00	7 3300 00	01 0001.0	7 9000	7.4760 05	7 7740 09	21 0/611
	1 1860-05	5 24 OF 07	80 0069	_	01 01 01 V	7. 8000	6.0530	7.7250 00	1 1070 12
7.20	1.158/-05	5.2630 07	1.5750 0.8		4.5740 10	7.4000 16	5.9210 05	7.4730 09	1.1970 12
7.40	1.1300-05	5.2820 07	1.5320 08	7,3430 09	4.5440 10	7.8000 16	-	7.6200 09	1.1970 12
7.60	1.1030-05	5.3010 07	1.4900 08	7,3470 09	4.4200 10	7.8000 16	4.0740 05	7.5660 09	1.1970 12
7.80	1.0750-05	5.3190 07	1.449() 08	7.15In 09	4.3010 10	7.8000 16	3.4120 05	7.5110 09	1.1970 12
9.00	1.0501-05	5.3360 07		7,1550 09	4.1ABD 10	7.8000 16	2.9600 05	7.4540 09	1.1970 12
8.20	1.0240-05	5,3520 07		7.359F 09	4.0790 10	7.8000 16	2.3990 05	7.3970 09	1,1970 12
64.6	9.991)-06	5,3680 07		7.3620 09	3.9750 10	7.8000 16	2.0150 05	7.3400 09	1,1970 12
	9.7430-06	4.3830 07	1.2960 08	7.3660 09	3.8760 10	7.8000 16	1.6950 05	7,2820 09	1,1970 12
	90-(1664-6	5.3970 07	1.2600 08	7.3690 09	3.7810 10	7.8000 14	1.4280 05	7.2230 09	21 0/61-1
00.6	9.2400-06	5.4100 07	1.2260 08	7.3730 09	3.5890 10	7.8000 16	1.2060 05	7.1650 09	21 0791-1
00.4	9.0200-0	5.4230 07	1.1920 08	7,3760 09	3.6020 10	7.8000 16	1.0200 05	7.1070 09	1.1970 12
	8.7470-06 8.5720-06	5.4350 07 5.4460 07	1.1270 08	7 3820 09	3.5160 10	7.9000	7. 35.00 04	00000	1070
	8.3520±06	5.456n 07	1.0960	7. 3850 09	3, 3590 10	7.8000 16	4. 2800 OA	00 00.00° 9	1.1970 12
	9-1370-06	5.4660 07	1.0660 08	7.3880 09	3.2840 10	7.8000 16	5.3600 04	6.8750 09	1.1970 12

71Mc (5)	c		I		ì		40×	2021	ONH	NN02	~	MONH	CLNO3
	1.000.0	٤	1.0940	20	1.0000	c	10 (100).	1.0000	1.0000	0000.4	00 00	1.000 09	6. 0000 .3
0.20	1,6540	^	1.5340	90	1.1160 6	9	1.7740 08	1.1990 09	1.0000 06	7.9520	20 05	1.0410-04	6.9590-05
0.40	1.5120 1	2	2.1170	9.0	1.3690 0	w	2.5040 08	1.1960 09	1.0000 06	8.1950	50 05	1.9580-05	9.2750-06
0.00	1.4450	~	2.4740	61	1.1690 0		3.1860 OH	1.1930 09	1.0010 04	8.6020	20 05	2.0300-05	1.5550-06
0.90	1.3690 1	2	7.1150	90	2.3120 0		3.8020 08	1.1890 09	1.0010 06	9.1500	90 00	2.3440-05	7.4460-06
1.00	1.2580 1	2	2.8750	90	2.9830 0	_	4,3540 08	1.1850 09	<u>-</u>	9.8190	90 05	2.7230-05	7.4160-06
1.20	1.1780 1	2	2.9720	98	3.7650 0	w	4.8470 08	1.1810 09	-	1.0590	30 O¢	3.0220-05	7.3930-06
1.40	1.0990.1	2	3.0220	90	4.5420	•	5.2M6D 08	_	-	1.1460	90 09	3.2470~05	7.3740-06
1.69	1.0290 1	~	3.0340	90	5.5920 0	۰	5.6750 08	1.1710 09	-	1.2400	90 00	3.5230-05	7.3610-06
1.80	9.6430 J	_	3.0190	9 .	_	۰ م	6.0180 08	1.1660 09	1.0030 06	1.3400	90 00	3.7320-05	7.3540-06
0.00	9.0700 1	=:	2.9820	9	_	9 6	6.3190 28	1.1510 09	1.0040 06	1.4440	90	3.9180-05	7.3520-06
2.2	1,555.	= :	3.76.2	9 9	0 (142) 0	<b>.</b>	MD 0555.0	60 (05)	00 00001	1.5530	2 2	50-0500°	7 3460-00
0	0.0410	= :	2.8650	9 6	0 0000	۰ ۰	5.812U U6	60 0051-1	1.0050 05	06000	- '	4.631U-05	1000000
	1 0250.7	= -	2.1720	9 6	0160	- h	7 1740 08	40 OC 1 - 1	1,0050 06	99.70		4.3060-05	7.340-00
	0000		0.64.6	9 6	_	. ~	7.1210 08	_	-	2.0080	90 08	4.5810-05	7.4210-06
	A. K.A.	: =	2.5470	2	1.4120 0	. ~	7.4410 08	_	-	2.5	30 00	4.6730-05	7.4470-06
	2000		2.4610	9	1.5160 0	. ~	7.5400 08		-	2.2380	90	4.7540-05	7.4760-06
3.60	5.940n 1	:=	2.3750	90	1.6160 0		7.5200 08	1.1160 09	1.0070 06	2,3510	10 06	4.8250-05	7.5080-06
3.80	5.7170 1	=	2.2920	90	1.7130 0	~	7,6830 08	1.1100 09	1.0080 06	2.4630	30 06	4.8870-05	7.5430-06
• • •	5.4740 1	_	2.2090	90	1.8080 0	_	7,7320 08	1.1040 09	1.0080 04	2,5730	30 06	4.9420-05	7.5790-06
4.20	5.2470 1	=	2.1280	90	1.8990 0	~	7.7570 08	1.1990 09	1.0080 06	2.6810	90 01	4.9880-05	7.6160-06
4.49	5.0360 1	=	2.0490	90	1.9850 0	~	7,7900 08	1.0930 09	1.0090 06	2.7870	20 06	5.0280-05	7.6540-06
4.50	4.9380 1	=	1.9720	80	2.0700 0	-	7,8020 08	1.0870 09	1.0090 06	2.8900	90 00	5.0620-05	7.6930-06
4.83	4.6530 1	=	1.8940	99	2.1510 0	_	7.804D 08	1.0M20 09	1.0090 06	2.9900	90 00	5.0890-05	7.7320-06
5.00	1 0644.4	=	1.8270	80	2.2280 0	~	7,7990 68	1.0760 09	1.0100 06	3.0880	80 06	5.1110-05	7.1720-06
5.29	4.3170 2	=	1.7580	90	2.3020 0	~	7,7850 08	1.0700 09	1.0100 06	3.1820	20 06 20	5.1290-05	7.8110-06
5.40	4.1539 1	=	1.6920	90	2,3730 0	~	7.7660 08	1.0650 09	1.0100 06	3.2730	30 06	5.1410-05	7.8500-06
5.60	4.0190 1	=	1.6290	90	2.4400 0	<u> </u>	7.7400 08	1.0590 09	1.0110 06	3.3610	10 06	5.1490-05	7.8890-06
. B.	3.4430 ]	=	1.5640	80	2.5040 0	<u>-</u>	7.7090 08	1.0540 09	1.0110 06	3.4460	90 09	5.1540-05	7.9270-06
00.0	3.7550 ]	= :	1.5100	6	2.5650 0	<u>-</u> '	7.5740 08	1.0480 09	1.0110 04	3.5280	9	5.1540-05	7.9040-06
6-20	3.6337 1	=:	1.4540	9	2.52410	- •	7.6350 08	1.0430 09	1.0110 05	3.6060	90 09	5,1520-05	90-0100-9
•	3.51.40	= :	1.4010	8	2.6799 0	_ •	7.5930 08		90 0210*1	3.5820	8	5.1460-05	8-03-0-0
E .	3.4040	٠.	1.35.0	0 0	2 1930 0		7 4000 00		1.0120 06	3.7300		20-0/61-0	
000	3.3000		1.3010	0 4	2.830	- *-	7 4490	1.0220 09	1.0120 06	3.0440		5.1630-03	00-040-0
200	11140	-	1.2100	9	2.4760		7.397D AR	1.0170 09	1.0120 06	3.9510		5.0550-65	A. 16An-06
7.60	3.0260	:=	1.1690	80	2.9200 0	~	7.3440 08	1.0120 09	1,0130 06	4.0100	90 00	5.0770-05	8.1980-06
7.60	2.9410 1	=	1.1270	90	2,9610 0	~	7.2890 08	1.0070 09	1.0130 06	4.0670	90 02	5.0570-05	8.2270-06
7.80	2.8400 1	=	1.0890	60	3.0000 0	~	7,2330 08	1.0020 09	1.0130 06	4.1210	10 06	5.0350-05	8.2540-06
9.00	2.7430 1	=	1.0510	90	3.0370 0	<u>~</u>	7.1770 08	9.9720 08	1.0130 04	4.1710	90 OF	5.0120-05	8.281D-06
8.20	2.7100 1	=	1.0150	60	3.0730 0	<u>-</u> 1	7.1200 08	9.9240 08	1.0130 06	4.2190	90 90 90	4.9870-05	8.3060-06
8.40	2.5400 1	=	9.8160	6	3.1070	<u>-</u>	7.0620 08	9.8760 08	1.0130 06	4.2640	<b>\$0 0</b>	4.9610-05	8.3300-06
6.50	2.5730 1	=	9.4920	6	3-1390 0	<u>-</u> 1	7.0040 08	9.8290 08	1.0140 04	4.3070	70 06	4.9340-05	6.3530-06
0.0	2.5080 1	=	9.1810	٥	3.1690 0	<u>-</u> •	80 0946.0	9.7820 08	1.0140 06	4.3470	20 06	4.9060-05	8.3750-06
00.0	2.4470	=	8.8840	-	3-1980	_ !	0.8880 08	9.7360 08	1.0140 06	4.3840	90 04	4.8770-05	90-0467
9.20	2.3980 1	=:	3.5990	2	3.4400		0.0670.08	90 00400	1.0140 06	0614-4	8	4.8470-05	2
	1 0111		9470	- 6	3.6760	: :	90 05 17.9	0000000	20140 00	0254-	2 : 2 :	4.6160-05	
	2.27.70	= =	9.000	5 6	8 0000		4.6.66	9.8560	20 0010-1	8000	8 1 8 2	40-060-00	
	2.1760 1		7.5760	; <del>c</del>	3,3230	: =	6.5980 08	9.5120 68	00 C0 T0 T	0.5360	: 1 : 1	4.7210-05	9
		:		į				1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1			}	11 118.01	

T=250 K, H=35 km

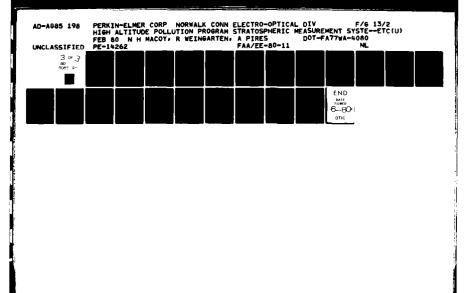
9-MM	REACTION	FORWARD HATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + H	9.800-07	3.060-14
5	20 + 20N+3 <<< £0N+5	4.710-17	7.460-67
3	NO2 + NO3 >>> NO2 + NO + 02	4.210-15	1.190-34
•	NO3 + NO >>> 2*NO2	1.900-11	3.290-32
5	NO + 03 >>> NOS + 02	6.360-15	1.080-56
4	102 + 03 >>> NO3 + 02	6.650-18	8.330-39
7	M + SON + OH - * EDNH	1.300-28	5.960-13
6	HN03 + H0 >>> H20 + N03	# • 000-14	2.800-29
9	0 + 0 + M >>> 02 + H	6.520-16	8.42D-59
10	0 + 02 + M >>> 03 + M	1.40D-16	3.910-13
11	0 + 03 >>> 2*02	1.450-15	0.0
15	0 + NO + M >>> NO2 + M	2.74D-14	2.030-48
13	0 + NOS >>> NO + OS	5.120-12	6.270-53
14	0 + NO2 + M ->>> NO3 + M	1.710-14	1.370-24
15	HO + HO >>> H2O + O	1.090-12	9.770-27
16	05 + 5+NO >>> 5+NO5	2.750-38	3.860-35
17	0 + 0H H-H + SON	0.0	0.0
19	0 + H0 >>> H + 05	4.20D-11	7.730-25
19	0 + HOS >>> HO + OS	1.080-11	5.450-60
20	02 + H + M >>> H02 + H	6.740-15	8.640-32
21	03 + H >>> H0 + 02	1.270-11	0.0
55	03 + HO >>> HO2 + O2	2.750-14	1.04D-4A
23	20#5 + 0H - S#05	4.45D-16	2.410-68
24	H + H0 + M >>> H20 + M	1.370-13	0.0
25	H + H02 >>> 2*H0	9.400-12	1.620-46
26	H + H05 >>> H5 + 05	1.040-11	2.550-61
27	H + H2O >>> H2 + H0	2.340-28	1.140-15
29	H + H202 >>> H2 + H02	8.360-15	5.620-29
50	H + H202 >>> H0 + H20	1.090-14	1 - 350-75
30	28H0 + M >>> H202 + M	7.H3D-14	2.10
31	HO + HOS >>> HSO + OS	1.120-11	3.89D-74
32	\$*H05 >>> H205 + 05	5.300-15	8.580-49
33	HUS + HSO >>> HSOS + HO	1.020-34	5.490-13
34	M + DAH <<< M + M + DA	4.260-15	6.670-34
35	H + SON >>> NO	3.050-36	3.010-11
34	NO + HO + M >>> HNO2 + h	5,600-13	5.150-50
37	NO + 408 >>> HO	1.650-13	7.470-21
34	H + H + M >>> H2 + M	1.710-16	0.0
34	HN04 + M >>> H02 + N02 + M	3.140-06	5.60D-14
40	CFH03 + M >>> CFO + H05 + H	7.900-00	4.320-14

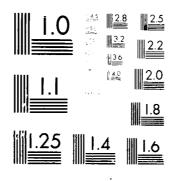
114c (c)	50211	20%	80%	07	0.3	20	H403	9	Н20
0.0	5.5000 07	2,2000 09	****** OA	HU UUU', 'S	1. 1001 12	4. 4000 JA	7.0000.2	5.0000 DK	בו טטטר יי
0.20	5.5non 07	2.2010 04	2.0000 06	5.4910 08	1.3000 12	3.400P 16	2.0000 07	_	5.3000 11
0.40	5.500n 07	2.202n 19	1.9990 06	5.4420 08	1.3000 12	3.8000 16		4.990D 06	5.3000 11
0.50	5.5000 07	90 OF 04.4	1.3940 06	4.47 10 OH	1.1000 12	3.4001 16	5.0000 07	_	5.300n 11
0.90		2.204n 09	_		1. 4000 12	3.400n 14	5.0010 07	4.9200 06	5.3000 11
.00		2.2050 09	_		1.3000 12	3. HOOD 16	70 0100°C	4.885D 00	11 0006.5
1.20	5.5000 07	2,2059 09		5.4450 08	1.3000 12	3.8000 16	5.0010 07	4.8510 06	5.3000 11
•	7.5001 07	2 2070 04	1.0070 06	5.4 John 0.8	21 0000 1	3.80001	5.0010 07	4.7830 06	5.3000 11
90.1	5.5000 07	2.20An 09	_		1.3000 12	3.8000 16	5.0010 07	0	5,3000 11
200	5.5000 07	60 0602-2			1.3000 12	3.8000 16	5.0010 07	4.7160 06	5.3000 11
2.20	5.5an'ı 07	2.21nn 09			1. 5000 12	3.8000 16	5.0010 07	4.6830 06	5.3000 II
2.40	5.5000 07	2.2110 09		0	1.3000 12	3.8000 16	_	4.6510 06	5.3000 11
2.60	5.5000 07	2,2120 09	1.9960 06		1.3000 12	3.8000 16	5.0020 07	4.618D 06	5.3000 11
2.80	5.500D 07	2.2130 09	_		1.3000 12	3.8000 16	5.002D 07	4.5460 06	5.3000 11
00°E	5.5000 07	2.2130 09	_		1.3000 12	3.8000 16	5.0020 07	4.5540 00	5,3000 11
3.20	5.5000 07	2.2140 09	-		21 0006 1	3,8000 15	3.00.00	40 (1275.4	2.2000
	70 0005.5	2.6150	1.3950 00	00 00 00 00	1 3000 12	3.0000	5 0000	90 0144.4	3000
50.0	70 0605.5	2.5150 09	•	3,3300 06	1.3000 12	3.0000 10	5.0020 67	> 0	11 0000
50.0	70 (1005.5	2 3160 09	40 0400		1 3000 16	3,0000 1	5.0020 07	9	5.3000
•	20000000	60 0016 6	•		21 0005 1	1 0000 F	5.00 S	4.3670.06	5. 3000 13
	5.5000 07	2 2200 00	1.0440		1. 4000 12	3. 8000 16	5.0030 07	4.337D 06	5.3000 11
9	5.5000 02	2.2210 09	_		1.3000 12	3.8000 16	5.0030 01	4,3060 06	5.3000 11
6.8	5.5000 07	2.2210 09	_		1.3000 12	3.8000 16	5.0030 07	4.2770 06	5.3000 11
5.00	5.509n 07	2.2220 09	_		1.3000 12	-	5.0030 07	4.2470 06	5.3000 11
5.20	5.5000 07	2.2230 09	_		1.3000 12	3.8000 14	5.0030 07	4.2170 06	5.3000 11
5.40	5.5007 07	2.224n 09	1.9930 06		1.3000 12	3.8000 16	5.0030 07	4.1880 06	5.3000 11
5.61	5.5000 07	2,2250 09	_		1.3000 12	3,8000 16	5.0032 07	0	5.3000 11
5.30	5.5000 07	2.2260 09	_		1. 400D 12	3.8000 16	5.0030 07	4.1310 06	5.3000 11
00.9	5.500th 07	2.2270 09	_		1.3000 12	3.8000 16	5.0040 07	4.102D 06	5.3000 11
6.20	5.5000 07	2.22An 09	_	0	1.3000 12	3.6000 16	2.0040 07	4.0740 06	5.3000 11
9	5.5000 07	2.229D 09	_		1.3000 12	3.8000 16	5.0040 07	4.0460 06	5.3000 11
6.60	5.500 07	5.2290 09	_		1.3000 12	3,8000 16	5.0040 07	90 0810°9	2.3000 11
08.9	5.500n 07		_	5,1980 08	1.3000 12	3.8000 16	5.0040 07	3.9900 06	5.3000 13
00.1	70 00005.2	2.231n 09		2	1. 4000 12	3.8000 16	2.0040 67	3.4660 06	3,3000
	5.500F 07	2 2230 00	1 99211 06	5 1720 08	1.3000 12	3. 8000 16	20000	•	2000
		_	_		1.3000 12	3.8000 16	5.0040 07	Ö	5,3000 11
7.80	5.5000 07	2,2340 09			1.3000 12	3.8000 16	5.0050 07	3,8550 06	5.3000 11
9.00	5.590n 07	2.2350 09			1.3000 12	3,8000 16	5.0050 07	3.8280 06	5.3000 11
9.20	5.500n 07	2.235n n9	-		1.3000 12	3.6000 16	5.0050 07	3.8020 06	5.3000 11
9.40	5.500h 07	2.2370 09	1.9910 06	5.1290 08	1.3000 12	3.8000 16	5.0050 07	3.7760 06	5.3000 11
8.69	5.5000 07	2.23AD 09			1.3000 12	3.8000 16	5.0050 07	3.7500 06	5.3000 11
8.83	5.5000 07	2.2390 09	_	5.1120 08	1.3000 12	3.6000 16	5.0050 07	3.7240 06	5.300D 11
00.6	5.5000 07	2.2400 09	_		1.3000 12	3.6000 16	5.0050 07	3.6990 06	3.3000 11
9.20	5.5000 07	2,24,00 09	1.9910 06	5.0950 08	1.3000 12	3.8000 16	5.0050 07	3.6740 06	5.3000 11
•	5.5000 07	2.2410 09	1.9910 06	5.0870.08	21 0006 1	3.6000 14	5.0030 0.	3.0490 00	3.3000 11
	3,000	7 2420 00	1.9910 06	7.070U VO	30000 12	3.0000 14	5 0000 B	3.0000 VV	5. 3000 II
	5.5000 07 5.5000 07	2.2440 09		5.06.00	1.3000 12	3.5000	5.0060 07	3.5750 06	5.3000
	_	** *****	** 1.71.49	200000	******	30000		10.77.74	

1100 (5)	c		1	ì	701		7074	321	YONH	*ON*	CLNO3
	2000	4	40 0000	1.0000.04	1.7000	6	A. 1000.	1.0000 06	7.0000 05	2. 3000 0A	4.0000 07
			2.7250-01		277		X 0000	40 0000	7.00.30 05	2. 300D 0B	4.0000 07
0	1.1920	5	9.3470-02	1.0000 06	1.8010	20	2.800D 08	1.0000 05	7,0060 05	2.3000 08	4.0000 07
0,0	4.1170	7	3.2040-02	1.0000 06	1.404D		_	1.0000 06	7.0090 05	2.3000 08	4.0000 07
0.80	1.4220	*	1.1010-02	1.0000 06	1.40 /0	_	_	_	7.0140 05	2.300P 0B	4.0000 07
1.00	0216.4	63	3.7900-03	1.0000 06	1.9100	6	_	-	7.0150 05	2.3000 08	4.0000 07
1.20	1.5990	6	1.3150-03	1.000h 06	1.9130	0	2.A00D 08	1.0000 06	7.0180 05	2.3000 08	4.0010 07
	5.4980	2	4.6640-04	1.0000 06	1. P160	2	_		7.0210 05	2.3000 08 2.3000 08	70 0100.4
9.1	2.0580	20	1.7539-64	1.0000 06	1.4200	2 6	0 0	0000	7.0240 05	2,3000 08	4.0010 07
	0.000	3 3	CD=(1000 - 1	90 0000	0520-1		20 0000 0	20000	7.0300.05	2 0000	7 0 0 0 · V
2.50	0.50.1	3 2	2-0405	90 0000	05281	200	2.3000 08	1,0000 85	7.0330 05	2,3000 08	4.0010 07
2.40	7.4430		2.4820-05	1.0000 06	1.8320	20	_	0000	7.0360 05	2,3000 08	4.0010 07
2.54	5.5010	8	2,3240-05	1.0000 06	1.8350	10	0	0000	7.0380 05	2.3000 08	4.0010 07
2.80	4.7917	00	2,2570-05	1.0000 06	1.8390	0	2.400U 08	1.0000 06	7.0410 05	2.300n 08	4.0010 07
3.00	1.5060	00	2.2210-05	1.0000 06	1.8410	6	0	_		2.3000 08	4.0010 07
C .	3690	2 8	50-0961-2	1.000n 06	2 4 4 D	~ ~	2.8000 08	1.0000 06	7.0470 05	80 000F 2	100000
	4 21 70	3 6	20-1550-05	1.0000 06	0048	3	2.8000000	90 0000		u ^	4.0020 07
	1560	3 6	2.1360-05	_	1.4520	2	•	1.0000 06		. ~	4.0020 07
00.4	0660	00	2.1170-05	1.0000 06	1.8550	20	Ö	1.0000 06	7.0570 05	2,3000 08	4.0020 07
4.20	4.0430	00	2.0940-05	1.0000 06	1.8580	0	2.8000 08	1.0000 06	7.0600 05	2,3000 08	4.0020 07
	3.0485	00	2,0800-05	1.0000 06	1,8610	0.1	2.8000 08	1.0000 06		~	4.0020 07
4.50	3.3340	5	2.0620-05	1.0000 06	1.8640	0	Ö	1.000n 06		~	4.0020 07
	3.8810	6	2.0440-05	1.0000 06	1.8660	20	0	1.0000 06		~	4.002D 07
<b>9</b>	3.8290	6	2.0270-05	1.0000 06	1.8690	20	2.8000 08	1.0000 06	7.0700 05	Ň	4.0020 07
5.70	3.7776	5 6	20-0000-2	1.0000 06	1.8720	20	0	1.0000 06	7.0730 05	2. 300n o	4.0000 67
	3 6 7 60 1	3 6	0.440	40 0000	1.07	5 6	000000000000000000000000000000000000000	90 0000	7 0700 05		4.0030 67
	7.6270		1.9540-05	1.0000 060	2000	-	200000000000000000000000000000000000000	1.0000		2.3000	4.0030.07
6.00	3.5747	00	1.9420-05	1.0000	1.8820	10	ō	1.0000 04	•	2.3000 0	4.0030 07
0.20	3.5300	8	1.9250-05	1.0000 06	1.8850	0	0	1.0000 06		~	4.0030 07
6.40	3.4937	e	1.9090-05	1.0000 06	1.8970	01	ō	1.0000 06		2.3000 0	4.0030 07
9.9	3.4367	6	50-45661	1.0000 06	0068.1	0.1	0	1.0000 06	0	2.3000 0	4.0030 07
9.40	1.040.	, i	20-0776-1	1.0000	1.89.50	5 6	80 0008.7	1.0000	7.0940 05	2,3000 08	4.0030 07
7.20	3.3000	. 0	1.8460-05	1.0000 06	1.8980	6		1.0000 06	9 0	2.3000 08	4.0030 07
7.40	3.2550	5	1.R300-05	1.000 06	1.900D	07	0	1.0000 06	0	2.3000 08	4.0040 07
7.60	3.2130	9	1.4150-05	1.0000 06	1.9030	20	2.8000 08	1.0000 06		~	4.0040 07
7.8n	3.1700	8	1.800D-05	1.0000 06	1.9050	0	0 000A.	1.0000 06	0	~	4.0040 07
9.00	3.1280	8	1.7850-05	1.0000 06	1.9070	0	.8000 0	1.0000 OK	0	2.3000 08	4.0040 07
H-20	3.0470	00	1.7710-05	1.0000 06	1.9100	2	õ	1.0000 06	•	2.3000 08	4.0040 07
C .	3.0460	6	1.7550-05	1.0000 06	1.9120	_	6	1.0000 04	7.1100 05	2,3000 08	4.0040 07
E (	3.006n	6 6	1.7420-05	90 0000-1	1.9150		õ	1.0000	0 (	2.3000.08	4.0040 67
	2.4561	9 6	1 7140-05	1.0000	2.6	2 6	2 0000 08	1.0000 06	7 7 140 05	2 3000 08	~ 0 0 0 0 · ·
		3 8	00-000	40 0000	1.9140	5 6	2 0000	0000	7 1160 05	2000000	
	2.8500	2 6	1.6860=05	1.0000 06	1.9240	5 6	2.4000 08		<b>•</b> •	2,3000 08	
3	2.8130	2	1.6730-05	1.0000 06	1.9260	6	2.8000 98	3,0000	7-1220 05	2.3600 08	
•	2.1760	8	1.6590-05	1.0000 06	1.9280	0	2.8000 08	1.0000 06	7,1250 05	2.3040 08	4.050 07
:	2.7390	0	1.6460-05	1.0000 06	1.9310	6	2.8000 08	1.0000 04	7.1270 05	2.3000 06	4.0050 07

T=300 K, H=35 km

R-NUH	REACTION	FORWARD HATE	BACKWAHD RATE
1	N205 + M >>> N02 +N03 + M	7.931)-04	1.440-14
2	SO + 200°5 <<< 500°5	2.410-16	1.750-58
3	NO2 + NO3 >>> NO2 + NO + O2	8.210-15	4.920-35
4	NO3 + NO >>> 2*HO2	1.900-11	6.980-29
5	NO + 03 >>> NO2 + 02	1.670-14	2.850-49
6	NOS + 03 >>> NO3 + 05	3.410-17	2.00D-34
7	HN03 + M >>> H0 + N02 + M	9.700-22	3.150-13
•	EDM + 05H << 0H + EDMH	8.000-14	1.250-26
•	0 + 0 + M >>> 07 + M	2.990-16	3.210-50
10	0 + 02 + M >>> 03 + M	8.280-17	6.650-10
11	0 + 03 >>> 2405	8.900-15	0.0
12	0 + NO + M >>> M	1.550-14	6.07D-39
13	0 + NOS >>> NO + OS	6.250-12	3.730-46
14	0 + NO2 + M ->>> NJ3 + M	1.430-14	1.140-24
15	HO + HO >>> H2O + O	1.570-12	4.630-24
16	05 + 5-00 >>> 5-005	1.930-38	2.260-31
17	NO + H-NU >>> NO + 0	0.0	0.0
15	0 + H0 >>> H + 02	4.200-11	2.160-55
19	0 + H02 >>> H0 + O2	1.510-11	8.510~52
21	05 + H + M >>> H05 + 4	4.030-15	3.280-25
21	n3 + н >>> но + o2	1.790-11	1.620-69
55	03 + HO >>> HO2 + O2	5.350-14	8.98D-43
23	03 + H02 >>> H0 + 2*02	1.040-15	1.530-63
24	H + HO + M >>> H2O + H	7.120-14	5.770-76
25	H + H05 >>> 5+H0	1.770-11	1.140-40
26	H + HOS >>> HS + US	1.310-11	6.800-53
27	H + H50 >>> H5 + H0	2.180-25	6.410-15
28	H + H505 >>> H5 + H05	2.130-14	2.960-26
29	н • H2O2 >>> H0 • H2O	2.760-14	2.950-45
30	2440 + M >>> H505 + M	J+5H()+14	2.610-65
31	HO + HOS >>> H2O + 02	1.570-11	1.980-63
32	\$640\$ >>> H50\$ + G5	3.210-17	1.980-42
33	HOS + HSO >>> HSOS + HO	6.110+35	8.570-13
34	NO + H + M >>> HNO + 4	2.910-15	7.450-27
35	NO + MO >>> NOZ + M	7.190-34	4.920-11
34	NO + HO + M >>> HNO2 + M	2.230-13	1.250-22
37	NO + HOZ >>> NOZ + HO	3.66D-13	3.740-19
38	н + н + и >>> н2 + м	1.430-16	1.230-69
39	1N04 + N >>> HO2 + NO2 + M	2.090-03	2.50D-14
40	:LN03 + M >>> CL0 + NO2 + H	1.15D-04	2.070-14





MICROCOPY RESOLUTION TEST CHART NATIONAL BUREAU OF STANDARDS-1963-2

1146 (5)	802N		×0×		N03		9		60		20			9		M20	
0.0	5.5000	10	2.2000	_		90		69	1.3000 1	~	3.8000	92	5.0000 07	5.0000	ŏ	5.3000	=
0.70	5.4991) (	10	2.2020	60	2.0240	Š		6	1.3000 1		3.A00D	٧_	5.0000 07	5.0660	_	5.3000	=
0.0	5.4980	10	2.2056	30	. 0.4.HE)	ę		Ŧ	1.30011		3.4000	7		5.0000	_	5, 3000	_
0.60	5.4970	10	2.2070	60	.0720	90		80	1.3000 1	•	3.8000	1,	0000	4.9350	90	5,3000	-:
0.90	5.4970	0.7	2.2100			96	050**	90	1.3000 1		3.800D	91	_	4.8720	_	5.3000	=
1.90	5.4967	10	2.2120			ş		ď.	1.3000 1		3.8000	٠.	.0000	4.8090	90	5.3000	_
1.20	5.495n (	10	2.2150			90		Ø :	1.3000		3.8000	91	5.0000 07	4.7470		5.3000	Ξ:
. 40	5.4940	2	2.2170			9		9 1	1.3000 1		3.8000	9:	20000000	0000	_	3.3000	Ξ:
	5.4930	7.	2.2200		1920	2 3	0216.6	200	1 0006 1		3.6000	9	5.0010 07	4.6600	-	3.3000	= :
1.84	5.4920	2	0/2/2			٥		<u> </u>	1 4000		20000	0 1	20010 07	0000	9 6	2000	=:
2.00	2.4910	- 1	2.2240	2 6		9 5	5.2660	0 0	1.3000	<b>.</b> .	3.5000	<u>.</u>	20010000			3000	==
	.000		2 2200		2470	9 4		9 6	1 0006		3.8000		5.00.00.00	40.394	<b>,</b> c	3000	::
0,0			2 2315		2100	2 4		C 0	0000	•	0000			4.3380	_	2000	:=
	CARA C		0466			9 4	2.5	9 6	1.3000		8000		5.0010 07	0000 · 4	Ö	2000	:=
3.00	5.4870	. ~	2.2340		0666	9		90	1.3000 1		3.800D	<u> </u>	5.0010 07	4,2290	_	5,3000	=
3.20	5.4860	70	2.2380		2,3830	9	300	90	1.3000		3.8000	2	5.001D 07	4.1750	Ö	5,3000	=
3.40	_	10	2,2410	60		90		90	1.300D 1	~	3.8000	91	5.0010 07	4.1230	_	5.300D	=
3.60	5.4840	0	2.243D		310	9		90	1.3000 1	~	3.800D	91	5.0010 07	4.0710	90	5.3000	=
3.80	5.4830 (	0	2.2450	60		90		90	1.3000 1	~	3.4000	9	_	4.0200	•	5.3000	=
4.00	5,4830 (	0.7	2.2480	60		90		99	1.3000 1	N	3.8000	92	0010	3.9700	_	5.3000	=
4.20	_	0.7	2.2500	60		90		69	1.3000.1	~	3.900D	9.		3.9200	0	5.3000	=
4.4	_	70	2.2520	60		90	4.9970	90	1.3000 1	~	3.8000	9	5.0010 07	3.871	0	5.3000	=
4.69	5.4400	07	2,2540			•	4.9760	90	1.3000 1	~	3.8000	91	5.0010 07	3.8230	_	5.3000	=
4.80	5.4790	10	2.2570	_	2.5740	9	4.9540	90	1.3000 1	N	3.8000	91	5.0010 07	3.776	_	5.3000	=
2.00	_	70	2.2590		2.5970	ş	4.9330	60	1.3000 1	۰.	3.8000	9	5.0020 07	3,7290	_	5.3000	=:
5.20	_	20	7.2610	60	2.4210	9	4.9110	æ	1 3000	N.	3.8000	9	0050	3.6830	_	5.3000	= :
5.40	5.4770	20	2.2630	0	2.6450	9	4.8900	80	1.3000	N I	3.8000	9	5,0020 07	3.6380	0	5.3000	= :
5.60	5.4760	20	2.2650	_	2.6690	٠ و	4.8680	80	1.3000 1	N I	3.8000	9	5.0020 07	3.5930		5.3000	<b>~</b> :
5.50	5.4750	٠,	7.26 AD		2.6930	e :	0.44.4	80	1 0006 -1	<b>.</b>	3.8000	9:	•	3.049	_	2.3000	= :
0.0	5.4740	- 1	2.2700		2.7160	9	4.8260	90	1.3000	v 1	3.8000	2:		3.5000	_	3.3000	= :
2.0	5.6730	2 1	75125	2 6	0047-2	9 8	0508.	9 6	1 2006 1	٠,	30000	<u>•</u>	200700	3.4030		3000	= :
	1000	5 6	2 2775	2 0	2.7880	9 4		0 d	1 3000		0000		5.00.00 07	124.6	9 6	3000	: =
9.9	5.4700		2.2790	6	2.9110	9	7430	90	1.3000 1	. ~	3.8000	2 4	5.0020 07	3,3390	_	5.3000	:=
7.00	5.4701)	6	2.2810		2.8350	90		80	1.3000 1	~	3.8000	2	5.0020 07	3.2990	_	5.300D	=
7.20	_	0.7	2.2830		2.8590	90		90	1.3000 1	~	3.8000	16	5.0020 07	3.2600	_	5.3000	=
7.40	5.45Bn (	16	2.2850		2.8830	9	4.6910	90	1.3000 1	~	3.8000	9	5.0020 07	3.2210	_	5.3000	=
00.7		57	2.2870		2.4060	2 :		8 6	1 0000 1	~ .	3.8000	<u>.</u>	5.0020 07	3.1820		3000	=:
E (	_	> 7	12000	-	0054.5	5 6		D 6	1 0000	, ·	20000	9	•	000100	_	0000	= :
60.0	3.4500	2 6	2040	2 0	2 0780	9 4	0000	0 a	1 0000	u n	3.0000	9 2	5.0020 07	3.1070	8 6	0000	==
			2000	5 6	2007	9 4	0000	0 6	0000			9 4		•	, ,		::
	0.40	5 6	2990		3.0050	9 4	4.0000	5 4	1 . 3000		0000	9 4			_		==
	6,000	. ~	2,3000	_	3.0490	9	4.5410	2 6	1 3000	10	1.8000	2 4	_	2.9645	_	5.3000	:=
0.0	5.4510	6	2,3020	2	3.0730	9	4.5210	90	1.3000	~	3.8000	÷		2.9300	_	5.3000	=
9.20	_	20	2,3040	60	3.0960	2	4.5010	80	1.3000	~	3.8000	16		2.8960	_	5.3000	Ξ
9.40	_	0	2.3060	6	3.1200	2	4.4820	80	1.3000 1	~	3.8000	9	5.0030 07	2.8620	90	5.3000	=
•••	5.4580	6	2.3080	6	3.1440	9	4.4620	80	1.3000	Per I	3,600	9	5.0030 07	2.6290	9	2.3000	=
0.0	5.4580	۱۵	2.3100	6	3.1680	2	4.4430	9	1 .3000	ivi i	3.5000	9:	000	2.1970	9	0.7660	=:
	_	20	2.3120	•	3.1910	ĕ	4.4230	£	1.3000		3.6000	•	5.003D 67		2	3.5	

1100 (5)	æ		τ	ŗ		702		<b>7</b> 0/1	Ź	ONE		NONH		401H		CLNO3	
•	1.0000	90	1.000n 06	1,0000 0	9	1.700n g	20	2.8000 08	3.1	0000	90	٥	50	2,3000	80	4.0000	6
0.20		50	6.5250-0]	1.0000	9	1.4030 0	~	2.4000 0ë	1.0	0000	90		9	2.2990	80	4.0000	~
0.40		Š	3.4140-01	1.0000	š	1.4190	~	2.400D 0	-	9006.	ş		50	2.2980	60	4.000n	0
0.50	1.404.1	9	1.7920-01	1.0000	٠	1.8350	-	2.4000 0H	_	.0000	90		90	2.2970	90	4.000D	٥,
0.80	7.9370 0	•	9.4030-02	1.0000	ō.	1.H50D	-	2.400U DE	-	0000	90	-	92	2,2960	90	4.0000	07
1.00	4.2227	*0	4.9449-02	1.0009 0	9	1.8660 0	~	2.8000 08		0000	90	_	25	2.2950	_	4.0000	20
1.20	2.2530 0	*	2.6120-02	_	ž	1.8820 0	<u>.                                    </u>	2.800D 0/	3	0000	90		5	2.2940	90	4.0000	٥,
٠٠٠	1.2080 0	•	1.3900-02	1.0000	ç	1.8570 0	_	2.8000 04		0000	9		5	2.2930	80	0000	2
1.60	6.5390	6	7.5950-03	1.0000	•	1.9130	<u>.</u> ,	2.8000 00	-	0000	90	_	i O i	2.2920	90	4.0000	6
1.83	3.5017	6	4.1520-03	1.0000	٥	1.9280	<u>.</u> 1	2.8000 0		0000	9	0010-	S	0162.2	80	4.0000	-
2.00	2.0420 0	60	2.3930-03	1.0000	9	1.9430	<b>-</b> r	2.8000 08		0000	Š	7.0120	en e	2.2900		4.0000	2 6
	•	5 6	50-000-00		0 4	00000	- +	200000000000000000000000000000000000000			ŝ		n u	0402.5	9 9	20000	. *
0.0	0 (1717)	20	7.6340=04	0000	9 4	0014.1		20000	-		9 6		ה עו ס כ	2 2880	9	0000	- 6
200		٠ <u>٠</u>	10-05-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05-10-05			0.00.5	- 1	2.4000 000	-		9	-		2.2870	0 6	3.9990	
3.00	_		5.1350-04		. •	2.0180 0		2.400D 06		0000	9	7.0170	. S	2.2860	0	3.9990	~
3.20	3.2057 0	20	4.7170-04	_	90	2.032D 0	-	2.9000 00	-	0000	90	_	0.5	2.2850	80	3.9990	20
3.40	3.0190 0	02	4.4710-04	1.0000	90	2.0470 (	-	2.9000 0	-	0000	90	7.0190	92	2.2840	80	3.9990	10
3.60	2.9197	02	4.3160-04	1.0000	90	2.0610	-	2.8000 00	-	.0000	90	7.0190	92	2.2830	90	3.9990	07
3.60	2.456n 0	20	4.2110-04		90	2.0760 6	_	2.800U 0	: :	0000	9	7.0200	5	2.2820	90	3.9990	20
00.4	2.8360 0	20	4.129n-04		90	2.6900	<u>-</u>	2.8000 0		0000	90	7.0210	S C	2.2810	<b>0</b>	3.9990	6
4.20	2.820D 0	02	4.061D-04		90	2.1040 0	<u> </u>	2.8000 0	-	.0000	90	7.0220	0	2.2800	80	3.9990	~
C	2.4100 0	95	4.0020-04	_	90	2.1190	<u>-</u>	2.8000 0	<u>:</u>	0000	90	7.0230	S .	2.2790	80	3.9990	2
4.40	2.8040	05	3.9450-04	_	90	2.1330 (	<u>-</u>	2.8000 0	-	0000	96	7.0240	<u>ر</u>	2.2780	80	3.9900	٥,
4.80	2.3000	25	3.8940-04	_	9	2.1470 (	<u>-</u> 1	2.8000 0		0000	ş,	7.0250	S 1	2.2770	8	3.9990	٥,
5.09	2.7970	~	3.8430-04	_	<u>ئ</u>	_	<u>-</u> '	2.800D 0	-	0000	90	7.0260	5	2.2760	8	3.9990	2
2,00	2.7940	2	3.7940-04	_	9	_	2	2.8000 0		0000	9	7.0260		2.2750	80	3.4990	2
C .	2.7927	25	3.7450-04		9	-	21	2.800D 0		0000	90	7.0270	5	0412.5	80	3.9990	2
60.0	2.790.)	۵ د	3.6980-04	0000-1	9 9	2.2020	<u>- r</u>	2.8000		0000	9 0	7.0280	ر د د	2.2730	80	0666	٠,
	4040	v 6	20001010101			001202	- 1	00000			9 2	0000	n u	2.2.2	9 6	2000	
00.0	2 7870	V 6	3.503(1-04 3.5600-04	-	9 4	0.24.20	- 1	2.6000 00			٠ د د	2000	n u	2 27 10	B 0	0666	` C
4	2 7840		3.5.0.04		9 5	2.2570	-	-	-		2	7.0310	ď	2 2 7 0 0	9 6	0000	
6.60	2.7820	20	3.4720-04	_	ş	2.2700 (	-	2.8000 08	٠	0000	9	7.0320	0.0	2.2690	90	3.9980	. ~
6.80	2.78In 0	20	3.4290-04	-	90	2.283D (	-	2.400D 08	-	0000	90	7.0320	95	2.2680	90	3.9980	0
7.00	_	20	3,3850-04	_	3	_	20	2.8000 00	÷	0000	90	7.0330	5	2.2670	90	3.9980	0
7.20	-	20	3.3450-04		ş		2	_	_	0000	96	7.034p	2	2.266D	80	3.9980	2
4.60	2.7770	21	3-3040-04	000001	9 0	Z 3230	_ :			0000	9 6	7.0340	n i	2.2650	80	3.9980	<u>-</u> :
60.	2.1750	70	3.4040-04		9 4	0000		2 2000			9 6	0550.7	יי מי	0.40	D 0	3.990	
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0 4	2 7710		3.10A0.04		9				-		9	2000	1 4	2.2605	9 6	3.000	
9.60	2,7705	. 0	3-0710-04		2	_	<u>~</u>	_	-	0000	90	7.0380	100	2,2590	80	3.9480	. 20
8.80	2,7695	20	3.0350-04	_	90	2.4130	~	_		.0000	9	7.0390	S	2.2580	8	3.9980	10
9.00	2.7680 (	20	2.9990-04	_	9	2.4260	=	2.H000 08	-	0000	90	7.0390	50	2.2570	90	3.9980	~
9.20	2.7670	95	2.9630-04	_	9	2.4390	<u>_</u>	2.800D 0	-	0000	90	7.0400	2	2.2560	8	3.9980	6
0.40	2.7650	20	2.9280-04	_ `	2 :	2.4510	<u>`</u> :	2.8060 0	-	0000	9 (	7.0410	5	2.2550	2	3.9960	5
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	2.7640	20	2.6600-04		2 1	00/4-2		80 0000			8	2	Ď.	2.5340	2 6		<b>-</b> 1
	Z.103U	20	**************************************		2	7001.9	-	-		2	<b>B</b>	7	Ď	263.7	9		5

T=700 K, H=35 km

R- WH	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + M >>> NO2 +NO3 + M	1.160 05	1.200-14
5	2003 >>> 2004 + 02	2.570-14	7.440-49
3	SO + 00 + 200 <<< 600 + 500	5.510-14	3.970-36
4	SON-S << 0N + EON	1.900-11	2.230-19
5	NO + 03 >>> NO2 + 02	2.650-13	4.54D-2A
6	NO2 + 03 >>> NO3 + 02	3.620-15	6.560-22
7	M + SON + OH <<< M + EONH	9.700-03	1.620-14
•	HN03 + H0 >>> H20 + N03	8.00D-14	4.74D-19
•	0 + 0 + M >>> 02 + M	2.300-17	3.640-22
10	M + E0 <<< M + 50 + 0	1.340-17	0.120-01
11	0 + 03 >>> 2*02	7.110-13	8.630-43
15	H + 50M <<< M + 0M + 0	2.180-15	5.170-12
13	0 + MOS >>> MO + OS	1.110-11	8.500-27
14	0 + N02 + M >>> N03 + M	6.110-15	4.890-25
15	HO + HO >>> H2O + O	4.530-12	2.040-16
16	05 + 5400 >>> 54NO5	7.04D-39	9.370-21
1.	NO2 + H-NIJ >>> NO + 0	0.0	0.0
11	0 + HO >>> H + OZ	4.200-11	2.110-15
19	0 + HUS >>> HO + OS	3.910-11	2.19D-2A
<b>2</b> n	M + SOH << M + H + SO	6.660-16	1.500-06
21	03 + H >>> H0 + 05	4.780-11	5.620-37
SS	03 + H0 >>> H02 + 02	3.590-13	8.31D-26
53	2042 + 0H << 20H + En	1-1AD-14	1.120-49
24	H + H0 + M >>> H2O + M	3.370-15	8.100-28
25	H + H02 >>> 2*H0	1.080-10	5.870-24
26	H + HU5 >>> H5 + Q5	2.550-11	0.030-29
27	H + H20 >>> H2 + H0	6.560-17	8.900-13
29	H + H202 >>> H2 + H02	3.060-13	1.770-16
29	H + H202 >>> H0 + H2U	3.980-13	1.020-35
30	24H0 + M >>> H2U2 + M	2./60-15	2.530-45
. 31	HO + HOZ >>> H2O + D2	4.060-11	7.730-33
35	\$+H05 >>> H\$US + QS	9.320-12	3.0211-24
33	HOS + HSO >>> HSOS + HO	2.720-21	3.070-12
34	NO + H + M >>> HNO + H	7.040-16	5.320-07
35	H + SON <<< OH + ON	2.230-21	2.020-10
31	NO + HO + M >>> HNO2 + M	1.150-14	1.430-03
3	NO + NOS >>> NOS + HO	3.600-12	2.680-14
3.	H + H + M >>> H2 + H	6.110-17	5.120-26
39	HN04 + M >>> H02 + N02 + M	1.76D 05	1.650-15
46	CLN03 + H >>> CLO + NO2 + M	9.080 04	6.530-16

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	-5740-04	7.2930	6	6.1115	0.7	2, 34.30	20	7. H150 11	1.400h 1		4.971F 07	2,1490	90	5.300p	=
0.90	2.4410-04	3.8910	60	6.1050	0	2.6820	60	6.6410 11	3.8000 16		4.9625 07	2.2440	90	5.3000	=
1.00	1.3790-04	2.2110	96	6.0580	0 7	2.4510	60	5.6970 11	3.8000 16	`	4.9520 07	2.3480	0.0	5.3000	=
1.20	8.7410-05	1.4160	90	6.017	0	2.9310	3	4.9430 11	3.8000 Je	_	4.9420 07	2.4610	60	5.3000	=
1.40	6.3200-05	1.0320	90	2.00	0	2.4700	5 i	4.3420 11	3.8000 16	•	4.9330 07	2.5800	86	5.3000	=:
1.60	5.0417-05	8.311D	20	5.9010	6	2.9910	<b>5</b> 6	3.8610 11	3.8000	· .	10 0526.0	7 9295	B 4	5.6440	= :
	4.2980-05	7.1610		3,4400	2 2	3,0030	2 0	3.4740 11	3.3000	•	70 0416.	1626.5	9 6	5.2000	= =
00.0	3.427.724.6	6.4330	5 6	717	5 5	3.0160	)   	2.0040	3.8000.1		4.4950 07	3.0770	96	2.2990	:=
7.5	3.2500-05	5.5010		5.5560	6	3,0210	6	2.6940 11	3.8000 16		4.8850 07	3.2000	90	5.2990	=
	3.0670-05	5.3340	70	5.5950	0	3.0240	60	2.5180 11	3.8000 16		4.876D 07	3.3210	90	5.2990	=
2.90	2,9250-05	5.1420	0.7	5.5340	0	3.0270	60	2.3690 11	3.9000 16		4.866D 07	3,4390	80	5.2990	=
3.00	2.8121-05	4.9970	10	5,4741)	0	3,0290	60	2.2420 11	3.8000 16	_	4.8570 07	3,5540	60	2.2990	=
3.20	2,7210-05	4.8890	0.7	5.4140	6	3.0300	60	2.1320 11	3.8000 16		4.8470 07	3,6660	90	2.2990	=
3.40	2,6460-05	4.8080	10	5,3550	01	3,0320	60	2.0350 11	3.8000 1	_	4.8380 07	3,7750	90	5.2990	= :
3,64	2,5850-05	4.7480	2	5,7960	0	3.0330	or .	1.9500 11	3.8000 14	·	4.8280 07	3.8800	90	5.2990	=:
3.80	2.5330-05	4.1050	6	5.2380	6	3.0340	60	1.8740 11	3.4000 10	_	10 0618.	3,9620	8	2.2990	<b>~</b> :
00.	2.4887-05	4.6740	6	5.1800	20	3.0350	7	1.8060 11	3,6000 16			0.00.		3.6790	<b>:</b> :
4.20	5.4500-05	4.4530	2	5.1230	0	3.0360	5	1.7430 11	3.8000		10 0009	00.1.4	80	3.67.60	= :
64.4	2.416/1-05	4.6400	6	5.0660	6	3.0370	٠ د	1.6860 11	3.8000	٠.	10 0161.4	0692.4	96	2.2980	=:
4.60	2.3460-05	4.6330	٥,	2.0100	0	3.0380	2	1.6330 11	3.800D 1		10 0797	0956.	9 9	094760	=:
4.80	2.3580-05	4.6300	2	4.9550	6	3.0380	5	1,5840 11	3,8000 16	<u> </u>	10 071.		9 6	3.6480	= :
5.00	2-3320-05	4.6310	٠,	0006	20	3.0390	6	11.5380 11	3.800D 16	•	10 000	4.3660	90	3.57480	= :
5.20	2.30H)-05	4.6350	20	4.46/	6	3.0400	6	1.4950 11	3.8000 16		7540 07	04000	9 6	2.2480	= :
5.40	2.2467-95	4.6410	ے ا	1920	2	3.0400	ž i	1.4550 11	3.8000	•	70 0547.	4.0860	9 6	3.6480	3:
2.60	2.2640-05	4.64AD	2	1390	2	3.0410	2 6	1.6170 11	3.6000 16	•	7350 07	4.7020	D 6	3.7480	3:
	2.24.310.5	4.57.			5	3.040	2 6	1. 15.0	3.0000	•	10 02 1 1		9 6	2000	= :
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6.80	2.1450-05	4.7090	10	4.4310	6	3.0440	60	1,2250 11	3.8000 1		4.6800 07	5.1640	90 (	5.2980	=
7.00	2,1269-05	4.7290	10	4.3823	6	3.0440	60	1.1980 11	3.8000 16		4.6710 07	5.2240	99	5.2980	=
7.20	2,1077-95	4.7310	0	4.1330	0	3.0450	60	1.1720 11	3.8000 16		4.662D 07	5.2810	90	5.2980	=
7.40	2.0480-05	4.7470	0.7	1.2841)	~	3.0450	60	1.1470 11	3.4000 14		4.653D 07	5.3370	80	5.2980	=:
7.60	2.0547-05	4.7520	10	4.2370	5	3.0460	6	1.1230 11	3.8000 10	•	4.6440 87	5.3910	9 6	2.2980	=:
7.80	50-0150-2	4.7630	2	1840	6	3.0400	5	11 00011	3.8000	_	10 0550.0	10000	9 6	2.6760	= :
8.00	2.0320-05	4.7749	2 10	4 1430	0	3.0400	60	11.08/0.1	3.8000 14	•	10 0020.	34440	84	5.2960	=:
02.8	50-1410-2	4.7840	2	0060	2	3.0470	5 6	11 0950 1	0009-6	٠.	10 0/10·1	00000	9 6	2000	=:
04.0	1.9960-05	4 . 7940	2	0.0200	6	3.0470	5 6	1.0360 11	3.8000 16	•	10 0800.0	3,5410	9 6	3.6980	= :
00.00	20-0879-1	0.00	- 6	4.0050	- P	3.0460	) C	11.010.1	3.6000	•	1.5940 07	5.637.3	9 6	1000 C	==
	10417	0000	5 6	3.0160	2 6	3.0400		0. 7440 10	0000		4.581n 07	7.7560	9 6	5.7980	:=
	1 9230-05	000		10. F. F.		20.0	è	0.080	3.8000		A-5720 07	5.7570		5.2980	:=
. 4.0	1.9050-05	4.8420	70	3,8290	6	3,0500	6	9.436D 10	3.8000		4.563D 07	3.8080	9	5,2980	=
0.00	1.6970-05	4.8510	6	3,7860	6	3.0500	6	9.2690 10	3.8000 16		4.5550 07	5.8470	8	5.2960	=
0.00	1.8707-05	4.8590	70	3.7440	0	3.0500	60	9.1080 10	3.8000 1		4.546D 07	5.8850	80 0	5.2970	=
10.00	1.8520-05	4.8680	0	3.7020	0	3.0510	ŝ	8.9520 10	3.8000 16	_	4.5370 07	5.9220	80 0	5.2970	=

CLN03 1.3590-03 8.5730-04 4.7130-04 2.5180-04 1.4310-04	4 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 -	30.00000000000000000000000000000000000	2,4960-05 2,4940-05 2,4940-05 3,0030-05 3,0030-05 3,0260-05 3,0260-05	3.000 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2.1020-05 2.1080-05 3.11210-05 3.11210-05 3.11210-05 3.11210-05
HNO4 22.3000 08 22.5530-03 5.6360-04 3.0530-04 1.0280-04 1.0280-04	4 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6		4 + 4 + 4 + 4 + 4 + 4 + 4 + 4 + 4 + 4 +		6.2210-05 6.3500-05 6.3500-05 6.4350-05 6.6320-05 6.6320-05 6.6320-05 6.6320-05 6.6320-05
HN02 7-0000 05 6-0900 05 7-0100 05 7-010 05 7-010 05	7.060 05 7.070 05 7.090 05 7.1140 05 7.1530 05 7.1730 05	7.2.170 05 7.2.400 05 7.2.800 05 7.3.400 05 7.3.400 05 7.3.400 05 7.3.400 05 7.3.400 05	7.4510 05 7.4010 05 7.5410 05 7.5720 05 7.6030 05 7.6080 05 7.5680 05	000000000	6.0520 05 6.0520 05 6.1640 05 6.2020 05 6.27410 05 6.3160 05
10000000000000000000000000000000000000			11.00000000000000000000000000000000000		
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HOZ 1.7000 07 1.3000 04 5.4540 07 4.6690 07 4.9710 07	5.4580 07 6.310 07 6.310 07 7.0710 07 7.4110 07 7.4110 07	8.3750 07 8.6780 07 9.2540 07 9.5260 07 9.7940 07 1.0050 08	1.0770 08 1.0990 08 1.1210 08 1.1420 08 1.1530 08 1.1920 08 1.2200 08		1.3840 08 1.4130 08 1.4250 08 1.4360 08 1.4560 08 1.4560 08 1.4560 08
1.0000 06 1.0010 06 1.0010 06 1.0100 06 1.0270 06 1.0330 06		1.1740 06 1.1950 06 1.2380 06 1.2410 06 1.2840 06 1.3320 06	1.381) 06 1.4300 06 1.4570 06 1.4830 06 1.5090 06 1.5350 06 1.5880 06	1.6140 06 1.6400 06 1.6570 06 1.7200 06 1.7200 06 1.7300 06 1.8250 06	1.8529 06 1.9149 06 1.9369 06 1.9569 06 1.9569 06 2.0989 06 2.0340 06
1.0000 06 5.14.0 06 1.5140 07 2.6320 07 3.9570 07	4.1910 07 4.1910 07 4.3040 07 4.3040 07 4.4570 07	4.5290 07 4.5430 07 4.5390 07 4.5240 07 4.5030 07 4.4770 07	4.3780 07 4.3400 07 4.2590 07 4.2170 07 4.1740 07 4.0880 07	3.9580 07 3.9580 07 3.9160 07 3.8710 07 3.7850 07 3.7850 07	3.5800 07 3.5800 07 3.5910 07 3.4620 07 3.3850 07 3.3860 07
1.0000 06 1.6950 11 2.7540 11 3.440 11 3.8560 11	4.2450 III 4.1450 III 4.0430 III 3.9430 III 3.7400 III	3.5290 3.5290 3.5299 11 0.500 11 0.500 11 0.500 11 0.500 11 0.500 11 0.500 11 0.500 11 0.500	2.5525 11 2.5765 11 2.5935 11 2.3580 11 2.2550 11 2.2550 11 2.1580 11	2.0420 11 1.9450 11 1.9450 11 1.9560 11 1.9560 11 1.757 11 1.7360 11	1.7937 11 1.6547 11 1.6547 11 1.5747 11 1.5167 11 1.5167 11 1.4667 11
1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0					

T=800 K, H=35 km

R-HUM	REACTION	FORWARD RATE	BACKWARD RATE
1	N205 + # >>> N02 +N03 + #	6.420 05	8.970-16
5	20 + 20Me2 - CCMe5	3.980-14	5.950-4a
3	SO + ON + SON <<< EON + CON	6.590-14	3.130-36
•	NO3 + NO >>> 20NO2	1.900-11	1.740-18
5	NO + 03 >>> NO2 + O2	3.430-13	4.420-26
6	NO2 + 03 >>> NO3 + 02	5.610-15	9.780-21
7	H + SON + OH << M + EONH	4.600-01	1.020-14
•	MN03 + H0 >>> H20 + N03	8.00D-14	2.430-19
9	0 + 0 + M >>> 0 + M	1.710-17	1.100-17
10	0 + 02 + M >>> 03 + M	1.070-17	5.47D 00
11	0 + 03 >>> 2*02	1.070-12	6.110-39
12	0 + N0 + H >>> N02 + H	1.720-15	1.640-09
13	0 + NOS >>> NO + OS	1.170-11	5.550-25
14	0 + NO2 + N ->>> NO3 + H	5.350-15	4.280-25
15	HO + HO >>> H2O + O	5.000-12	1.060-15
16	05 + Seno >>> Senos	6.400-39	8.78D-2n
17	NO2 + H-NU >>> NO + 0	0.0	0.0
19	0 + H0 >>> H + UZ	4.200-11	9.550-15
19	0 + HOS >>> HO + OZ	4.28D-11	3.430-26
21	P + SOH << # + H + SO	5.330-16	7.950-05
21	03 + H >>> HG + O2	5.250-11	6.310-34
25	03 + HO >>> HO2 + O2	4.30D-13	3.240-24
53	03 + HOS >>> HO + S+OS	1.460-14	2.350-48
24	H + HO + M >>> H2O + M	2.0AD-15	2.060-23
25	H + H05 >>> 5eH0	1.260-10	2.160-55
26	H + H05 >>> H5 + 05	2.710-11	1.450-26
27	H + H20 >>> H2 + H0	4.090-16	1.410-12
28	H + H202 >>> H2 + H02	3.930-13	9.47D-18
29	+ H202 >>> H0 + H20	5.110-13	6.020-37
30	2*HU + M >>> H2OZ + M	2.060-15	1.700-03
31	HO + HOZ >>> H2O + OZ	4.440-11	5.700-3n
32	20H0Z >>> H20Z + 0Z	9-100-12	1.530-22
33	HO2 + H20 >>> H202 + H0	5.190-20	3.460-12
34	NO + H + M >>> HNO + M	5.840-16	3.470-05
35	NO + HO >>> NO2 + H	3.300-20	2.300-10
36	N + SONH << N + OH + ON	8.270-15	7.860-02
37	NG + HOZ >>> NGP + HG	4.460-12	7.66D-14
39	H + H + M >>> HZ + M	5.350-17	5.640-22
39	HN04 + M >>> H02 + N02 + M	9.250 05	1.210-15
40	CLN03 + M >>> CL0 + NO2 + M	5.870 05	3.770-16

7 1 MF (C.)	40614	70.	600	Š	10	20	E ONI	НĢ	H20
0.0	5.5000 07	2.200n 09	2.0000 06	5.500D 0A	1.300n 12	3.4000 16	5.0000 07	\$.0000 06	5.3000 11
0.00	7.3770-05	8.922n n8	5.921n 07	2.1450 09	4.1900 11	3.400P 16	4.5610 07	3,1730 08	5.2990 11
04.6	1.157:-05	1.414D UN		7.1400 09	1	3,4000 16	4.1610 07	4. H590 08	5.2090 11
0.50	50-0502.2	2.6940 01	_	3.0540 09	*.5+0f) 10	3. HOOO 16	3,7950 07	6.6860 08	5.2970 11
0.90	9.2190-07		5.7840 07	3.0780 09	6.5110 10	3.8000 16	3.4623 07	8.5300 08	5.2960 11
1.00	7.1290-07		5.7180 07	3.0940 09	6.0110 10	3.8000 16	3,1590 07	1.0340 09	5.2950 11
1.20	6.5540-07	8.4310 05	5.4520 07	_	5.7650 10	3.8000 16	2.9810 07	1.2110 09	5.2940 11
C .	6.4547-07		5.5460 07	_	5.6130 10	۰.	2.628D 07	1.3830 09	5.2930 11
1.60	6.3427-07		_	_	5.4890 10	3,8000 16	2.3970 07	1.5510 09	5,2930 11
1.30	6.2190-07		5,4570 07	_	5. 3750 10	3.800D 16	2.1860 07	1.7130 09	2.2920 11
50.5	10-0591-01		5,3940 07	3.1000 09	5.2660 10	3.8000 16	10 0466.1	1.8/00 09	2.2910 11
6.20	6.0560-07		5.33In 07	-	01 0091.2	3.8000 16	1.8190 07	50 CCL. C	11 0067.5
0.0	5.9711-67		5,2590 07	•	01 0840.4	3,8000 16	10 0650-1	2.1700 09	11 0682.5
2007		90 (1001.90	10 (1102.4		4.9580 10	3,9000 16	20 0016.1	60 0215.2	2.6660 11
90.0	70-00-00		3.1401 07	3.1040 09	01 0254.4	3.8000 15	1.3510 07	60 00000	2,0000 11
00.6	5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6		5 0270 07	_	4.6770 10	3. 9000	1.1490 07	2.7110 00	5.2840 11
	70-040-0		10 06 BO 4		2 6897	3. 8000 16	70 04 90 1	2 8 150 60	5.2860.11
	5.5560-07		4.9100 07		4.5030 10	3.8000 16	9.5570.06	2,9540 09	5.2650 11
3,80	5-4610-07		4.8520 01	_	4.4200 10	3.8000 16	8.7180 06	3,0680.09	5.2840 11
00.4	5.1987-07	_	10 0961.4	_	4.3380 10	3.8000 16	7.9520 06	3.1780 09	5.2840 11
4.20	5.3370-07	_	4.7390 07	_	4.2590 10	3.8000 16	7,2530 06	3.2830 09	5.2830 11
	5.277-07		4.58411 07	3.1200 09	4.1820 10	3.8000 16	6.6160 06	3,3840 09	5.2830 11
4.60	5.2190-07		4.5290 07	3,1220 09	4.1080 10	3.8000 16	6.0350 06	3.4810 09	5.2820 11
4.80	5.1530-07		4.5740 07	_	4.0350 10	3.8000 16	5.5050 06	3.5740 09	5.2820 11
5.00	5.1080-07		4.5210 07	3.1240 09	3,9640 10	3,8000 16	_	3,6630 09	5.2810 11
5.20	5-054:-07		4.4580 07	_	3.8950 10	3.8000 16	4.580D 06	3.7470 09	5.2810 11
5.40	5.002-01		4.4150 07	3.1250 09	3.4280 10	3.8000 16	4.1780 06	3,8280 09	5.2800 11
5.69	4.9517-07	8.1260 06	4,3639 07	3.1260 09	3.7620 10	3.800D 16	3.8110 06	3.9060 09	5.2800 11
5.80	4.9010-07	_	4.3120 07	3.1270 09	3.6790 10	3.8000 15	3.4760 06	3,9790 09	5.2800 11
6.00	4.8520-07	8.1540 06	4.2610 07	3.1280 09	3.6370 10	3.8000 16	3.1710 06	4.0490 09	11 0612.2
6.20	4.80411-07	8.1690 06	4.2110 07	3.1290 09	3.5760 10	3.8000 14	2.8920 06	4,1150 09	5.2790 11
6.40	4.7560-07	A.1850 05	4.1610 07	3290 09	3.5170 10	3.8000 16	2.6380 06	4.1790 09	5.2780 11
6.60	4.7177-07	8.202n 06	4.1120 07	3.130n 09	3.4500 10	3,8000 16	2.4060 06	4,2380 09	5.2780 11
6.80	4.6540-07	8.2190 06	4.0640 07	_	3.4030 10	3,8000 16	2.1950 06	4.2950 09	5.2780 11
7.00	4.5190-07		4.0160 07	_	3.3490 10	3,8000 16	2.0020 06	4.3490 09	5.2780 11
7.70	4.5750-07	8.2550 06	3.9640 07	-	3.2950 10	3,8000 16	1.8260 06	4.3990 09	5.2770 11
	4.5317-07	8.2730 05	3,9220 07	330	3.2430 10	3.8000 16	1.6660 06	4.44.70 09	5.2770 11
09.	70-UHH-01	-	3.8750 07	3,1330 09	3.1930 10	3.8400 16	90 00251	4.4920 09	5.2770 11
	0-1,600	9. 31/0 00	70 (+OF D • 5	_	3.14.30 10	3.8000 16	1.3800 06	4.0340 09	11 0//2:5
9.00	4.40 JU-07	8.3310 06	3,7850 07	_	3.0950 10	3,8000 16	1.2640 06	4.5740 09	5.2770 11
9.20	4.3511,-07	8.3510 06	3.7400 07	320	3.0470 10	3.8000 16	1.1530 06	4.611B 09	5.2760 11
9.40	4.3200-07	8.3710 05	3.6960 07	350	3.0010 10	3.8000 16	1.0520 06	4.6460 09	5.2760 11
8.59	4.2790-07	3910 06	3,4520 07	_	2.4560 10	3.8000 16	9.5970 05	4.6790 09	5.2760 11
05.0	4.2399-07	8.411n 05	3,6090 07	3,1360 09	2.9120 10	3.8000 16	8.7540 05	4° 7090 00	5.2760 11
00.6	4.1990-07	9.4310 00	3.5660 07	3,1370 69	2.9700 10	3.8000 16	7.9860 05	4.7370 09	5.2760 11
9.20	4.159n-07	8.4510 06	3.5240 07	3,1370 09	2.8280 10	3.8000 16	7.2850 05	4.763D 09	5.2760 11
04.6	4.120n-07	8.472D 06	3.4830 07	3,1380 09	2,7870 10	3.8000 16	6.6460 05	4.7870 09	5.2760 11
09.0	4.0910-07	9.4920 06	3.4420 07	3,1380 09	2.7470 10	3.8000 16	6.0620 05	4.8090 09	5.2750 11
00.0	4.0435-07	8.5120 06	3.4010 07	3,1390 09	2.707D 10	3.8000 16	5.5300 05	4.8300 09	5.2750 11
10.00	4.0040-07	8,5330 06	3,3610 07	3,1390 09	2.6690 10	3.8000 16	5.0450 05	4.8480 09	5.2750 11

1.0000 00	1.0000	9	-	9	1. /000		2. A000 06	3 1.0000	90			2,3000 08	4.0000 07
	2.4280 0	~ :			2.0120	5	2.7990 06	000001	900		50	2.3500-05	5.1590-05
• •	6.783D		1.0220	£ 6	3,1560		7.7950 08		5 6		ເຂ	1.1850-06	1.5610-06
•	8.5830 0	~	_		4.3110	20		. –	90		5	6.4340-07	6.6000-07
-		80	_	9:	5.2530	6		1.0000	90	6.6040	ر د م	6.1460-07	5.1690-07
	1.3020 0	0 60	1.1660	9 9	7.0690		2.7430 08		90	6.5210		7.6670-07	4.7910-07
_	.4260	9	_	90	7.9400	20	_	-	90 0	6.4930	2	8.5470-07	4.7560-07
~	_	80	1.3070 0	90	8.7840	0,	2.7760 08	_	90	6.4750	s :	9.4120-07	4.7340-07
	0149.	E	1.3965	90	0509.6	<u> </u>	2.77.10 08	0000	9 6	6.4630	បក	1.10750-06	10-091/-4
	-	9 60	1.6120	9	1.1160	8	_	-	90	6.4680	Š	1.1860-06	4.6930-07
_	_	90	1.7400	90	1.1900	90	_	_	90 0	6.4810	2	1.2620-06	4.6840-07
_	_	- 60	1.4790 0	90	1.2620	9	_	_	90	6.5020	2	1.3350-06	4.6760-07
10	.0270	e (	2.0310	9	1.3310	69	_	<b></b> .	90	6.5280	ž.	1.4070-06	4.6700-07
٠.	0280.2	<b>D</b> 0	2.1950	9 4	1.3970	8 6	2 7250 08		9 6	0196.0	บัก	1.4750-06	4.6600-07
	1740		2 6560	9 4	6230	9 6		-	9	4.6450	Š	1.6070-06	4.6610-07
	2.2110		2.7530	9 9	1.5830	80		-	90	6.6950	ເຮ	1.6690-06	4.6600-07
	2.244n (	8	2,9600	90	1.6400	80	2.7160 08	_	90 0	6.7500	20	1.7300-06	4.6610-07
		6	3.1769 (	90	1.6940	90	_	_	90 0	6.8100	Š	1.7880-06	4.6630-07
	2950		3.4000	90	1.7470	80	2.7030 08	010011	90	6.8740	٠ د د	1.8440-06	4.6650-07
	0000	 	3.87&n	9 9	1.8450	9 6	9 6		96	7.0150	S &	1.9510-06	4.6730-07
	_		4.1210	ş	1.8910	8			90	-	5.5	2.0020-06	4.6790-07
	_	•	4.3750	9	1.9350	90		_	90 0		\$	2.0510-06	4.6850-07
	_	80	4.6350	90	1.9760	80	_	~	90		50	5.0990-06	4.6910-07
	2.3570	<b>8</b> 6	7 0000	9 4	2.0160	<b>9</b> 9	2.6600 08	02001	9 6	7,3370	č i	2-1440-06	4.6990-07
	_	-	5.4430	90	2.0900	90		-	9 6	7.5140	. 5	2.2310-06	4.7150-07
	2.3490	96	_	90	2.1250	90	•	_	90	7.6070	2	2.2720-06	4.7240-07
	2.343h	Ē	6.0010	90	2.1570	90	ē	_	90 0	7.7010	5	2.3110-06	4.7330-07
	2.3341	D 0	6.6840	e 4	2.1.00	D 0	5 6		90	7.7960	<u>د</u> د	2.3490-06	10-00-01
	7.31.20		3.857D	9 2	2.2450	9	2.6060 08	0200.1	9 6	7.0020	ה	2.4200-06	10-026/**
	2.2980	8	7.1450	90	2.2710				36	-		2.4530-06	4.7730-07
	2.2830	80	7.4340	90	2,2950	_	2.5910 0	8 1.002b	0,00		0.5	2.4850-06	4.7840-07
		9	_	9	2,3160	90	Ö	-	900	6.2950	55	2.5160-06	4.7950-07
		80	_	9	2.3400	80	_	_	Š	8.3970	5	2.5450-06	4.8060-07
	_	80	_	9	2.3600	8 6	_	_	90	8.500D	5	2.5740-06	4.6170-07
	2.2140	9	8.5920	9	2,3790	8	0	_	90	8.6030	S.	2.6600-06	4.8290-07
		8	9.9800	9 :	2.3970	E (	0		90	8.7070	5	2.6260-06	4.8400-07
	2.1740		9.16/11	9 5	200	E 6	2.5430 0	1.0030	96	8.8110	i S	2.6510-06	4.8520-07
			9.7360	9	2.4430		<b>S</b>	0.0001			ת מ	2.4040-00	4.8750-67
	2.1100		1.0020	20	2.4570	80	Ġ	-	200	0-1220		2.7170-06	4.8870-67
	2.0980		1.0300	0	2.4690		2.5100 0	1.0030	9	9.2250	. <u>.</u>	2.7370-06	1-8990-07
	2.0660	80	1.0580	0	2.4800	80	2.5020 0	8 1.0030	900	9.3280	2	2.7560-06	
	2.0430	2	1.0850	6	2.4900	8	2.4940 0	B 1.003	900	9.4300	20	2.7740-06	1.0224.4
	2.0200	9	1.1120	-	2.5000	9	2.4560 0	F00"I 0	90	9.5320	2	2.7910-06	

<b>そ</b> つれーと	REACTION	FORWARD RATE	BACKWARD RATE
-	N205 + M >>> N02 +N03 + H	4.050-06	1,270-13
~	2*N03 >>> 2*N02 + 02	4-710-17	7.460-62
e	NO2 + NO3 >>> NO2 + NU + 02	4.210-15	1.190-34
•	NO3 + NO >>> 2*NO2	1.900-11	3.290-32
S	NO + 03 >>> NOZ + 02	6.360-15	1.080-56
ø	NO2 + 03 >>> NO3 + 02	6.650-18	8.330-39
7	HN03 + M >>> HO + N02 + M	5.360-28	2.460-12
œ	HNO3 + HO >>> H20 + NO3	8.000-14	3.760-30
o	0 + 0 + M >>> 02 + M	2.690-15	1.440-57
10	0 + 05 + M >>> 03 + M	5.760-16	1,620-12
==	0 + 03 >>> 2402	1.920-15	0.0
12	0 + NO + M >>> NO2 + M	1.130-13	8.390-48
13	0' + NO2 >>> NO + O2	5.120-12	6.270-53
14	0 + NO2 + M >>> NO3 + H	7.070-14	5.660-24
15	HO + HO >>> H2O + O	1.09D-12	9.170-27
97	02 + 2*N0 >>> 2*N02	2.750-38	3.880-35

(S)	N205	20N	NO3	ON	03	20	HNO3	웃	H20
0.0		6.3000 09	2.0000 06	7.0000 09	4.300D 12	1.4100 17	۵	1.000D 06	1.00001
0.50	6.5000 08	6.3950 09	1.9610 06		4.3000 12	1.4100 17	3.000D 09		1.0000 11
1.00			1.9280 06		4.300D 12	1.4100 17			1.00001
1.50			1.8990 06	6.7180 09	4.3000 12	1.4100 17		9.7660 05	1.00001
2.00			1.875D 06		4.3000 12	1.4100 17		9.6870 05	1.00001
2.50			1.8560 06		4.3000 12	1.4100 17		9.6080 05	1.00001
3.00			1.8400 06	60 (1877.9	4.2990 12			-	1.00001
3.50								9.4480 05	1.00001
<b>4.</b> 00			1.8200 06					_	1.00001
4.50			1.8140 06	6.1890 09	4.2990 12	1.4100 17	3.0000 09	9.2870 05	1.0000.1
5.00					4.2990.12		-	_	1.0000 11
5.50								_	1.00001
6.00			1.8140 06				_	_	1.00001
6.50					4.2990 12		_	-	1.00001
7.00			1.8260 06			•		_	1.00001
7.50			1.8360 06					-	1.00001
8.00			1.8470 06					_	1.00001
8.50			1.8590 06			-	_	_	1.00001
9.00			1.8740 06	5.4720 09			3.0000 09	_	1.00001
9.50			1.8900 06				3.000D 09	_	1.00001
00.0			1.9080 06			-	3.000D 09	_	1.00001

25 km  $HNO_3$ ,  $N_2O_5$ , 0,  $300^9$ K

R-NCH	REACTION	FORWARD RATE	BACKWARD RATE
7	N205 + M >>> NOZ +NO3 + M	3.270-03	5.940-14
~	2*N03 >>> 2*N02 + 02	2.410-16	1.750-58
۳	NO2 + NO3 >>> NO2 + NO + 02	8.210-15	4.920-35
•	NO3 + NO >>> 2*NO2	1.900-11	6-980-29
ທ	NO + 03 >>> NO2 + 02	1.670-14	2.850-49
¢	NO2 + 03 >>> NO3 + 02	3.410-17	2.000-34
7	HNO3 + M >>> HO + NO2 + M	4.010-21	1.300-12
œ	HNO3 + HO >>> H2O + NO3	8.000-14	1.690-27
o	0 + 0 + M >>> 02 + M	1.230-15	5.480-58
10	0 + 02 + M >>> 03 + M	3.420-16	2.740-09
11	0 + 03 >>> 2*02	8.900-15	0.0
12	0 + NO + H >>> NOZ + H	6.400-14	2.510-38
13	0 + NO2 >>> NO + O2	6.250-12	3.730-46
*1	0. + NOZ + M >>> NO3 + M	5.890-14	4.710-24
15	HO + HO >>> H2O + O	1.570-12	4.630-24
16	02 + 2*N0 >>> 2*N02	1.930-38	2.260-31

TMF (C)	SUCN	Z	CON		S C N	ON	60	20	HNO3	9	H20
0.0			3000	9	2,0000 06	7.0000 09	4.3000 12	1.1800 17	3.0000 09	1.0000 06	1.0000 11
0.50				60	3,3580 06	6.7530 09	-	1.1800 17		_	1.0000
1.00				30		6.5140 09	4.300D 12	1.1800 17			1.00001
1.50	6.4680 08		7.0190	60	5.8980 06	6.2840 09	4.2990 12	1.1800 17	3.0000 09	9.8720 05	1.0000 11
2.00				60	7.0960 06	6.0620 09	4.2990 12		3.0000 09		1.0000
2.50				60	_	5.8470 09	4.2990 12				1.00001
3.00				60		5,6410 09	4.2990 12	1.1800 17	3.000D 09	9.7320 05	1.00001
3.50				60	1.0480 07	5.4410 09	4.2980 12				1.0000 11
00.4				60	1.1550 07	5.2480 09	~				1.00001
4.50				60	1.2600 07	5.0630 09	4.2980 12	1.1800 17	3.000D 09		1.00001
5.00				30	1,3640 07	4.883D 09	~				1.0000
5.50				60	1.4660 07	4.7100 09					1.0000
00.9				60	1.5670 07	60 0575.5	4.2980 12				1.00001
6.50				60	1.6670 07	4,383D 09	4.2970 12				1.0000 11
7.00				60	1.7660 07	4.2270 09	4.2970 12				1.00001
7.50				60	1.8650 07	4.078D 09	~				1.00001
8.00				60	1.9630 07	3,9330 09	4.2970 12				1.0000 11
8.50				60	2.0620 07		_				1.00001
9.00				50	2.1600 07	3,6590 09	_				1.00001
9.50				60	2.2580 07	3.5290 09	~		3.0000 09		1.00001
10.00				60	2,3570 07						1.0000

25 km HNO<sub>3</sub>, N<sub>2</sub>O<sub>5</sub>, 0, 400<sup>0</sup>K

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
÷	N205 + M >>> N02 +N03 + M	1.330 01	2,170-14
8	2*N03 >>> 2*N02 + 02	1.860-15	2,850-54
m	NO2 + NO3 >>> NO2 + NO + O2	1.890-14	1.630-35
•	NO3 + NO >>> 2*NO2	1.900-11	1.000-24
'n		5.600-14	5.390-40
٠	NO2 + 03 >>> NO3 + 02	2.620-16	5.960-29
^	HN03 + M >>> H0 + N02 + M	1.200-12	4.750-13
<b>a</b>	HN03 + H0 >>> H20 + N03	8.000-14	3.490-24
σ	0 + 0 + M >>> 02 + M	4.360-16	5.060-48
01	0 + 02 + H >>> 03 + M	1.680-16	2,820-05
11	0 + 03 >>> 2*02	6.050-14	6.810-66
12	0 + NO + M >>> NO2 +	2.950-14	1.650-26
13	0 + NO2 >>> M2	8.030-12	1,100-37
14	c	4.420-14	3.540-24
		2.500-12	1.020-20
	20 *5 < C C	1.240-38	1.090-26

						Ç	ć	(		ę	
Z	N205		204		502	2	50	20	TOPE	£	271
Ġ	6.500n o	98	6.3000		2.0000 06	7.000D 09	4.300D 12	8.8400 16	3.000D 09	1.000D 06	1.0000 11
8		35	7.8040		6.2160 08	6.1750 09	4.2990 12	8.8400 16	3.000D 09	9.9830 05	1.00001
0		33	8.5650		5.9360 08	5.4440	4.2980 12		3.0000 09	9.9640 05	1.00001
æ		03	9.2310	60	5.7030 08	4.801D 09	4.2980 12	8.8400 16	3.000D 09	9.9430 05	1.00001
00		33	9.8160		5.5160.08	4.2340	4.2970 12		_	9.9210 05	1.00001
٥		33	1.0330		5,3660 08	3.736D	4.2970 12		3.0000 09		1.00001
Φ		33	1.0780		5.2480 08	3.2960	4.2960 12		_	9.8730 05	1.00001
0		33	1.1180		5.1570 08	2.9090	4.2960 12		_	_	1.00001
o		33	1,1530			2.5670	4.2960 12		_		1.00001
Q,		33	1.1830			2.2660	4.2950 12		_		1.00001
σ	9.8660 0	33	1.210D		5.0020 08	2.000D	_		_		1.000D 11
7		74	1.2340			1.7660	_		_	_	1.00001
~		74	1.2550			1.5590	4.295D 12		_	9.7110 05	1.0000 11
_		74	1.2730			1.3760	_		_		1.00001
~		40	1.2890			1.2150	4.2940 12		_	_	1.00001
-		34	1.3030			1.0730	4.2940 12		_	_	1.00001
~		40	1.3150			0.4740	-		_	_	1.0000 11
-		74	1.3260			8.3660	~	-	_	_	1.00001
~		*	1.3350		5.0950 08	7.3880	4.2940 12	-	3.000D 09	_	1.00001
~		40	1.3440		0		4.2940 12	-	3.0000 09	9.5050 05	1.00001
~		4	1.3510		5.1810 08		4.2940 12		_	9.4750 05	1.00001

25 km  $HNO_3$ ,  $N_2O_5$ , Q,  $550^{\circ}$ K

AUX-R	REACTION	FORWARD RATE	BACKWARD RATE
-	N205 + M >>> N02 +N03 + M	1.100 04	8.790-15
8	2*N03 >>> 2*N02 + 02	9.880-15	7.980-51
е	NO2 + NO3 >>> NO2 + NO + O2	3.730-14	6.640-36
•	NO3 + NO >>> 24NO2	1900-11	2,540-21
S	NO + 03 >>> NO2 + 02	1.500-13	2.090-32
•	NO2 + 03 >>> NO3 + 02	1.400-15	1,810-24
7	HN03 + M >>> H0 + N02 + M	7.060-06	1.560-13
æ	HN03 + H0 >>> H20 + N03	8.000-14	1.800-21
Φ	0 + 0 + H >>> 02 + H	1.720-16	9.450-31
10	0 + 02 + M >>> 03 + M	8.610-17	4.970-02
11	0 + 03 >>> 2*02	2.900-13	3,430-51
12	0 + NO + M >>> NO2 + M	1.440-14	7.090-17
13	0 + NO2 >>> NO + O2	9.850-12	9-330-31
14	0 + NOZ + M >>> NO3 + H	3.210-14	2.570-24
15	HO + HO >>> H20 + O	3.650-12	5.560-18
16	02 + 2*N0 >>> 2*N02	8,650-39	6.750-23

H20	1.00001	.0000	.0000	.0000	1.00001	1.00001	1.0000.1	1.0000.1	1.00001	1. 0000	1.00001	0000	.0000	1.00001	0000	1.0000.1	1.0000.1	1.0000.1	1.00001	1.00001	11 0000
	90	90	90	90	90	90	90	90	90	90	90	90	90	90	90	90	90	90	90	90	
9	0000°1 60	_	09 1.0200	•	_	_	09 1.0590	0690 1 60		0680.1 60	0660.1 60										
HN03	3.000D	3.0000	3.0000	3*;000D	3.000D	3.000D	3.000D	3.000D	3.0000	3.000D	3.0000	3.0000	3.000D	3.0000	3.0000	3.000D	3.0000	3.000D	3.0000	3.0000	3.000D
02	6.4300 16	6.4300 16	_	_	$\overline{}$	_	6.4300 16	_	_		6.4300 16										
03	4.300D 12	4.240D 12	4.1990 12	4.1590 12	4.120D 12	4.0820 12	4.0440 12	4.0070 12	3.9710 12	3.9350 12	3.900D 12			3.7970 12		3,7310 12	3.6990 12	3.6680 12	3.6370 12	3.6060 12	3.5760 12
02	7.0000 09	5.8000 09	5.2820 09		4.780D 09	4.662D 09	4°5890 09	4.5440 09	4.5170 09	4.5010 09		4.4860 09	4.484D 09				60 Q064.4	4.4920 09	4.495D 09	4.498D 09	4.5020 09
NO3	5.0000 06	6.3910 08	6.3460 08				6.4020 08	6.4310 08	6.4590 08	6.4850 08	6.5090 08	5290	6.5470 08	5610		6.5800 08		5870	6.587D 08	-	6.5790 08
NO2	6.3000 09	_	8.6850 09	_	_	_	9.3730 09	_	_	9.453D 09	9.460D 09	9.4630 09	9.463D 09	0	0	9.4570 09	9	0	0	0	9.4430 09
N205		4.1750 00		_				4.8460 00			4.9280 00						4.9830 00				4.9720 00
TIME (S)	0.0	0.50	1.00	1.50	2.00	2.50	3.00	3.50	00.4	4.50	5.00	5.50	00.9	6.50	7.00	7.50	8.00	8.50	9.00	9.50	10.00

25 km HNO<sub>3</sub>, N<sub>2</sub>O<sub>5</sub>, 0, 600°K

A-NUM	REACTION	FORWARD RATE	BACKWARD RATE
-	N205 + M >>> N02 +N03 + M	<b>4.80</b> D 04	7.070-15
~	2*N03 >>> 2*N02 + 02	1.430-14	4.660-50
m	NO2 + NO3 >>> NO2 + NO + O2	4.340-14	5.430-36
•	NO3 + NO >>> 2*NO2	1.900-11	1.450-20
S.	NO + 03 >>> NO2 + 02	1.670-13	1.020-30
•	NO2 + 03 >>> NO3 + 02	2.020-15	1.790-23
1	HN03 + M >>> H0 + N02 + M	2.100-04	1.150-13
<b>6</b> 0	HN03 + H0 >>> H20 + N03	8.00D-14	7.210-21
Φ	0 + 0 + M >>> 02 + M	1.370-16	6.300-27
10	0 + 02 + H >>> 03 + H	7.310-17	2,580-01
11	0 + 03 >>> 2*02	4.110-13	6.340-48
12	0 + NO + M >>> NO2 + M	1.210-14	9.650-15
13	0 + NO2 >>> NO + O2	1.030-11	3.230-29
14	X + EON <<< X + ZON + O	2.950-14	2,360-24
35	HO + HO >>> H2O + 0	3.970-12	2.260-17
16	02 + 2*N0 >>> 2*N02	7.980-39	4.630-22

:	=	=	11	11	1	11	1	1	77	11	11	=	1	11	=	11	11	1	=	11	~
H20	0000	0000	00000	0000	0000	0000	0000	0000	0000	0000°	0000	0000	0000	0000	0000	0000	0000	0000	0000	0000	0000
I.	<b>:</b>	-	-	-	<del>-</del>	-	-	-	-	۲.	<b>:</b>	<b>:</b>	-	-	<b>:</b>	<del>:</del>	<b>:</b>	-	-:	<b>.</b> ;	~
			_								90 (										
오	1.0000	1,3140	1.6290	1.943D	2,2570	2,5710	2.8850	3.1990	3.5120	3.8260	4.139D	4.452	4.7650	5.0780	5,3910	5.703	6.016	6.3280	6.6400	6.952	7.264
,	60	•	Φ.	o.	•	Φ	<b>J</b>	Φ	Φ.		60										
	_	000							_			_	_	_	_	_					
HINO3	3.0000	3.0000	2.9990	2.9990	2.9990	2.998D	2.9980	2.99	5.99	5.99	2.997D	5.99	2.99	2.99	2.99	2.99	2.99	2.99	2.99	2.9940	0466
	91				- •						16				•	- •					
20	.8900	.8900	.8900	0068	.8900	.8900	.8900	.8900	9890D	0068	5.8900	9890D	9890D	.8900	.8900	.8900	.8900	0068*	.8900	.8900	.8900
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	_		_	0 15		_		_	_	_	0 12	_	_	_			_	_	_	_	
03	4.300	3.9290	3.6640	3.431	3.224	3.0370	2.869	2.717	2.578	2.452	2.3370	2.230	2,133	2.0420	1.959	1.881	1.8090	1.742D	1.6790	1.6210	1.5650
	60		-	_		-			0.7	01	70	0.7	10	10	10	10	10	0.7	10	01	70
00	7.0000	8.1990	9,3350	9,7370	0506.6	9.9990	1.0070	1.0130	1.0180	1.0220	1.0270	1.0310	1.0350	1.0380	1.0420	1.0450	1.0480	1.0510	1.0530	1.0560	1.0580
	٥			90		90	90		80	90	90	<b>2</b> 0	20	30	00	80	20	ø	08	80	œ.
	000		2430 0	9510 0															5440 0	407D 0	
NO3	2.0000	6.4600	6.24	5,95	5,64	5.3420	5.05	4.77	4.5050	4.2520	4.01	3.78	3,57	3,37	3.18	3.0100	2.84	2.6890	2.54	2.40	2.28
											50										
N02	300D	7580	6430	2700	1340	0020	0310	0020	9780	9560	9360	9180	9020	8860	8710	8580	8450	8320	8210	8100	1990
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	90 G	0-01	0-01	10-0	0-0	70-0	10-G	0-0	10-0	10-0	0-0	10-0	0-0	0-0	10-0	0-0	0-01	10-0	10-0	0-0	0-0
N205	6.500	5.473	4.2660-01	3.740	3,433	3.199	2.995	2.809	2.636	2.475	2.3250-01	2.184	2.053	1.930	1.815	1.709	1.609	1.516	1.430	1.349	1.274
TIME (S)	0.0	0,50	1.00	1.50	2.00	2.50	3.00	3.50	00.4	4.50	5.00	5.50	6.00	9.50	7.00	7.50	8.00	8.50	9.00	9.50	10.00

25 km,  $HNO_3$ ,  $N_2O_5$ , 0,  $700^{\circ}$ K

TON-W	REACTION	FORWARD RATE	BACKWARD RATE
-	N205 + M >>> N02 +N03 + M	4.800 05	4.940-15
~	2*N03 >>> 2*N02 + 02	2.570-14	7.440-49
m	NO2 + NO3 >>> NO2 + NO + O2	5.510-14	3.970-36
4	NO3 + NO >>> 2*NO2	1.900-11	2,230-19
ហ	NO + 03 >>> NO2 + 02	2.650-13	4.540-28
•	NG : + 03 >>> NO3 + 02	3.620-15	6.560-22
~	HN03 + M >>> H0 + N02 + M	4.010-02	6.700-14
æ	HN03 + H0 >>> H20 + N03	8.000-14	6.380-20
٥	0 + 0 + M >>> 02 + M	9.500-17	6.210-21
10	0 + 02 + M >>> 03 + M	5.550-17	3,360 00
11	0 + 03 >>> 2+02	7.110-13	8.630-43
12	M + 20N 4 4 W + 0	9.010-15	2-140-11
13	0 + NO2 >>> NO + O2	11-011-1	8.500-27
14	0 + NO2 + M >>> NO3 + M	2.530-14	2.020-24
15	HO + HO >>> H2O + O	4.530-12	2.040-16
16	20N+2 << 0N+2 + 20	7.040-39	9.370-21

7000	00000	20000	
00000	0960	999 AM	
H20 1.000D 9.9990 9.9980	9.9960 9.9960 9.9950 9.9950 9.9940	9.9940 9.9940 9.9940 9.9930 9.9930	0.0000 0.0000 0.0000 0.0000 0.0000 0.0000
00 00 08 08	999999		
HO 1.000D 6.049D 1.188D 1.758D	2.316D 2.862D 3.396D 3.917D 4.425D	5.4060 5.8780 6.3380 6.7850 7.2210	7.6450 8.0560 8.4560 8.8450 9.2220 9.5870
6666	00000	00000	00000
HN03 3.000D 2.940D 2.882D 2.825D	2.4690 2.6600 2.6600 2.6600	2.4060 2.4060 2.33590 2.2660	2.1340 2.1340 2.0910 2.0500 2.0500
2000W	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~		~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~
	91199		9 9 9 9 9 9
02 5.0000 5.0000 5.0000	5.0010 5.0010 5.0010 6.0010		5.0010 5.0010 5.0010 6.0010
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03 4.300D 1.266D 8.002D 6.071D	4.904D 4.112D 3.540D 3.106D 2.766D	2.2680 2.2680 2.0800 1.9210 1.7840	.5600 .4680 .3860 .3120 .2460
3 4 4 8 9	44444		
9	22222		
NO 7.000D 1.366D 1.386D 1.397D	1.4080 1.4170 1.4270 1.4350 1.4440	4590 1.4590 1.4730 1.4730 1.4790	1.4910 1.4960 1.5020 1.5070 1.5110
-			44444
•			
N03 2.0000 6.1520 5.4490	4.2390 3.7310 3.2810 2.830 2.5310	1.9490 1.9490 1.4990 1.3140	1.0110 8.866U 7.781D 6.8320 6.0030 5.2790
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3554		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	
NO2 5.3000 3.8470 3.1780 3.2410	330 469 521 564 564	63 67 67 67 67 67 67 67 67	3.7290 3.7410 3.7530 3.7640 3.7740
• • • • • • • • • • • • • • • • • • • •	.,		
N205 6.5000 08 2.4320-03 1.7790-03	. 4510-03 . 3060-03 . 1700-03 . 0430-03		3.8730-04 3.4090-04 3.0010-04 2.6430-04 2.3290-04
N205 .5006 .4326 .7796	170 170 170 170 170	273	643 643 643 643 643 643
1ME (S) 0.0 0.50 1.00	0.00 m 4	- 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	4.50 8.00 9.00 9.50
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25 km,  $HNO_3$ ,  $N_2O_5$ , 0,  $800^{\circ}$ K

R-NUM	REACTION	FORWARD RATE	BACKWARD RATE
~	N205 + M >>> N02 +N03 + M	2.650 06	3,700-15
~	2*NO3 >>> 2*NO2 + 02	3,980-14	5.950-48
m	NO2 + NO3 >>> NO2 + NO + O2	6.590-14	3.130-36
•	NO3 + NO >>> 2*NO2	11-006-1	1.740-18
'n	NO + 03 >>> NOZ + 02	3.430-13	4.420-26
٠	NO2 + 03 >>> NO3 + 02	5.610-15	9.780-21
7	HN03 + M >>> H0 + N02 + M	1.900 00	4.200-14
æ	HN03 + H0 >>> H20 + N03	8.000-14	3,280-19
Φ	0 + 0 + M >>> 02 + M	7.080-17	1.870-16
10	0 + 02 + M >>> 03 + M	4.430-17	2.260 01
11	0 + 03 >>> 2*02	1.070-12	6.110-39
12	0 + NO + M >>> NOZ + M	7.) [0-15	6.780-09
13	G + NO2 >>> NO + 02	1.170-11	5.550-25
14	0 + NO2 + M >>> NO3 + M	2.210-14	1.770-24
15	HO + HO >>> H2O + O	5.000-12	1.060-15
16	02 + 24NO >>> 24NO2	6.400-39	8.780-20

08 1.5720 10 1.7920 11 4.4010 16 1.1610 09 1.8330 09 1.6520 10 1.7920 11 4.4010 16 1.7400 08 2.7590 09 1.6520 10 1.7920 11 4.4010 16 1.7400 08 2.7590 09 1.7090 10 1.3940 11 4.4010 16 2.6080 07 2.8270 09 1.7090 10 1.1930 11 4.4010 16 2.6080 07 2.8280 09 1.7090 10 1.1930 11 4.4010 16 2.6080 07 2.8280 09 1.7090 10 9.7280 10 4.4010 16 3.9100 06 2.7700 09 1.7370 10 8.1980 10 4.4010 16 5.8910 05 2.7000 09 1.7420 10 7.5980 10 4.4010 16 5.8910 05 2.6640 09 1.7420 10 7.6780 10 4.4010 16 5.3030 05 2.6640 09 1.7420 10 6.2230 10 4.4010 16 8.5040 03 2.5530 09 1.7440 10 5.8670 10 4.4010 16 8.5040 03 2.5630 09 1.7440 10 5.8670 10 4.4010 16 5.3140 03 2.4980 09 1.7440 10 5.8670 10 4.4010 16 8.5040 03 2.4980 09 1.7490 10 5.2640 10 4.4010 16 3.3140 03 2.4980 09 1.7500 10 4.4010 16 3.3140 03 2.4980 09 1.7500 10 4.4010 16 3.3340 03 2.4980 09 1.7500 10 4.4010 16 3.3340 03 2.3370 09 1.7520 10 4.5580 10 4.4010 16 3.3340 03 2.3370 09 1.7520 10 4.5580 10 4.4010 16 3.3340 03 2.3370 09 1.7520 10 4.5580 10 4.4010 16 3.3340 03 2.3370 09 1.7520 10 4.5580 10 4.4010 16 3.3280 03 2.3370 09 1.7520 10 4.5580 10 4.4010 16 3.3280 03 2.3370 09	ME (S)	N205	N02	NO3	NO 0000	03	02	HN03	HO 0000	H20
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